

REFERENCES

1. R.R.V.A. Rios, M. Gontijo, V.P. Ferraz, R.M. Lago and M.H. Araujo, *Devulcanization of styrenebutadiene (SBR) waste tire by controlled oxidation*. Journal of the Brazilian Chemical Society, 2006. 17(3): p. 603-608.
2. H. Mhaimun, *Scanning Electron Microscope : SEM*. 2012: Mae Fah Luang University.
3. P.N. Brouwer, *Theory of XRF*. 2010: PANalytical B.V.
4. A.W. Marek and A.S. Micheal, *Pyrolysis of scrap tires*. chemtech, 1996. 49.
5. B. Adhikari, D. De and S. Maiti, *Reclamation and recycling of waste rubber*. Progress in Polymer Science, 2000. 25: p. 909-948.
6. S. Miao and B.H. Shanks, *Mechanism of acetic acid esterification over sulfonic acid-functionalized mesoporous silica*. Journal of Catalysis, 2011. 279(1): p. 136-143.
7. V.L. Shulman, *Chapter 21 - Tyre Recycling*, in *Waste*, Letcher, T.M. and Vallero, D.A., Editors. 2011, Academic Press: Boston. p. 297-320.
8. J. Zhang, Q. Zhou, X.-H. Jiang, A.-K. Du, T. Zhao, J. van Kasteren and Y.-Z. Wang, *Oxidation of natural rubber using a sodium tungstate/acetic acid/hydrogen peroxide catalytic system*. Polymer Degradation and Stability, 2010. 95(6): p. 1077-1082.
9. R. Dittmeyer and G. Emig, *Simultaneous Heat and Mass Transfer and Chemical Reaction*, in *Handbook of Heterogeneous Catalysis*. 2008, Wiley-VCH Verlag GmbH & Co. KGaA.
10. A.I. Isayev, *Chapter 15 - Recycling of Rubbers*, in *The Science and Technology of Rubber (Fourth Edition)*, Mark, J.E., Erman, B., and Roland, C.M., Editors. 2013, Academic Press: Boston. p. 697-764.
11. J.Y. Park, D.K. Kim and J.S. Lee, *Esterification of free fatty acids using water-tolerable Amberlyst as a heterogeneous catalyst*. Bioresour Technol, 2010. 101(1): p. S62-5.
12. M. Sienkiewicz, J. Kucinska-Lipka, H. Janik and A. Balas, *Progress in used tyres management in the European Union: a review*. Waste Management, 2012. 32(10): p. 1742-51.
13. Q. Qu, Q. Gu, Z. Gu, Y. Shen, C. Wang and X. Hu, *Efficient removal of heavy metal from aqueous solution by sulfonic acid functionalized nonporous silica*



- microspheres*. *Colloids and Surfaces A: Physicochemical and Engineering Aspects*, 2012. **415**: p. 41-46.
14. T. Sata, T. Yoshida and K. Matsusaki, *Transport properties of phosphonic acid and sulfonic acid cation exchange membranes*. *Journal of Membrane Science*, 1996. **120**(1): p. 101-110.
 15. C.S. Caetano, L. Guerreiro, I.M. Fonseca, A.M. Ramos, J. Vital and J.E. Castanheiro, *Esterification of fatty acids to biodiesel over polymers with sulfonic acid groups*. *Applied Catalysis A: General*, 2009. **359**(1-2): p. 41-46.
 16. V.K. Sharma, F. Fortuna, M. Mincarini, M. Berillo and G. Cornacchia, *Disposal of waste tyres for energy recovery and safe environment*. *Applied Energy*, 2000. **65**(1-4): p. 381-394.
 17. S.B. Liang and Y.C. Hao, *A novel cryogenic grinding system for recycling scrap tire peels*. *Advanced Powder Technology*, 2000. **11**(2): p. 187-197.
 18. A. Yilmaz and N. Degirmenci, *Possibility of using waste tire rubber and fly ash with Portland cement as construction materials*. *Waste Manag*, 2009. **29**(5): p. 1541-6.
 19. S.J. Pickering, *Recycling technologies for thermoset composite materials—current status*. *Composites Part A: Applied Science and Manufacturing*, 2006. **37**(8): p. 1206-1215.
 20. J.W. Jang, T.S. Yoo, J.H. Oh and I. Iwasaki, *Discarded tire recycling practices in the United States, Japan and Korea*. *Resources, Conservation and Recycling*, 1998. **22**: p. 1-14.
 21. K.A. Dubkov, S.V. Semikolenov, D.P. Ivanov, D.E. Babushkin, G.I. Panov and V.N. Parmon, *Reclamation of waste tyre rubber with nitrous oxide*. *Polymer Degradation and Stability*, 2012. **97**(7): p. 1123-1130.
 22. Y. Huang, R.N. Bird and O. Heidrich, *A review of the use of recycled solid waste materials in asphalt pavements*. *Resources, Conservation and Recycling*, 2007. **52**(1): p. 58-73.
 23. J.D. Martinez, N. Puy, R. Murillo, T. Garcia, M.V. Navarro and A.M. Mastral, *Waste tyre pyrolysis – A review*. *Renewable and Sustainable Energy Reviews*, 2013. **23**: p. 179-213.
 24. D.A. Tillman and N. Stanley Harding, *Chapter 6 - Tire-derived Fuel as an Opportunity Fuel*, in *Fuels of Opportunity*, Tillman, D.A. and Harding, N.S., Editors. 2004, Elsevier: Oxford. p. 227-263.
 25. M. Marc, *Devulcanization of rubber and other elastomers*. 2013, Google Patents.



