

## CHAPTER 9

### CONCLUSIONS

#### 9.1 Principal Conclusions

The following major conclusions have been obtained from the stochastic analysis of convective diffusional deposition of polydisperse aerosols on a dust loaded fiber.

(1) The average profile of deposited particles on the fiber surface was affected by both the Peclet number  $Pe$  and the interception parameter  $R$  and to a lesser extent by the geometric standard deviation  $\sigma_g$ . When  $Pe = 0$  (pure interception), the profile was known to be uniform all over the entire surface. As  $Pe$  gradually increased, the effect of small convection caused a peak to appear around the front stagnation point. Further increase in  $Pe$  then caused the peak to split and shift away from the front stagnation point, because the convective effect became dominate.

(2) The collection efficiency raising factor increased with  $Pe$  but decreased as  $R$  increased. The effect of  $\sigma_g$  on was inconclusive because the effect of  $\sigma_g$  on was minor.

(3) The size distribution of deposited particles was tentatively concluded to be log-normal at small  $\sigma_g$  and  $Pe$ . In case of large  $\sigma_g$  and  $Pe$  the sample size distribution seemed slightly different from log-normal.

(4) As long as the Pe number and the interception parameter of a polydisperse aerosols were the same as those of a monodisperse system, the effects of polydispersity, namely  $\sigma_g$ , were slight and hard to detect. Unless a very large  $\sigma_g$ , say,  $\sigma_g > 1.4$  or more, was used, it would be all right and more convenient to predict the behavior of a poly disperse system by a corresponding monodisperse one. In any case, a much larger sample size than 50 would be necessary to yield more definite conclusions on the effects of  $\sigma_g$ .

## 8.2 Recommended Future Work

An interesting extension of this work would be to determine the drag force acting on deposited particles, so that pressure drop across a fibrous filter mat might be obtained as a function of filtration time. To do this, a mathematical model that could estimate the drag force acting on dendrites of various configurations is required. Then all the data obtained in the present work might be fed to the pressure drop model, thus eliminating the necessity of simulating dendritic deposition again.

Pendse et al. (1981) determined experimentally the hydrodynamic drag force in a uniform flow field acting on a spherical body with small particles attached to its surface. The experimental data were then used to substantiate the approximate force expressions derived from available theories for several types of collector-particle geometries. They also developed procedures for applying these results to the prediction of the pressure drop across a filter bed. Nevertheless, similar work on a cylindrical body has not yet appeared, and some simplified but reliable procedure must still be developed to treat dendrites of infinitely different configurations before the recommended future work could be attempted.

APPENDICES

## APPENDIX A

## NOTATION

a	Constant used in eqn (6.6.4)
$a_k(\theta)$	Function defined by eqn (3.1.8)
A	Filtration area of a fibrous filter ( $\text{cm}^2$ )
$A(t)$	Fluctuating term used eqn (4.3.1) ( $\text{cm/s}$ )
b	Constant used in eqn (6.6.4)
$b_k(\theta)$	Functions defined by eqn (3.1.9)
B	Mobility of an aerosol particle ( $\text{s/gm}$ )
c	Particle concentration ( $\text{g/cm}^3$ )
$c_0$	Approaching mass concentration of aerosols
$c_e$	Effluent particle concentration ( $\text{g/cm}^3$ )
$c_i$	Influent particle concentration ( $\text{g/cm}^3$ )
$C_s$	Cunningham slip factor (-)
d, $d_p$	Diameter of an aerosol particle ( $\mu\text{m}$ , $\text{cm}$ )
$d_g$ , $d_{pm}$	Geometric mean diameter of an aerosol particle ( $\mu\text{m}$ )
D	Diffusion coefficient of aerosol particle ( $\text{cm}^2/\text{s}$ )
$f_i$	Observed frequencies of the $i^{\text{th}}$ class
$F_i$	Theoretical frequencies of the $i^{\text{th}}$ class
h	Thickness of filter mat ( $\mu\text{m}$ , $\text{cm}$ )
H	Half height of generation plane (-)
$j_k^{(s)}$	Particle flux on the surface of a particle in the $k^{\text{th}}$ layer of a dendrite due to the s component of flow ( $s = r$ , or $\theta$ )
k	Boltzmann's constant ( $\text{erg/K}$ )

