ลักษณะสมบัติการเร่งปฏิกิริยาแสงของไททาเนียมไดออกไซด์ที่เจือชาตุต่างๆและปรับสภาพด้วย กระบวนการไฮโดรเทอร์มัลภายใต้การกระดุ้นด้วยแสงที่มองเห็น

นางสาวฐาปนันท์ พุทธา

วิทยานิพนธ์นี้เป็นส่วนหนึ่งของการศึกษาตามหลักสูตรปริญญาวิทยาศาสตรดุษฎีบัณฑิต สาขาวิชาการจัดการสิ่งแวดล้อม (สหสาขาวิชา) บัณฑิตวิทยาลัย จุฬาลงกรณ์มหาวิทยาลัย ปีการศึกษา 2552 ลิขสิทธิ์ของจุฬาลงกรณ์มหาวิทยาลัย

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PHOTOCATALYTIC CHARACTERISTICS OF TITANIUM DIOXIDE DOPED WITH VARIOUS ELEMENTS AND HYDROTHERMAL TREATMENT UNDER VISIBLE-LIGHT ACTIVATION

Miss Thapanan Putta

A Dissertation Submitted in Partial Fulfillment of the Requirements for the Degree of Doctor of Philosophy Program in Environmental Management (Interdisciplinary Program) Graduate School Chulalongkorn University Academic Year 2009 Copyright of Chulalongkorn University

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	UNDER VISIBLE-LIGHT ACTIVATION
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จุฬาลงกรณ์มหาวิทยาลัย

ฐาปนันท์ พุทธา : ลักษณะสมบัติการเร่งปฏิกิริยาแสงของไททาเนียมไดออกไซด์ที่เจือ ธาตุต่างๆและปรับสภาพด้วยกระบวนการไฮโดรเทอร์มัลภายใต้การกระดุ้นด้วยแสงที่ มองเห็น (PHOTOCATALYTIC CHARACTERISTICS OF TITANIUM DIOXIDE DOPED WITH VARIOUS ELEMENTS AND HYDRO-THERMAL TREATMENT UNDER VISIBLE-LIGHT ACTIVATION) อ. ที่ปรึกษาวิทยานิพนธ์หลัก: รองศาสตราจารย์ ดร. จินต์ อโณทัย, อ. ที่ปรึกษา วิทยานิพนธ์ร่วม: Professor Ming-Chun Lu, Ph.D., 119 หน้า.

ในงานวิจัยนี้ สารเร่งปฏิกิริยาแสงไททาเนียมไดออกไซค์ชนิดใหม่ที่เจือทั้งสเตนและ ปรับสภาพด้วยกระบวนการไฮโครเทอร์มัลได้ถูกพัฒนาและทดสอบความไวปฏิกิริยาของการ เร่งปฏิกิริยาแสงโดยใช้ 2-คลอโรฟีนอลเป็นสารเป้าหมาย วิธีการสังเคราะห์และสภาวะที่ เหมาะสมได้แจกแจงไว้อย่างละเอียด สารเร่งปฏิกิริยาแสงนี้สามารถถูกกระคุ้นอย่างมี ประสิทธิภาพภายใต้การฉายแสงสีฟ้าและมีความไวปฏิกิริยาเกือบเทียบเท่ากับ Degussa P-25 ที่ ผลิตเพื่อการค้าภายใต้การฉายแสงอัลตราไวโอเล็ต โดย 2-คลอโรฟีนอลที่ 0.01 มิลลิโมลาร์ สามารถถูกกำจัดได้ทั้งหมดภายใน 120 และ 90 นาทีด้วยกระบวนการเร่งปฏิกิริยาแสงที่ใช้ ไททาเนียมไดออกไซด์เจือทั้งสเตนร้อยละ 0.5 โดยโมลและปรับสภาพด้วยกระบวนการ ไฮโครเทอร์มัลภายใต้การฉายแสงสีฟ้าและ Degussa P-25 ภายใต้การฉายแสงอัลตราไวโอเล็ต ตามลำดับ โครงสร้างผลึกซึ่งเป็นตัวแปรสำคัญที่ควบคุมพฤติกรรมการตอบสนองของ ไททาเนียมไดออกไซด์ภายใต้การฉายแสงอัลตราไวโอเล็ตไม่มีผลกระทบที่สำคัญภายใต้การ ลายแสงที่มองเห็น จลนพลศาสตร์การเร่งปฏิกิริยาแสงของการออกซิเคชั่น 2-คลอโรฟีนอล ด้วยไททาเนียมไดออกไซด์ที่เจือทั้งสเตนร้อยละ 0.5 และปรับสภาพด้วยกระบวนการ ไฮโดรเทอร์มัลภายใต้การฉายแสงสีฟ้าสามารถอธิบายได้ด้วยแบบจำลองของ Langmuir-Hinshelwood โดยมีค่า k และ K เท่ากับ 3.00×10⁴ มิลลิโมลาร์/นาที และ 239.13 ต่อมิลลิ-โมลาร์ ตามลำดับ

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PHOTOCATALYTIC CHARACTERISTICS OF TITANIUM DIOXIDE DOPED WITH VARIOUS ELEMENTS AND HYDROTHERMAL TREATMENT UNDER VISIBLE-LIGHT ACTIVATION. THESIS ADVISOR: ASSOCIATE PROFESSOR JIN ANOTAI, Ph.D., THESIS CO-ADVISOR: PROFESSOR MING-CHUN LU, Ph.D., 119 pp.

In this study, a new tungsten-doped titanium dioxide photocatalyst with hydrothermal treatment has been developed and tested for its photocatalytic activity by using 2-chlorophenol as the target compound. The synthetic procedure and optimum conditions were described in details. This photocatalyst could be effectively activated by blue-light irradiation and its activity was almost comparable to those of the commercial Degussa P-25 under ultraviolet irradiation. 2-chlorophenol at 0.01 mM could be removed completely in 120 and 90 minutes by the photocatalysis using 0.5% by mole tungsten-doped titanium dioxide with hydrothermal treatment under blue-light irradiation and the P-25 under ultraviolet irradiation, respectively. Crystalline structure which is a very important factor controlling the response behavior of the titanium dioxide under ultraviolet irradiation did not have any significant effect under visible-light irradiation. Photocatalytic kinetics of 2-chlorophenol oxidation by the 0.5% tungsten-doped titanium dioxide with hydrothermal treatment under blue-light irradiation could be sufficiently explained by the Langmuir-Hinshelwood model with kr and K of 3.00×10-4 mM/min and 239.13 1/mM, respectively.

