PREPARATION OF CHITOSAN-TITANIUM DIOXIDE BEADS FOR PHENOL DEGRADATION

Miss Punnida Nonsuwan

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้ในงานวิจัยนี้ได้พัฒนาการสังเคราะห์บีดสามชนิดเพื่อใช้เป็นทางเลือกสำหรับการบำบัด ้ฟื้นอลในน้ำเสีย ทำการสังเคราะห์บึดไททาเนียมไดออกไซด์ผสมกับไกโตซาน และ บึดไททาเนียม ้ใดออกไซด์ดัดแปรที่กราฟท์บนบีดไคโตซาน โดยไกโตซานทำหน้าที่เป็นตัวพยุงไททาเนียมได ้ออกไซด์ นอกจากนี้ทำการสังเคราะห์ไททาเนียมไดออกไซด์สเฟียร์โดยจะใช้ไคโตซานทำหน้าที่ ้เป็นตัวยึดไททาเนียมไดออกไซด์ไว้ด้วยกัน จากนั้นทำการศึกษาการดูดซับและปฏิกิริยาสลายฟีนอล ้โดยแสงของไคโตซานและตัวเร่งปฏิกิริยาไททาเนียมไคออกไซด์ชนิดต่าง ๆ พบว่าบืดไททาเนียม ้ใดออกไซด์ดัดแปรที่กราฟท์บนไคโตซานมีความสามารถในการกำจัดฟีนอลได้ดีที่สุด จึงเลือกมา ทำการศึกษาถึงผลของความเข้มข้นของกลูทาราลดีไฮด์และเวลาที่ใช้ในการเชื่อมระหว่างกลูทาราล ้ดีไฮด์และไททาเนียมไดออกไซด์ ในขั้นตอนของการคัดแปรไททาเนียมไดออกไซด์ พบว่าภาวะที่ เหมาะสมในการคัดแปรไททาเนียมไดออกไซค์คือการใช้กลูทาราลดีไฮค์เข้มข้น 3.75% โคยบ่มเป็น เวลา 1 ชั่วโมง การสลายตัวของฟีนอลขึ้นอยู่กับหลายปัจจัย ได้แก่ ระยะห่างระหว่างหลอดยุวีและ ้ผิวหน้าของสารละลาย การกวนสารละลาย ความเข้มข้นของไททาเนียมไคออกไซด์ที่ใช้กราฟท์บน ้ใกโตซานบึด อุณหภูมิในการทำปฏิกิริยา ความเข้มของแสงยูวี และความเข้มข้นเริ่มต้นของฟีนอล ้จากการทดลองพบว่าบืดไททาเนียมไดออกไซด์ดัดแปรที่กราฟท์บนไคโตซาน ที่ความเข้มข้นของ ้ใททาเนียมใคออกไซด์ดัดแปรเท่ากับ 1% (โดยน้ำหนักต่อปริมาตร) เป็นความเข้มข้นที่ดีที่สุด ้สำหรับการเกิดปฏิกิริยาเมื่อเทียบกับความเข้มข้นอื่น ๆ เมื่อเพิ่มระยะห่างระหว่างหลอดยุวีและ ้ผิวหน้าของสารละลาย และเพิ่มความเข้นข้นเริ่มต้นของฟีนอล มีผลทำให้การสลายตัวของฟีนอล ้ลดลง ในขณะที่การเพิ่มอุณหภูมิของปฏิกิริยาและความเข้มของแสงทำให้ฟีนอลเกิดการสลายตัว มากขึ้น ทั้งนี้การกวนสารละลายในขณะเกิดปฏิกิริยาก็ช่วยเพิ่มการสลายตัวของฟีนอลเช่นกัน เมื่อ ทคสอบประสิทธิภาพของบีคไททาเนียมไคออกไซค์คัคแปรที่กราฟท์บนไกโตซานคังกล่าวในการ ้กำจัดฟืนอล พบว่ามีประสิทธิภาพลดลงเพียง 10% หลังผ่านการใช้ซ้ำ 5 ครั้ง

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In this research, three types of beads as alternative means for phenol treatment were developed. Titanium dioxide blended chitosan beads (chitosan-TiO₂) and modified titanium dioxide (TiO₂) grafted chitosan were synthesized through the use of chitosan as a recovery agent. In addition, TiO₂ spheres were prepared which exploited chitosan as a binder. The adsorption-photodegradation of phenol in the presence of chitosan and various UV irradiated titanium dioxide (TiO₂) catalysts was investigated. The results revealed that modified TiO₂ grafted chitosan beads showed the best ability to remove phenol. The effect of glutaraldehyde concentration and glutaraldehyde incubation time on the modification of TiO₂ was investigated. An optimum condition was to use 3.75% of glutaraldehyde and incubated for 1 h. The degradation of phenol depended on several parameters such as the distance between UV lamp and surface of the solution, agitation of solution, modified TiO₂ concentration that was grafted on chitosan beads, reaction temperature, light intensity and initial phenol concentration. The modified TiO₂ grafted on chitosan beads at 1% (w/v) of modified TiO₂ exhibited the best concentration for the degradation of phenol when compared with other concentrations. An increase of the distance between UV lamp and surface of the solution and initial phenol concentration showed a decrease of phenol photodegradation. On the other hand, when the reaction temperature and light intensity increased, the removal of phenol increased. Besides, the agitation of solution during the photodegradation process had an effect on the enhancement of phenol degradation. The efficiency of modified TiO_2 grafted chitosan beads at 1% (w/v) of modified TiO₂ to degrade phenol was about 10% decrease when they were reused after 5 times.

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LIST OF ABBREVIATIONS

%	percentage
μm	micrometer (s)
А	absorbance
C_0	the initial phenol concentration
Ct	the concentration of phenol in solution at a given time
cm	centimeter
cm ⁻¹	unit of wave number
°C	degree Celsius (centrigrade)
D	the distance between UV lamp and the surface of the solution
%DD	degree of deacetylation
g	gram (s)
FTIR	Fourier Transform Infrared
h	hour (s)
kDa	kilodalton
kV	kilovolt
mL	milliliter (s)
ml/h	milliliter per hour
min	minute (s)
nm	nanometer (s)
рН	power of hydrogen ion or the negative logarithm (base ten)
SEM	Scanning Electron Microscopy
W	watt
w/v	weight/volume
w/w	weight/weight
XRD	X-ray diffraction

CHAPTER I INTRODUCTION

Nowadays, water pollution is becoming a very serious problem that must be solved, especially wastewater from industries which are contaminated with fat, oil, insecticide, detergent, organic and inorganic substances. From the disclosure of Greenpeace Southeast Asia shows that each year the production and importation of chemical reagents for Thai industries are more than 30.4 million tons (Greenpeace Southeast Asia, 2011: online). It is not amazing that industrial wastewater will inevitably be contaminated with these reagents and are often released in water without any further treatments. To avoid water pollution, these compounds need to be removed or degraded before being released to the environment.

Phenol is an organic compound that becomes the most abundant pollutant in industrial wastewater because it is widely used in various manufacturing processes such as dyes, pharmaceuticals, pesticides and solvents. Due to its toxicity, phenol in wastewater needs to be degraded to an acceptable level before it is discharged to the environment. The destruction of phenol by using titanium dioxide (TiO₂) catalyst in photocatalysis process was reported to degrade phenol to harmless end products such as CO_2 , H_2O . Nevertheless, TiO_2 powder has some limitations in recovering and recycling process at industrial scale. Therefore, in this work we are interested in the use of chitosan as a support for TiO_2 to degrade phenol from wastewater and various parameters which effect phenol photodegradation will be studied.

1.1 Phenol

Phenol is one of a number of chemically active compounds which is found throughout nature, especially in plants. Their molecules consist of hydroxyl functional group (OH) bonded to the ring of an aromatic compound — a molecule that includes at least one ring of carbon atoms. The word *phenol* may also refer to carbolic acid (C_6H_5OH) (Figure 1.1), the simplest form of this group of chemicals and heralded the toxicity.

Figure 1.1 Structure of phenol.

Phenol is a white crystalline (at room temperature), odorous and toxic chemical compound which is widely used as a raw material in the manufacture of other chemical products. It is vastly used in the synthesis of dyes, pharmaceuticals, pesticides and solvents (Keith and Telliard, 1979; Rubin et al., 2006; Laoufi et al., 2008). The physical and chemical properties of phenol are shown in Table 1.1. Phenol was originally isolated from coal tar streams, but through technological advances it is now almost entirely produced synthetically. The dominant process in use today is the distillation from petroleum and synthesis by oxidation of cumene (a product of benzene and propylene reaction) and the subsequent cleavage of cumene

hydroperoxide to form phenol and acetone, and by vapor-phase hydrolysis of chlorobenzene (Figure 1.2) (Carey, 2000). In 2004, the total annual capacity of phenol production approached 3 billion kilograms (CMR, 2005).



Figure 1.2 Industrial synthesis of phenol (Carey, 2000).

Common synonyms	acidum carbolicum, acidum phenolicum,		
	benzophenol, carbolic acid,		
	hydroxybenzene,		
	monohydroxybenzene,		
	oxybenzene, phenic acid, phenyl		
	hydroxide, phenylic acid, phenylic		
	alcohol		
Description	colourless to light pink solid		
Molecular formula	C ₆ H ₅ OH		
Molecular weight	94.11 g/mol		
Density	1.0576 g/cm ³ @ 20° C		
Boiling point	181.75° C		
Melting point	40.9° C		
Vapor pressure	0.3513 torr @ 25° C		
Odor threshold	40 ppb (150 mg/m^3) (Amoore and		
	Hautala, 1983)		
Solubility	86,000 ppm in water, very soluble in		
	alcohol, carbontetrachloride, acetic		
	acid and liquid sulfur dioxide; soluble		
	in chloroform, ethyl ether, carbon		
	disulfide; slightly soluble in benzene		
Henry's Law Constant	3.97 x 10 ⁻⁷ ATM-m ³ /mol (25 °C)		
Conversion factor	1 ppm = 3.85 mg/m^3		

 Table 1.1 Physical and chemical properties of phenol (HSDB,2008)

1.1.1 Phenol toxicity

Phenol is rapidly absorbed following inhalation, ingestion and through the skin. The noxious influence of phenols and their derivatives concerns acute toxicity, histopathological changes, mutagenicity and carcinogenicity (Michałowicz and Duda, 2006). Acute ingestion and skin exposure can cause systemic effects such as anorexia, headache, dark urine, hypothermia, hypotension, arrhythmia and coma. Chronic exposure of phenol may cause skin irritation, inflammation, anorexia, weight loss, salivation, muscle weakness, liver and kidney damage (IRIS, 2002).

