

REFERENCES

1. Williamson, S.J. Fundamentals of Air Pollution.
Massachusetts: Addison-Wesley Reading ,1973.
2. Pitt, J.N., Jr. J. Air Poll. Contr. Ass. 19(1969): 658.
3. Kummer, J.T. J. Phys. Chem. 90(1986): 4747.
4. . Prog. Energy Combust. Sci. 6(1980): 177.
5. Haung, T.-J., Yu, T.-C., and Chang, S.-H. Appl. Catal. 52(1989): 157.
6. Pajonk, G.M., Teichner, S.J., and Conner, W.C. Adv. in Catal. 34(1986): 19.
7. Sermon, P.A., and Bond, G.C. Catal. Rev. 8(1973): 211.
8. Dowden, D.A. Catalysis VIII, p. 211. London: Chemical Society, 1980.
9. Hofman, K.A. Ber. 51. (1918): 1526.
10. Bessalow, P., And Kobozew, N.J. J. Phys. Chem. 9(1937): 815.
11. Pieters, H.A.J. Chem. Weekblad. 28(1931): 250.
12. Garner, W.E., Gray, T.J., and Stone, F.S. Discussions Faraday Soc. 8(1950): 246.
13. , , . Proc. Roy. Soc. A197
(1949): 294-314.
14. Winter, E.R.S. J. Chem. Soc. (1955): 2766.
15. Kobayashi, H., Takezawa, N., Shimokawabe, M. and Tkahashi, K.
In Poncelet, G., Grange, P., and Jacobs, P.A., eds.
Preparation of Catalysis III, p. 697. Amsterdam:
Elsevier, 1983.
16. Evans, J.W., Wainwright, M.S., Bridgewater, A.J., and Young, D.J.
Appl. Catal. 7(1982): 475.

17. Miro, E.E., Ardiles, D.R., Lombardo, E.A., and Pentunchi, J.O. J. Catal. 97(1986): 43.
18. Strohmier, B.R., Leyden, D.E., Field, R.S., and Hercules, D.M. J. Catal. 94(1985): 514.
19. Huang, T.-J., Jang, W.G., and Chang, S.H. J. Chin. Inst. Chem. 18(1987): 77.
20. Pepe, F., Angeletti, C., De Rossi, S., and Jacono, M. Lo. J. Catal. 91(1985): 69.
21. Robinson, W.R.A.M., and Mol., J.C. Appl. Catal. 44(1988): 165.
22. El-Shobaky, G.A., El-Nabarawy, T., and Fagal, G.A. Appl. Catal. 44(1988): 165.
23. Barbier, J., Dumas, J.M., Gerno, C., and Hadrane, H. Appl. Catal. 67(1990): L1.
24. Huang, T.-J., and Yu, T.-C. Appl. Catal. 71(1991): 275.
25. Fabio, B. Noronha, and Schmal Martin. Appl. Catal. 78(1991): 125.
26. Satterfield, C.N. Heterogeneous Catalysis in Practice. New York: McGraw-Hill, 1980.
27. Attkins, P.W., Holker, J.S.E., and Holliday, A.K. eds. Heterogeneous Catalysis. 2nd ed. Oxford: Clarendon Press, 1987.
28. Kirk-Othmer. Encyclopedia of Chemical Technology. 4(1978): 772-793.
29. Milton Orchin. Catalysis. 5(1957): 1-2.
30. Stone, F.S. In D.D. Eley, P.W. Selwood, and Paul B. Weisz (eds.), Adv. in Catalysis. vol. 13, pp. 1-50. New York: Academic Press, 1962.
31. Garner, W.E., and Veal, F.J. J. Chem. Soc. (1935): 1487.
32. Ward, T. J. Chem. Soc. (1947): 1247.
33. Stone, F.S., and Tiley, P.F. Proc. Roy. Soc. A211(1952): 472.