ศูนย์วิทยทรัพยากร

Field of Study: Environmental Management Academic Year: 2009 Student's Signature The pancin Rutha Advisor's Signature No Co-Advisor's Signature Min Church

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CONTENTS

	Page
ABSTRACT (IN THAI)	iv
ABSTRACT (IN ENGLISH)	v
ACKNOWLEDGEMENT <mark>S</mark>	vi
CONTENTS	vii
LIST OF TABLES	Х
LIST OF FIGURES	xii
CHAPTER I INTRODUCTION	1
1.1 Research Rationale	1
1.2 Objectives	2
1.3 Hypothesis	3
1.4 Scopes of the Study	3
1.5 Obtained Results	3
CHAPTER II BACKGROUNDS AND LITERATURE REVIEWS	4
2.1 Theoretical Backgrounds	4
2.1.1 Advanced Oxidation Processes	4
2.1.2 Photocatalytic Process	4
2.1.3 Titanium Dioxide	5
2.1.3.1 Titanium Dioxide in Industrial Applications	5
- 2.1.3.2 Titanium Dioxide in Environmental Applications	5
2.1.3.3 Properties of Titanium Dioxide	6
2.1.3.4 Photocatalysis of Doped Titanium Dioxide	8
2.1.3.5 Synthesis Titanium Dioxide Process	9
2.1.3.5.1 Sol-Gel Process	9
2.1.3.5.2 Hydrothermal Process	12
2.1.4 Adsorption Isotherm	12
2.1.4.1 Langmuir Adsorption Isotherm	13
2.1.4.2 Freundlich Adsorption Isotherm	14
2.1.5 Langmuir-Hinshelwood Expression	14

viii Page

	Pag
2.1.6 Properties of 2-Chlorophenol	15
2.2 Literature Reviews	19
2.2.1 Photocatalysis of Doped Titanium Dioxide	19
2.2.2 Sol-Gel and Hydrothermal Methods	20
2.2.3 Photocatalysis of 2-Chlorophenol and Phenolic Compounds	21
CHAPTER III METHODOLOGY	23
3.1 Materials and Chemicals	23
3.1.1 Chemicals	23
3.1.2 Reactor	24
3.2 Experimental Procedures	24
3.2.1 Titanium Dioxide Synthesis	25
3.2.1.1 Synthesis of Titanium Dioxide by Sol-Gel Process	25
3.2.1.2 Synthesis of Titanium Dioxide with Hydrothermal	
Treatment	25
3.2.2 Determination of the Titanium Dioxide Activity	26
3.3 Experimental Scenarios	27
3.3.1 Modification of Titanium Dioxide Synthesis	27
3.3.1.1 Sol-Gel Process	27
3.3.1.2 Element Doping	28
3.3.1.3 Hydrothermal Treatment	28
3.3.2 Adsorption Study	29
3.3.3 Photocatalytic Activity Investigation	29
3.4 Analytical Methods	32
3.4.1 Identification of Crystalline Structure	32
3.4.2 Identification of Morphology	32
3.4.3 UV-VIS Absorption Spectra Analysis	32
3.4.4 Point of Zero Charge (pzc) Analysis	32
3.4.5 Surface Area Analysis	32
3.4.6 Laser Particle Size Distribution Analysis	32
3.4.7 Elemental Concentration	32
3.4.8 Measurement of 2-Chlorophenol	33

ix Page

CHAPTER IV RESULTS AND DISCUSSION	34
4.1 Titanium Dioxide Synthesis	34
4.1.1 Optimizing Sol-Gel Conditions	34
4.1.1.1 Effect of Calcination Temperature	34
4.1.1.2 Effect of Ramp Rate	38
4.1.1.3 Effect of Dissolution Temperature	40
4.1.2 Enhancement of Visible-Light Photocatalysis by Doping	42
4.1.2.1 Effect of Doping Element	42
4.1.2.2 Effect of Sol Catalyst on 0.5% W/TiO ₂	48
4.1.2.3 Effect of Hydrothermal Treatment	50
4.1.3 Physical Properties of Synthetic Titanium Dioxide	54
4.2 Adsorption of 2-chlorophenol	56
4.3 Kinetics study	61
4.3.1 Direct Photolysis and Volatilization	61
4.3.2 Effect of Titanium Dioxide Dose	62
4.3.3 Effect of pH	63
4.3.4 Effect of Light Wavelength	64
4.3.5 Kinetics Determination	66
4.3.6 Reusability of Synthetic Titanium Dioxide	69
CHAPTER V CONCLUSSION	71
5.1 Conclusions	71
5.2 Recommendations for Future Study	72
REFERENCES	73
APPENDICES	79
APPENDIX A	80
APPENDIX B	85
BIOGRAPHY	119

LIST OF TABLES

Table		Page
2.1	Comparison between rutile and anatase	8
2.2	MSDS of 2-chlorophenol	17
3.1	Conditions for the study of calcinations temperature effect	29
3.2	Conditions for the study of ramp rate effect	29
3.3	Conditions for the study of catalyst effect	29
3.4	Conditions for characterizing the 2-chlorophenol adsorption onto	
	TiO ₂ surface	30
3.5	Conditions for characterizing the P-25 catalytic activity under blue	
	and UV light irradiation	30
3.6	Conditions for determining the effect of TiO_2 dose under blue light	
	irradiation	30
3.7	Conditions for determining the effect of pH on TiO ₂ photocatalytic	
	activity	31
3.8	Conditions for determining the effect of light wavelength on TiO_2	
	photocatalytic activity	31
3.9	Conditions for determining the effect of 2-chlorophenol on TiO_2	
	photocatalytic activity	31
4.1	Effect of calcinations temperature on the crystallize size and weight	
	fraction of anatase and rutile phases	35
4.2	Band gap energy of the TiO ₂ calcined at various temperatures	37
4.3	Mole ratio of dopant to Titanium	42
4.4	Band gap energy of doped TiO ₂	45
4.5	Crystal size, band gap energy and weight fraction of anatase and	
	rutile phase of the synthetic TiO_2 compare to the Degussa P-25	55
4.6	BET specific surface area, pore volume and size of the synthetic	
	TiO ₂ compared to Degussa P-25	56
4.7	Comparison the particle size distribution between synthetic TiO_2	
	and Degussa P-25	56