K	Hydrodynamic factor
$Kn_f$	Fiber Knudsen coefficient, $= l/R_f$ (-)
$Kn_p$	Particle Knudsen coefficient, $= l/r_p$ (-)
l	Mean free path of an aerosol particle ( $\mu\text{m}$ )
L	Total length of all the fiber in unit volume of filter ( $\mu\text{m}$ , m)
L	Sample size (-)
m	Loaded mass of particles in a unit filter volume ( $\text{gm}/\text{cm}^3$ )
$m_k$	Expected particle number in the $K^{\text{th}}$ layer of a dendrite
$M(\theta)$	Integer function of $\theta$ defined by eqn (3.2.12)
$M^{\text{th}}$	Order of particle captured
n	Number of samples
n	Particle number concentration
n	Standard normal random vector $= (n_x, n_y, n_z)$
N	Member of a dendrite
$N(\tau, \theta)$	Frequency function of number of dendrites per unit length of fiber at time $\tau$ and angle $\theta$ , taking into account both sides of the fiber
P	Position vector (cm)
P	Dimensionless position vector (-)
Pe	Peclet number (-)
r	Radial cylindrical coordinate
r	Position vector (cm)
$r_p$	Radius of an aerosol particle ( $\mu\text{m}$ )
R	Interception parameter (-)
$R_f$	Radius of fiber ( $\mu\text{m}$ ), also Dimensionless radius of fiber (-)

$R_c$	Radius of Kuwabara cell ( $\mu\text{m}$ ), also Dimensionless radius of Kuwabara cell (-)
$R_{i,j}^{(s)}$	Rate of increase of $m_i$ by deposition on particles occupying the $i^{\text{th}}$ layer due to the flow component in $s$ direction ( $s = r, \text{ or } \theta$ )
$s$	Standard deviation
$t$	Time (s)
$t$	Filtration time (s)
$T$	Dimensionless time (-)
$T$	Temperature ( $^{\circ}\text{C}$ )
$u$	Velocity vector of fluid stream (cm/s)
$u_s, U_s$	Superficial velocity through the filter (cm/s)
$U_{\infty}$	Approaching velocity of fluid stream (cm/s)
$U$	Dimensionless velocity vector of fluid stream (-)
$v$	Velocity of aerosol particle (cm/s)
$v$	Velocity vector of aerosol particle (cm/s)
$w$	Relative velocity vector of particle to air (cm/s)
$w_{pm}$	Mass of an average aerosol particle, $d_p = d_{pm}$ (cm/s)
$w_{cap}$	Accumulated mass of particles captured on the effective fiber length (gm)
$w_M$	Average mass of captured particle no. $M$ on the effective fiber length (gm)
$w_{M,i}$	Mass of captured particle no. $M$ of the Monte Carlo sample no. $i$ on the effective fiber length (gm)
$W$	Probability function defined by eqn (4.3.3)
$W_M$	Average total mass of incoming particles generated on the entire generation plane between the $M^{\text{th}}$ and the $(M+1)$ -st captures on fiber section III (gm)

- $W_{M, i}$  Total mass of incoming particles generated on the entired generation plane between the  $M^{\text{th}}$  and  $(M+1)$ -st captures on fiber section III of Monte Carlo sample no.  $i$  (gm)
- $\bar{x}$  Sample mean
- $X, Y, Z$  Dimensionless spatial coordinates (-)
- $y$  Half distance apart of the limiting trajectories (cm)
- $Z_1, Z_2, Z_3, Z_4, Z_5$  Dimensionless length of fiber section I, II III, IV, V respectively (-)