34. Dell, R.M., and Stone, F.S. Trans. Faraday Soc. 50(1954): 501.
35. Garner, W.E. ed. Chemisorption. London: Butterworths, 1957.
36. Winter, E.R.S. In D.D. Eley, W.G. Frankenburg, and V.I. Komarewsky (eds.), Adv. in Catalysis, vol. 10, pp. 196-239. New York: Academic Press, 1958.
37. Teichner, S.J., and Morrison J.A. Trans. Faraday Soc. 51(1955) : 961.
38. Marcellini, R.P., Rane, and Teichmer, S.J. Proc. 2nd Int. Congr. Catalysis, Paris, 1961.
39. Eischen, R.P., and Pliskin, W.A. Adv. in Catalysis, vol. 9, p.662. New York: Academic Press, 1957.
40. Blyholder, G. Proc. 3rd Int. Congr. Catalysis, Amsterdam: North Holland Publishing Co., 1964.
41. Teichner, S.J., Marcellini, R.P., and Rue, P. Adv. in Catalysis. vol. 9, p. 458. New York: Academic Press, 1957.
42. Cove, J., Gravelle, P.C., Rane, R.E., Rue, P., and Reichner, S.J. Proc. 3rd Int. Congr. Catalysis, Amsterdam: North Holland Publishing Co., 1964.
43. Dry, M.E., and Stone, F.S. Discussions Faraday Soc. No. 28 (1959): 192.
44. Keier, N.P., Roginskii, S.Z., and Sazenova, I.S. Izv. Akad. Navk. SSSR Otd. fiz. Nauk 21(1957): 182.
45. Hegedus, L.L., ed. Catalyst Design Progress and Perspectives. New York: John Wiley & Sons, 1987.
46. Stiles, A.B. Catalyst Supports and Supported Catalysts. London: Butterworth Publishers, 1987.
47. Kung, H.H. Studies in Surface Science and Catalysis, vol. 45, Chap. 6. Amsterdam: Elsevier, 1989.

48. Page, J.-F.L., et al. Appl. Heterogeneous Catalysis.
Translated by Miller, B. Ethel, and Miller, L. Ryle.
France: Imprimerie Nouvelle, 1987.
49. Chen, B.-H., and White, J.M. J. Phys. Chem. 86(1982): 3534.
50. Campuzano, J.C. The Chemical Physics of Solid Surfaces and Heterogeneous Catalysis, 415. Amsterdam: Elsevier, 1990.
51. Petchsriudom, M. Effect of preparation on Copper Catalysts for Carbon Monoxide Oxidation. Master's Thesis,
Chulalongkorn University, 1991.
52. Foger, K. In J.R. Anderson, and R.L. Garten(eds.), Catalysis Science and Technology, p. 291. Berlin: 1984.
53. Tauster, S.J., Fung, S.C., and Garten, R.L. J. Amer. Chem. Soc. 100(1978): 170.
54. Thomas, J.M., and Thomas, W.J. Intro. to the Principles of Heterogeneous Catalysis. London: Academic Press, 1967.
55. Bournonville, J.P., and Martino, G. Studies in Surface Science and Catalysis, vol. 6, p. 159. Amsterdam: Elsevier, 1980.
56. Gentry, S.J., Hurst, N.W., and Jones, A. J. Chem. Soc. Faraday Trans. 1 77(1981): 603.
57. Poltarak, O.M., and Boronin, V.J. Russ. J. Phys. Chem. 40 (1966): 1436.
58. Barbier, J., Morales, A., and Maurel, R. Bulletin of the Chemical society of France. 1(1977): 31.
59. Tomanek, D., Mukherjee, S., Kumar, V., and Bennemann, J.H. Surface Sci. 11(1982): 114.
60. Lokhov, Y.A., Mussil, Z., and Davydov, A.A. Kinet. Katal. 20 (1979): 207.
61. Rotgerink, H.G.J.L., Mercera, P.D.L., Ommen, L.G.V., and Ross, J.R.H. Appl. Catal. 45(1988): 239-256.

APPENDIX A

SAMPLE OF CALCULATIONS

1. Preparation of 8% Cu/Al₂O₃ Catalyst with Incipient Impregnation

Method

Reagent : Copper(II)Nitrate (Cu(NO₃)₂.3H₂O) Analar grade ;

Purity 99.5 % ; Molecular weight = 241.6,

manufactured by Merck Co., Ltd.

(Atomic weight of copper = 63.54)

Support : Alumina (Al₂O₃) ; type KNH-3 ; pore volume = 1.0 cc./gm.

from Sumitomo Aluminium Smelting Co., Ltd.