26. P. Sutanto, F.L. Laksana, F. Picchioni and L.P.B.M. Janssen, *Modeling on the kinetics of an EPDM devulcanization in an internal batch mixer using an amine as the devulcanizing agent*. Chemical Engineering Science, 2006. 61(19): p. 6442-6453.
27. J.B. Macleod, M.E. Moir, R.D. Myers and P. Nicholson, *Rubber devulcanization process*. 1997, Google Patents.
28. M.M. Hassan, R.O. Aly, S.E.A. Aal, A.M. El-Masry and E.S. Fathy, *Styrene butadiene-based blends containing waste rubber powder: Physico-mechanical effects of mechanochemical devulcanization and gamma irradiation*. Journal of Industrial and Engineering Chemistry, 2013. 19(5): p. 1735-1742.
29. B. Maxwell, *Process of reclaiming rubber and refining reclaimed rubber*. 1979, Google Patents.
30. E.T. Azar, *Cryogenic tire recycling system*. 1995, Google Patents.
31. D.S. Novotny, R.L. Marsh, F.C. Masters and D.N. Tally, *Microwave devulcanization of rubber*. 1978, Google Patents.
32. J. Chen and A. Isayev, *Continuous ultrasonic devulcanization of vulcanized elastomers*. 1994, Google Patents.
33. A. Pelofsky, *Rubber reclamation using ultrasonic energy*. 1973, Google Patents.
34. M. Okuda and Y. Hatano, *Devulcanization method of rubber using ultrasound*. 1987, JP Patent.
35. C. Yao, S. Zhao, Y. Wang, B. Wang, M. Wei and M. Hu, *Microbial desulfurization of waste latex rubber with Alicyclobacillus sp.* Polymer Degradation and Stability, 2013. 98(9): p. 1724-1730.
36. F.P. Ballistreri, G.A. Tomaselli and R.M. Toscano, *Selective and mild oxidation of thiols to sulfonic acids by hydrogen peroxide catalyzed by methyltrioxorhenium*. Tetrahedron Letters, 2008. 49(20): p. 3291-3293.
37. F.P. Ballistreri, G.A. Tomaselli and R.M. Toscano, *Selective oxidation reactions of diaryl- and dialkyldisulfides to sulfonic acids by CH₃ReO₃/hydrogen peroxide*. Tetrahedron Letters, 2009. 50(46): p. 6231-6232.
38. J. Heveling, *Heterogeneous Catalytic Chemistry by Example of Industrial Applications*. Journal of Chemical Education, 2012: p. 121009094645009.
39. P. Dupont, J.C. Védrine, E. Paumard, G. Hecquet and F. Lefebvre, *Heteropolyacids supported on activated carbon as catalysts for the esterification of acrylic acid by butanol*. Applied Catalysis A: General, 1995. 129(2): p. 217-227.



