#### CHAPTER 4

### EXPERIMENTAL METHODS

## 4.1 Preparation of Catalysts

The vanadosilicate catalysts were prepared by the improved method of Catalyst Engineering Laboratory, Department of Hydrocarbon Chemistry, Faculty of Engineering, Kyoto university (9,17). TPABr (tetra-n-propyl ammonium bromide,  $\left[ (CH_3CH_2CH_2)_4N \right]$  Br ) was used as an organic template.

## 4.1.1 Preparation of Reagents

### 1) Decantation Solution

Al-solution : composed of

vc1 <sub>3</sub>		-	x	g
TPABr	18.	-	7.53	**
H <sub>2</sub> O		-	60.0	ml
(conc.)H <sub>2</sub> SO <sub>4</sub>		=	3.37	"

### B1-solution:

wat	er gla	SS		=	69.0	g
(9.3%	Na <sub>2</sub> 0,	29%	SiO <sub>2</sub> )			
H <sub>2</sub> 0				=	45.0	ml

### Cl-solution:

NaC1	=	26.27	g
Но	=	104.0	g

### 2) Gel Solution:

A2-solution:

	vc1 <sub>3</sub>	=	x	g
	TPABr	=	5.72	"
	NaC1	-	11.95	"
	H <sub>2</sub> O	=	60.0	ml
(cor	nc.)H <sub>2</sub> SO <sub>4</sub>	=	3.37	11

B2-solution:

water	glass	-	69.0	g
н <sub>2</sub> о		-	45	m1

C2-solution:

TPABr	=	2.16	g
NaC1	777	40.59	11
NaOH	-	2.39	"
H <sub>2</sub> O	-	208.0	m]
(conc.)H <sub>2</sub> SO <sub>4</sub>	-	0.98	11

3) Stock solution of 1 M  $\mathrm{NH_4NO_3}$  1000 ml

# 4.1.2 Preparation of Decantation Solution and Gel Precipitate

Formation: Firstly, a decant solution was prepared by adding 60 ml of Al-solution and 45 ml aqueous solution of Bl-solution to 104 ml of Cl-solution, as shown in Figure 4.1, with vigorous stirring. From Figure 4.1, Al-solution was added by the microfeeder at a volumetric flow rate 12.0 cc/min and Bl-solution was added from a 50 ml. burette by the manual control to keep the pH of a mixed solution to constant at 9.8, since it is expected that this pH value is suitable for

- 1. pH meter
- 2. C-solution
- 3. B-solution
- 4. Homogenizer speed controller
- 5. Homogenizer
- 6. Adjustable base
- A-solution contains in syringe (100 ml)
- 8. Micro-feeder

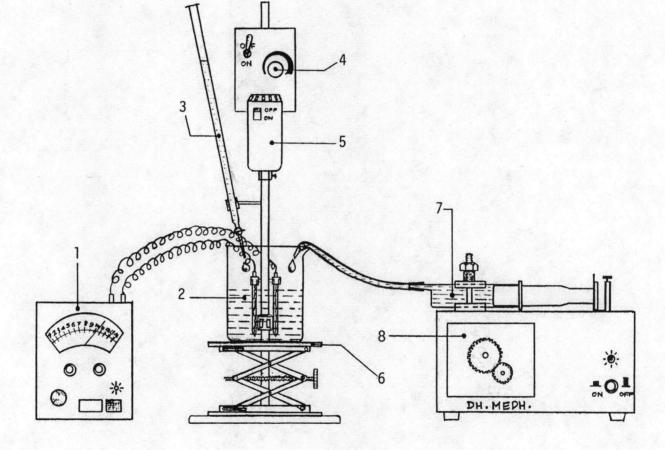


FIGURE 4.1 Preparation method for decant solution and gel precipitate formation

precipitation. After the mixing has ended, take the beaker C-solution out off the set. Let the precipitate settle down and measure the sedimentation time of the precipitate. The precipitating was removed form the supernatant solution by a centrifuge and the supernatant solution was kept for mixing with gel precipitate. Secondly, a gel mixtured was prepared by adding 60 ml of A2-solution and 45 ml of B2-solution to 208 ml of C2-solution. The method of mixing and condition are the same as the preparation of decantation solution, except that before mixing adjust the pH of solution between 9.8-10 with H<sub>2</sub>SO<sub>4</sub>(conc.) Measure the sedimentation time of precipitate and separate the precipitate from solution by centrifuge. The precipitated gel mixture was milled by powder miller (Yamato-Nitto, UT-21), Figure 4.2, as follows

milled 15 min. — centrifuged 15 min (for removed the water out) — milled 15 min. — centrifuged 15 min — milled 30 min.

