ผลของภาวะการกรองแบบจุลภาคต่อประสิทธิภาพการกรองและการสเตอริไลส์แบบเย็น ของแบบจำลองไวน์ข้าวไทย

นางสาวจินตนา ศรีผุย

วิทยานิพนธ์นี้เป็นส่วนหนึ่งของการศึกษาตามหลักสูตรปริญญาวิทยาศาสตรดุษฎีบัณฑิต สาขาวิชาเทคโนโลยีทางอาหาร ภาควิชาเทคโนโลยีทางอาหาร คณะวิทยาศาสตร์ จุฬาลงกรณ์มหาวิทยาลัย ปีการศึกษา 2549 ลิขสิทธิ์ของจุฬาลงกรณ์มหาวิทยาลัย

EFFECTS OF MICROFILTRATION CONDITIONS ON FILTRATION PERFORMANCE AND COLD STERILIZATION OF THAI RICE WINE MODEL

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STERILIZATION OF THAI RICE WINE MODEL

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งานวิจัยนี้ศึกษาผลของ 1) การแยกของแข็งออกจากน้ำหมักก่อนการกรองแบบจุลภาคโดยวิธีการกรอง ผ่านผ้าขาวบาง การตกตะกอน 3 ชั่วโมง และการปั่นเหวี่ยงที่ 3000 g นาน 30 นาที 2) ภาวะที่ใช้ในการกรอง แบบจุลภาคได้แก่ ขนาดช่องว่างของเมมเบรน (0.10, 0.22 และ 0.45 ไมครอน) ความดันการกรอง (ΔP ที่ 138, 276, 414 และ 552 กิโลปาสคาล) และความเร็วของการกวน (0 และ 100 รอบต่อนาที) 3) ขนาด การกระจายขนาดและความเข้มข้นของของแข็งต่อประสิทธิภาพการกรองแบบจุลภาคได้แก่ เพอมิเอทฟลักซ์ และความต้านทานจำเพาะของเค้ก (α) และลักษณะของไวน์ข้าวที่ผ่านการกรองแบบจุลภาคได้แก่ pH และ ปริมาณของกรดทั้งหมด แอลกอฮอลล์ ของแข็งที่ละลายได้ทั้งหมด ยีสต์ แบคทีเรียและแบคทีเรียที่สร้าง กรดแลคติคสำหรับขจัดจุลินทรีย์และอนุภาคของแข็งเพื่อนำไปใช้ในการสเตอริโลส์ไวน์ข้าวแบบเย็น

ขนาดช่องว่างของเมมเบรนและความเร็วของการกวนไม่มีผลต่อ α แต่ α เพิ่มขึ้นตาม Δ P ตามสมการ $\alpha=4.13\times10^{8}(\Delta P)^{0.98}$ โดยค่าคอมเพรสซิบิลิตี้ของเค้กเท่ากับ 0.98 ซึ่งบ่งว่ากากไวน์ข้าวมีลักษณะที่ ถูกบีบอัดได้สูง ขนาดช่องว่างของเมมเบรนและ Δ P ไม่มีผลต่อลักษณะของไวน์ข้าวที่ผ่านการกรอง แบบจุลภาคและไม่พบจุลินทรีย์ในไวน์ข้าวที่ผ่านการกรองแบบจุลภาค

ผลการทดลองพบว่า ในทุกกรณีของขนาดและการกระจายขนาด (1–20, 1–200, และ 1–400 ไมครอน) ค่า α และความเข้มข้นของของแข็งในหน่วยร้อยละโดยน้ำหนัก (C) มีความสัมพันธ์แสดงได้ ดังสมการ $\alpha=j+k$ C เมื่อ j และ k เป็นค่าคงที่ และที่ความเข้มข้นเดียวกัน ขนาดของแข็งที่ใหญ่กว่าและ ช่วงการกระจายขนาดที่กว้างกว่าให้ค่า α ที่ต่ำกว่า นอกจากนี้ยังพบว่าที่ทุกความเข้มข้นที่ศึกษาคือร้อยละ 0.2, 0.5, และ 1.0 โดยน้ำหนัก เมื่อร้อยละโดยน้ำหนักของของแข็งที่มีขนาดใหญ่กว่า 45 ไมครอน (W) เพิ่มขึ้น ทำให้ค่า α ต่ำลง โดยสามารถแสดงความสัมพันธ์ได้อย่างดี ($r^2>0.99$) ดังสมการ $\alpha=x(1/e^w)$ เมื่อ x และ y เป็นค่าคงที่

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JINTANA SRIPUI: EFFECTS OF MICROFILTRATION CONDITIONS ON FILTRATION PERFORMANCE AND COLD STERILIZATION OF THAI RICE WINE MODEL. THESIS ADVISOR: ASST. PROF. PASAWADEE PRADIPASENA, Sc. D., THESIS CO-ADVISOR: ASST. PROF. CHIDPONG PRADISTSUWANNA, Ph.D., ASSOC. PROF. WILLIAM L. KERR, Ph.D., 104 pp.