Calculation for prepared 8% Cu/Al₂O₃ catalyst

basis on : 8% Cu/Al₂O₃ catalyst = 10 gm.

Al₂O₃ = 10 * (92/100) gm.

= 9.2 gm.

Cu = 10 * (8/100) gm.

= 0.8 gm.

Pore volume of Al₂O₃ (KNH-3) = 1.0 cc./gm.

Pore volume of Al₂O₃ (KNH-3) 9.2 gm.

= 9.2 * 1.0

= 9.2 cc.

Copper(Cu) prepared from Cu(NO₃)₂.3H₂O

$$\begin{aligned}
 \text{Copper(Cu) } 0.8 \text{ gm. prepared from } \text{Cu(NO}_3)_2 \cdot 3\text{H}_2\text{O} \\
 = 0.8 * (241.6/63.54) \\
 * (100/99.5) \\
 = 3.057 \text{ gm.}
 \end{aligned}$$

Use $\text{Cu(NO}_3)_2 \cdot 3\text{H}_2\text{O}$ weight 3.057 gm. made to cupric nitrate solution volume of 9.2 cc. for impregnating on 9.2 gm of Al_2O_3 support.

2. Preparation of 0.3% Pt-8% Cu/ Al_2O_3 Catalyst with Incipient Impregnation Method

Reagent : Copper(II)Nitrate ($\text{Cu(NO}_3)_2 \cdot 3\text{H}_2\text{O}$) Analar grade ;

Purity 99.5 % ; Molecular weight = 241.6,

manufactured by Merck Co., Ltd.

(Atomic weight of copper = 63.54)

Chloroplatinic acid ($\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$) ; Molecular weight

= 517.92, manufactured by WAKO PURE CHEMICAL INDUSTRIES CO., LTD.

(Atomic weight of Platinum = 195.1)

Support : Alumina (Al_2O_3) ; type KNH-3 ; pore volume = 1.0 cc./gm.

from Sumitomo Aluminium Smelting Co., Ltd.

Calculation for prepared 0.3% Pt-8% Cu/ Al_2O_3 catalyst

basis on : 0.3% Pt-8% Cu/ Al_2O_3 catalyst = 10 gm.

Al_2O_3 = 10 * (91.7/100) gm.

= 9.17 gm.

Cu = 10 * (8/100) gm.

= 0.8 gm.

Pt	= 10 * (0.3/100)	gm.
	= 0.03	gm.
Pore volume of Al_2O_3 (KNH-3)	= 1.0	cc./gm.
Pore volume of Al_2O_3 (KNH-3) 9.17 gm.	= 9.17 * 1.0	
	= 9.17	cc.
Copper(Cu) prepared from $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$		
Copper(Cu) 0.8 gm. prepared from $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$	= 0.8 * (241.6/63.54)	
	* (100/99.5)	
	= 3.057	gm.

In this study, 25 ml. of stock solution of chloroplatinic acid was prepared by dissolving 1 gm. of chloroplatinic acid in distilled and de-ionized water.

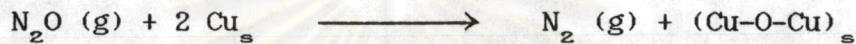
Platinum (Pt) prepared from the stock solution of chloroplatinic acid.

Platinum 0.03 gm. prepared from the stock solution of chloroplatinic acid. = 0.03 * (25/0.3767)
= 1.99 cc.

Each of the reagents used, $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$ 3.057 gm. and chloroplatinic acid from the stock solution 1.99 cc., is made to the impregnating solution volume of 9.17 cc. for impregnating on 9.17 gm. of Al_2O_3 support by using the consecutive impregnation method.

3. The Determination of Copper Active Sites By Reaction with Nitrous Oxide [16]

Copper active sites of catalyst was measured by reaction with nitrous oxide. The methods were based upon the decomposition of a nitrous oxide molecule on a copper active site which was accompanied by the liberation of one nitrogen molecule according to



where the subscript 's' signified surface atom.

Calculation of Copper Active Site on Copper Catalysts

Example weight of 8% Cu/Al₂O₃ catalyst = 0.252 gm.