### 4.1.3 Crystallization

The milling precipitate and the supernatant of decant solution would mix together. The mixture was heated for crystallization in an autoclave from room temperature  $\frac{90 \text{ min.}}{160^{\circ} \text{ C}} = \frac{4.2 \text{ h}}{210^{\circ} \text{ C}} = 210^{\circ} \text{ C}$  under a pressure of 3 kg/cm<sup>2</sup> (guage) of N<sub>2</sub> gas. Allowed the hot mixture to cool at room temperature in an autoclave over-night. The product crystals were washed with distilled water, to remove Cl<sup>-</sup>out of the crystals, about 8 times by using the centrifugal seperator (about 15-20 min for each time) and dry in oven at  $110-120^{\circ}\text{C}$  for at least 3 h.

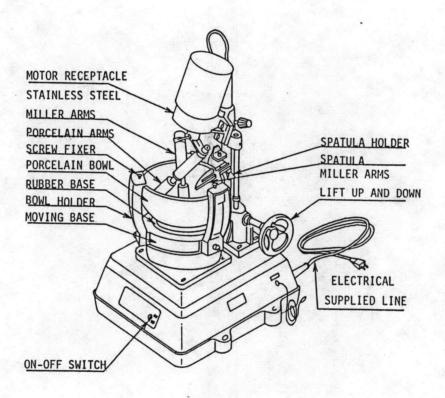


FIGURE 4.2 POWDER MILLER (YAMATO-NITTO, UT-21)

# 4.1.4 <u>First Calcination to Furnish the Pore Structure and</u> Channel Dimensions in Crystals.

Weighing 6-7 g of dry crystals in the porcelain container, which have the shape like a boat, and heat in furnace as follows;

room temperature  $60 \text{ min} 540^{\circ} \text{ C}$ , keep constant at this temperature 3.5 h.

At this step TPABr was burned and created the cavities and channels occuring in the crystals. The calcined crystal was cooled to room temperature in a dessicator.

### 4.1.5 Ion-exchange

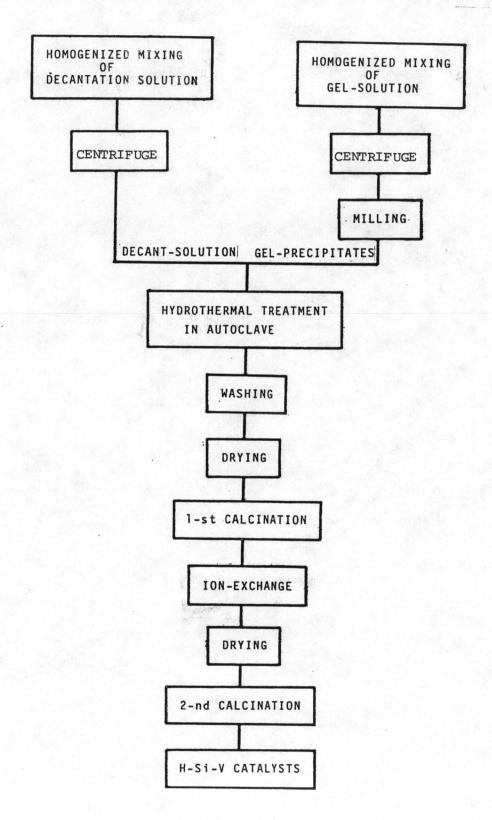
About 1.5 g of calcined crystal was mixed with 45 ml of 1 M  $\mathrm{NH_4NO_3}$  and heated on stirring hot plate at  $80^{\circ}$  C for 1 h. Washing the ion-exchange crystal with distilled water 2 times by using centrifugal seperator. Repeat ion-exchange step again 1 time, and then dry ion-exchange crystal in oven at  $110^{\circ}-120^{\circ}$  C for at least 3 h.