1.1.2 Metabolism of phenol (IRIS, 2002)

Phenol metabolic pathway is shown in Figure 1.3. After oral uptake of phenol, the liver, lungs and the gastrointestinal mucosa are the most important sites of phenol metabolism (WHO, 1994). Phenol is directly conjugated with glucuronic acid or sulfate to phenyl glucuronide or phenyl sulphate, respectively. It has been shown to be major metabolic pathways in several species. However, phenol that is not directly conjugated will be a substrate for oxidation reactions. The oxidation products of phenol were hydroquinone and catechols which were generated by the cytochrome P450 2E1 isozyme (CYP2E1), a member of the cytochrome P450 mixed-function oxidase system. These products can be further oxidized by CYP2E1 to trihydroxybenzene or by peroxidation to benzoquinone. Alternatively, the conjugation reactions of hydroquinone or catechol metabolites can occur. In addition, some studies have suggested that biphenols and diphenoquinones can also be produced when peroxidative metabolism of phenol takes place.



Figure 1.3 Metabolic pathways for phenol (IRIS, 2002).

1.1.3 Phenol treatment methods

Many different treatment methods have been used for the removal of phenol from wastewater, for example microbial degradation (Folsom et al., 1990; Al-Mahin et al., 2010), incineration, solvent extraction (Egorov et al., 2008; Juang et al., 2008), adsorption (Shawabkeh and Abu-Nameh, 2007) and membrane process (Lee et al., 2008; Wu and Li, 2008).

1.1.3.1 Microbial degradation

Phenol is decomposed by microbes such as *Pseudomonas* and *Candida tropicalis* (Al-Mahin et al., 2010). The microbial species possess enzyme systems that are released for the degradation of phenol to harmless end product.

1.1.3.2 Incineration

High concentration of phenol can be eliminated by incineration. The waste is feed to the incinerator with controlling feed rates in order to result in complete combustion. However, before feeding to the furnace, metals, glass and masonry need to be removed to decrease emission of heavy metals from incinerators and limit emission of other pollutants (Environmental and safety services, 1999).

1.1.3.3 Solvent extraction

The extraction solvents for instance cyclohexane, ethyl acetate, chloroform, kerosene and etc. were used to extract phenol from an aqueous solution (Schellin and Popp, 2005). The optimization of extraction conditions such as adjusting the pH-value for the convertion of the compounds into their polar form and the extraction time are necessary. Furthermore, the addition of some compounds will also have to be investigated in order to enhance the extraction process (Khachatryan et al., 2005).

1.1.3.4 Adsorption

There are many adsorbents that have been used for the removal of phenol. Adsorption onto activated carbon is generally used (Tancredi et al., 2004). Recently, polymeric adsorbents for example chitin, chitosan and alginate have extensively been applied as an alternative to activated carbon owing to the cheap cost and adsorptionregeneration properties. Organic pollutants were flown through the column that contained adsorbent or incubated with adsorption materials to remove them from aqueous phase by ionic adsorption. pH, contact time, initial concentration of adsorbents and amount of biosorbent on its adsorption were an important factors for the removal of organic substances (Nadavala et al., 2009).

<u>1.1.3.5 Membrane process</u>

Membrane process has been considered to eliminate some organics pollutants from wastewater. The principle of this method was the use of pressure driven membrane processes for the removal of low molecular weight organic compounds from wastewater (Bódalo et al., 2008). For the removal of phenol, the experiment conditions such as feed phenol concentration, pressure and pH were studied so as to enhance the removal efficiency (Bódalo et al., 2009).

Although the method described above show the capability for the removal of phenol, they have some disadvantages. Despite the use of microorganisms in treatment of phenolic compound in polluted wastewater produce nontoxic end products, the processes for microbial screening, culture and optimize condition finding are difficult and time consuming. Moreover, when the environment changes, the microbes probably will not be active and may generate secondary toxic intermediates (Busca et al., 2008; Patra and Munichandraiah, 2008).

The air pollution may occur on incineration process. The large quantities of black smoke and the emission of high levels of dioxins were taken place in incomplete combustion which are dangerous to human (Duff, 2006: online).

Solvent extraction, adsorption and membrane process methods are found to be ineffective because they only transfered the organic pollutants from water to another medium without degradation or mineralization of organic pollutants (Thiruvenkatachari et al., 2008).

Recently, a new treatment technology known as a photocatalysis process has been developed. It is capable of the destruction of many organic compounds including phenol to safe end products such as CO_2 , H_2O and mineral acid (Qourzal et al., 2006; Shawabkeh et al., 2010).

1.2 Photocatalytic process

Photocatalysis has become an integral part of the advanced oxidation processes (AOPs). Advances in chemical water and wastewater treatment have led to the development of methods termed AOPs or advanced oxidation technologies (AOTs). AOPs can be generally defined as aqueous phase oxidation methods based on the generation of highly reactive species such as hydroxyl radicals (primarily but not exclusively). These procedures may also be combined with ultra sound reactors, UV irradiation and specific catalysts. This results in the generation of hydroxyl radicals in the mechanisms leading to the degradation of the target pollutant (Vinu and Madras, 2010).

The word photocatalysis is composed of two parts: photo (means light) and the word catalysis (means decompose). It describes a process which light is used to activate a substance, the photocatalyst, which accelerates the rate of chemical reaction without the transformation itself. The photocatalytic reactions may take place homogeneously or heterogeneously. In homogeneous photocatalysis, the reactants and the photocatalysts exist in the same phase. A heterogeneous reaction consists of two phases between a solid photocatalysis (metal or semiconductor) and a fluid containing reactants and products. However, heterogeneous photocatalysis is more studied extensively because it has a potential to be used in various environmental applications. The semiconductors are especially used as photocatalyst due to light absorption properties, charge transport characteristic and exited state lifetime (Kondarides, 2012; online).

Semiconductor photocatalysts (TiO₂, SnO₂, ZnO, WO₃ and etc.) are semiconductors that are able to accelerate chemical reactions on light absorption, typically sunlight (Robertson, 1996). The absorbed photons from the utilizing the energy, photocatalysts can be applied to be used in a wide variety of important chemical processes. Solar fuels production especially hydrogen (H₂) is the ideal fuel for the future because it is clean, energy efficient and renewable energy generated via photocatalytic water splitting over titania and non-titania based photocatalysts (Liao et al., 2012). Environmental remediation also used photocatalyst to destroy many organic pollutants for air or water purification (Bhatkhande et al, 2001; Yu and Brouwers, 2009).

The molecular orbitals of semiconductors have a band structure. The interested bands in photocatalysis are the occupied valence band and the unoccupied conductance band. They are separated by an energy distance, called the energy band gap (E_g) (Figure 1.4). When the semiconductor is irradiated with light of higher energy than that of the band gap, an electron is promoted from the valence band (VB) to the conduction band (CB) and positive hole (h^+) in the valence band is generated. The electron (e^-) and hole (h^+) pair may recombine with the production of heat. However, they can become involved in electron transfer reactions with other species in the solution if they are separated (Robertson, 1996). The band energy of some semiconductor photocatalysts is shown in Table 1.2.



Figure 1.4 In a semiconductor, electrons can be moved from the orbitals in the valence band to the orbitals in the conduction band on illumination.

Semiconductor	Valence band	Conductance	Band gap	Band gap
	(eV)	band (eV)	(eV)	wavelength
				(nm)
TiO ₂	+3.1	-0.1	3.0	380
SnO ₂	+4.1	+0.3	3.9	318
ZnO	+3.0	-0.2	3.2	390
ZnS	+1.4	-2.3	3.7	336
WO ₃	+3.0	+0.2	2.8	443
CdS	+2.1	-0.4	2.5	497
CdSe	+1.6	-0.1	1.7	730
GaAs	+1.0	-0.4	1.4	887
GaP	+1.3	-1.0	2.3	540

 Table 1.2 The band positions of some semiconductor photocatalysts (Robertson, 1996)

Semiconductors can be used in photocatalysis as particle dispersions or in photoelectrochemical mode. Several hybrid structures have been envisaged to improve photocatalytic performance of semiconductors such as semiconductor-semiconductor or semiconductor-metal and semiconductor-support. The major goals for designing semiconductor-metal composite are to improve the catalytic properties and to enhance the photocatalytic effect in the UV-visible light region (Dawson and Kamat, 2001; Weiss et al., 2001).

The photocatalytic degradation based on oxidation-reduction reaction to exterminate organic pollutant molecules, titanium dioxide (TiO_2) is one of the well known semiconductors that has successfully been used as a photocatalyst because of its high efficiency, non-toxicity, stability, low cost and high activity (Thiruvenkatachari et al., 2008).

1.2.1 Titanium dioxide (TiO₂) photocatalyst

Titanium dioxide (TiO₂) is a semiconductor which shows excellent photocatalyst in various fields. The main advantages of TiO₂ are its photochemical inertness when exposed to acidic and basic compounds, nontoxicity, high oxidizing power and relatively low cost, which make it a competitive candidate for many photocatalysis applications (Castellote and Bengtsson, 2011). Three different crystalline modifications of TiO₂ exist, there are anatase (tetragonal), brookite (orthorhombic) and rutile (tetragonal), the crystal structures are represented in Figure 1.5 (Carp et al., 2004). The anatase form exhibits the highest overall photocatalytic activity. Basic physical properties of the anatase-type TiO₂ are listed in Table 1.3.



Figure 1.5 The crystal structures of anatase (a), rutile (b), and brookite (c) (Carp et al., 2004).

Crystal form	Tetragonal system		
Density (g/cm ³)	3.90		
Refractive index	2.52		
Permittivity	31		
Thermal stability	Change to rutile type at high temperature		
	(~800 °C)		

Table 1.3 Basic physical properties of anatase-type of TiO_2 (Castellote and Bengtsson, 2011)

1.2.2 The application of TiO₂

Titanium dioxide is the most widely used white pigment in products such as paints, coatings, plastics, paper, inks, fibres, food and cosmetics because of its brightness and high refractive index (> 2.4) (CERAM Research Ltd, 2002: online). When it is combined with other colours, soft pastel shades can be achieved. Titanium dioxide is allowed to be used at relatively low levels to achieve its technical effect because of the high refractive index that surpassed by few other materials (Hashimoto et al., 2005).

The food applications of titanium dioxide are broad. It is used as colour additive in foods, chewing gum and bubble gum in general at levels not exceed 1%. However, in Japan TiO_2 is used as a food colour without limitation. Besides, TiO_2 is even used in cosmetic and skin care products for example lipsticks, sunblock, soap and body powder (DaNa, 2011: online).

In the environmental applications, environmental remediation includes the degradation, sequestration, or other process approaches, TiO_2 exhibits the benefits for cleanup wastes that results in decreased risks to human and animals by chemical and

radiological contaminants. In 1977, Frank and Bard reported the reduction of CN^{-} in water by using TiO₂ photocatalysis. It was the first use of TiO₂ for the remediation of pollutants. This has led to a dramatic increase in the research in this area due to the utilization of free solar energy for water and air purification.