This research studied effects of 1) solid-liquid separations of fermented liquor by filtration through cheesecloth, sedimentation for 3 hrs., and centrifugation at 3000xg for 30 min.; 2) operating conditions of microfiltration such as membrane pore size (0.10, 0.22, and 0.45 μ m), transmembrane pressure (ΔP at 138, 276, 414, and 552 kPa), and stirring speed (0 and 100 rpm); and 3) size, size distribution, and concentration of suspended solids on microfiltration performance in terms of permeate flux and specific cake resistance (α), as well as microfiltered rice wine characteristics including pH, titratable acidity, alcohol content, total soluble solids content, total suspended solids content, and yeast, bacteria, and lactic acid bacteria counts. Microfiltration was used to eliminate microorganisms and suspended solids in rice wine for cold sterilization.

The results showed that the three solid-liquid separation methods affected concentration, size, and size distribution of suspended solids as well as yeast and bacteria counts. Centrifugation gave the lowest suspended solid concentration (0.02 wt%) as well as size and size distribution (0.3-20 μ m) and resulted in the greatest permeate flux and α . However, the separation methods did not affect the characteristics and taste of microfiltered rice wine. Microfiltration could eliminate microorganisms since the microorganisms were not detectable in the microfiltered rice wine. Thus, microfiltration could be used for cold sterilization of rice wine.

The membrane pore size and stirring speed did not affect the α . The α was increased with ΔP following the equation $\alpha = 4.13 \times 10^8 (\Delta P)^{0.98}$. Compressibility of cake was 0.98 indicating that the cake of rice wine was highly compressible. The membrane pore size and ΔP did not affect the microfiltered rice wine characteristics. Yeast, bacteria and lactic acid bacteria were not detectable in all microfiltered rice wine.

In addition, the results showed that the correlation of the α and the suspended solid concentration (C; wt%) for all size and size distributions (1-20, 1-200, and 1-400 μ m) could be expressed as $\alpha = j + kC$ where j and k are the empirical constants. At the same concentration, the greater the size and size distribution of suspended solids, the lower the α . Moreover, for all suspended solid concentration (0.2, 0.5, and 1.0 wt%), as wt% of suspended solids which having size \geq 45 μ m (W) increased, the α decreased. The correlation could be expressed as $\alpha = x(1/e^{yW})$ with a high correlation ($r^2 > 0.99$), where x and y are the empirical constants.

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NOMENCLATURE

A = Membrane area (m^2)

 A_p = Cross sectional area per particle

 A_{pR} = Relative cross sectional area per particle

 A_{TR} = Relative total surface area on each layer of membrane surface occupied by particles

 A_T = Total surface area on each layer of membrane surface occupied by particles

C = Concentration of suspended solids (kg of suspended solids /100 kg feed)

 $C_{w/v}$ = Weight by volume concentration of suspended solids ($g_{TSS}/100 \text{ ml RW}$)

D = Diameter of particle (cm)

 D_{vg} = Geometric mean diameter of volume equivalent diameter on a number basis

 D_{void} = Void diameter (μm)

i = Sample number in Table 4.8

j = Empirical constants in Equation 4.2

 $J = Permeate flux (m^3/m^2 \cdot s)$

 J_o = Initial permeate flux $(m^3/m^2 \cdot s)$

 J_{ss} = Steady state flux (L/h·m²)

 $J_{\rm m}$ = Mass permeate flux (kg/h·m²)

k = Empirical constants in Equation 4.2

k' = Empirical constants in Equation 2.23

k" = Empirical constants in Equation 2.23

K = Kozeny constant

m = Mass of cake (kg)

n = Cake compressibility

N = Numbers of particles per volume of rice wine

 N_R = Relative numbers of particles per volume of rice wine

 ΔP = Transmembrane pressure (Pa)

 ΔP_c = Pressure drop across the cake (Pa)

 ΔP_m = Pressure drop across the membrane (Pa)

Q = Feed flow rate (mL/min)

r = Particle radius (m)

 R_c = Cake resistance (m⁻¹)

 R_m = Membrane resistance (m⁻¹)

RW = Rice wine

 RW_f = Rice wine obtained by filtration through cheesecloth

RW_s = Rice wine obtained by sedimentation

RW_c = Rice wine obtained by centrifugation

 R_t = Total resistance (m⁻¹)

s = Slope of the plot between $1/J\ vs.\ V$

S = Solids surface area per unit volume of solids (m^2/m^3)

t = Filtration time (s)

 $T = Temperature of feed (^{O}C)$

v = Velocity of permeate (m/s)

V = Volume of permeate (m³)

w = Mass of cake per unit area of membrane (kg/m²)

W = Gram of suspended solids having size larger than 45 μm per 100 gram of total suspended solids in rice wine

x = Empirical constants in Equation 4.3

y = Empirical constants in Equation 4.3

Greek letters

 α = Specific cake resistance per unit mass (m/kg)

 α_o = Specific cake resistance at reference pressure (m/kg)

 α_1 = Specific cake resistance per unit thickness (m/kg)

 δ = Cake thickness (m)

 ϵ = Porosity of the cake

 κ = Dynamic shape factor

 μ = Dynamic viscosity of permeate (Pa·s)

 v_{TSS} = Volume of a suspended solid particle (ml)

 v_{RW} = Volume of rice wine per particle (ml)

 v_{RWR} = Relative volume of rice wine per particle

 $\rho = Density of permeate (kg/m³)$

 ρ_{RW} = Density of rice wine (g/ml)

 ρ_s = Density of the particles comprising the cake (kg/m³)

 ρ_{TSS} = Density of total suspended solid (g/ml)

 σ_g = Geometric mean standard deviation

Subscript

i = property of sample number "i"