4.8	Effect of light color on the photocatalytic activity of the synthetic	
	TiO ₂	64
4.9	Pseudo-first order rate constant for 2-chlorophenol photocatalytic	
	oxidation under different initial concentrations	69



xi Page

LIST OF FIGURES

Figure		Page
2.1	Schematic of photocatalytic process	7
2.2	Crystallize form of TiO ₂	8
2.3	Mechanism of sol-gel process	11
2.4	2-Chlorophenol molecular structure	16
2.5	Simplified mechanism for the photocatalytic degradation of 2-chloro-	
	phenol	18
3.1	Schematic diagram of the photocatalytic reactor	24
3.2	Schematic for TiO ₂ synthesis by sol-gel method	26
3.3	Schematic for TiO ₂ synthesis by hydrothermal method	27
3.4	Experiment schematic for photocatalytic activity investigation	28
4.1	XRD patterns of sol-gel synthetic TiO ₂ without doping calcined at	
	various temperatures	35
4.2	UV-VIS absorption spectrograph of sol-gel synthetic undoped TiO_2	
	calcined at various temperatures	37
4.3	Photodegradation of 0.01 mM 2-chlophenol at calcine temperature	
	200°C and 300°C under blue light irradiation	38
4.4	XRD pattern of undoped TiO ₂ calcined at various ramp rates	39
4.5	Photodegradation of 0.01 mM 2-chlophenol of the TiO_2 at various	
	ramp rate under blue light irradiation	39
4.6	UV-VIS absorption spectrograph of sol-gel synthetic undoped TiO_2	
	at temperature control in dissolution stage	41
4.7	The photodegradation of 0.01 mM 2-chlophenol at various	
	temperature and curing time control in dissolution stage under blue	
	light irradiation	41
4.8	Absorption spectrographs of the TiO_2 doped with tungsten under the	
	optimum sol-gel conditions	43
4.9	Absorption spectrographs of the TiO_2 doped with fluorine under the	
	optimum sol-gel conditions	43

4.10	Absorption spectrographs of the TiO_2 doped with platinum under the	
	optimum sol-gel conditions	44
4.11	Absorption spectrographs of 0.5% W/TiO ₂ , 1% F/TiO ₂ and	
	0.5% Pt/TiO ₂ compare to undoped TiO ₂ and Degussa P-25	45
4.12	XRD pattern of the 0.5% W/TiO ₂ (a) 0.5% W/TiO ₂ compared with	
	undoped TiO ₂ and Degussa P-25; (b) an enlargement of (a) at 2θ of	
	25.28	46
4.13	Photodegradation of 0.01 mM 2-chlophenol at various doped TiO_2	
	compare to undoped TiO ₂ and Degussa P-25 under blue light	
	irradiation	47
4.14	Absorption spectrographs of 0.5% W/TiO ₂ with different catalyst	
	prepared under optimum conditions	49
4.15	Effect of acid catalyst on XRD patterns of the 0.5% W/TiO ₂ prepared	
	under the optimum sol-gel conditions	49
4.16	Photodegradation of 0.05 mM 2-chlophenol by 0.5% W/TiO ₂ with	
	different acid catalysts under blue light irradiation	50
4.17	Absorption spectrographs of 0.5% W/TiO ₂ prepared at the optimum	
	sol-gel conditions with different hydrothermal treatment time	51
4.18	Effect of hydrothermal treatment time on the photodegradation of	
	0.01 mM 2-chlorophenol under blue light irradiation	52
4.19	XRD pattern of TiO ₂ synthesized under various conditions	52
4.20	Photodegradation of 0.01 mM 2-chlophenol by TiO ₂ synthesized	
	under various conditions under blue-light irradiation as compared to	
	Degussa P-25 under blue-light and UV irradiations	53
4.21	SEM micrographs of synthetic TiO_2 and Degussa P-25. (a) Degussa	
	P-25, (b) undoped TiO ₂ , (c) 0.5% W/TiO ₂ , and (d) 0.5% W/TiO ₂ with	
	hydrothermal treatment	55
4.22	Particle size distribution of the synthetic TiO_2 : (a) undoped TiO_2 , (b)	
	0.5% W/TiO ₂ , and (c) hydrothermal-treated 0.5% W/TiO ₂	57
4.23	Adsorption of 2-chlorophenol on synthetic TiO ₂ and Degussa P-25	58

xiv
Page

		U
4.24	Adsorption of 2-chlorophenol onto the surface of 0.5% W/TiO ₂ with	
	hydrothermal treatment	59
4.25	Isotherm plot of the 2-chlorophenol adsorption onto 0.5% W/TiO ₂	
	with hydrothermal treatment	59
4.26	Langmuir adsorption isotherm plot for hydrothermal-treated	
	0.5% W/TiO ₂	60
4.27	Freundlich adsorption isotherm plot for hydrothermal-treated	
	0.5% W/TiO ₂	60
4.28	Volatilization, photolysis and photocatalytic oxidation of	
	2-chlorophenol irradiated by blue light or UV in present of Degussa	
	P-25	61
4.29	Effect of undoped TiO ₂ dose on photocatalytic degradation of	
	2-chlorophenol irradiated by blue light	62
4.30	Point of zero charge of the synthetic TiO ₂	63
4.31	Effect of pH on photocatalytic degradation of 2-chlorophenol	
	irradiated by blue light	64
4.32	Photocatalysis of 2-chlorophenol under different light irradiation in	
	present of undoped TiO ₂	65
4.33	Photocatalysis of various initial concentration of 2-chlorophenol	
	under blue light irradiation in present of undoped TiO ₂ :	
	(a) degradation time-profile, and (b) 1 st -order plot	67
4.34	Photocatalysis of various initial concentration of 2-chlorophenol	
	under blue light irradiation in present of 0.5% W/TiO ₂ with	
	hydrothermal treatment: (a) degradation time-profile, and	
	(b) 1 st -order plot	68
4.35	Langmuir-Hinshelwood plot of Table 4.9	69
4.36	Photocatalysis of 2-chlorophenol under blue light irradiation in	
	present of fresh and used hydrothermal-treated 0.5% W/TiO ₂	70