- N₂O peak area of nitrous oxide reaction
= 2688 unit

- N₂O peak area after nitrous oxide reaction
= 2864 unit

Used N₂O in nitrous oxide reaction = 176 unit

Standard N₂O peak area of 1 cc. = 2864 unit

Volume of N₂O in reaction = (176/2864) * 1 cc.
= 6.145 * 10⁻² cc.

Mole of N₂O in reaction = 6.145 * 10⁻² / 24860
= 2.473 * 10⁻⁶ mole

(Volume of gas 1 mole at 30 °C = 24860 cc.)

Copper active sites on catalysts = (mNN_s) / w

m = moles of nitrous oxide in reaction (mole)

$N = \text{Avogadro's number} = 6.02 * 10^{23}$

$N_s = \text{Surface stoichiometry of } Cu_s/O_{ads} = 2$

$w = \text{Weight of copper catalysts}$

Copper Active Sites of 8% Cu/Al₂O₃ catalysts

$$= (2 * 2.472 * 10^{-6} * 6.02$$

$$* 10^{23}) / 0.252$$

$$= 7.5 * 10^{17} \text{ sites/gm.}$$

4. BET Surface Area Calculation [26]

From BET equation :

$$\frac{x}{v(1-x)} = \frac{1}{v_m C} + \frac{C-1}{v_m} * \frac{x}{C} \quad (4.1)$$

where : $x = \text{ratio of partial pressure } P/P_\infty$

$P_\infty = \text{saturated vapour pressure of } N_2$

(or adsorbed gas)

$P = \text{equilibrium vapour pressure of } N_2$

$v = \text{amount of adsorption at the equilibrium, c.c.}$

at the NTP/gm of sample

$v_m = \text{amount of adsorption to cover the surface, c.c.}$

at the NTP/gm of sample

$C = \exp(E_1 - E_2 / RT) \quad (4.2)$

where : $E_1 = \text{heat of adsorption of the first layer}$

$E_2 = \text{heat of condensation of adsorbed gas}$

assume $C \rightarrow \infty$, then

$$\frac{x}{v(1-x)} = \frac{1 * x}{v_m C} \quad (4.3)$$

let : $v_m = v_m$

v_m = mean amount of adsorption to form the N_2
complete monolayer

v = amount of adsorption measuring by G.C.

$x = P/P_\circ$

$$\frac{P_b V}{273} = \frac{P_t V}{T} \quad (4.4)$$

where : V = constant volume

P_b = pressure at 0°C

P_t = pressure at $t^\circ\text{C}$

$T = 273.15 + t, \text{ K}$

$P_b = (273.15/T) * P_t = 1 \text{ atm}$

partial pressure

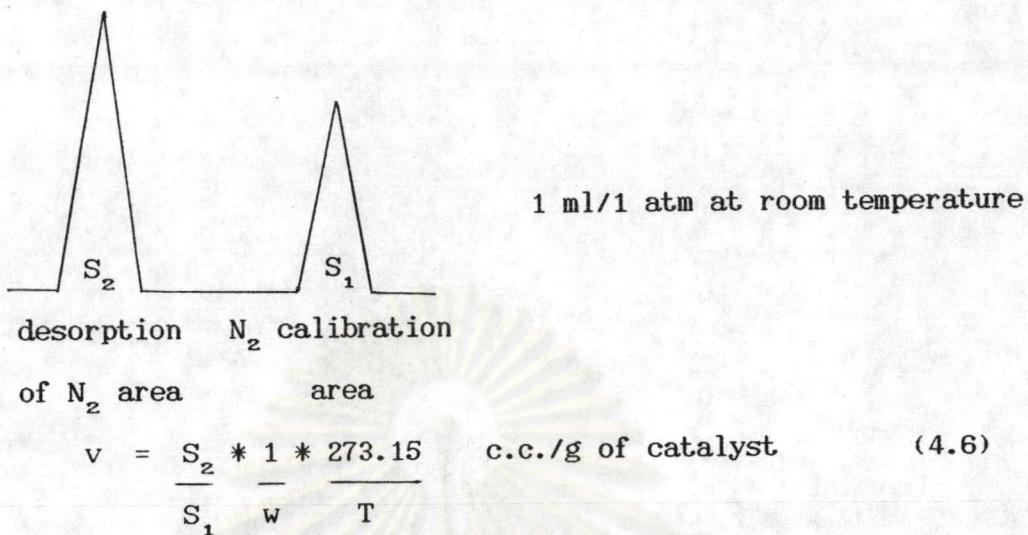
$$P = \frac{[\text{Flow of } (\text{He}+N_2) - \text{Flow of He}] * P_b}{\text{Flow of } (\text{He}+N_2)} \quad (4.5)$$