Wang et al. (1977) reported the use of TiO_2 surfaces with excellent antifogging and self-cleaning abilities. The semiconducting properties of TiO_2 photocatalyst is responsible for the removal of various organic pollutants such as benzene (Einaga et al., 1999), 2,4-dichlorophenol (Trillas et al., 1999; Li et al., 2002), DDT (Quan et al., 2005) and dyes (and Albanis, 2006).

1.2.3 Oxidation-reduction reaction of TiO₂

In photocatalysis, light of energy greater than the band gap of the semiconductor, excites an electron from the valence band (VB) to the conduction band (CB). In the case of anatase TiO₂, the energy band gap is 3.2 eV, therefore UV light ($\lambda \leq 387$ nm) is required. The diagram of photocatalytic degradation is shown in Figure 1.6. An electron (e⁻) was excited to the CB when the absorption of a photon occurs to generate a positive hole (h⁺) in the VB (eq.1) (Pillai et al., 2012). The e⁻ and h⁺ interact with molecular oxygen that adsorbed on TiO₂ surface to produce superoxide radical anions, O₂⁻⁻ (eq.2), and with water to yield the highly reactive hydroxyl radicals, HO• (eq.3), respectively. This radical species oxidize a large number of organic substrates to safe end products (eq.4) (Emeline et al., 2001; Horikoshi et al., 2001; Laoufi et al., 2008).

$$TiO_2 + hv \longrightarrow e^{-}_{cb} + h^{+}_{vb}$$
(1)

$$e_{cb}^{-} + O_2(ads) \longrightarrow O_2^{-}$$
 (2)

$$h^+_{vb} + Ti-OH_2 \longrightarrow HO^{\bullet}_{ads} + H^+$$
 (3)

$$HO_{ads}^{\bullet} + Pollutant \longrightarrow Photooxidized product \longrightarrow CO_2 + H_2O$$
(4)



Figure 1.6 Diagram of photocatalytic degradation of TiO_2 .

1.3 Phenol destruction by TiO₂ photocatalyst

The intermediates such as catechol, hydroquinone and benzoquinone occurred from the reaction of phenol photocatalytic oxidation in the presence of irradiated TiO₂ were detected (Lupetti et al., 2004). The possible mechanism of the destruction of phenol is shown in Figure 1.7 (Sobczynski et al., 2004). UV illumination of TiO₂ suspension leads to charge carriers (electron (e⁻) and hole (h⁺)) generated at the surface of the photocatalyst. Photoinduced holes have sufficient oxidizing power to react with hydroxide ions or water molecules producing hydroxyl radicals (•OH). This •OH attacks on the substrate. It has been shown that dihydroxybenzene (catechol, resorcinol and hydroquinone) and *p*-benzoquinone exist in equilibrium solution. It is possible that *p*-benzoquinone can be produced in three different ways: (1) hydroquinone molecule was attacked by •OH, (2) in the reaction of phenol molecule with holes photogenerated in TiO₂ and (3) hydroquinone was directly oxidized by oxygen dissolved in water. Moreover, hydroquinone can be hydrated further to create glycerin and ethanedial. However, 40% of p-benzoquinone solution has a fast oxidation in the presence of illuminated TiO2 which can lead directly to oxygencontained aliphatic compounds with no further hydroxylation of the compound. In addition, about 60% of the compounds were transferred into hydroquinone. Four compounds of aliphatic intermediates including formic and acetic acids in the reaction mixture were detected. CO₂ and H₂O are the harmless end products of the reaction.



Figure 1.7 The possible mechanism of the destruction of phenol on TiO_2 photocatalyst (Sobczynski et al., 2004).

1.4 Chitosan

In the 21st century, science and technology has moved forward to the renewable raw materials and more environmentally friendly. The natural biopolymer chitin is one of the most common natural polysaccharide after cellulose. Chitosan is the derivative of chitin prepared by the de-*N*-acetylation of chitin which makes up the shells, crabs, shrimp and the cell wall of fungi (Chao et al., 2004).

Chitosan is a natural polymer generally obtained by the deacetylation of chitin which is found in the exoskeletons of shellfish i.e. crab, lobster and shrimp, the cell walls of fungi, cuticles of insects and some algae. Chitosan is a linear polymer of α (1 \rightarrow 4)-linked 2-amino-2-deoxy- β -D-glucopyranose. It is easily derived by N-deacetylation of chitin and is consequently a copolymer of N-acetylglucosamine and

glucosamine linked by β -(1-4)-glycosidic linkages (Dutta et al., 2004). The structure of chitosan (Figure 1.8) consists of reactive amino and hydroxyl groups that make chitosan very useful in biomedical field and has been found to be highly biocompatible, cosmetic and other applications using its derivative. Chitosan dissolves easily at low pH while it is insoluble at higher pH ranges (Dutta et al., 2004).



Figure 1.8 Structure of chitin and chitosan.

The degree of deacetylation (%DD) has a significant effect on the solubility and rheological properties of polymer. The degree of deacetylation is one of the most important chemical characteristics of chitosan. Chitosan solubility, biodegradability, reactivity, and adsorption of many substrates depend on the amount of protonated amino groups in the polymeric chain (Rinaudo, 2006). This determines the content of free amino groups in the polysaccharide. Methods for checking the removal of acetyl groups in chitosan include UV spectrophotometry, IR spectrometry, gas chromatography and dye adsorption (Mi et al., 1999). The main attractive force in the development of chitosan is that chitin is the second abundant polymer in nature next to cellulose and thus, more economic. Moreover, chitosan has many beneficial properties such as biocompatibility, biodegradability, hydrophilicity, nontoxicity, anti-bacterial property and high flexibility. For example, they can be formulated into beads, fibers, capsules, powders, gels, membranes, hydrogels and etc. which make chitosan based materials has been applied in food processing, pharmaceutical, agriculture. In addition, chitosan exhibits good adsorption ability for many organic pollutants which has been widely used in the environmental treatment for example, the removal of dye, heavy metals and organic substances (Nawi et al., 2010; Ravi Kumar, 2000; Zheng et al., 2004).

1.4.1 Application of chitosan

1.4.1.1 Food processing

Chitosan has been widely used in food industry because it is non-toxic to human. These biopolymers offer a wide range of unique applications including bioconversion for the production of value-added food products, preservation of foods from microbial deterioration, formation of biodegradable films and clarification and deacidification of fruit juices (Dutta et al., 2004). Other applications of chitosan in food industry are listed in Table 1.4.

1.4.1.2 Cosmetics

Chitosan and hydrophobic substances are compatible with various biologically active components and thus, find a wide application in cosmetics. Chitosan is a natural cationic gum that becomes viscous when mixed with acid which simplifies its interaction with skin covers and hair. It is possible to modify chitosan to chitosan derivatives with varying chain lengths and thus, different properties. For instance, to improve chitosan solubility, the chemical reactions such as acylation, alkylation hydroxyalkylation and carboxyalkylation were employed (Aranaz et al., 2010). In cosmetics the properties operated are bacteriostatic, fungistatic, film-forming, moisture retaining and controlled release of active agent. Some of the applications mentioned in cosmetics are creams, lotions, colour cosmetics (eye shadow, lipstick, make-up, nail polish), shampoo, toothpaste.
Table 1.4 Food applications of chitin, chitosan and their derivatives (Shahidi et al.,

1999)

Area of application	Example
Antimicrobial agent	Bactericidal
	Fungicidal
	Measure of mold contamination in
	agricultural commodities
Edible film industry	Controlled moisture transfer between
	food and surrounding environment
	Controlled release of antimicrobial substances
	Controlled release of antioxidants
	Controlled release of nutrients, flavours
	and drugs
	Reduction of oxygen partial pressure
	Controlled rate of respiration
	Controlled enzymatic browning in fruits
	Reverse osmosis membranes
Additive	Clarification and deacidification of fruits
	and beverages
	Natural flavor extender
	Texture controlling agent
	Emulsifying agent
	Food mimetic
	Thickening and stabilizing agent
	Colour stabilization
Eta	

Etc.

1.4.1.3 Agriculture

Chitosan has many potential applications in agriculture because the polymer is essentially naturally occurring and biodegradable. Therefore, it should not cause any pollution problems. Chitosan is found to accelerate and enhance growth. Chitosan can be used as seed coating because it has many beneficial effects, such as inhibition of fungal pathogens in the vicinity of the seeds and addition of potting mixture/soil and enhancement of plant-resistant response against diseases (Tseng, 2009: online).

1.4.1.4 Pharmaceutical and biomedical

Chitosan have demonstrated their effectiveness for all forms of dressingsartificial skin, bandages and sponges for surgical treatment because its biocompatibility with human body tissue (Tseng, 2009: online). Chitosan is an excellent medium for reducing side effect, to be used in direct tablet compression, as a tablet disintegrant for the production of controlled release solid dosage forms or for the improvement of drug dissolution (Ravi Kumar, 2000).

1.4.1.5 Wastewater treatment

The biopolymer chitosan can be used as an effective flocculating agent for organic compounds, as a chelating agent and toxic heavy metals trapper, as well as an adsorption medium for dyes and small concentrations of petroleum product, phenols, PCBs and etc. present in various industrial wastewaters. In addition, the amino groups in chitosan are reactive functional groups that can be altered chemically for the production of other chitinous derivatives with specific useful characteristics, for example, as effective absorptive agents. Chitosan exhibiting different physicochemical characteristics, i.e., molecular weight, crystallinity, deacetylation, particle size, and hydrophilicity, differ in their effectiveness as waste treatment agents. Regenerated chitosan and other chitinous membranes could be broadly used for osmosis, reverse osmosis, micro-filtration, desalination and dialysis (No and Meyers, 2000; Dutta et al., 2004). Moreover, chitosan acts as a support for enzyme immobilization and for other catalysts in order to degrade various organic pollutants from wastewater.

Shao and coworkers (2007) studied the immobilization of polyphenol oxidase (PPO) on cross-linked chitosan–SiO₂ gel for treating phenol solution. The efficiency for the removal of phenol (10 mg phenol/L) by the immobilized PPO was 86%, and retained about 60% removal efficiency after five recycles. The enzyme was stabilized with 73 and 58% retention of activity after 10 and 20 days, respectively, at 30°C under optimized conditions.

There are many researchers focused on the use of chitosan and TiO_2 for environmental treatment including Zainal and coworkers (2009). They suggested the newly explored TiO_2 –Chitosan/Glass as an alternative material via photodegradationadsorption process for wastewater treatment. Approximately, 87% of total methyl orange was removed when four layers of TiO_2 –chitosan/glass photocatalyst was used. This research work suggested a new method having an advantage of photodegradation–adsorption process in order to reduce various wastewater pollutants.

Liu and coworker (2010) prepared chitosan/activated fiber/TiO₂ membrane to remove 2,4-dichlorophenol (2,4-DCP). The results showed that the lower the initial concentration of 2,4-DCP, the higher the removal rate of 2,4-DCP from aqueous

solution by this material. It can be regenerated up to six cycles by UV-photocatalytic degradation process with 90% efficiency.