CHAPTER I

INTRODUCTION

1.1 Research Rationale

Semiconductor photocatalysis has been proven to be a high efficient process for environmental remediation, air purification, deodorization, sterilization, and water treatment (Fujishima and Honda., 1972; Hoffmann et al., 1995). Among the semiconductor photocatalysts, titanium dioxide (TiO₂) is the most preferred and has been extensively studied for environmental purification applications because of its physical and chemical stability, good characteristics of powerful oxidation strength, non-toxicity and inexpensiveness (Ao et al., 2008). Unfortunately, major drawbacks in the popularization of TiO₂ are the large band gap (3.2 eV) which requires high activated energy and limiting the photocatalytic activity of TiO₂ only to the ultraviolet region and the high recombination rate of the electron-hole pair.

Many researchers have consistently attempted to improve the TiO₂ lightactivated property. The first and most common modification is to stretch its absorptivity down to the visible range which is abundant in solar light. Visible light energy accounts for 42% of the solar spectra compared with only 3% of the ultraviolet portion. Since, solar energy is clean, renewable, and ideally inexpensive, using solar energy to perform the photocatalytic processes has become the researchers' long-time dream. The second modification, which is also of interest by several researchers, is to reduce the electron recombination rate. Several main approaches have been investigated to achieve these purposes. Firstly, doping TiO₂ with transition metal to introduce defects into the TiO₂ lattice in the band-gap of TiO₂ to inhibited the phase transformation and assists the charge separation efficiency (Xu et al., 2004; Murakami et al., 2008; Lorret et al., 2009; and Wang, Chen et al., 2009). Secondly, couple TiO₂ with other semiconductors in order to enhance the charge separation in the photocarrier generation process (Albonetti et al., 2008; Xiao et al., 2008). The third possibility is to modify TiO₂ by surface deposition of noble metal to decrease charge carrier recombination by providing an electron sink (Chen, Ku and Kuo, 2007).

Many techniques have been used to produce the TiO_2 doped various elements, co-precipitation, and chemical vapor deposition (Stakheev, Shpiro and Apijok, 1993; Khouw et al., 1994) but sol-gel process is considered as one of the most promising alternatives. This is because it presents a number of advantages such as low calcination temperature, flexibility of processing, and homogeneity at molecular level. This method allows obtaining the anatase phase, which has high activity in photocatalytic applications (Fox and Dulay, 1993; Kato et al., 1994), at low temperature. Hydrothermal processing represents an alternative to the calcination for the crystallization of titanium under mild temperatures. It has been widely applied in the synthesis of zeolites and in the production of advanced ceramic powders with ultrafine particle size. In the hydrothermal treatment, grain size, particle morphology, crystalline phase, and surface chemistry can be controlled via processing variables such as nature of solvent, pH, reaction temperature and pressure, aging time and also additive. Typically, under various hydrothermal conditions, products of TiO₂ with different morphologies and micro structural forms have been yielded.

This research mainly focused on the improvement of TiO_2 photoactivity in the visible range by doping with several transition or noble metals as well as treating with hydrothermal treatment. 2-chlorophenol was selected as the target compound because it is an important toxic chemical commonly present in wastewater. It has wide applications as a biocide and disinfectant, and is an intermediate product in the manufacture of pesticides, dyestuffs and preservatives. Similar to other chlorinated aromatic compounds, 2-chlorophenol can adversely impact the ecosystem, either directly or indirectly, and can function as a carcinogenic agent (Ilisz et al., 2002). This has led to an increasing demand for efficient and economical treatment for 2-chlorophenol. The photocatalytic oxidation behavior of 2-chlorophenol revealed as a result of this research will provide valuable information for future 2-chlorophenol treatment.

1.2 Objectives

The main objective of this study is to use the sol-gel process to synthesize TiO_2 doped with various elements which can be activated by the visible-light. The specific objectives of this study are:

 To study the photocatalytic activity of TiO₂ doped with various elements by using 2-chlorophenol as an organic probe. 2. To studies the optical and structural properties of TiO₂ doped with various elements by using BET, SEM, XRD, XRF, UV-VIS spectrophotometer and Point of zero charge (pzc) methods.

1.3 Hypothesis

Doping and hydrothermal treatment can expand the photocatalytic activity of TiO_2 down to the visible light region.

1.4 Scopes of the Study

All experiments in this research were conducted in the laboratory scale. The scopes of this work were as follows:

1. Sol-gel and hydrothermal technique was used to synthesize TiO₂

2. All the photocatalytic processes were done with synthetic wastewater using 2-chlorophenol as an organic probe.

3. All the photocatalytic experiments were conducted at 1 atm and 25°C.

1.5 Obtained Results

This research provides valuable information on the synthetic TiO_2 which could be activated by visible light. This visible-light activated TiO_2 is a very useful photocatalyst and can be applied in the field practice with lower operative cost due to no need of an expensive UV light irradiation. The fundamental knowledge in the TiO_2 synthesis can serve as a solid platform for further improvement. In addition, the kinetics of 2-chlorophenol photodegradation by TiO_2 with visible-light irradiation is also included which can be applied to treat 2-chlorophenol contaminated wastewater in the future.

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CHAPTER II

BACKGROUNDS AND LITERATURE REVIEWS

2.1 Theoretical Backgrounds

2.1.1 Advanced Oxidation Processes

Advanced oxidation processes (AOPs) represent an alternative approach, including ultraviolet (UV) radiation, ozone, and hydrogen peroxide, either individually or in combination, which is used to destroy hazardous organic contaminants. The AOPs technologies can refer to two stage of sequential reaction. The first is the formation of the strong oxidants such as hydroxyl radicals (•OH) and the second is the reaction of these oxidants with organic/inorganic pollutants. However, the term of AOPs refers specifically to processes in which oxidation of organic contaminant occurs via •OH. The •OH is a powerful oxidant, short lived, highly reactive, and a non-selective oxidant which can oxidize many pollutants. These radicals react with pollutants and lead to degradation reaction. In some cases, AOPs can lead to complete oxidation of organic contaminants resulting in carbon dioxide (CO₂) and water (H₂O) without generating any harmful byproducts. Application of AOPs can cover many fields such as detoxification of persistent organic pollutants (POPs), disinfection and purification of contaminated air and wastewater steam, oxidative degradation of organic compounds, bactericidal and non-biodegradable compounds.