## 4.1.6 Second Calcination

The removal species, i.e.  $\mathrm{NH}_3$ ,  $\mathrm{NO}_{\mathrm{X}}$ , were decomposed by thermal treatment the ion-exchange crystal in a furnace at  $540^{\circ}$  C, with the temperature operating line the same as above. The vanadosilicate just prepared were tableted to provide the MTG reaction. Charge ratios of Si/V were changed from 40 to infinity.

The summary of preparation steps of these catalysts are shown in Figure 4.3.

FIGURE 4.3 Flow chart diagram of catalyst preparation by the improved method of Catalyst Engineering Laboratory, Dept. of Hydrocarbon Chemistry, Kyoto University





## 4.2 Reaction Engineering Test

## 4.2.1 Preparation of the Catalyst for the Reaction Test

A 120 mg of fine powder crystal of desired Si/V charged ratio catalyst was weighed to make 1 tablet catalyst, and to make 3 tablets for each Si/V charged ratio catalyst. Tablet sizes were then measured (appendix.C.). Tableted catalysts were crushed into 7-15 mesh in size and a 210 mg portion was packed into a quartz microtube fixed bed reactor of 6 mm i.d. The height of catalyst bed was then measured.

### 4.2.2 Reaction Method

The reaction is carried out in the reactor as shown in Figure 4.4, The procedure used to operate this reactor is as follows;

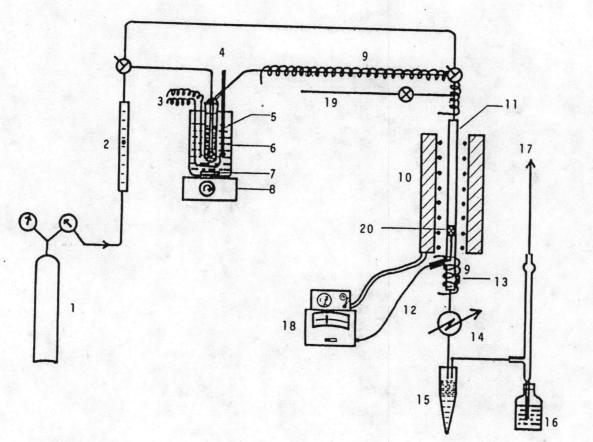
- (1) Adjust the outlet pressure of N  $_2$  gas to 1  $\mbox{kg/cm}^2$  , and allow the gas to flow through a rotameter.
- (2) Adjust 2 three way valves to allow gas to pass through the upper line through the reactor and measure the outlet gas flow rate by using a bubble flowmeter.
- (3) Heat up the reactor by raising the temperature as follow:

from room temperature  $\xrightarrow{20 \text{ C/min}} 450^{\circ}\text{C}$  (hold constant 30 min.) adjust to

The required reaction temperature and wait until the required reaction temperature becomes constant (the

reactor temperature was controlled by an on-off controller).

(4) At the same time switch on the heating line, magnetic



1. N<sub>2</sub> gas

- 2. Flow indicator
- 3. Electrical heater
- 4. Thermometer
- 5. Water bath
- 6. Tube contains MeOH
- 7. Magnetic bar
- 8. Magnetic stirror controller
- 9. Heating line
- 10. Reactor furnace
- 11. Reactor
- 12. Thermocouples
- 13. Position for take sample
- 14. Condenser
- 15. Receiver
- 16. Outlet gas flow meter
- 17. Vent line
- 18. On-off temperature controller
- 19. Tubing line for using micro tube pump
- 20. Catalyst bed

FIGURE 4.4 DIAGRAM OF MTG REACTION EXPERIMENT FOR MICRO TUBE REACTOR.

stirrer and water bath.