## Greek Letters

$\alpha$	Packing density of a filter ( $\text{cm}^3$ fiber/ $\text{cm}^3$ filter)
$\beta$	Reciprocal of relaxation time of a particle ( $\text{s}^{-1}$ )
$\gamma$	Rate of particle approaching a clean fiber per unit length
$\epsilon$	Small positive number
$\theta$	Angular cylindrical coordinate measured counter clockwise from the down stream stagnation point (deg.)
$\lambda$	Collection efficiency raising factor ( $\text{cm}^3/\text{gm}$ )
$\lambda$	Filter coefficient ( $\text{cm}^{-1}$ )
$\lambda_0$	Clean filter coefficient ( $\text{cm}^{-1}$ )
$\eta$	Collection efficiency of a single fiber (-)
$\eta_0$	Collection efficiency of a clean single fiber (-)
$\mu$	Sample mean
$\mu$	Fluid viscosity ( $\text{gm}/\text{cm}\cdot\text{s}$ )
$\rho$	Coordination number, that is, maximum number of particles in the (k + 1)-st layer which can be attached directly to the same particle of the k <sup>th</sup> layer
$\rho_f$	Fiber density ( $\text{gm}/\text{cm}^3$ )
$\rho_p$	Particle density ( $\text{gm}/\text{cm}^3$ )
$\phi_{i,j}^{(s)}$	Fraction of $\gamma$ colliding with a target particle in the i <sup>th</sup> layer to become part of the j <sup>th</sup> layer owing to the s component of flow (s = r, or $\theta$ )
$\sigma$	Standard deviation
$\sigma$	Standard deviation of normal standard random number n (cm)

$\sigma_g$	Geometric standard deviation of particle diameter (cm)
$\tau$	Dimensionless time (-)
$\tau$	Time measure from beginning of aerosols flow through the filter (s)
$\tau$	Relaxation time (s)
$\tau_f$	Duration of filtration time (s)
$\tau_{ug}$	Duration of period of unhindered dendrite growth (s)
$\nu$	Degree of freedom
$\nu_0(\theta)$	Function of $\theta$ which depended on collection mechanism defined by Payatakes (1977)
$\chi(t; \tau, \theta)$	Dendritic age distribution function at time $\tau$ and angular position $\theta$
$\chi^2$	Chi-square statistic
$\psi$	Kuwabara stream function of flow around a fiber

## SUBSCRIPTS

D	Diffusion
f	Fiber
I	Interception
i	$i^{\text{th}}$ Monte Carlo sample
i	$i^{\text{th}}$ step
g	Geometric
k	$k^{\text{th}}$ layer of a dendrite
m	Mean, geometric mean
M	Dust loaded
M	$M^{\text{th}}$ captured order
p	Particle
r	r direction
x	x direction
y	y direction
z	z direction
$\theta$	$\theta$ direction
O	Initial
1, 2, 3, 4, 5,	Number of sections

## APPENDIX B

## RANDOM NUMBERS GENERATION

The effectiveness of the stochastic simulation is intimately connected with the quality of the random numbers being used.

Appendix B summarizes the methods used in this investigation to generate random numbers, and gives listings of FORTRAN IV subroutines employed for generation of random numbers. Furthermore statistical tests of their properties have already been carried out but they are not reproduced here.

#### B.1 Methods of Generating Uncorrelated Random Numbers.

When a computer subprogram is used, as in this study, to generate a sequence of random numbers, each particular sequence will be completely defined by its starting value or seed. The term "pseudo-random numbers" is sometimes used to describe such numbers.

The algorithms used to generate the uncorrected uniform and normal random numbers in this study were developed by Pike and Hill (Collected Algorithms from CACM). The general procedure was :

- (1) select a nonrepetitive starting value,
- (2) generate a uniformly distributed random number lying between 0 and 1 and with a mean of 0.5,
- (3) if appropriate, use two uniform random numbers from (2) to generate a normally distributed random number with a mean of 0.0 and a standard deviation of 1.0,
- (4) repeat steps (2) and (3) until a sequence of random numbers have been obtained.

Pike and Hill recommended that the starting value should be an odd integer between 1 and 67, 108, 863. Subroutine START breaks up a starting value into two integral numbers in order to prevent overflowing without having to use double-precision integers on the IBM 370/138 computer. To generate several starting values for separate sequence of random numbers, the following procedure was adopted : (1) an odd number between 1 and 67, 108, 863 was selected from a random number table, (2) the number was used to generate a sequence of uniform random numbers, (3) subroutine RESTRT was used to transform each uniform random number in the sequence in to a new starting value later used.