2.1.2 Photocatalytic Process

Photocatalysis is one of the AOPs. It consists of two words, the first word is "photo" which is light; and the second is "catalyst" which is the process by which the rate of a chemical reaction is increased by mean of the addition of species known as a catalyst to the reaction. Therefore, photocatalysis means the process which requires irradiation to initiate the catalytic reaction, without the radiation, the reaction cannot proceed. This technique is very useful for the degradation of non-biodegradable organics or toxic pollutants. Moreover, they are much more efficient than the conventional techniques such as coagulation, precipitation, adsorption on activated carbon and which lead to the complete mineralization and also detoxicification of pollutants, and in the case of halogenous compounds to the formation of halogenous ions purification. Lhomme, Brosillon and Wolbert (2008) investigated photocatalytic degradation of pesticides in pure water and a commercial agricultural solution on titanium dioxide (TiO₂) coated media.

2.1.3 Titanium Dioxide

2.1.3.1 Titanium Dioxide in Industrial Applications

Titanium dioxide, also known as titanium (IV) oxide or titania, is the naturally occurring oxide of titanium with the chemical formula TiO_2 . In the industrial work, it is the most widely used white pigment because of its brightness and very high refractive index. This pigment is used extensively in plastics, paints, coatings, papers, inks, and other applications for its UV resistant properties where it acts as a UV absorber, efficiently transforming destructive UV light energy into heat. When deposited as a thin film, its refractive index and color make it an excellent reflective optical coating for dielectric mirrors and some gemstones. TiO_2 is even used in food stuffs, for instance in the wrapping of salami, as well as medicines (i.e. pills and tablets) and toothpaste. In cosmetic and skin care products such as sunscreens, lipsticks, body powder, and soap.

2.1.3.2 Titanium Dioxide in Environmental Applications

In environmental works, starting in the late 1960s, TiO_2 began with photoelectrochemical solar energy conversion and then shifted into the area of environmental photocatalysis, including self-cleaning surfaces, and most recently into the area of photoinduced hydrophilicity, which involves not only self-cleaning surfaces, but also antifogging ones. One of the most interesting aspects of TiO_2 is that the types of photochemistry responsible for photocatalysis and hydrophilicity are completely different, even though both can occur simultaneously on the same surface (Fujishima, Rao and Tryk, 2000). TiO_2 is the most preferable photocatalyst because of its physical and chemical stability and non-toxicity. It is well known as a photocatalyst for water and air treatment as well as for catalytic production of gases. Also in development is a paving stone that uses the catalytic properties of TiO_2 to remove nitrogen oxide from the air, breaking it down into more environmentally benign substances that can then be washed away by rainfall. Other experiments with TiO₂ Son, Ko and Zoh (2009) investigated kinetics and mechanism of photolysis and TiO_2 photocatalysis of triclosan. The results were compared in TiO_2 only in the dark condition, photolysis, and TiO₂ photocatalysis with a UV-A lamp. TiO₂ photocatalysis more effectively degraded and mineralized triclosan compared to TiO₂ only and photolysis conditions.

2.1.3.3 Properties of Titanium Dioxide

 TiO_2 is consisted of two band gaps; the first is valence band (VB), the highest occupied band full of electron, and the second band is conduction band (CB), the lowest unoccupied band. The bands are separated by different energy level which is called "band gap energy." As the TiO₂ absorbs energy greater than band gap energy, it will produce electron and hole pairs. The electron of the VB of TiO₂ becomes excited when illuminated by light. The excess energy of this excited electron promoted the electron to the CB of TiO_2 therefore creating the negative-electron (e) and positive-hole (h^+) pair (Equation (2.1)). This stage is referred as the semiconductor's "photo-excitation" state. Wavelength of the light necessary for photo-excitation of 3.2 eV (band gap energy) is 380 nm. The h^+ of TiO₂ could pull an electron from OH- or water molecule to form •OH as shown in Equations (2.2) and (2.3). The e^{-1} reacts with oxygen molecule to form super oxide anion ($\bullet O_2$) (Equation (2.4)). This $\bullet O_2$ powerful oxidizing agents will disintegrate and rearrange the structure of the organic pollutants and convert them into CO₂ and H₂O. The photoexcitation of electron and hole pairs can recombine as e⁻ returns to its original state. Therefore, it should have electron acceptor, for example O_2 to obstruct the recombination. The overall process is illustrated in Figure 2.1 below.

$$TiO_{2} + hv \longrightarrow e^{-} + h^{+} \qquad (2.1)$$

$$h^{+} + OH^{-}(surface) \longrightarrow OH \qquad (2.2)$$

$$h^{+} + H_{2}O \longrightarrow OH \qquad (2.3)$$

$$O_{2} + e^{-} \longrightarrow O_{2}^{-} \qquad (2.4)$$

(2.4)



Figure 2.1 Schematic of photocatalytic process.

Normally, TiO₂ crystallizes have three polymorphic forms which are anatase, rutile, and brookite, as shown in Figure 2.2. Rutile and anatase have been used as the catalysts in heterogenous photocatalysis while brookite is usually found only in mineral ores. The photocatalytic activities of these two crystals mainly depend on their structure. Rutile will be more stable at high temperatures while anatase will be more stable at low temperatures. The structure of TiO₂ will depend largely on the calcination temperature. Wetchakun and Phanichphant, (2008) concluded that the anatase to rutile transformation occurred at a temperature between 700 °C and 800 °C.