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40. J.E. Castanheiro, A.M. Ramos, I.M. Fonseca and J. Vital, *Esterification of acetic acid by isoamylic alcohol over catalytic membranes of poly(vinyl alcohol) containing sulfonic acid groups*. Applied Catalysis A: General, 2006. 311: p. 17-23.
41. Y. Liu, E. Lotero and J.G. Goodwin, *Effect of water on sulfuric acid catalyzed esterification*. Journal of Molecular Catalysis A: Chemical, 2006. 245(1-2): p. 132-140.
42. A.A. Yehia, M.A. Mull, M.N. Ismail, Y.A. Hefny and E.M. Abdel-Bary, *Effect of chemically modified waste rubber powder as a filler in natural rubber vulcanizates*. Journal of Applied Polymer Science, 2004. 93(1): p. 30-36.
43. X. Tian, L.L. Zhang, P. Bai and X.S. Zhao, *Sulfonic-acid-functionalized porous benzene phenol polymer and carbon for catalytic esterification of methanol with acetic acid*. Catalysis Today, 2011. 166(1): p. 53-59.
44. H. Ismail, N.F. Omar and N. Othman, *The Effect of Kenaf Fibre Loading on Curing Characteristics and Mechanical Properties of Waste Tyre Dust/Kenaf Fibre Hybrid Filler Filled Natural Rubber Compounds*. Bioresources, 2011. 6(4): p. 3742-3756.
45. M.M. Hassan, N.A. Badway, M.Y. Elnaggar and E.-S.A. Hegazy, *Thermo-mechanical properties of devulcanized rubber/high crystalline polypropylene blends modified by ionizing radiation*. Journal of Industrial and Engineering Chemistry, 2013. 19(4): p. 1241-1250.
46. F. Shirini and O.G. Jolodar, *Introduction of N-sulfonic acid poly(4-vinylpyridinum) chloride as an efficient and reusable catalyst for the chemoselective 1,1-diacetate protection and deprotection of aldehydes*. Journal of Molecular Catalysis A: Chemical, 2012. 356: p. 61-69.
47. K. Kamegawa, K. Nishikubo, M. Kodama, Y. Adachi and H. Yoshida, *Dissolution-aggregation behavior of water-soluble nanographites and their adsorptive characteristics for 2-naphthol in aqueous solutions*. Journal of Colloid and Interface Science, 2003. 268(1): p. 58-62.
48. Q. Yang, L. Wang, W. Xiang, J. Zhou and J. Li, *Grafting polymers onto carbon black surface by trapping polymer radicals*. Polymer, 2007. 48(10): p. 2866-2873.
49. D.D. Jiang, Q. Yao, M.A. McKinney and C.A. Wilkie, *TGA/FTIR studies on the thermal degradation of some polymeric sulfonic and phosphonic acids and their sodium salts*. Polymer Degradation and Stability, 1999. 63(3): p. 423-434.



50. S. Gan, H.K. Ng, P.H. Chan and F.L. Leong, *Heterogeneous free fatty acids esterification in waste cooking oil using ion-exchange resins*. Fuel Processing Technology, 2012. **102**: p. 67-72.



APPENDICES



APPENDIX A

Calculation in the Characterization of the Catalyst

1. Calculation of the sulfur content from XRF

Crumb rubber	100	g	had SO ₃	3.010	g
SO ₃	1	mol	=	80.000	g
Crumb rubber	100	g	had SO ₃	0.038	mol

From the calculation, crumb rubber 100 g had 1.204 g of sulfur and 1.806 g of oxygen which equaled to 0.038 mol and 0.113 mol, respectively. The detected sulfur content from XRF found 0.380 mmol per 1 g of crumb rubber.

2. Calculation of the sulfur content from Bomb Calorimetry

The sulfur content of the original and oxidized crumb rubber was found by following the ASTM D3177, the standard for the estimation of sulfur content in coal. This calculation used the equation below;

$$\text{Sulfur content (\%)} = \frac{(A - B) \times 13.738}{C} \quad (\text{A1})$$

where; A is weight of burned crucible with sample (g)

B is weight of empty crucible (g)

C is weight of sample (g)

Example;

CR-HNO ₃ (6M)	weight of burned crucible with sample	20.2920	g
	weight of empty crucible	20.2515	g
	weight of sample	0.8814	g
	sulfur content	0.63	% by mass

3. Calculation of the sulfur loss from the oxidation

$$\text{Sulfur loss (\%)} = \frac{(A - B)}{A} \times 100 \quad (\text{A2})$$

where; A is the sulfur content of the original crumb rubber
(g sulfur/g rubber)

B is the sulfur content of the oxidized crumb rubber
(g sulfur/g rubber)

Example;

CR-HNO ₃ (6M)	the sulfur content of the original crumb rubber	0.0121 g sulfur/g rubber
	the sulfur content of the oxidized crumb rubber	0.0056 g sulfur/g rubber
	sulfur loss	54.0 %

4. Calculation of the swelling ratio

The swelling ratio of samples was measured by swelling test following ASTM D471. The swelling ratio (Q) was calculated according to the equation below;

$$\text{Swelling ratio } (Q) = \frac{M - M_0}{M_0} \quad (\text{A3})$$

where; M is weight of the swollen sample (g)

M_0 is weight of the original sample (g)

Q is swelling ratio

Example;

CR-HNO ₃ (6M)	weight of the swollen sample in toluene	0.54 g
	weight of the original sample	0.21 g
	swelling ratio in toluene	1.55



5. Calculation of the sol/gel content

The sol and gel content of samples were measured by the determination of gel fraction following ASTM D3616. The gel content was calculated after the weight of sample changed by the equation below;

$$Sol (\%) = \frac{W_0 - W_d}{W_0} \times 100 \quad (A4)$$

$$Gel(\%) = 100 - Sol (\%) \quad (A5)$$

where; W_0 is the initial mass of sample (g)
 W_d is the total dried mass of sample (g)
 Sol is the dissolved rubber fraction in the solvent (%)
 Gel is the undissolved rubber fraction in the solvent (%)

Example;

CR-HNO ₃ (6M)	the initial mass of sample	0.2069 g
	the total dried mass of sample	0.1706 g
	the dissolved rubber fraction in the solvent	17.6 %
	the undissolved rubber fraction in the solvent	82.4 %