$$= 0.3 \text{ atm}$$

N_2 saturated vapour pressure, $P_\circ = 1.1 \text{ atm} = 836 \text{ mm.Hg}$

$x = P/P_\circ = P/1.1$

How to measure v



where : w = weight of sample

$$v_m = \frac{v[1 - (\text{flow of He+N}_2 - \text{flow of He})/1.1]}{\text{flow of He+N}_2} \text{ c.c.NTP/g of cat.} \quad (4.7)$$

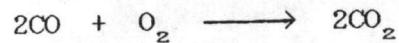
$$S_b = S * v_m \quad (4.8)$$

where : S = surface area from literature of N₂
= 4.373 m²/c.c. of N₂

so that : S_b = 4.373 v_m m²/g of catalyst

5. Material Balance for CO Oxidation Reaction

For CO oxidation reaction, the chemical equation is expressed as follows:



At the reaction temperature of 220 °C;

$$\text{The amount of CO in feed steam} = 3.955 * 10^{-7} \text{ mole}$$

$$\text{The amount of CO in effluent} = 2.361 * 10^{-7} \text{ mole}$$

Because 1 mole of CO convert to 1 mole of CO₂.

So, the amount of CO₂ should have been obtained from the reaction

$$= 1.594 * 10^{-7} \text{ mole}$$

The actual amount of CO₂ from the reaction

$$= 1.575 * 10^{-7} \text{ mole}$$

$$\% \text{ error} = 1.2 \%$$

APPENDIX B
Physical Properties of Carbon Monoxide

Property	Value
mol. wt.	28.011
m.p.	68.09 K
b.p.	81.65 K
H, fusion (68 K) ^a	0.837 kJ/mol
H, vaporization (81 K) ^a	6.042 kJ/mol
density [273 K, 101.33 kPa(1atm)]	1.2501 g/L
sp. gr., liquid, 79 K ^b	0.814
sp. gr., gas, 298 K ^c	0.968
critical temperature	132.9 K
critical pressure	3.496 MPa(34.5 atm)
critical density	0.3010 g/cm ³
G° formation (298 K) ^a	-137.16 kJ/mol
H° formation (298 K) ^a	-110.53 kJ/mol
S° formation (298 K) ^a	0.1975 kJ/(mol.K)
C _p ° (298 K) ^a	29.1 J/(mol.K)
C _v ° (298 K) ^a	20.8 J/(mol.K)
autoignition temperature	925 K
flammability limits in air ^d	
upper limit, %	74.2
lower limit, %	12.5

^a To convert J to cal, divide by 4.184

^b With respect to water at 277 K.

^c With respect to air at 298 K.

^d Saturated with water vapor at 290 K.

Ambient Air Quality Standard of Thailand (1981)

Pollutants	average value (mg/m ³)				methods of measurement
	1 h	8 h	24 h	1 yr	
Carbon Monoxide (CO)	50	20	-	-	Non-Dispersive Infrared Detection
Nitrogen Dioxide (NO ₂)	0.32	-	-	-	Gas Phase Chemiluminescence
Sulfur Dioxide (SO ₂)	-	-	0.3	0.1*	Pararosanniline
Suspended Particulate Matter (SPM)	-	-	0.33	0.1*	Gravimetric
Photochemical Oxidant (O ₃)	0.20	-	-	-	Chemiluminescence
Lead (Pb)	-	-	0.01	-	Wet Ashing