The properties of anatase and rutile such as crystalline form, gibbs free energy, and density are the same or nearly the same. However, the structure between rutile and anatase are different thus makes them differ slightly in crystal habit. The band gap energy of anatase is 3.2 eV, which corresponds to UV light (380 nm), while the band gap energy of rutile is 3.0 eV corresponding to violet light (413 nm). The difference in band gap comes from the level of conduction band edge of anatase which is higher than that of rutile by about 0.2 eV. The VB energies for anatase and rutile are similar and both of them can generate VB hole and sequentially the •OH. On the other hand, the CB energy for rutile is closely than anatase to the potential required to reduce water to hydrogen gas. Therefore, the photogenerated CB electrons and VB holes of rutile can easily recombine with each other before they can do anything useful unlike in the case of anatase. Typically, the TiO₂ can be used in two forms: suspension or immobilized. The anatase type of TiO₂ generally shows a higher photoactivity than another type of TiO₂ by comparison of physical properties as shown in Table 2.1.



Figure 2.2 Crystallize form of TiO₂ (Smyth, 2009).

Properties	Rutile	Anatase
Crystalline form	Tetragonal system	Tetragonal system
Band gap energy (eV)	3.0	3.2
Gibb free energy (kcal/mole)	-212.6	-211.4
Melting point (°C)	1858	Change to rutile at high temperature (~800)
Hardness (Mohs)	6.0-7.0	5.5-6.0
Permittivity	114	31
Density (g/cm ³)	4.250	3.894
Lattice constant a (Å)	4.58	3.78
Lattice constant c (Å)	2.95	9.49

Table 2.1 Comparison between the comparison b	een rutile and anatase.
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2.1.3.4 Photocatalysis of Doped Titanium Dioxide

Recently, TiO₂ has been utilized as a photocatalyst for environmental remediation such as air-purification, deodorizing, sterilization, self-cleaning and water treatment. However, it is facing with two major limits in real practice. Firstly, TiO₂ requires UV of the wavelength (λ) less than 380 nm, whose energy exceeds the band gap of 3.2 eV of the anatase crystalline phase; hence, utilizing only a very small fraction of sunlight, which is only 3% of UV portion. Secondly, TiO₂ has a high

recombination rate of electron-hole pairs because it has wide band gap energy. The mechanism of TiO_2 photocatalysis mainly depends on the semiconductor interfacial redox reactions of electrons and holes. The efficiency of TiO_2 photocatalysis is low for its application because the photogenerated electron-hole pairs recombine rapidly after excitation leading to low charge carrier transfer rate on semiconductor surface.

Recently, most of the research is focused on improving the TiO_2 properties. It is generally recognized that the improved photocatalysts should allow the use of the main part of solar spectrum or even the illumination of interior lighting. Therefore, the major aim in the development of TiO_2 -based materials is to extend the photoactivity from 3.2 eV into visible light range in order to utilize solar light more efficiently (Yang et al., 2008). Efforts have been made using chemical or physical methods, to enhance the photocatalytic activity of TiO_2 through modification of crystal structure, crystal size and surface area with different group of elements such as transition metal ions (Hathway et al., 2009; Saepurahman, Abdullah and Chong, 2010), non-metallic atoms (Todorova et al., 2008) and noble metals (Zhang X., Zhang F. and Chan, 2006).

2.1.3.5 Synthesis Titanium Dioxide Process

2.1.3.5.1 Sol-Gel Process

Sol-gel process is a flexible solution process for making ceramic and glass materials. In general, the sol-gel process involves the transition of a system from a liquid "sol" (mostly colloidal) into a solid "gel" phase. Applying the sol-gel process, it is possible to fabricate ceramic or glass materials in a wide variety of forms: ultrafine or spherical shaped powders, thin film coatings, ceramic fibers, microporous inorganic membranes, monolithic ceramics and glasses, or extremely porous aerogel materials. Among the available techniques, for instance co-precipitation, vapor deposition, etc., the sol-gel process is undoubtedly the simple (Chao et al., 2003) and the cheap one (Sonawane, Kale and Dongare, 2004).

The sol-gel processing for TiO_2 synthesis refers to the hydrolysis and condensation of alkoxide-based precursors such as tetra(n-butoxyl) titanium ($Ti(O-Bu)_4$). The reactions involved in the sol-gel chemistry started form the hydrolysis, water and alcohol condensation reaction of metal alkoxides as shown in

Equations (2.5) to (2.7), lead to the formation of new phase (sol-gel) can be described as follows:

$$Ti-O-R + H_2O \longrightarrow Ti-OH + R-OH (hydrolysis)$$
 (2.5)

$$Ti-O-H + HO-Ti \longrightarrow Ti-O-Ti + H_2O$$
 (water condensation) (2.6)

Ti-O-R + OH-Ti \longrightarrow Ti-O-Ti + R-OH (alcohol condensation) (2.7)

Sol-gel method of synthesizing nanomaterials is very popular amongst chemists and is widely employed to prepare oxide materials and can be characterized by a series of distinct steps as follows:

-Step 1: Formation of different stable solutions of the metal alkoxide or solvated metal precursor (the sol).

-Step 2: Gelation resulting from the formation of an oxide- or alcoholbridged network (the gel) by a polycondensation or polyesterification reaction that results in a dramatic increase in the viscosity of the solution.

-Step 3: Aging of the gel (Syneresis), during which the polycondensation reactions continue until the gel transforms into a solid mass, accompanied by contraction of the gel network and expulsion of solvent from gel pores. Phase transformations may occur concurrently with syneresis. The aging process of gels can exceed 7 days and is critical to the prevention of cracks in gels that have been cast.

-Step 4: Drying of the gel, when water and other volatile liquids are removed from the gel network. This process is complicated due to fundamental changes in the structure of the gel. The drying process has itself been broken into four distinct steps: (i) the constant rate period; (ii) the critical point; (iii) the falling rate period; and (iv) the second falling rate period. If isolated by thermal evaporation, the resulting monolith is termed a xerogel. If the solvent (such as water) is extracted under supercritical or near super critical conditions, the product is an aerogel.

-Step 5: Dehydration, during which surface-bound R-OH groups are removed, there by stabilizing the gel against rehydration. This is normally achieved by calcining the monolith at temperatures up to 800°C.

-Step 6: Densification and decomposition of the gels at high temperatures (T>800°C). The pores of the gel network are collapsed, and remaining organic species are volatilized.