(5) Set the partial vapour pressure of MeOH to the requirement by adjust the temperature of waterbath followed the Antonic equation (18),

$$\log p = A - \frac{B}{t+C} \tag{4.1}$$

where p = vapour pressure of MeOH in mm Hg.

t = temperature, OC

A,B,C are constants

For MeOH, at range -14°C to 65°C,

A = 7.89750, B = 1474.08, C = 229.13 (See also appendix A-4)

- (6) Start to run the reaction by adjust 2 three way valves to allow  $N_2$  gas to pass through the line to the saturator setting in the water-bath use to carry MeOH vapour to the reactor, and at that time the reaction time is taken as zero.
- (7) Take samples to analysis at 1 and 3 hours time on stream, products are analysed by three gas chromatographs where
- 7.1) CO and MeOH were analysed using MS-5A column 3.5 mm  $\phi$  x 2 m and Porapak-T column 3.5 mm  $\phi$  x 2 m respectively, and the gas chromatograph uses for this analysis was a Shimadzu model GC-8A,

Setting condition of G.C. are;

Injection/detector temperature : 130° C

Column temperature : 100° C

Current : 60 mA

Attenuation : 2

Carrier gas : Ar

Detector : TCD

Regulator Pressure :  $6 ext{kg/cm}^2$ MS-5A Column Pressure :  $1.6-1.7 ext{kg/cm}^2$ Porapak-T column Pressure :  $0.75-0.8 ext{kg/cm}^2$ 

Recorder Shimadzu Model R-111

Chart Speed : 5 mm/min

The recorder was connected to a digital integrator TAKEDA-RIKEN MODEL TR-2213

7.2)  $C_1^{-C}_4$  hydrocarbons were analysed by using VZ-10 column(3 mm  $\phi$  x 6 m) and gas chromatograph YANACO MODEL G-1800;

Setting condition of G.C. are;

100° C Injection Temperature 80° C Column Temperature  $1 \times 10^{-3}$ Sensitivity Attenuation 15 Air Carrier gas He kg/cm<sup>2</sup> Regulator pressure of He  $2.5 \text{ kg/cm}^2$ Regulator pressure of H<sub>2</sub> 2 kg/cm<sup>2</sup> Column pressure Detector kg/cm<sup>2</sup> H, pressure for detector 0.5

The Recorder connect to a digital integrator TAKEDA-RIKEN MODEL TR-2213.

7.3)  $C_5 - C_{11}$  hydrocarbons (gasoline fraction) were analysed using a silicone-OV-101 (0.25 mm.  $\phi$  x 30 m) column and a gas chromatograph Shimadzu MODEL GC.-4C PTF.

Setting condition of G.C. are;

:	150°C
	150°C
	40°C
:	120°C
:	3°C / min
:	10 <sup>2</sup> MΩ
:	0.01 V
	FID-4C
•	DIFF. 1
•	$0.2 \text{ kg/cm}^2$
•	6 kg/cm <sup>2</sup>
	$2.5 \text{ kg/cm}^2$
	$0.5 \text{ kg/cm}^2$
:	1 kg/cm <sup>2</sup>

(Air supply by air compressor through the pack bed of silica gel for adsorbed the moisture.)

A recorder connected to a Shimadzu C-Rl-A chromatopac, where the program condition of the recorder were

CAL PM	1
WIDTH	5
SLOPE	70
DRIFT	10
MIN AR	3
T-DBL	15
LOCK	0

STP TM	70
ATTEN	0
SPEED	7
METHOD	41
SPL WT	100
IS WT	1

## 4.2.3 Study of Optimum Operating Condition

- 4.2.3.1 Influence of Vanadium Element on the Activity and Selectivity. To study this effect, the vanadosilicate catalysts charged ratio 40, 90, 200, 400, 1600, 3200 and  $\infty$  were prepared. The reaction conditions for this purpose were SV(space velocity) = 2,000 h<sup>-1</sup>, reaction temperature 300 and 360° C, and MeOH concentration = 20 %, N<sub>2</sub> gas = 80 %, reaction time 1 and 3 h. time on stream.
- 4.2.3.2 Effect of Space Velocity The vanadosilicate catalysts charged ratio 200, 400 and  $\infty$  were chosen for this study. The reaction conditions were reaction temperature  $300^{\circ}$  C, MeOH concentration = 20 %, N<sub>2</sub> gas = 80 % reaction time 1 and 3 h time on stream, and the space velocity varied at 500, 1000, 2000, 4000 and 8000 h<sup>-1</sup>.
- 4.2.3.3 Effect of Reaction Temperature To study this effects Si/V charged ratio 1600 and 90 catalysts were used, where the reaction were SV = 2000 h $^{-1}$ , MeOH concentration = 20 %, N $_2$  gas = 80 %, and the reaction temperature varied at 260, 280, 300, 330, 360 $^{\circ}$  C for Si/V charged ratio 1600 catalyst and for Si/V charged ratio 90 catalyst, the reaction temperature varied at 300, 330, 360, 390 and 420 $^{\circ}$  C.

