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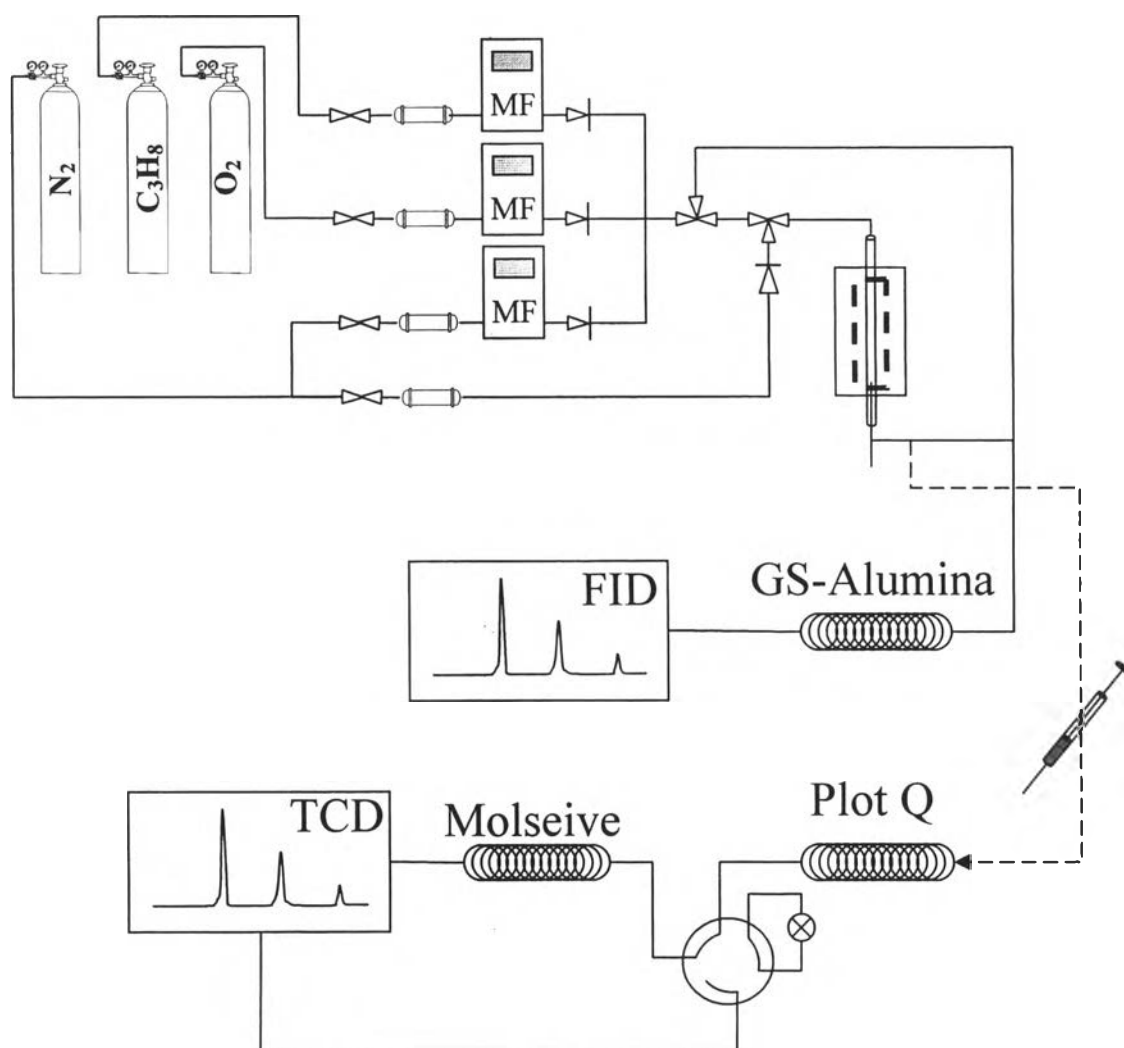
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APPENDICES

Appendix A Reactor diagram for testing VS-1 zeolite by oxidative dehydrogenation reaction



Appendix B Constructing calibration of hydrocarbon compound with FID detector. (GS-Alumina Column)

From
$$f_i = \frac{A_{STD} \times G_i \times f_{STD}}{A_i \times G_{STD}}$$

And
$$m_i = \frac{f_i \times A_i}{\sum f_i \times A_i}$$

- When
- f_i = response factor of component
 - f_{STD} = response factor of standard component
 - A_i = GC peak area of component
 - A_{STD} = GC peak area of standard component
 - G_i = mass of component
 - G_{STD} = mass of standard component
 - m_i = unknown mass of component

Propane was selected as a standard component ($f_{STD} = 1$)

Component	f_i
Methane	1.03532
Ethane	1.02381
Ethylene	0.93305
Propane	1
Propylene	0.95951

Appendix C Constructing calibration of gas carrier, reactance and carbon oxide product with TCD detector. (PlotQ and Molveise column)

From
$$(RMR)_i = \frac{A_i}{A_{STD}} \frac{n_{STD}}{n_i} (RMR)_{STD}$$

And
$$y_i = \frac{A_i / (RMR)_i}{\sum A_i / (RMR)_i}$$

When $(RMR)_i$ = relative molar response factor of component

$(RMR)_{STD}$ = relative molar response factor of standard component

A_i = GC peak area of component

A_{STD} = GC peak area of standard component

n_i = mole of component

n_{STD} = mole of standard component

y_i = unknown mole of component

Propane was selected as a standard component ($(RMR)_{STD} = 1$)

Component	$(RMR)_i$
Propane	1
Nitrogen	0.57415
Oxygen	0.62457
Carbon monoxide	0.37439
Carbon dioxide	0.57889