Nawi and coworker (2011) immobilized the mixture of TiO_2 and chitosan onto a glass plate for phenol removal. The results showed that the reduction rate by the bilayer TiO_2 /chitosan system was faster than the TiO_2 single layer system and slightly better than the TiO_2 powder used in a slurry mode. The adsorption effect of chitosan was negligible and the photodegradation of phenol was largely due to the photocatalytic performance. It represented a good alternative for mineralization of organic pollutants in wastewater.

Chitosan biopolymer has exhibited multifunctional operation with TiO_2 in heterogeneous photocatalysis technology. It is used as a stabilizer, a recovery agent, for enhancing the adsorption capacity of chitosan- TiO_2 adsorbent in the removal of metal ions and for increasing the adsorption-photocatalytic process of the dye species and organic pollutants. Therefore, in this research some alternative materials for wastewater treatment were prepared. We mainly focused on the use of chitosan as a binder and recovered agent for TiO_2 potocatalyst in phenol photodegradation process.

1.5 The objectives of this research

The aim of this study was to prepare three types of $Chitosan-TiO_2/TiO_2$ beads and to study their photocatalytic activity towards phenol.

1.6 The scopes of research

The scopes of this work were as follows:

- 1. Preparation of chitosan-TiO₂ beads where chitosan acted as an entrapped agent.
- 2. Preparation of TiO_2 beads where chitosan acted as a binder.
- 3. Preparation of modified of TiO_2 grafted chitosan beads.
- 4. Characterization of obtained beads by using SEM, IR and XRD.
- 5. Study for their photocatalytic degradation of phenol.
- 6. Selection for the best bead and optimization for the photocatalytic degradation of phenol.
- 7. Study of the reusability of the selected bead for the removal of phenol.

1.7 Obtained results

This research provides valuable information on the preparation of beads from chitosan and TiO_2 for phenol photocatalytic degradation which can be further applied for industrial wastewater treatment.

CHAPTER II

MATERIALS AND METHODS

2.1 Materials

- Titanium dioxide powder (The sun chemical Co., LTD, Thailand)
- Chitosan with MW 200-250 kDa and a degree of deacetylation (DD) of 85%

(Biolife, Thailand)

2.2 Chemicals

- Phenol (Carlo Erba Reagents)
- Glacial Acetic acid (Carlo Erba Reagents)
- Methanol (Merck, Germany)
- Hydrochloric acid (Carlo Erba Reagents)
- Sodium hydroxide (Carlo Erba Reagents)
- Ethanol, commercial grade
- Ethanol (Carlo Erba Reagents)
- Paraffin oil (Carlo Erba Reagents)
- Petroleum ether 35-60 °C (Mallinckrodt Chemicals)
- Tween 80 (Acros Organics)
- Glutaraldehyde 25 wt% (Acros Organics)
- Acetone (Carlo Erba Reagents)
- Titanium tetraisopropxide 99+% (Acros Organics)
- 3-minopropyl trietoxysilane 99% (Acros Organics)

- 4-aminoantipyrine, reagent grade (Sigma Aldrich, USA)
- Potassium ferricyanide, analytical grade (Analar)

2.3 Instruments

Syringe pump (NE-300, New Era Pump Systems)

Analytical balance (AG204, Mettler Toledo)

Scanning electron microscope (XL30CP, Philips)

Micropipette (100-10000 µl) (Volumate, Mettler Toledo)

Micropipette (1-5 ml) (Volumate, Mettler Toledo)

pH-meter Thermo (Orion* 2 star, Fisher Scientific)

Magnetic stirrer (HTS-1003, LMS)

UV-VIS Spectrophotometer (8453(G1103A), Agilent)

UV/VIS lamp (G 10 W, Synvania ultraviolet)

Fourier Transform infrared spectroscopy (Spectrum One, Perkin Elmer)

X-ray diffractometer (X'pert PW 3710, Philips)

Stirring motor (RW 20 digital, IKA)

Oven (FED-EED, WTB Binder)

Centrifuge (Centra MP 4R, IEC)

Bench Furnace (201 comtroller, Carbolite)

Filter paper Syringe Syringe needle Aquarium air pump

2.4 Preparation of beads

In this research, various types of beads were prepared in order to find appropriate type of beads for the removal of phenol.

2.4.1 Preparation of chitosan beads

Chitosan solution was first prepared by dissolving 2%(w/v) of chitosan in 1%(v/v) of acetic acid and filtered. The viscous solution was extruded dropwise using a 26 gauge syringe needle into a beaker containing 10%(w/v) NaOH in 50%(v/v) EtOH solution dissolved in DI water, with a dropping rate of 60 mL/min. Beads were gently stirred for 30 min and washed with DI water until the pH is neutral. The beads were further washed with 250 mL of 50, 75, 100%(v/v) EtOH and acetone, consecutively. The microparticles were dried at room temperature and kept in the oven at 100 °C for 24 h.

2.4.2 Preparation of chitosan-TiO₂ beads

Two sizes of chitosan-TiO₂ beads were prepared to study for the effect of surface area of the beads for the immobilization of TiO₂. It consisted of beads in the diameter range of 500-600 μ m and the diameter range less than 100 μ m.

2.4.2.1 Diameter range of 500-700 μm

Chitosan-TiO₂ was prepared by the addition of various concentration of TiO₂ (0.1, 1, 3 and 50% by wt of chitosan) into 2%(w/v) chitosan solution which dissolved in 1%(v/v) of acetic acid. The solution was stirred until it was homogeneous and beads were produced as described in section 2.4.1.

2.4.2.2 Diameter range less than 100 µm

In this study, chitosan-TiO₂ beads were prepared using the suspension crosslinking technique (Denkbas and Odabasi, 1999).

The homogeneous solution of chitosan-TiO₂ at TiO₂ 1% by wt of chitosan was added dropwise into the dispersion medium which consisted of 500 mL of paraffin oil and petroleum ether (25/35, v/v) and Tween 80 0.02 mL/mL medium as an emulsifier. During this process, the medium was stirred with a mechanical stirrer at 1000 rpm for 10 min. After that, glutaraldehyde at 0.033 mL/mL medium was added into the dispersion medium and then stirred for 1 h. Then, 0.033 mL/mL medium of glutaraldehyde was added again into the same medium and stirred for 2 h. The microspheres were collected by centrifugation at 3500 rpm, 25 °C for 15 min and washed twice with 100 mL of petroleum ether and twice with 100 mL of acetone. The microspheres were then dried in an oven at 50 °C for 24 h.

2.4.3 Preparation of TiO₂ spheres

TiO₂ spheres were prepared according to Vega et al., 2011. Titanium tetraisopropoxide (Ti(OPr)₄) was used as the precursor of TiO₂. 0.01 mol of Ti(OPr)₄ was added to the solution containing ethanol, DI water, and HCl (37%) in the ratio of 1:0.25:0.1 with continuous mixing by stirrer. The mixture was stirred for 2 h at 25 °C. Commercial TiO₂ powder (5% wt of Ti(OPr)₄) which was used as the filler material was added to the clear sol and the solution was stirred vigorously with magnetic stirring. The homogeneous solution was then added to the 3%(w/v) of chitosan solution and then stirred for 30 min. Sphere formation was produced as described under section 2.4.1. Finally, the spheres were dried at 80 °C for 20 h in the oven and calcined in the furnace at 600 °C for 3 h to remove the remaining chitosan. This type of beads, chitosan acted as a binder in order to make spheres before it was removed.

2.4.4 Preparation of modified TiO₂ grafted chitosan beads

2.4.4.1 Modification of TiO₂ surface

The modified TiO₂ grafted chitosan beads were prepared according to Simi et al., 2009 and Andrzejewska et al., 2004. Four grams of TiO₂ was treated with 4 g NaOH in 100 mL distilled water. The reaction was refluxed at 85 °C for 2 h. After, precipitate was collected, 46.8 mL of 3-aminopropyl trietoxysilane, 140.7 mL of DI water and 46.8 mL of EtOH were added and the pH was adjusted to 1 with concentrated HCl. The reaction was refluxed at 85 °C for 8 h and the precipitate was collected by centrifugation at 4000 rpm, 25 °C for 15 min and washed with EtOH until the pH is neutral. The modified sample was dried at 100 °C overnight in the

oven and ground with mortar. The ground modified sample was mixed with 0.1%(w/v) glutaraldehyde in isopropanol. This medium was stirred using magnetic stirrer for 8 h at 25 °C. Precipitate formed was washed with isopropanol, centrifuge at 4000 rpm, 25 °C for 15 min. The modified sample was dried at 80 °C overnight in the oven.

In this part of the study, concentration of glutaraldehyde 0, 0.1, 1, 2, 3.75, 5 and 10% (w/v) were used. The concentration that gave the best result was selected to study for the effect of glutaraldehyde incubation time. The incubation time (1, 2, 4, 6, 8 and 10 h) of glutaraldehyde with ground modified sample were then investigated.

2.4.4.2 Modified TiO₂ grafted chitosan beads

Various amount of modified TiO₂ (0.01, 0.1, 1, 5 and 10% (w/v)) were dispersed in a mixture of DI water:ethanol (1:9 v/v). The suspensions of modified TiO₂ consisted of various amount of modified TiO₂ in 5 mL of DI water. The mixture was sonicated for 10 min and 45 mL of ethanol was added to give a total volume of 50 mL. The mixture was sonicated again for 20 min. The suspension was then mixed with 30 g of wet chitosan beads from section 2.4.1 and sonicated for 20 min. Modified TiO₂ grafted chitosan beads were washed five times with 100 mL of mixture of DI water:ethanol (1:9 v/v) and dried at 100 °C in the oven overnight. Beads were kept in a vacuum desicator for further study.

2.5 Characterization of beads

2.5.1 Scanning Electron Microscope (SEM)

The morphology of various types of beads was observed by SEM (Phillips, XL30CP). The samples were mounted directly onto the SEM sample holder using double-side sticking tape and were gold spray-coated. Scanning was carried out under high vacuum with electron voltage of 20 kV.

2.5.2 X-ray diffractometer (XRD)

To determine the crystal structure and crystallinity, TiO_2 and modified TiO_2 were investigated by XRD (Rigaku, DMAX) with Cu K α radiation (λ =0.15406 nm) at a voltage of 40 kV and current of 30 mA. The prepared sample was taken to expose to the x-ray diffraction chamber. The X-ray diffraction patterns were recorded in the 20 angle range of 5° to 80°.

2.5.3 Fourier Transform Infrared – Attenuated Total Reflectance (FTIR-ATR)

The distinctive functional groups were recognized by FTIR-ARR (Perkin Elmer, Spectrum One). An attenuated total reflection accessory operates by measuring the changes that occur in a totally internally reflected infrared beam when the beam comes into contact with sample directly. The samples were scanned between 4000 and 500 cm^{-1} .