Note : * = Geometric mean

**Specification of Alumina Support (Al_2O_3) Type KNH-3
from Sumitomo Aluminium Smelting Co., Ltd.**

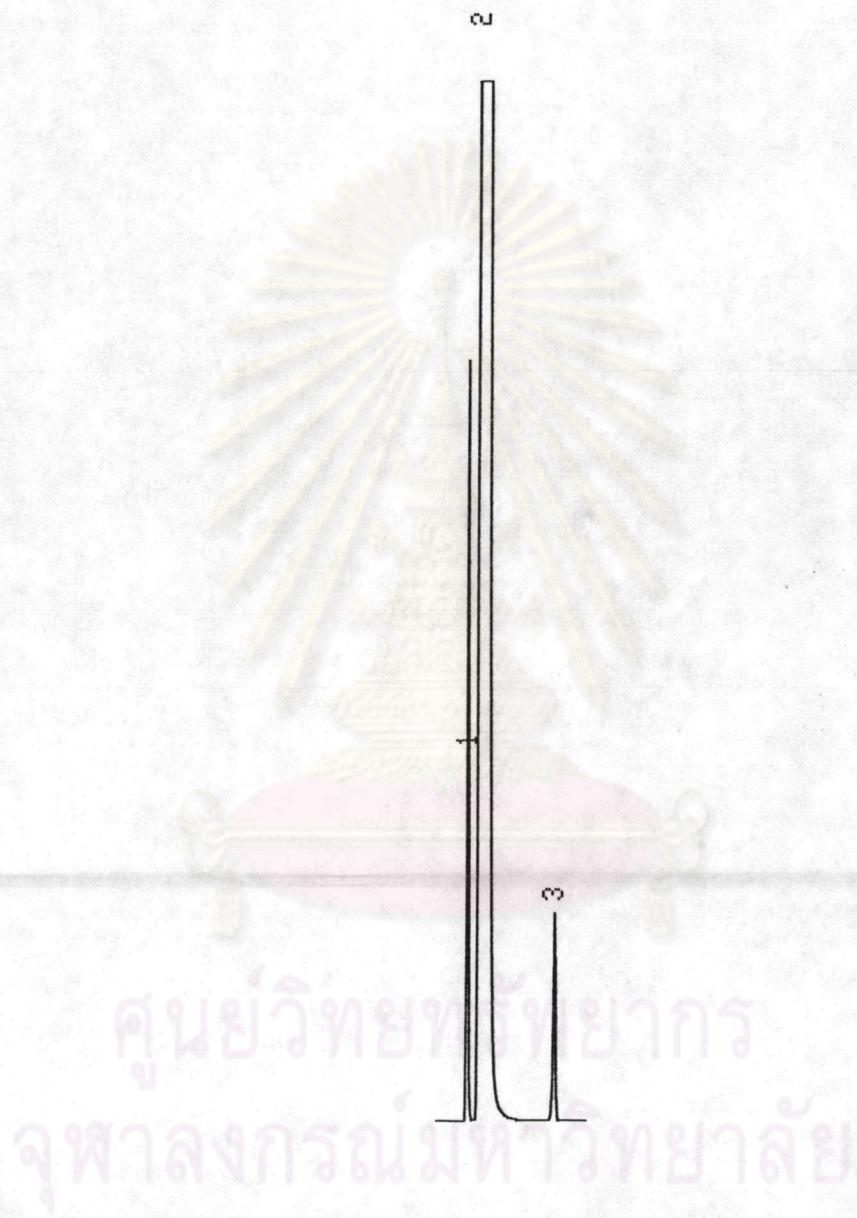
Chemical Composition (weight percent)

- Al_2O_3	60-70	%
- SiO_2	30-35	%
- Fe_2O_3	0.3-0.5	%
- TiO_2	0.5-0.7	%
- CaO	0.1-0.2	%
- MgO	0.2-0.4	%
- Na_2O	0.3-0.4	%
- K_2O	0.2-0.3	%
- $\text{ZrO}_2 + \text{HfO}_2$	0.03-0.04	%

Physical Properties

- Bulk Density (g/cc)	1.3-1.5
- Apparent Specific Gravity	3.1-3.3
- Packing Density (lb/ft^3)	20-25
- Pore Volume (cc/g)	1.0-1.3
- Surface Area (m^2/g)	340-350

Sample of Chromatogram



PKNO	TIME	AREA	CONC	NAME
1	1.343	15266	1.1923	OXYGEN
2	1.803	1250138	97.6190	NITROGEN
3	5.218	15226	1.1887	CARBON MONOXIDE
<hr/>				
TOTAL		1280630	100	

VITA

Mr. Thawatchai Majitnapakul was born on January 13, 1968. He received his Bachelor Degree of Science, Department of Chemistry, Faculty of Science, Mahidol University in 1989.



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