The typical steps that are involved in sol-gel processing are shown in the schematic diagram below (Figure 2.3). Navarrete et al. (1996) investigated on the effect of preparation conditions on sol-gel mix and found to be the determining factor in the textural properties of the solids. The hydrolysis catalyst used was an important factor on the specific surface area, acidity and basicity as well as activity. In the gelation and age of gel step, the reactions were impracticably slow room temperature, often requiring several days to reach completion. For this reason, acid or base catalysts were added to the formulation. The amount and type of catalyst used played important roles in the microstructural, physical and optical properties of the final aerogel product. Acid catalysts could be any protic acid such as H₂SO₄, and HCl. Basic catalyst usually uses ammonia or more commonly ammonia and ammonium fluoride. Aerogels prepared with acid catalysts often showed more shrinkage during supercritical drying and might be less transparent than base catalyzed aerogels.



Figure 2.3 Mechanism of sol-gel process (Chemat Technology, 2010).

2.1.3.5.2 Hydrothermal Process

Hydrothermal synthesis can be defined as a method of synthesis of single crystals which depends on the solubility of minerals in hot water under high pressure. The crystal growth is performed in an apparatus called "autoclave". Possible advantages of the hydrothermal method over other types of crystal growth include the ability to create crystalline phases which are not stable at the melting point. Also, materials which have a high vapor pressure near their melting points can also be grown by the hydrothermal method. The method is also particularly suitable for the growth of large good-quality crystals while maintaining good control over their composition.

In general, hydrothermal synthesis is a prospective method to obtain nanocrystalline titanium particles, where polymorphism, particle size and crystallinity could be controlled under high pressure. Moreover, it is a low temperature technique for materials development, widely applied in industrial processes for ceramic synthesis. The hydrothermal technique requires autoclave instrumentation and relies on the extensive heating of the nanoparticles diluted over an aqueous solution or slurry. The way to modification nanoparticle size and specific active area importantly affects the desired properties of the photocatalysts by varying the surface to volume ratio, by affecting the photo excited charge transfer and by influencing the surface hydroxyl concentration. The hydrothermal procedure of titanium powder at relatively low temperature ensures finely modification the properties of the modified titanium particles by only varying the duration of the treatment without the danger of the anatase phase transformation to rutile. Thus, optimum properties like increased roughness and complexity of the photocatalyst surfaces, and amplified hydroxyl content per unit area can be combined with improved interconnection of the nanoparticles and adhesion to the substrate. Control of the above factors by fine tuning of the autoclave parameters can lead to efficient immobilized titanium photocatalysts (Kontos et al., 2005).

2.1.4 Adsorption Isotherm

Photocatalytic decomposition rate is influenced by many factors such as activity and surface area of photocatalyst, adsorption and desorption of reactants/products. In the photodegradation process of TiO_2 , the disappearance of the pollutant depends on two mechanisms, pollutants adsorb on the TiO_2 surface and

oxidation reaction by the •OH. Both mechanisms occur on the TiO_2 surface. For this reason, the adsorption of organic molecules on the TiO_2 plays an important part in the photocatalytic process. Therefore, it is important, in the first step, to determine the isotherm of adsorption.

2.1.4.1 Langmuir Adsorption Isotherm

Langmuir adsorption isotherm was developed by Irving Langmuir in 1916 to describe the dependence of the surface coverage of an adsorbed gas on the pressure of the gas above the surface at a fixed temperature. The basic idea behind the Langmuir model is the coverage of the surface by a monomolecularic layer. The Langmuir adsorption isotherm was developed by assuming:

- A fix number of accessible sites are available on the adsorbent surface, all which have the same energy.

- Adsorption is reversible. Equilibrium is reached when the rate of adsorption of molecule onto the surface is the same as the rate of desorption of molecule from the surface. The rate at which of adsorption proceeds is proportional to the driving force, which is the difference between the amount of adsorbed at a particular concentration and the amount that can be adsorbed at that concentration. At the equilibrium concentration, this difference is zero.

- Adsorption is monolayer or unilayer.

Langmuir adsorption isotherm can be written as Equation (2.8):

$$q_{e} = \frac{q_{max} bC}{bC+1}$$
(2.8)

where " q_e " represents moles of adsorbate per unit weight of adsorbent, "b" is rate constant ratio between adsorption and desorption, " q_{max} " is maximum moles of adsorbate per unit weight of adsorbent, and "C" is adsorbate aqueous concentration. This Equation is a linear line when plotted inverse q_{max} and inverse concentration rewritten as Equation (2.9):

$$\frac{1}{q_{e}} = \frac{1}{q_{max}b} \left(\frac{1}{C}\right) + \left(\frac{1}{q_{max}}\right)$$
(2.9)

2.1.4.2 Freundlich Adsorption Isotherm

The most multisite adsorption isotherm for rough surface is the Freundlich adsorption isotherm. This isotherm is used commonly to describe the adsorption characteristics of activated carbon used in water and wastewater treatment. Freundlich adsorption isotherm is defined as shown in Equation (2.10) and its linearized form is illustrated in Equation (2.11):

$$q_{\max} = K_F C^{\frac{1}{n}}$$
(2.10)

$$\log q_e = \log K_F + \frac{1}{n} \log C \tag{2.11}$$

where " K_F " and "n" are constants for a given adsorbate and adsorbent at the particular temperature.