2.6 The photocatalytic experiments

In this work, the photodegradation chamber was designed as shown in Figure 2.1. Two-hundred milliliters of phenol aqueous solution and 0.3-0.5 g of beads were loaded into a beaker and oxygen was flown through the solution using aquarium air pump. The distance between UV lamp and the surface of solution was set at 15 cm in a dark chamber. The beads and the solution were then irradiated under UV lamp (G 10 W, Synvania ultraviolet) for 8 h. At the desire irradiation time interval, 2 mL portions of the solution were sampled. The concentration of phenol was analyzed by colorimetric assay using 4-aminoantipyrine (4-AAP) and potassium ferricyanide (K₃Fe(CN)₆). One milliliter of 10 mM 4-AAP in 100 mM carbonate buffer pH 10 and 1 mL of 10 mM K₃Fe(CN)₆ in 100 mM carbonate buffer pH 10 were added respectively into 1 mL of phenol sample. The mixture was incubated for 6 min and the absorbance was then read at 510 nm (Wagner and Nicell, 2002). The % reduction of phenol was calculated by the formula:

% Reduction =
$$[(C_0 - C_t)/C_0] * 100$$

Where C_0 and C_t are the initial phenol concentration and the concentration of phenol in solution at a given time.

The distance between UV lamp and the surface of the solution (10, 15, 20 cm), the stir of the solution, modified TiO_2 concentration (0.01, 0.1, 1, 5, 10% (w/v)), temperature (20, 30, 40, 50, 60 °C), light intensity (10, 20, 30 and 40 W) and initial phenol concentration (10, 25, 50 and 100 mg/L) were varied, respectively, in order to investigate the effects of these parameters on phenol degradation. An optimum condition was then chosen for further study.



Figure 2.1 Photodegradation chamber for phenol degradation.

2.7 Recycling test

For each new cycle, beads were filtered using colander, washed 3 times with 50 mL of DI water and once with 50 mL of EtOH. The beads and the washing solution were shaken by mechanical shaker for 10 min and beads were collected by colander before next washing. The washed beads were then dried in oven at 100 °C before use in the next cycle.

CHAPTER III

RESULTS AND DISCUSSION

In this work, various types of beads were prepared through the use of chitosan as a recovery agent and binder and as a support for TiO₂ photocatalyst in the phenol photodegradation process. The materials were characterized by Scanning Electron Microscope (SEM), X-ray diffractometer (XRD) and Fourier Transform Infrared Spectroscopy (FT-IR). The effects of parameters on phenol photodegradation were investigated.

3.1 Characterization of chitosan-TiO₂ beads

Chitosan-TiO₂ beads were prepared for the photodegradation of phenol. Chitosan solution was mixed with TiO₂ powder and then the beads were produced by dropping into a beaker containing 10%(w/v) NaOH in 50%(v/v) EtOH solution using syringe needle. Chitosan acted as a recovery agent for TiO₂ which was trapped inside chitosan-TiO₂ beads. Chitosan beads without TiO₂ were also prepared and used as a control.

The microstructure of chitosan beads and chitosan-TiO₂ beads were analyzed using Scanning Electron Microscope (SEM). SEM analysis gives the information about the sample's surface, topography and composition. The result is shown in Figure 3.1, both beads had spherical shape with the size range of 500-700 μ m and had rather smooth surface.

The beads were then subjected to the Energy-dispersive X-ray spectroscopy (EDX) analysis to investigate what elements were found on the surface of the beads. The result is illustrated in Figure 3.2. It showed that the surface of the chitosan beads and chitosan-TiO₂ beads contained a mixture of C and O which were the main elements of chitosan structure (Larnoy et al., 2011). However, the surface of chitosan beads were contaminated with a small amount of Si and Mg while the surface of chitosan-TiO₂ beads were contaminated with a small amount of Si and Ca. These elements were not the component of chitosan, they maybe spreaded in the air and adhered on the surface of beads. Nevertheless, TiO₂ particles could not be observed on the surface of chitosan-TiO₂ beads. It was presumed that TiO₂ was thus, immobilized in the internal chitosan microsphere.



Figure 3.1 SEM picture of 2% (w/v) chitosan in 1% (v/v) acetic acid (a) and chitosan-TiO₂ beads at 1 % of TiO₂ by wt of chitosan (b).



Figure 3.2 EDX pictures of chitosan beads (a) and chitosan-TiO $_2$ beads (b).

3.2 Phenol photodegradation of chitosan-TiO₂ beads

3.2.1 The effect of TiO₂ dosage of chitosan-TiO₂ beads on phenol photodegradation

Although TiO_2 could not be observed on the surface of chitosan- TiO_2 beads, they were tested for the removal of phenol by photodegradation process.

The dosage of TiO₂ is an important parameter in photocatalytic degradation process. To determine the optimum dosage of photocatalyst, various amount of TiO₂; 0, 0.1, 1, 3 and 50% wt of TiO₂ to chitosan) was prepared. 0.5 g of beads was mixed with 10 mg/L of 500 mL phenol solution. The % reduction of phenol at desired time was calculated (see Appendix A) and plot against reaction time. It can be seen from Figure 3.3 that the % reduction of phenol in the presence of TiO₂ catalyst after 8 h UV irradiation was higher when compared with the reaction mixture without the TiO₂ photocatalyst. The reduction of phenol using chitosan-TiO₂ beads after 8 h UV irradiation at 0.1, 1, 3 and 50% wt of TiO₂ to chitosan were 28.52, 35.67, 32.81 and 28.95%, respectively while chitosan beads without TiO_2 showed 23.08% reduction of phenol. This could be explained by the fact that chitosan has the adsorption ability to remove several organic pollutants including phenol and phenol also was degraded by photolysis process (Nawi et al., 2011; Wu et al., 2001; Zheng et al., 2004). The presence of chitosan-TiO₂ could remove phenol from 5-13 % higher than the reaction mixture without TiO_2 . For some reasons, TiO_2 may not be able to degrade phenol efficiently because TiO₂ was not observed on the chitosan surface and thus, resulting in the shielding by chitosan layer. Moreover, from SEM picture (Figure 3.1),

chitosan-TiO₂ had a spherical shape in the size range of 500-700 μ m, the surface area per gram support was maybe too low to react with all of phenol molecules. To enhance the surface area per gram support, the smaller size of the beads were then synthesized. However, chitosan-TiO₂ at 1% wt of chitosan was shown to be the best material for phenol removal in comparison with other TiO₂ concentration. Hence, chitosan-TiO₂ at 1% was chosen to compare the capability on phenol degradation with the chitosan-TiO₂ beads in the diameter range less than 100 µm.



Figure 3.3 Effect of the dosage of TiO₂ catalyst on phenol removal (chitosan beads (\bullet), chitosan-TiO₂ 0.1% (\blacksquare), chitosan-TiO₂ 1% (\blacktriangle), chitosan-TiO₂ 3% (\times), chitosan-TiO₂ 50% (\times). Condition: chitosan-TiO₂ beads = 0.5 g, initial phenol concentration = 10 mg/L, 500 mL and the distance between UV lamp and the surface of the solution = 15 cm. The error bars represent the standard deviation of three experiments.

3.2.2 Effect of surface area on phenol photodegradation

Chitosan-TiO₂ beads in the diameter range less than 500-700 μ m were prepared by water in oil (W/O) suspension crosslinking technique. SEM picture of these beads is presented in Figure 3.4. It can be seen that the beads had spherical shape in the size range of 20-100 µm (Figure 3.4a). Moreover, the surface of the beads was rather rough. The phenol photodegradation of chitosan-TiO₂ beads of both sizes were investigated as previously described. The result (Figure 3.5) indicated that the removal of phenol by the beads in the diameter range of 500-700 µm was higher than the size range of 20-100 μ m about 10%. Both types of beads were subsequently subjected to surface area analysis by Brunauer-Emmett-Teller (BET) surface area analyzer method. The chitosan-TiO₂ beads in the diameter range of 20-100 µm showed higher BET surface area (average 4.56 m^2/g) which should facilitate the adsorption of phenol and should enhance the phenol photodegradation than that of the size range of 500-700 μm (1.73 $m^2/g).$ This could be explained by the fact that the medium (paraffin oil and petroleum ether (25/35, v/v)) which was used in W/O emulsification suspension method to produce chitosan-TiO₂ beads in the diameter range 20-100 µm was maybe embedded in the pore of beads. In washing step, paraffin oil could not be washed out completely from the chitosan pore which made it act as a barrier to obstruct phenol adsorption on chitosan and hinder the reaction between UV light and TiO₂ that was contained in chitosan-TiO₂ beads.



Figure 3.4 SEM picture of chitosan-TiO₂ 1.0 % wt chitosan in in the diameter range 20-100 μ m at 100X (a) and 1,500X (b).



Figure 3.5 Phenol photodegradation of chitosan-TiO₂ beads in the diameter range 500-700 μ m (•) and 20-100 μ m (•). Condition: chitosan-TiO₂ beads = 0.5 g, initial phenol concentration = 10 mg/L, 500 mL and the distance between UV lamp and the surface of the solution = 15 cm. The error bars represent the standard deviation of three experiments.

From the results in Figure 3.3 and 3.5, chitosan was used as a recovery agent to store TiO_2 in chitosan beads. The chitosan behaved as a wall to hinder the reaction between TiO_2 and phenol solution. In order to eliminate the negative effect of chitosan, chitosan was then used as a binder to produce TiO_2 spheres. Chitosan solution was mixed with synthetic TiO_2 sol and the beads were formed. After that the spheres were heated at 600 °C to remove any residual chitosan and TiO_2 spheres were generated. The spheres were further characterized and tested for phenol photodegradation.

3.3 Characterization of TiO₂ spheres

TiO₂ spheres had an average diameter of 500-700 μ m (Figure 3.6a). When zoomed in the surface of TiO₂ spheres, an assemblage of spherical particles of TiO₂ in varying size ranging from 30 to 300 nm in diameter was observed (Figure 3.6b).



Figure 3.6 SEM images of TiO_2 spheres (a) and the surface of TiO_2 spheres (b).

TiO₂ spheres were then ground and characterized by X-ray diffractometer (XRD) to determine the crystal structure and crystallinity. XRD patterns of commercial TiO₂ powder and ground-TiO₂ sphere are illustrated in Figure 3.7. XRD patterns of commercial TiO₂ which had diameter ranging from 100 to 200 nm showed strong diffraction peaks at 25°, 37° and 48° (Figure 3.7a). These are the characteristics of TiO₂ in anatase form (Thamaphat et al., 2008). The XRD pattern of commercial TiO₂ showed that it is an anatase form which is the most active form of TiO₂. Ground-TiO₂ spheres had diameter ranging from 20 to 50 nm. The diffraction pattern was found to be the same as that of the commercial TiO₂ but lower intensity

was obtained (Figure 3.7b). This could be due the fact that amorphous TiO_2 particles were found. In calcination step, chitosan- TiO_2 sphere were heated at 600 °C to remove chitosan and then TiO_2 spheres were produced. The temperature used for calcination might be too low and thus, an amorphous structure appeared in the sample. It has been shown that an increase in calcined temperatures increased crystallinity of TiO₂ (Wongkaew et al., 2010; Zang et al., 2002).