4.2.3.4 Effect of MeOH Concentration For this purpose, the vanadosilicate charged ratio 1600 catalyst was chosen. To study this effect, the reaction conditions were at  $SV = 2000 \text{ h}^{-1}$ , reaction temperature  $300^{\circ}$  C, and the MeOH concentration varied at 5, 10, 20, 40 and 100 %. For MeOH concentration 100 %, it was fed to the reactor by using a microtube pump. At GHSV = 2000 h<sup>-1</sup> change to WHSV as shown in appendix A-2.

## 4.3 Physical Properties Measurement

For study the physical properties of vanadosilicate catalyst, the following properties are measured;

- 4.3.1 <u>BET surface area</u>: BET surface area of catalysts were measured by  $N_2$  adsorption with continuous flow at liquid nitrogen temperature range by using He as a diluted gas Figure 4.5. The procedure for BET measurement of Figure 4.5 are as follows;
- 1. adjust outlet pressure of He gas regulator to 7 kg/cm  $^2$  and adjust He pressure in column to 2.6 kg/cm  $^2$ 
  - 2. line on
- 3. set oven temperature at  $50^{\circ}\mathrm{C}$  and detector supply on and wait for steady about 30 min.
  - 4. measure flow rate of He and record room temperature
- 5. Open and adjust N  $_2$  pressure regulator at 3.5 kg/cm  $^2$  and adjust to 3 kg/cm  $^2$  for column
- 6. mix  $\rm N_2$  and He gas for get the  $\rm N_2$  mole fraction = 0.3 by calculating as follows:
  - mole fraction of  $N_2 = \frac{\text{Flow rate of } (N_2 + \text{He}) \text{flow rate of He}}{\text{Flow rate of } (N_2 + \text{He})}$

- 7. weigh about 40 mg of sample and put into sample U-tube bottle (Figure 4.5)
- 8. adjust TANK knob from close to open for about 3-4 sec and then close
- 9. adjust TUBE knob from close to open about 3-4 sec and close
  - 10. repeat steps 8 and 9 again twice
- ll. cooling mixed gas tube using liquid  $\mathbf{N}_2$  to trap the moisture in mixed gas
  - 12. place sample U-tube bottle at sample position
  - 13. adjust COCK 1 knob from SHORT to EVAP.
  - 14. adjust COCK 2 knob from CAL to SAMP
- 15. heat sample by adjusting AC line on and set temperature at  $300^{\circ}\text{C}$  for 30 min
- 16. cooling sample to room temperature and set recorder at the condition :

chart speed 20 mm/min
mV range 256 mV
injection temperature 1
record at POS

- 17. cool sample with liquid  $N_2$  and run recorder
- 18. measure  $\rm N_2$  desorption by take liquid  $\rm N_2$  out and heat sample by water (at room temperature) run speed chart at 40 mm/min and adjust mV range to suitable range, record to NEG.
- 19. adjust TUBE knob from close to open about 10 sec and then close
- 20. wait for about 10 min then adjust COCK 2 knob from SAMP to CA 2 and recorder conditions being the same as  $N_2$  desorption measurement (calculation of BET surface area, see appendix A-5)