6. Calculation of the acid content from the titration

The acid content of the oxidized crumb rubber was measured by an acid-base titration method. The result of this part was represented as mmol/g of the oxidized crumb rubber which measured from the ion-exchange capacity or the acid content (H⁺). The acid content was calculated from the equation below:

$$Acid\ content = \frac{A \times B}{C} \quad (A6)$$



where; A is NaOH content in titration (mL)
 B is Composition of NaOH (mol/L)
 C is weight of samples (g)
 Acid content is the H^+ exchange capacity (mmole/g sample)

Example from the direct titration method with DI 10 mL+THF 10 mL;

CR-HNO ₃ (6M)	NaOH content in titration	1.83	mL
	Composition of NaOH	0.05	mol/L
	weight of samples	0.1076	g
	the H^+ exchange capacity	0.85	mmol/g sample

7. Calculation of the catalyst recovery from the esterification

After the esterification, catalyst was removed from the product to recover. Catalyst was cleaned by using 150 mL of hexane. Then, the catalyst recovery was calculated by following the equation below;

$$\text{catalyst recovery (\%)} = \frac{(A - B)}{A} \times 100 \quad (A7)$$

where; A is weight of catalyst before esterification (g)
 B is weight of catalyst after esterification (g)
 Catalyst recovery is catalyst recovered after esterification (%)

Example from the esterification of octanoic acid with octanol on the effect of catalyst loading ;

CR-HNO ₃ (6M) 1%	weight of catalyst before esterification	0.0715	g
	weight of catalyst after esterification	0.0245	g
	catalyst recovered after esterification	34.27	%

APPENDIX B

The Calibration Curve in the Esterification

The calibration curve was applied to analyze the acid conversion in the esterification. This curve was plotted by the data obtained from the chromatogram of octanoic acid. Y-axis was the mass ratio of octanoic acid and standard solution while X-axis was the peak area ratio of octanoic acid and internal standard solution. This method used methyl undecanoate (C₁₁) as the internal standard. Table B1 shows the mass ratio and peak area ratio for plot the calibration curve of octanoic acid.

Table B1 The mass ratio and peak area ratio of octanoic acid to internal standard for plot the calibration curve of octanoic acid

Mass ratio of octanoic acid to internal standard	Peak area ratio of octanoic acid to internal standard
0.4222	0.4376
0.7601	0.7603
1.2857	1.2571
1.7190	1.7994
2.2730	2.3411
2.4298	2.4460



Figure B1 shows the calibration curve of the octanoic acid which has R^2 more than 0.99. This calibration curve has the accuracy and able to use in the quantitative analyzing.

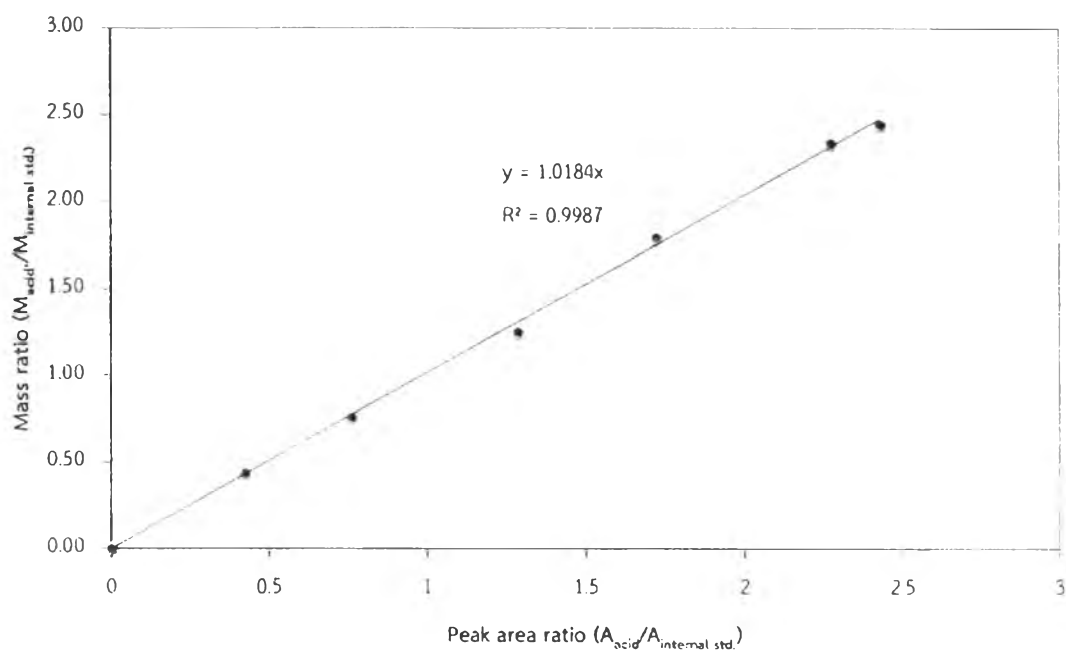


Figure B1 The calibration curve of the octanoic acid



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APPENDIX C

Calculation in the Octanoic Acid Conversion in the Esterification

1. The octanoic acid conversion
 - a. The calibration curve of the octanoic acid was used to calculate the remained octanoic acid after the esterification.
 - b. The peak area ratio of octanoic acid to internal standard was obtained from chromatogram of GC which was calculated in the equation from calibration curve below;