	A	B	C	D	E	F	G	H	I	J	K	L	M	N	O	P
18																
19																
20	Methane					0.722474	0.800756	0.79867	0.75463							
21	Ethane					0.039656	0.045135	0.043482	0.041312							
22	Ethlene					0.859733	0.960374	0.948752	0.900892							
23	Propane					1	1	1	1							
24	Propylene					0.453199	0.490601	0.483784	0.467034							
25	Cabondioxide					0.05427	0.058737	0.059452	0.055859							
26	Oxygen					0.614564	0.672976	0.636664	0.658142							
27	Nitrogen					20.44119	22.00784	21.37079	21.01135							
28	Carbonmonoxide					0.388857	0.440758	0.43508	0.405426							
29																
30	Mole fraction of feed nitrogen					0.84703										
31	Mole fraction of feed oxygen					0.05008										
32	Mole fraction of feed propane					0.10289										
33																
34	Methane					0.0294	0.030243	0.030984	0.029834							
35	Ethane					0.001614	0.001705	0.001687	0.001833							
36	Ethlene					0.034986	0.036272	0.036807	0.035818							
37	Propane					0.040694	0.037768	0.038795	0.039534							
38	Propylene					0.018442	0.018529	0.018768	0.018464							
39	Carbondioxide					0.002208	0.002218	0.002306	0.002208							
40	Oxygen					0.025009	0.025417	0.024699	0.026019							
41	Nitrogen					0.831824	0.8312	0.829075	0.830664							
42	Carbonmonoxide					0.015824	0.016647	0.018879	0.016028							
43						1	1	1	1							
44										Average						
45	% Propane Conversion					61.16	63.98	63.09	62.32	62.64						
46	% Oxygen Conversion					50.96	50.20	51.73	49.05	50.49						
47	% Propylene Selectivity					18.00	17.54	17.47	17.79	17.70						
48	% Carbonmonoxide Selectivity					15.44	15.76	15.71	15.44	15.59						
49	% Cabondioxide Selectivity					2.16	2.10	2.15	2.13	2.13						
50	% Ethane					1.57	1.61	1.57	1.57	1.58						
51	% Ethylene					34.14	34.34	34.26	34.32	34.27						
52	% Methane					28.69	28.64	28.84	28.75	28.73						
53						100.00	100.00	100.00	100.00	100.00						

	F	G	H	I	J	K	L	M	N	O	P
34	0.0294	0.030243	0.030984	0.029834							
35	0.001614	0.001705	0.001687	0.001833							
36	0.034986	0.036272	0.036807	0.035818							
37	0.040694	0.037768	0.038795	0.039534							
38	0.018442	0.018529	0.018768	0.018464							
39	0.002208	0.002218	0.002306	0.002208							
40	0.025009	0.025417	0.024699	0.026019							
41	0.831824	0.8312	0.829075	0.830664							
42	0.015824	0.016647	0.018879	0.016028							
43	1	1	1	1							
44					Average						
45	61.16	63.98	63.09	62.32	62.64						
46	50.96	50.20	51.73	49.05	50.49						
47	18.00	17.54	17.47	17.79	17.70						
48	15.44	15.76	15.71	15.44	15.59						
49	2.16	2.10	2.15	2.13	2.13						
50	1.57	1.61	1.57	1.57	1.58						
51	34.14	34.34	34.26	34.32	34.27						
52	28.69	28.64	28.84	28.75	28.73						
53	100.00	100.00	100.00	100.00	100.00						

	F	G	H	I	J	K	L	M	N	O	P
45	61.16	63.98	63.09	62.32	62.64						
46	50.96	50.20	51.73	49.05	50.49						
47	18.00	17.54	17.47	17.79	17.70						
48	15.44	15.76	15.71	15.44	15.59						
49	2.16	2.10	2.15	2.13	2.13						
50	1.57	1.61	1.57	1.57	1.58						
51	34.14	34.34	34.26	34.32	34.27						
52	28.69	28.64	28.84	28.75	28.73						
53	100.00	100.00	100.00	100.00	100.00						

	F	G	H	I	J	K	L	M	N	O	P
45	61.16	63.98	63.09	62.32	62.64						
46	50.96	50.20	51.73	49.05	50.49						
47	18.00	17.54	17.47	17.79	17.70						
48	15.44	15.76	15.71	15.44	15.59						
49	2.16	2.10	2.15	2.13	2.13						
50	1.57	1.61	1.57	1.57	1.58						
51	34.14	34.34	34.26	34.32	34.27						
52	28.69	28.64	28.84	28.75	28.73						
53	100.00	100.00	100.00	100.00	100.00						

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2. Phiriyawirut, P., Magaraphan, R., Jamieson, A. M., and Wongkasemjit, S. (2003) MFI zeolite synthesis directly from silatrane via sol-gel process and microwave technique. Materials Science and Engineering A, 361, 147-154
3. Phiriyawirut, P., Magaraphan, R., Jamieson, A. M., and Wongkasemjit, S. (2003) Morphology study of MFI zeolite synthesized directly from silatrane and alumatrane via the sol-gel process and microwave heating. Microporous and Mesoporous Materials 64, 83-93
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Presentations:

1. Phiriyawirut, P., Magaraphan, R., Jamieson, A. M., and Wongkasemjit, S. (2003, September) Effect of Reaction Parameters on Morphology of Synthesized MFI. Paper presented at 1st International Meeting on Applied Physics, Badajoz, Spain.

2. Phiriyawirut, P., Magaraphan, R., Jamieson, A. M., and Wongkasemjit, S. (2002, April) Silica Based Zeolite Synthesis Directly from Silatrane via Sol-Gel Process and Microwave Technique. Paper presented at RGJ-Ph.D. Congress III, Pattaya, Chonburi, Thailand.