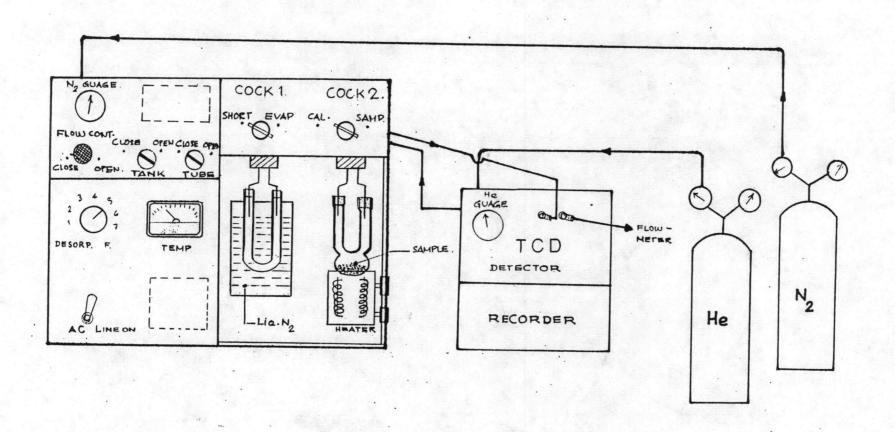


Figure 4.5 Diagram of BET surface area measurement system

- 4.3.2 X-ray diffraction: The catalysts Si/V charged ratio range from  $\infty$  to 40 were prepared for XRD, and measured by Mr. T. Miyake. The method for preparing sample for XRD is shown in appendix B-1.
- 4.3.3 Acidity of catalysts For study the acidity of catalysts, measured by using the technique of temperature program desorption of NH<sub>3</sub>. The catalysts Si/V changed ratio from  $\infty$  to 40 were measured; where about 150 mg of sample was put into sample disc and N<sub>2</sub> gas was flown through the sample set at 50 ml/min. A dry sample was taken for finding the dry weight and heated at a temperature programe of 20 °C/min to the final temperature of 430 °C, during which weight loss and temperature lins were measured by a recorder at chart speed 5 mm/min and 10 mg per chart full scale was setted. Then, cooling sample to 60 °C, and seted 5 mg per chart full scale. Flow rate of NH<sub>3</sub> was adjusted at 50 ml/min, the recorded weight increased up to a constant value. Finally, NH<sub>3</sub> desorption was measured by heating the sample at a temperature program rate of 10 °C/min to the final temperature of 600°C

## 4.3.4 Chemical Composition Analysis

To study the actual Si/V charge ratio of prepared catalysts, the samples, Si/V charged ratio from  $\infty$  to 40 were made into solutions for atomic absorption measurement. The method used for preparing the sample solution and the standard solution is explained in appendix B-2. These samples were measured by Mr.K.Fukuda.

## 4.3.5 Scanning Electron Microscope (SEM)

To study the outside structure of vanadosilicate catalysts, Si/V charged ratio  $\infty$  , 90, and 40 were chosen for this purpose by

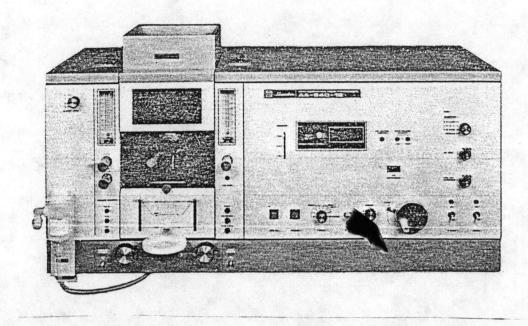


Figure 4.6 Atomic Absorption Equipment

using the scanning electron microscope as detector. These catalysts were measured by Mr. Sakamoto and Miss T. Ukawa.

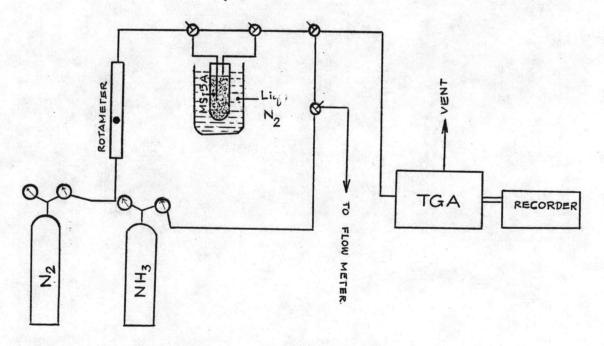


Figure 4.7 Flow chart of TPD(NH<sub>3</sub>) measurement system