$$y = 1.0184x \quad (C1)$$

where; x is the peak area ratio of octanoic acid and internal standard solution

y is the mass ratio of octanoic acid and standard solution

Example from the esterification of octanol with octanoic acid on the effect of catalyst loading ;

CR-HNO₃(6M) 1% the peak area ratio of octanoic acid and internal standard solution 0.4910

the mass ratio of octanoic acid and standard solution 0.3821

the remained octanoic acid from the esterification 0.0012 g

- c. The remained octanoic acid from the esterification was obtained from the calculation.



d. The octanoic acid conversion was calculated by the equation below;

$$\text{octanoic acid conversion}(\%) = \frac{(A - B)}{A} \times 100$$

where; A is initial mass of octanoic acid (g)
 B is mass of octanoic acid after the esterification (g)
octanoic acid conversion is the conversion of octanoic acid to the ester product (%)

Example from the esterification of octanol with octanoic acid on the effect of catalyst loading ;

CR-HNO ₃ (6M) 1%	initial mass of octanoic acid	0.0024 g
	mass of octanoic acid after the esterification	0.0012 g
	octanoic acid conversion	50.8 %

2. The retention time (R_t) of alcohol, carboxylic acid and ester product was shown in table C1.

Table C1 The retention time (R_t) of alcohol, carboxylic acid and ester product

Substance	Retention time (min)
Internal standard C ₁₁ (Methyl undecanoate : C ₁₂ H ₂₄ O ₂)	5.76
Octanol (C ₈ H ₁₈ O)	3.89
Octanoic acid (C ₈ H ₁₆ O ₂)	4.55
Octyl octanoate (Ester product : C ₁₆ H ₃₂ O)	7.87
2-ethyl-1-hexanol (C ₈ H ₁₈ O)	3.56
2-ethyl-1-hexyl octanoate (Ester product : C ₁₆ H ₃₂ O)	7.89