To break up the cyclic nature of a very long sequence, a new starting value is used for each record of the Monte Carlo simulation.

## B.2 Random Number Generators

### B.2.1 Starting Value

```

SUBROUTINE START(ISTR)

C
C
C   SUBROUTINE START TRANSFORMS THE STARTING VALUE ISTR SO THAT IT
C   MAY BE USED BY SUBROUTINE RANDOM OR SUBROUTINE RND WITHOUT
C   CAUSING OVERFLOWING OF THE INTEGER NUMBER
C   THE VALUE OF STRT MUST BE AN ODD NUMBER OBTAINED FROM A TABLE
C   OF RANDOM NUMBERS, PREFERABLY BETWEEN 42758321 AND 67108863
C
C
C   ISTR = STARTING VALUE
C

```

```
COMMON/CMN2/ RUNF,RRM,IY1,IY2
```

```
C
```

```
I = 2*(ISTR/2)+1
IY2 = I/16384
IY1 = I-16384*IY2
RETURN
END
```

```
SUBROUTINE RESTRT
```

```
C
C
C
C
C
C
```

```
SUBROUTINE RESTRT YIELDS A NON-REPETITIVE STARTING VALUE FOR
THE RANDOM NUMBER GENERATORS
```

```
COMMON/CMN2/ RUNF,RNRM,IY1,IY2
```

```
C
```

```
I = 0
J = 0
DO 100 K = 1,3
```

```
C
```

```
CALL RANDOM
```

```
C
```

```
I = I+IY1
J = J+IY2
100 CONTINUE
IY1 = MOD(123*I,16384)
IY2 = MOD(789*J,4096)
RETURN
END
```

### B.2.2 Uniform Random Number Generator

Subroutine RANDOM was used to generate a uniform random numbers, whose values lie between 0 and 1

```
SUBROUTINE RANDOM
```

```
C
C
C
C
C
```

```
SUBROUTINE RANDOM GENERATES A UNIFORM RANDOM NUMBER WITH A MEAN
OF 0.5 AND A RANGE OF 0.0 TO 1.0
THE SEQUENCE OF RANDOM NUMBERS HAS A LIMITING CYCLE LENGTH OF
```

```

C
C
C   RUNF = UNIFORMLY DISTRIBUTED RANDOM NUMBER
C
C
C   COMMON/CMN2/ RUNF,RNRM, IY1,IY2
C
C   IY = 3125*IY1
C   N = IY/16384
C   IY1 = IY-16384*N
C   IY = 3125*IY2+N
C   IY2 = IY-4096*(IY/4096)
C   RUNF = DFLOAT(16384*IY2+IY1)/67108864.0D0
C   RETURN
C   END

```

### B.2.3 Normal Random Number Generator

Subroutine RND was used to generate a normal random number with a mean of 0.0 and a standard deviation of 1.0.

```

SUBROUTINE RND
C
C
C   SUBROUTINE RND GENERATES A STANDARD NORMAL RANDOM NUMBER USING
C   TWO UNIFORM RANDOM NUMBERS
C
C
C   RNRM = NORMALLY DISTRIBUTED RANDOM NUMBER
C
C
C   COMMON/CMN2/ RUNF,RNRM,IY1,IY2
C
C
C   CALL RANDOM (FIRST TIME)
C
C   IX = 3125*IY1
C   N = IX/16384
C   IX = IX-16384*N
C   IY = 3125*IY2+N
C   IY = IY-4096*(IY/4096)
C   R = DFLOAT(16384*IY+IX)/67108864.0D0
C   X = SQRT(-2.0*ALOG(R))
C

```

```
C  
C CALL RANDOM (SECOUND TIME)  
C  
IX = 3125*IX  
N = IX/16384  
IT1 = IX-16384*N  
IY = 3125*IY+N  
IY2 = IY-4096*(IY/4096)  
R = DFLOAT(16384*IY2+IY1)/67108864.0D0  
RNRM = X*COS(6.283185*R)  
RETURN  
END
```