Figure 3.7 X-ray diffraction of TiO_2 powder in anatase form; commercial TiO_2 (a), and ground- TiO_2 sphere (b).

3.4 Phenol photodegradation of TiO₂ spheres

The ability of three types of materials as photocatalysts for the degradation of phenol was investigated. Chitosan-TiO₂ beads at 1.0% wt of chitosan, TiO₂ spheres and commercial TiO₂ powder containing 100 mg of TiO₂ were mixed with 10 mg/L of 500 mL phenol solution. The distance between UV lamp and the surface of solution was set at 15 cm in a dark chamber. The beads and the solution were then irradiated under UV lamp for 8 h. The degradation efficiency of phenol during UV illumination is illustrated in Figure 3.8.

TiO₂ powder was found to be highly photoactive in phenol degradation. After 8 h of UV irradiation, 75% of phenol was degraded. For the degradation of phenol in the presence of chitosan-TiO₂ beads and TiO₂ spheres, 43 and 31% of phenol degradation were observed, respectively. TiO₂ spheres should exhibit better activity for the removal of phenol due to the fact that the surface of TiO₂ spheres contained very small particle size of TiO₂. Hence, they should have high surface area to react with phenol. Furthermore, the effect of chitosan was negligible because chitosan was completely removed by calcination. However, TiO₂ spheres showed the smallest ability for phenol degradation which had an ability to adsorb phenol. Consequently, chitosan-TiO₂ beads showed higher removal of phenol than that of TiO₂ sphere. In addition, XRD pattern indicated that TiO₂ sphere was in amorphous form which was shown to have lower photocatalytic activity than that of crystalline TiO₂ (Singh and Ghuman, 2012). Moreover, TiO₂ spheres were fragile and tended to break easily when they were mixed with phenol solution which resulting in the difficulty to recover TiO₂ in recovering process.

Therefore, the modification of TiO_2 in order to immobilize it on the surface of the chitosan beads was attempted to improve the efficiency and reusability.



Figure 3.8 The photocatalytic degradation of phenol in the presence TiO_2 powder (•), chitosan-TiO₂ beads in the diameter range 500-700 µm (•) and TiO_2 spheres (•). Condition: the amount of TiO_2 in TiO_2 powder, chitosan-TiO₂ beads and TiO_2 spheres = 200 mg, initial phenol concentration = 10 mg/L, 500 mL and the distance between UV lamp and the surface of the solution = 15 cm. The error bars represent the standard deviation of three experiments.

3.5 The Modification of TiO₂ surface

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 TiO_2 powder was modified which involves two steps. First, TiO_2 was treated with silane coupling agent. They are able to condense with silanol groups of the hydrolyzed silane coupling agent. The reaction mechanism with 3aminopropyltriethoxysilane can be illustrated as shown in Figure 3.9. At the beginning, aminosilane undertakes hydrolysis with formation of silanol groups:

Figure 3.9 The hydrolysis of 3-aminopropyltriethoxysilane (Andrzejewska et al., 2004).

The condensation with silanol groups on the TiO_2 surface occurs as shown in Figure 3.10.



Then, a Schiff's base formation takes place between the surface of TiO_2 and glutaraldehyde to generate modified TiO_2 . Light brown precipitate indicates the formation of Schiff's base with glutaraldehyde. This Schiff's base forms a covalent

bond with NH_2 group of chitosan to produce modified TiO_2 grafted chitosan beads. The scheme of the reaction is presented in Figure 3.11.



Figure 3.11 Formation of Schiff's base and attachment of TiO_2 to chitosan beads (Simi and Abraham, 2009).

3.6 Characterization of modified TiO₂ and modified TiO₂ grafted chitosan beads

Fourier Transform Infrared – Attenuated Total Reflectance (FTIR-ATR) spectroscopy provides information on the nature of the precursor materials used and the newly synthesized modified TiO_2 grafted chitosan beads catalysts. FTIR-ATR spectra for commercial TiO_2 , modified TiO_2 , chitosan, and modified TiO_2 grafted chitosan beads are presented in Figure 3.12.

Spectrum peak of TiO₂ should locate at 400-500 cm⁻¹ which refers to the vibration of Ti–O bonds in the TiO₂ lattice (Gao et al., 2003; Nur, 2006). Nevertheless it did not appear on the spectrum of TiO₂ in Figure 4.12 due to the limitation of an instrument that can scan only between 4,000 and 500 cm⁻¹.

FTIR-ATR spectrum of modified TiO₂ confirmed desirable linkage of modified TiO₂. Absorption peak at 912 cm⁻¹ corresponded to Ti-O-Si bond (Puzenat and Pichat, 2003). The Si-O vibration showed the band at around 1000-1200 cm⁻¹ (Siqueira et al., 2007) and the region at 1640 cm⁻¹ which attributed to the formation of Schiff's base (C=N bond) (Simi and Abraham, 2009). The peak at 2931 cm⁻¹ corresponded to the stretching of C-H group. The band at 3231 cm⁻¹ was assigned to OH vibration.

Absorption band of chitosan at 1640 cm⁻¹ and 3355cm⁻¹ were assigned to its amine (-NH₂) and hydroxyl (-OH) functional groups (Brugnerotto et al., 2001). C-H stretching showed the adsorption band at 2871 cm⁻¹.

FTIR-ATR spectrum of modified TiO_2 grafted chitosan beads showed the combination of chitosan beads and modified TiO_2 . When NH_2 of chitosan beads was cross-linked with C=O of modified TiO_2 , the Schiff's base peak occurred at 1646 cm⁻¹.



Figure 3.12 FTIR-ATR spectra of TiO_2 , modified TiO_2 , chitosan and modified TiO_2 grafted chitosan.

The crystalline structure of material was characterized by X-ray diffraction. The X-ray powder diffraction patterns of TiO_2 and modified TiO_2 are shown in Figures 3.13. Both of them represented the peaks at scattering angles of 25.3, 37.8, 48.05 and 62.69° indicating that both preparation of TiO_2 were in anatase phase (Tong et al., 2008). No crystalline phase ascribed to rutile or brookite could be found. This achievement suggested that modified TiO_2 can be used as a photocatalyst in photodegradation process.



Figure 3.13 X-ray diffractograms of TiO_2 (a) and modified TiO_2 (b).

Next, the modified TiO₂, chitosan beads and modified TiO₂ grafted chitosan beads at 0.01% TiO₂ (w/v) and 1% TiO₂ (w/v) were subjected to SEM analysis (Figure 3.14a-g). The modified TiO_2 had a good dispersion in EtOH:DI water (9:1, v/v). The average diameter of modified TiO₂ particles is 150-200 nm (SemAfore program) as shown in Figure 3.14a. The modified TiO_2 was coated on to the smooth surface of chitosan beads, the thickness of TiO_2 layer depended on the concentration of modified TiO₂. Figure 3.14b, SEM micrograph of modified TiO₂ grafted chitosan beads at 0.01% TiO₂ (w/v) looked the same as that of the chitosan beads without TiO_2 which had smooth surface (Figure 3.14e). However, modified TiO_2 can be observed on the surface of these beads when zoomed in its surface (Figure 3.14c). On the contrary, the agglomeration of modified TiO₂ particles can be clearly seen on the beads at 1% TiO₂ (w/v) of modified TiO₂ and its surface (Figure 3.14f and g). When the bead was broken, the layer of modified TiO₂ that was grafted on the surface of chitosan beads is illustrated in Figure 3.14d and h. The surface of chitosan beads grafting with 1% of modified TiO₂ was found to be thicker than that of chitosan beads grafting with 0.01% TiO₂. The thicker layer was due to the aggregation of modified TiO₂. Modified TiO₂ grafted chitosan beads at 1% TiO₂ (w/v) were then chosen for further study because they can be use in many cycles on phenol photodegradation before the erosion of TiO₂ occurred.



Figure 3.14 SEM pictures of modified TiO_2 (a), modified TiO_2 grafted chitosan beads at 0.01%(w/v) of modified TiO_2 at 100X (b) and 5,000X (c), the broken beads of modified TiO_2 grafted chitosan beads at 0.01%(w/v) of modified TiO_2 (d), chitosan beads (e), modified TiO_2 grafted chitosan beads at 1%(w/v) of modified TiO_2 at 100X (f) and 5,000X (g) and the broken beads of modified TiO_2 grafted chitosan beads at 1%(w/v) of modified TiO_2 grafted chitosan beads at 1%(w/v) of modified TiO_2 at 100X (f) and 5,000X (g) and the broken beads of modified TiO_2 grafted chitosan beads at 1%(w/v) of modified TiO_2 h.

3.7 Phenol photodegradation of modified TiO₂ grafted chitosan beads

3.7.1 Optimization of modified TiO₂ synthesis

The effect of glutaraldehyde concentration and glutaraldehyde incubation time were optimized.

3.7.1.1 Effect of concentration of glutaraldehyde

Glutaraldehyde serves as a cross-linking agent and was used to link the modified TiO₂ on the surface of chitosan beads through primary amine group by Schiff base linkage to produce the layer of modified TiO₂ grafted on chitosan surface. The ground sample which already modified with 3-aminopropyl triethoxysilane was mixed with various concentration of glutaraldehyde (0, 0.1, 1, 2, 3.75, 5 and 10% (w/v)) in isopropanol and incubated at 25 °C for 8 h with agitation using magnetic stirrer. The modified TiO₂ at 1% (w/v) was dispersed in 50 mL EtOH:DI water (9:1, v/v) and coated onto 30 g of wet chitosan beads. Beads were washed five times with the mixture of DI water:ethanol (1:9 v/v) and dried at 100 °C. Three hundred milligrams of modified TiO₂ grafted chitosan beads were loaded into the beaker containing 200 mL of 10 mg/L of phenol and the air was flown through the solution. The distance between UV lamp and the beads was set at 15 cm in a dark chamber. Under UV irradiation, the removal of phenol at several % glutaraldhyde is shown in Figure 3.15.



Figure 3.15 Effect of % glutaraldehyde on the removal of phenol at 8 h. Condition: modified TiO₂ grafted chitosan beads = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL and the distance between UV lamp and the surface of the solution = 15 cm. The error bars represent the standard deviation of three experiments.