3. The chromatogram from the esterification of alcohol with carboxylic acid without catalyst

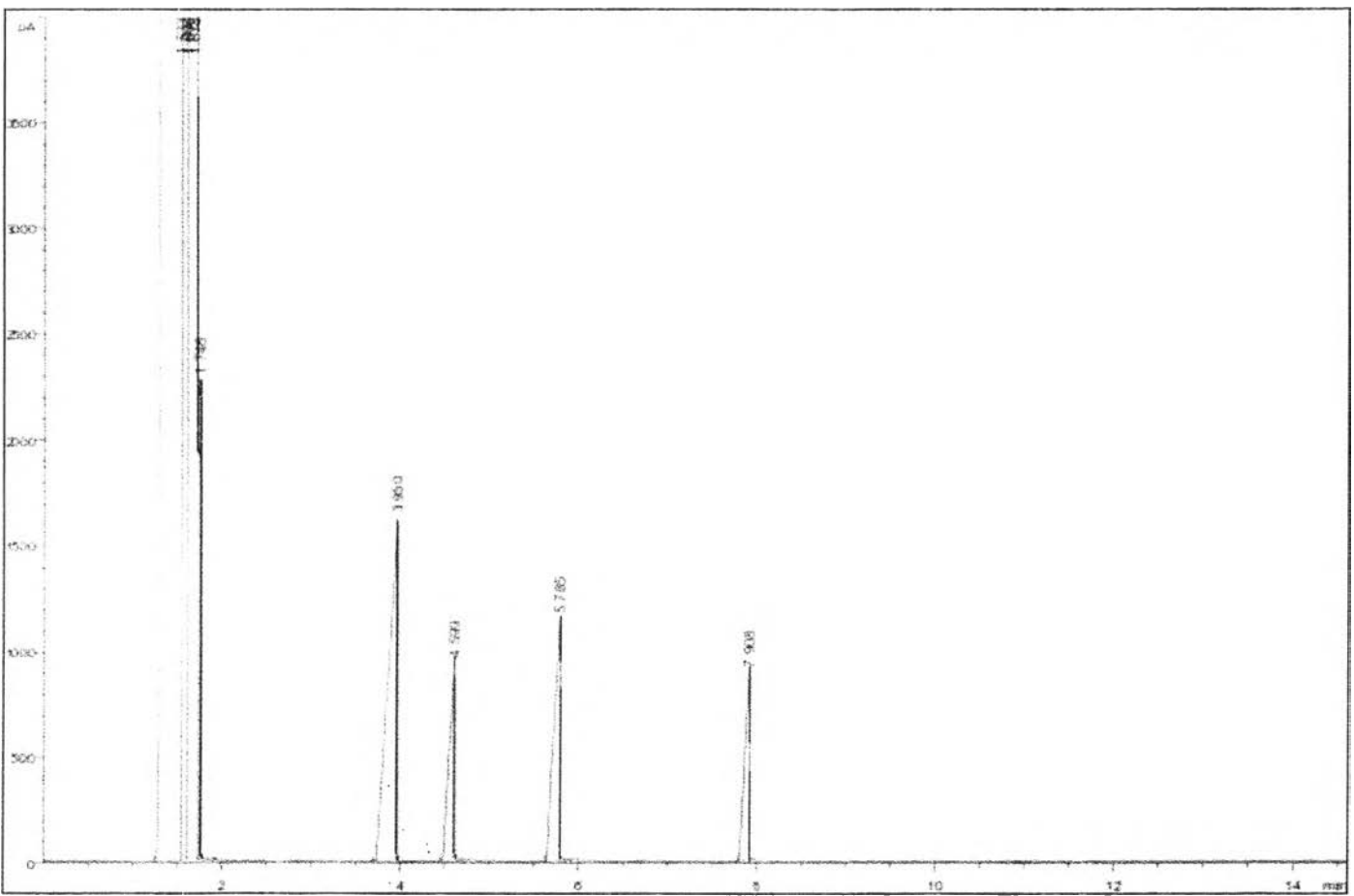


Figure C1 Chromatogram from the esterification of octanol with octanoic acid

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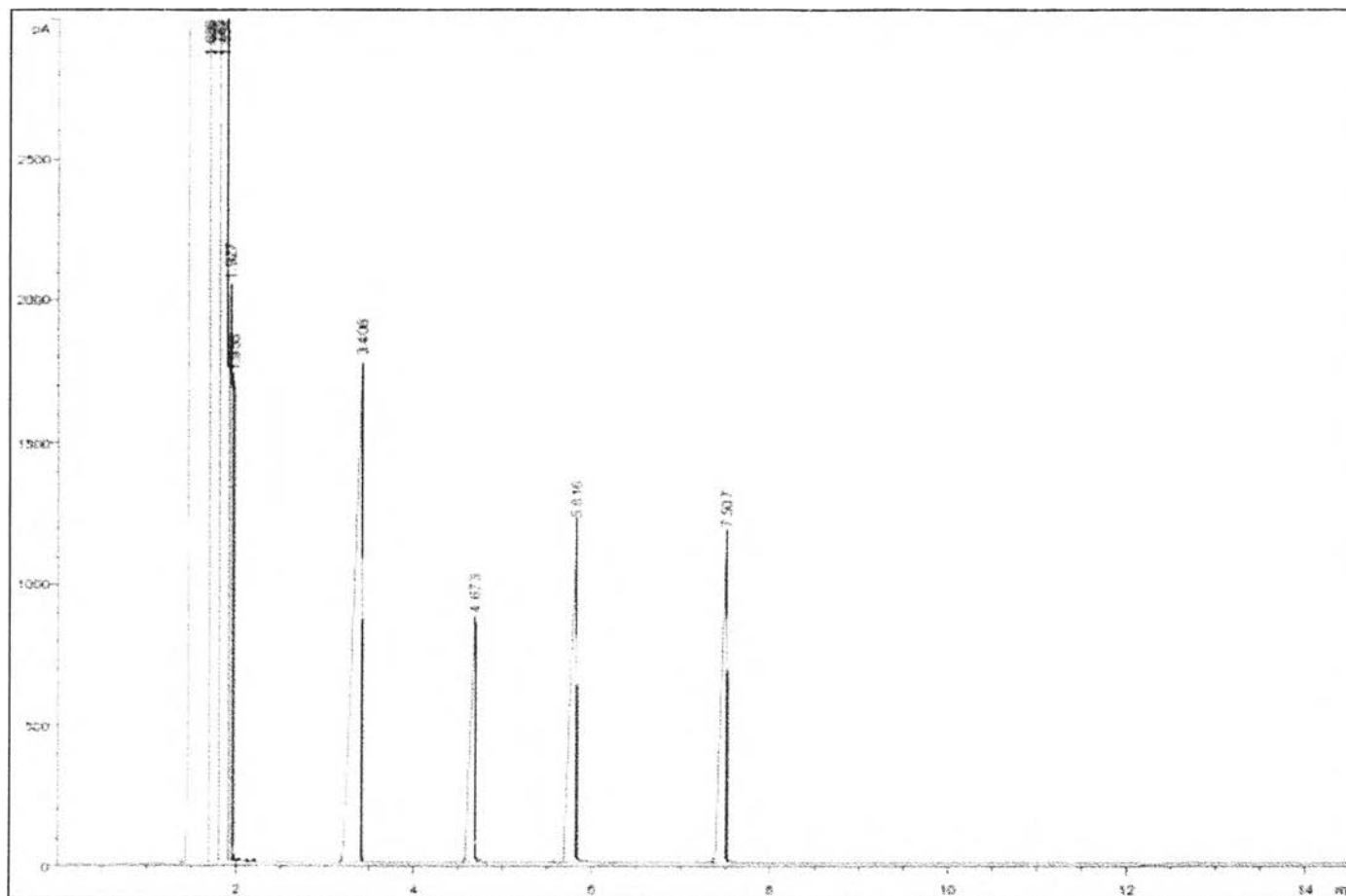


Figure C3 Chromatogram from the esterification of 2-ethyl-1-hexanol with octanoic acid

4. The chromatogram from the esterification of alcohol with carboxylic acid by using the oxidized crumb rubber as catalyst

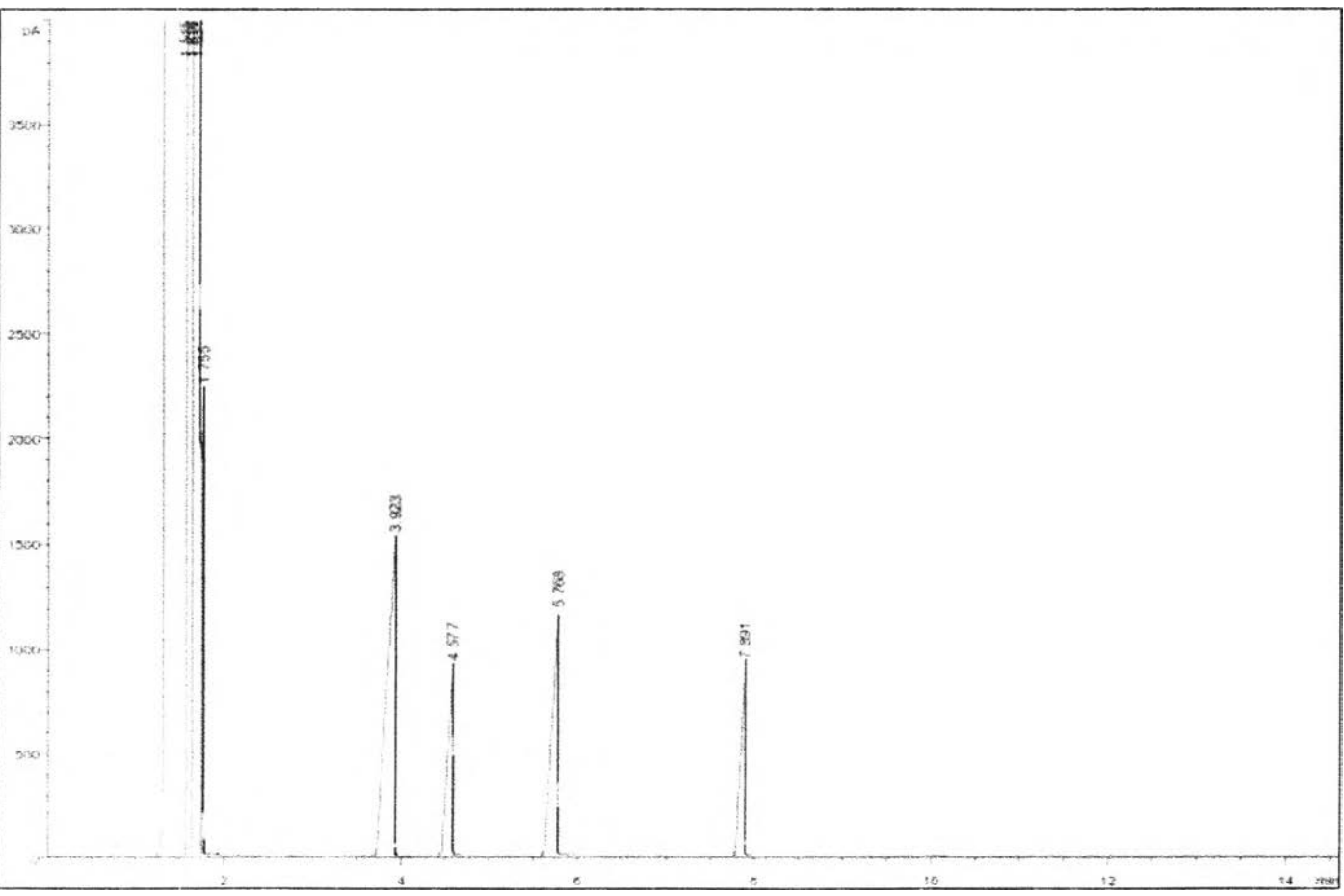


Figure C5 Chromatogram from the esterification of octanol with octanoic acid by using CR-HNO₃ (6M) as the catalyst