The removal of phenol was found to increase with increasing amount of glutaraldegyde and reached plateau when glutaraldehyde concentration was higher than 3.75%. This was because of the in excess of glutaraldehyde. Therefore, the concentration of glutaraldehyde at 3.75% was selected for further study.
3.7.1.2 Effect of glutaraldehyde incubation time

Glutaraldehyde at 3.75% (w/v) in isopropanol was added into the ground sample which was modified with 3-aminopropyl triethoxysilane. The incubation time between glutaraldehyde and 3-aminopropyl triethoxysilane at 1, 2, 4, 6, 8, 10 h were studied. Modified TiO₂ at 1% (w/v) was grafted on chitosan beads. Three hundred milligrams of modified TiO₂ grafted chitosan beads were mixed with 200 mL of 10 mg/L of phenol. The beads and the solution were then irradiated under UV lamp for 8 h. The distance between UV lamp and the beads was set at 15 cm in a dark chamber. The % reduction of phenol is represented in Figure 3.16.



Figure 3.16 Effect of glutaraldehyde incubation time (1 h (\bullet), 2 h (\bullet), 4 h (\bullet), 6 h (\times), 8 h (\times), 10 h (\bullet)). Condition: modified TiO₂ grafted chitosan beads = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL and the distance between UV lamp and the surface of the solution = 15 cm. The error bars represent the standard deviation of three experiments.

From the result above, the % reduction of phenol from 1 to 8 h of all incubation time of glutaraldehyde was indifferent. It can be seen that the incubation time of glutaraldehyde did not have an effect on the removal of phenol. This could be explained by the fact that the Schiff's base formation between modified TiO_2 and glutaraldehyde (figure 3.17) was already complete at 1 h. So the incubation time at 1 h was chosen for the next experiment.

Glutaraldehyde

Schiff's base

+

Figure 3.17 The formation of Schiff's base between modified TiO_2 and glutaraldehyde.

3.7.2 Effect of parameters on phenol photodegradation

From previous investigation, glutaraldeyde at 3.75% (w/v) was allowed to incubate with modified sample for 1 h. After the modified TiO₂ grafted chitosan beads were prepared, the optimum condition for phenol degradation was studied. Three hundred milligrams of modified TiO₂ grafted chitosan beads were mixed with 200 mL of 10 mg/L phenol solution and the air was flown through the solution. The reaction was set under UV light in the dark chamber.

3.7.2.1 Effect of distance between UV lamp and surface of the solution

The distance between UV lamp and surface of the solution was related to the light intensity (Caimei et al., 2003). This parameter was investigated by changing the vertical distance between the light source and the surface of the phenol solution at 10, 15 and 20 cm. In this experiment, 0.01% (w/v) modified TiO_2 grafted chitosan was used as a photocatalyst.



Figure 3.18 Effect of distance between UV lamp and surface of the solution on photocatalysis at 10 cm (\bullet), 15 cm (\bullet) and 20 cm (\bullet). Condition: modified TiO₂ grafted chitosan beads at 0.01% (w/v) of modified TiO₂ = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL. The error bars represent the standard deviation of three experiments.

When the distance between the light source and the sample solution increased, the degree of photocatalysis decreased (Figure 3.18) owing to the less intense light used to catalyze phenol by TiO_2 . The stronger light intensity led to more photon received by TiO_2 photocatalyst and thus, more OH⁻ radicals were generated to degrade organic pollutant (Caimei et al., 2003). Moreover, the closer distance between the light source and the material could help more phenol molecules react with UV light in photolysis process. Hence, the distance between UV lamp and surface of the solution at 10 cm was selected for the next experiment.

3.7.2.2 Effect of agitation between catalyst and phenol solution

One of the problems in the use of immobilized catalyst for photocatalysis degradation is the limitation in mass transport because the catalyst is immobilized on a solid support (Minsker et al., 2001). From previous experiment, the beads and phenol solution were not thoughly mixed. Only the air flown though the solution that helped the mixing between catalyst and phenol solution. This problem can be overcome by increasing the rate of agitation between the photocatalyst and phenol solution. When the solution was stirred, the beads (0.01% (w/v) of modified TiO₂ grafted chitosan beads) were physically moved all around the solution to enhance its kinetic energy. The beads could then react quickly with photon from UV light and phenol molecule in the solution (Ling et al., 2004). Consequently, the phenol photocatalyst was used as a control which also exhibited the removal of phenol because phenol could be degraded by photolysis process (Nawi et al., 2011; Wu et al., 2001). However, the reaction mixture containing photocatalyst showed higher

% reduction of phenol. Therefore, phenol solution containing modified TiO₂ grafted chitosan beads for all experiments was allowed to stir during photodegradation process.



Figure 3.19 Effect of the agitation between phenol solution and TiO_2 grafted chitosan beads on phenol photocatalysis process (0.3 g beads, stirring (\times), 0.3 g beads, no stirring (\bullet), 0 g beads, stirring (\bullet), 0 g beads, no stirring (\bullet)). Condition: modified TiO₂ grafted chitosan beads at 0.01% (w/v) of modified TiO₂ = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL and the distance between UV lamp and the surface of the solution = 10 cm. The error bars represent the standard deviation of three experiments.

3.7.2.3 Effect of modified TiO₂ concentration

The modified TiO₂ at 0.01, 0.1, 1, 5 and 10% (w/v) were grafted onto chitosan beads. The removal of phenol is presented in Figure 3.20. The result can be divided into two groups. The first group was the chitosan beads which were coated with modified TiO₂ at 1, 5 and 10% (w/v). These beads showed the reduction of phenol of more than 80% while other modified TiO₂ concentrations (0.01 and 0.1 % TiO₂ (w/v) grafted chitosan beads) represented approximately 75% approximately after 8 h photodegradation. The % reduction after 8 h did not differ much between these two groups. However, during the photocatalysis reaction, the phenol degradation in the first group exhibited approximately 15-30% better phenol removal than the second group. For some reasons, it was found that the outer surface of the grafted beads at 1, 5 and 10% (w/v) of modified TiO₂ were eroded by the stirring process which caused the dispersion of modified TiO₂ powder into the reaction solution. The rate of phenol degradation thus, increased because the UV light could penetrate into the suspension which increased the number of hydroxyl, and superoxide radicals (Laoufi et al., 2008). However, the second group did not erode upon stirring and thus, did not disperse in the solution. The modified TiO₂ grafted chitosan beads of 1% (w/v) of modified TiO₂ were selected for further study because at higher TiO₂ concentration, phenol photodegradation did not increase due to the shielding effect of TiO₂ powder, resulting in erosion and dispersion of TiO_2 in the solution.



Figure 3.20 Effect of TiO₂ concentration at 0.01% (w/v) (\bullet), 0.1% (w/v) (\bullet), 1% (w/v) (\bullet), 5% (w/v) (\times) and 10% (w/v) (\star).Condition: modified TiO₂ grafted chitosan beads = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL and the distance between UV lamp, the surface of the solution = 10 cm and stirred reaction mixture. The error bars represent the standard deviation of three experiments.

3.7.2.4 Effect of reaction temperature

To investigate the difference of the reduction of phenol clearly, the photodegadation time at 5 h was used because the degradation reached plateau after 8 h.

Effect of temperature on the degradation of phenol is exhibited in Figure 3.21. As the solution temperature increased, the percent reduction of phenol increased. The degradation rate also enhanced when the temperature was risen up (Figure 3.22). This increase could be explained by the enhancement of the reaction rate took place between the phenol molecules and the hydroxyl radicals. Furthermore, the enlargement of the degradation was presumably due to the increasing collision frequency of phenol molecules (Kim and Lee, 2010). Although the temperature at 60 °C showed the highest phenol degradation, the temperature at 30 to 40 °C was acceptable for the degradation of phenol because it was similar to the environmental temperature. However, temperature at 30 °C was chosen for next study because it used lower electric energy for temperature adjustment.



Figure 3.21 Effect of reaction temperature on phenol photocatalytic degradation (20 °C (•), 30 °C (•), 40 °C (•), 50 °C (×), 60 °C (*)). Condition: modified TiO₂ grafted chitosan beads at 1% (w/v) of modified TiO₂ = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL, the surface of the solution = 10 cm and stirred reaction mixture. The error bars represent the standard deviation of three experiments.



Figure 3.22 The relationship of rate constant vs. reaction temperature at 2 h of degradation time.

3.7.2.5 Effect of light intensity

Intensity of UV radiation has been reported to be an important parameter to control the photoactivity (Lee et al., 2004). In section 3.7.2.1, the distance between UV lamp and surface of the solution which involved light intensity was studied and the distance at 10 cm was chosen for the degradation of phenol. In order to gain higher removal of phenol, light intensity was varied with the fixed distance between UV lamp and surface of the solution at 10 cm. This experiment was conducted under different light intensities of 0, 10, 20, 30 and 40 W by changing the number of lamps which located over the reaction. The results showed that the removal of phenol increased with increasing light intensity as represented in Figure 3.23. The reason was that higher light intensity can produce more photon received by catalyst, resulting in higher generation of e^- and h^+ and then more OH⁻ radical was created which led to high efficiency of phenol photocatalytic degradation (Lee et al., 2004; Subramanian and Kannan, 2008). In an unirradiated reaction which was used as a control, approximately 15% of phenol was removed due to the adsorption of phenol onto TiO₂ particles and chitosan beads (Laoufi et al., 2008).



Figure 3.23 Effect of UV light intensity on phenol photogedradation (0 W (\bullet), 10 W (\bullet), 20 W (\bullet), 30 W (\times), 40 W (\star)). Condition: modified TiO₂ grafted chitosan beads at 1% (w/v) of modified TiO₂ = 0.3 g, initial phenol concentration = 10 mg/L, 200 mL, the surface of the solution = 10 cm, stirred reaction mixture and reaction temperature = 30 °C. The error bars represent the standard deviation of three experiments.

The semilogarithmic plots of concentration was plotted to examine the kinetic order reaction. The data gave a straight line. This finding indicated that the photocatalytic degradation of phenol using modified TiO₂ grafted chitosan beads can be described by the pseudo first-order kinetic model (Mahvi et al., 2007; San et al., 2000) (Figure 3.24) where $\ln C_t = -kt \text{ C} + \ln C_0$ (C_0 is the initial concentration and C_t is the concentration of phenol at time *t*). The first-order rate constants were estimated (see Appendix B) in Table 3.1.



Figure 3.24 Plot of $\ln C_t/C_0$ vs. time for photodegradation of phenol (0 W (\checkmark), 10 W (\blacksquare), 20 W (\blacktriangle), 30 W (\times), 40 W (\divideontimes)).

UV light intensity (W)	Rate constant $(x10^{-3} \text{ min}^{-1})$	r	
0	0.6	0.998	
10	2.8	0.997	
20	6.5	0.998	
30	8.6	0.997	
40	9.5	0.996	

Table 3.1 First order rate constants for phenol photodegradation at various intensity

 of UV light

The degradation rate of phenol at 20, 30 and 40 W of light intensity increased 2.3, 3.1 and 3.4 times, respectively when compared with 10 W of light intensity. The rate of phenol degradation when the 40 W-light source was used should have been 4 times higher when compared of that 10 W because the intensity of light was increased 4 times (Lee et al., 2004). This might be due to the fact that the generated light source exceeded the area of beaker containing the reaction solution as shown in Figure 3.25. Thus, some irradiation of UV light did not reach the phenol solution. The light intensity at 20 W was selected for the study on the effect of initial phenol concentration.