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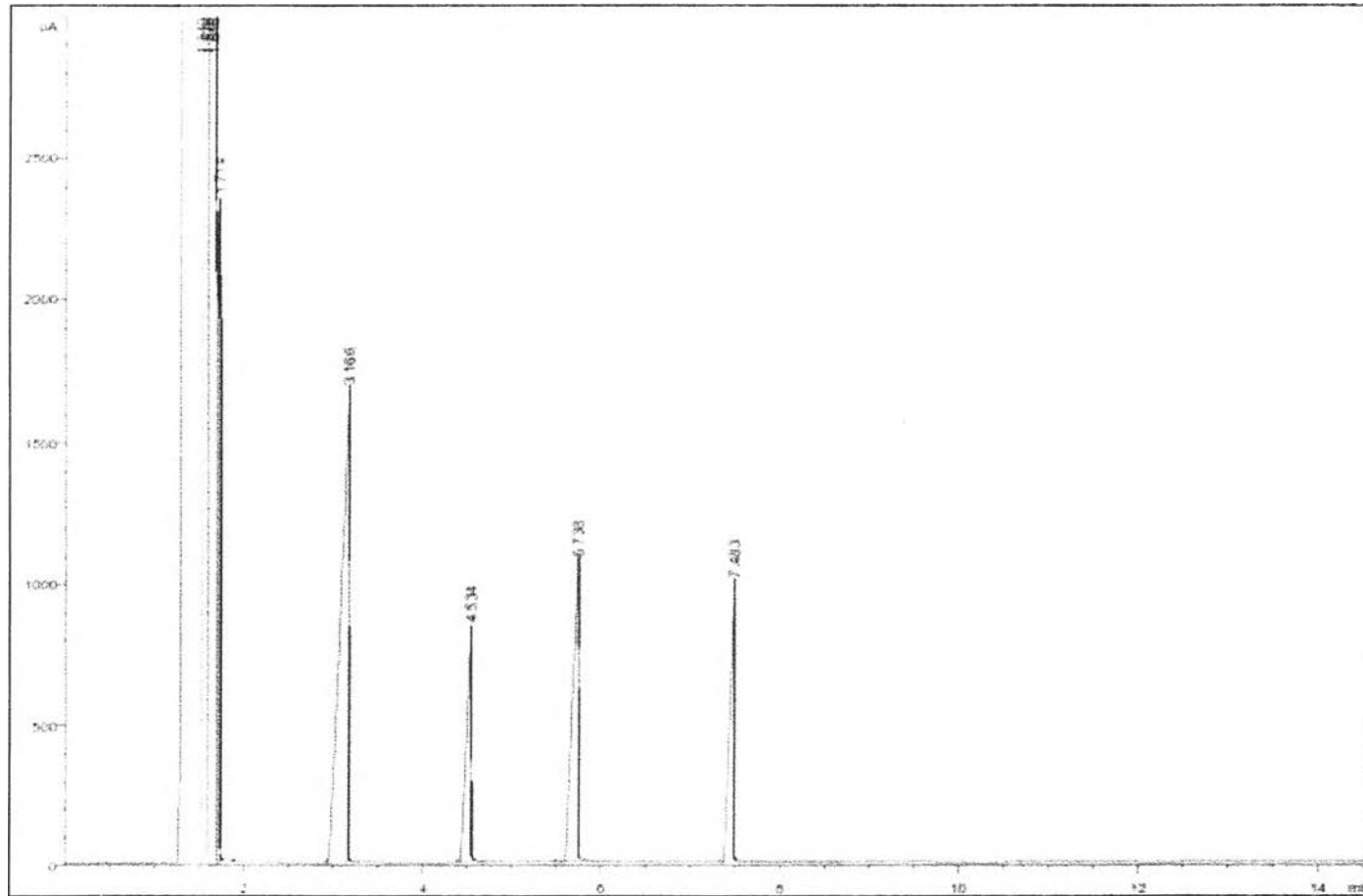


Figure C6 Chromatogram from the esterification of 2-ethyl-1-hexanol with octanoic acid by using CR-HNO₃ (6M)

VITA

Mr. Natdanai Charoensuk was born on May 17, 1989 in Ratchaburi, Thailand. He graduated with a Bachelor's degree of Science, majoring in the Chemical Technology, Faculty of Science, Chulalongkorn University in 2010. He has continued to study in Master's degree, majoring in Petrochemistry and Polymer Science, Faculty of Science, Chulalongkorn University, Bangkok, Thailand since 2011 and finished his study in 2014. He has attended to the Pure and Applied Chemistry International Conference 2013 (PACCON 2013) on January 23-25, 2013 at the Bangsaen Beach, Chonburi, Thailand which organized by Faculty of Science, Burapha University and the Chemical Society of Thailand with the oral presentation in topic of "Sulfonic Acid-Containing Rubber Prepared from Waste Tire".