Figure 3.25 The UV lamp covered the beaker of phenol solution.

3.7.2.6 Effect of initial phenol concentration

In 2010, Thailand imported phenol for all industrial was of 189,735.58 tons (Pollution Control Department, 2010). The water standard level of phenol in industrial wastewater must not exceed 1.0 mg/L (Pollution Control Department, 2012: online). As the concentration of pollutant is an important factor in wastewater treatment, the initial concentration of phenol was investigated over the range of 10 to 100 mg/L. In order to see the difference of the removal of phenol among various phenol concentration tested, an irradiation time of 2 h was chosen and the result is shown in Figure 3.26. The rate constant k together with the correlation coefficients r is collected in Table 3.2. The result showed that the rate of photodegradation decreased as the initial phenol concentration increased. This could be explained by the fact that when the initial phenol concentration was extended, the generation of hydroxyl radicals on catalyst surface was reduced due to the adsorption of more phenol molecules and its intermediates on TiO₂ surface (Daneshvar et al., 2005). This caused the lack of active site available for hydroxyl radicals adsorption on the surface of catalyst. Thus, large amount of adsorbed phenol acted as an inhibitor that influenced the reaction between phenol molecules and hydroxyl radicals because they could not contact each other directly (Wong et al., 2011). In addition, the absorption of light by the substrate at high concentrations might intercept the photons before they could reach the photocatalyst surface and hence, the amount of hydroxyl free radical production was reduced (Lam et al., 2010). Besides, the amount of photocatalyst was too low to degrade phenol at high concentration completely.



Figure 3.26 Percent reduction of phenol at 2 h in various initial phenol concentrations. Condition: modified TiO_2 grafted chitosan beads at 1% (w/v) of modified $TiO_2 = 0.3$ g, initial phenol concentration = 10 mg/L, 200 mL, the surface of the solution = 10 cm, stirred reaction mixture, reaction temperature = 30 °C and light intensity = 20 W.

Initial phenol concentration (mg/L)	$k (x 10^{-3} \min^{-1})$	r
10	6.5	0.998
25	4.3	0.997
50	2.6	0.998
100	1.7	0.997

Table 3.2 First order rate constants for phenol photocatalytic degradation at different

 initial phenol concentrations

3.8 Reusability

The modified TiO₂ grafted chitosan beads at 1% (w/v) of modified TiO₂ were washed 3 times with DI water by mechanical shaker for 10 min each time and once with EtOH for 10 min. The washed beads were then dried in oven at 100 °C before being reused in the next cycle under the same condition: 200 mL of 10 mg/L of phenol solution, 10 cm of the distance between light source and the surface of solution, 300 rpm of agitation rate, 10 W of light intensity and irradiation time of 8 h.



Figure 3.27 The recycling of modified TiO₂ grafted chitosan beads at 1% (w/v) of modified TiO₂: cycle 1(•), cycle 2 (•), cycle 3(•), cycle 4 (×) and cycle 5 (*).

It can be seen in Figure 3.27 that the efficiency of modified TiO_2 grafted chitosan beads to degrade phenol was about 10% decrease when they were reused after 5 times. In each recycling process, the erosion of modified TiO_2 was not observed. The modified TiO_2 grafted chitosan photocatalyst can be used in many cycles due to the properties of TiO_2 that are chemical stability, low solubility and powerful oxidation strength (Hu and Yuan, 2005). It demonstrated that modified TiO_2 grafted chitosan beads is a good material for the removal of phenol.

CHAPTER IV

CONCLUSION

4.1 Conclusion

Chitosan-TiO₂ beads, TiO₂ beads and modified TiO₂ grafted chitosan beads were prepared for the photocatalytic degradation of phenol. SEM picture of chitosan-TiO₂ beads presented a spherical shape in the size range of 500-700 μ m. The surface of beads was rather smooth. TiO₂ particles were found to be immobilized in the internal of chitosan beads where Ti element on the surface of chotisan-TiO₂ beads could not be detected by EDX analysis. Chitosan-TiO₂ beads at 1% wt of chitosan showed the best material for phenol removal when compared with other TiO₂ concentrations (0.1, 3, 5, 10% wt of chitosan). It was then used to compare with chitosan-TiO₂ beads in the diameter range 20-100 μ m under the same concentration. The result indicated that chitosan-TiO₂ beads in the diameter range of 20-100 μ m had less efficiency to remove phenol than chitosan-TiO₂ beads in the size range of 500-700 μ m.

To eliminate the negative effect of chitosan from the shielding effect on TiO_2 to react with UV light, TiO_2 spheres were synthesized. Chitosan was acted as a binder to generate spheres before it was removed by calcination at 600 °C. TiO_2 spheres had the same diameter as found in that of chitosan- TiO_2 beads but its surface consisted of TiO_2 particle from 30-300 nm in diameter. XRD pattern of ground TiO_2 spheres exhibited an active anatase form which was effective in photocatalytic degradation process. The photodegadation of 10 mg/L of phenol 500 mL using commercial TiO₂ powder, chitosan-TiO₂ beads at 1% wt of chitosan and TiO₂ spheres which contain 100 mg of TiO₂ was investigated. TiO₂ spheres showed the least phenol degradation (31%) while commercial TiO₂ powder and chitosan-TiO₂ beads at 1% wt of chitosan represented 75 and 43%, respectively. Moreover, it was fragile and broke easily which might not be proper for recovering process.

Modified TiO₂ grafted chitosan beads were thus, prepared to enhance the phenol degradation efficiency and material reusability. 3-Aminopropyl trietoxysilane and glutaraldehyde were main reagents to modify TiO₂. The optimum condition for the modification of TiO₂ chain was to use 37% (w/v) of glutaraldehyde and the incubation time was 1 h. Various parameters that had an effect on the phenol reduction using modified TiO₂ grafted chitosan beads as a photocatalyst were investigated. The modified TiO₂ at 1% (w/v) showed the best concentration to graft on chitosan beads. The increase of distance between UV lamp and the surface of phenol solution, temperature and light intensity related with the decrease of phenol photodegradation. In addition, the degradation of phenol increased when the initial phenol concentration was decreased. The stirring of solution during the photodegradation process showed that phenol degradation can be improved by approximately 20%. Moreover, the efficiency of modified TiO₂ grafted chitosan beads for phenol degradation still retained at 90% after being reused for 5 cycles.

4.2 Suggestion

Modified TiO₂ grafted chitosan beads can be used as an alternative material for wastewater treatment. In addition, they can be applied to be used in fluidized bed reactor for the removal the pollutants in aqueous or gas phase. The photodegradation of phenol from authentic industrial wastewater using modified TiO₂ grafted chitosan beads should be further determined in order to study the efficiency of the material in wastewater treatment. Furthermore, modified TiO₂ grafted chitosan film can be explored in order to improve its utilization. Other parameters such as pH of reaction, the agitation rate, the position of UV lamp (vertical or horizontal), %DD of chitosan and kinetic study should be further investigated.

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APPENDICES

Appendix A

Calculation of %reduction of phenol

A1 Calibration curve of phenol

The concentration versus absorbance of phenol solution at 510 nm was presented in Table A1. They show a linear relationship with the correlation coefficient = 0.9996 (Figure A1).

Concentration (mg/L)	Absorbance (510 nm)		
0	0		
2.5	0.11		
5	0.24		
7.5	0.35		
10	0.48		
20	0.96		
25	1.22		

Table A1 Absorbance of phenol solution determined by UV-Vis spectrophotometer



Figure A1 Standard calibration curve of phenol.

A2 Example of the calculation of phenol reduction

<u>Effect of TiO_2 dosage of chitosan- TiO_2 beads on phenol photodegradation</u>

Experimental condition	
Amount of 10 mg/L of phenol	500 mL
Amount of chitosan-TiO ₂ at 1 % wt of chitosan	0.5 g
Distance between light source and surface of solution	15 cm

The calibration curve of phenol at the concentration of 10 to 25 mg/L showed the straight line with the equation:

$$Y = 0.0483X$$

Where y = Absorbance of phenol

X = Concentration of phenol

Table A2 Effect of chitosan-TiO₂ beads at TiO₂ 1 % wt of chitosan on phenol photodegradation

Time (h)	A510	Concentration (mg/L)	%Reduction
0	0.4826	9.99	0
1	0.4386	9.08	9.11
2	0.4218	8.73	12.61
3	0.3907	8.09	19.02
4	0.3692	7.64	23.52
5	0.3559	7.37	26.23
6	0.3357	6.95	30.43
7	0.3220	6.67	33.23
8	0.3107	6.43	35.64

1.1 Initial concentration of phenol

From equation Y = 0.0483X

Initial phenol concentration = Absorbance
$$/ 0.0483$$

= 9.99 mg/L

1.2 Concentration of phenol after 8 h

From equation Y = 0.0483X

Concentration of phenol
$$= 0.3107/0.0483$$

$$= 6.43 \text{ mg/L}$$

1.3 %Reduction of phenol

% Reduction = $[(C_0-C_t)/C_0]*100$

Where C_0 = Initial phenol concentration

 C_t = Concentration of phenol in solution at a given time.

%Reduction of phenol at 8 h = [(9.99-6.43)/9.99)*100= 35.64

Appendix B

Calculation of rate constant

B1 Example of the calculation of rate constant

First-order kinetic model; $\ln C_t = -kt \operatorname{C+ln} C_0$

where C_0 = The initial concentration and (mg/L)

 C_t = The concentration of phenol at time t (mg/L)

 $k = \text{Rate constant (min}^{-1})$

Plot $-\ln(C_t/C_0)$ versus reaction time (*t*) yields a straight line, the slope is rate constant (k) as showed in Figure B. The rate constant was equal to 9.5×10^{-3} min⁻¹.

UV light intensity	Time (h)	Concentration	C_t/C_0	$-\ln(C_t/C_\theta)$
(W)		(mg/L)		
40	0	0.02	1	0
40	0	9.93	1	0
	0.5	7.84	0.79	0.24
	1	6.37	0.64	0.45
	1.5	5.13	0.52	0.65
	2	3.70	0.37	0.99
	3	2.12	0.21	1.56
	4	1.09	0.11	2.21
	5	0.57	0.057	2.86

 Table B1 Effect of light intensity



Figure B1 Plot of $\ln C_t/C_0$ vs. time for photodegradation of phenol at 40 W.

VITAE

Miss Punnida Nonsuwan was born on September 27th, 1987 in Kalasin, Thailand. She received a Bachelor Degree of Science, major in Chemistry from Silpakorn University in 2009. Since 2010 she has been a graduate student in the program of Biotechnology, Faculty of Science, Chulalongkorn University.