2.1.5 Langmuir-Hinshelwood Expression

Langmuir-Hinshelwood expression is one of kinetic model that widely used to analyze the heterogeneous photocatalytic oxidation, especially in the presence of preadsorption or dark adsorption prior the irradiation (Roa et al., 2003; Vargas and Núñez, 2008; Merabet, Bouzazab and Wolbert, 2009; Tsai et al., 2009). This model was developed base on the assumption of no competition with reaction byproducts. The photocatalytic oxidation of organic pollutant over TiO_2 should comply with the following Equation (2.12):

$$r = -\frac{dC}{dt} = \frac{k_r KC}{1 + KC}$$
(2.12)

where "r" is the reaction rate for the oxidation of organic pollutant (mM.min⁻¹), " k_r " is the specific reaction rate constant for the oxidation of organic pollutant (mM.min⁻¹), "K" is the equilibrium adsorption constant of organic pollutant (mM⁻¹), and "C₀" is the initial concentration of organic pollutant (mM). This Equation is a linear line when plotted between inverse initial rate and inverse concentration as shown in Equation (2.13). Slope (1/k_rK) and interception (1/k_r) are positive.

$$\frac{1}{r} = \frac{1}{k_r} + \frac{1}{k_r K} \frac{1}{C}$$
(2.13)

The constants, k_r and K, can be obtained from the intercept and slope of the line formed when "1/r" is plotted against "1/C". The integrated form of Equation (2.12) is shown in Equation (2.14):

$$t = \frac{1}{k_{r}K} \ln\left(\frac{C}{C_{0}}\right) + \frac{1}{k_{r}}(C_{0} - C)$$
(2.14)

Plotting between " $t_{1/2}$ " and initial concentration of organic pollutant should be a linear line as in the following Equation (2.15)

$$\mathbf{t}_{1/2}^{*} = \frac{0.5C_{0}}{k_{\rm r}} + \frac{\ln 2}{k_{\rm r}K}$$
(2.15)

Where " $t_{1/2}$ " is the half-life when there is no competitive effect from intermediates.

2.1.6 Properties of 2-Chlorophenol

2-Chlorophenol or ortho-chlorophenol is a benzene that is substituted with hydroxyl group (-OH) in first position and covalently bonded chlorine atoms in second or ortho position. 2-Chlorophenol is produced by electrophilic halogenation of phenol with chlorine. It has a medicinal smell and is a slightly acidic liquid. According to the Notification of the Ministry of Industry No. 6 (1997), 2-chlorophenol is classified as a toxic hazardous waste and the industrial effluent standard for 2-chlorophenol is less than 1 mg/L. 2-Chlorophenol has been used as a biocide and disinfection and is also used as an intermediate in chemical industry. It is toxic to a wide range of organisms. 2-Chlorophenol is also used to preserve wood. It is used as an intermediate in the production of pesticides, dyestuffs and preservative. This chemical compound has an appearance as a light amber liquid at room temperature. 2-Chlorophenol is toxic to plants, fish and invertebrates. It spills have resulted in fish kills. Exposure to large quantities of 2-chlorophenol impairs algae reproduction and primary production. Biodegradation in soils is lightly to be reasonably rapid (dayweeks) and it binds moderately with soil/sediment particles, however for significant spills to land, leaching to groundwater may be possible. Bioaccumulation of 2-chlorophenol appears to be moderate. Explosive exposure to 2-chlorophenol can effect if swallowed, inhaled, or absorbed through the skin. 2-Chlorophenol may cause long-term adverse effects in the aquatic environment. It may cause eye and skin damage, respiratory tract irritation, central nervous system effects, liver and kidney gastrointestinal system damage. The molecular structure and MSDS are shown in Figure 2.4 and Table 2.2.

In wastewater, 2-chlorophenol represents an important water pollutant and has been named as the priority pollutant by the USEPA. The stability of the C-Cl bond in halo-hydrocarbons is responsible for their toxicity and persistence in the biological environment. The main entry routes of 2-chlorophenol to the aquatic environment are discharges from plants manufacturing it, or from plants, and those employ it as intermediate in the production of higher chlorinated phenols or phenoxy herbicides. Indirect sources include discharges from paper mills as a by-product of chlorine-based bleaching, and from slow microbial breakdown of herbicides during post-application period. The compound is also used as a solvent for extracting sulfur and nitrogen compounds from coal. 2-Chlorophenol is very toxic and poorly biodegradable in water. A wastewater stream containing 2-chlorophenol over 200 mg/l may not be treated effectively by direct biological methods.

There are many researches studied on the oxidation of 2-chlorophenol under photocatalytic, electrocatalytic, and Fenton's oxidation under various conditions to determine the influence of pH and the formation of oxidation intermediates and products. It has been observed that the types and distribution of intermediates was depending largely on the oxidation process and experimental conditions. Catechol and cyclopentadienic acids were reported to be the major intermediates from the degradation of 2-chlorophenol by photolysis whereas phenol, hydroquinone, benzoquinone, chlorohydroquinone, and hydroxyl hydroquinone were identified



Figure 2.4 2-Chlorophenol molecular structure.

Property	Information
	2-Chlorophenol / 2-hydroxychlorobenzene/
Name	o-Chlorophenol / 1-chloro-2-hydroxybenzene, o-
	chlorophenic acid, chlorophenolate
CAS number	95-57-8
Molecular formula	C ₆ H ₅ ClO
Molar mass	128.56 g/mol
Appearance	colorless to light brown liquid
Density	1.262 g/cm ³ , liquid
Melting point	8°C
Boiling point	173.0 - 175.0 °C
Flash point	63°C (closed cup)
Solubility in water	Slightly Soluble (20-25°C)
Vapor Density	4.4 (Air = 1)
Vapor Pressure	0.3 kPa (20°C)
Odor Threshold	1.24 ppm

under the photocatalysis. Figure 2.5 shows the photodegradation pathway of 2-chlorophenol as proposed by Ilisz et al. (2002). It starts with the addition of •OH to the aromatic moiety (1) leaded to the formation of chlorodihydroxycyclohexadienyl radical, •OH addition in the para position to 2-chlorophenol (2), followed by H-abstraction (3), leaded to chlorohydroquinone, while addition in ortho position (4), followed by chlorine-abstraction from the bezene ring (5) and yielded pyrocatechol. The chlorodihydroxycyclohexadienyl radical formed in the first step may disproportionate into 2-chlorophenol and chlorohydroquinone, accompanied by water elimination (6). Although •OH often seems to be a plausible explanation for heterogeneous photocatalytic transformations observed in the aqueous phase, the possibility of direct hole oxidation can not be excluded. Since direct electron transfer from 2-chlorophenol to a semiconductor (7) could also give a positive radical, which could be converted into an chlorodihydroxycyclohexadienyl radical after nucleophilic water addition (8), or into chlorophenoxyl radical after deprotonation (9). (In the



Figure 2.5 Simplified mechanism for the photocatalytic degradation of 2-chlorophenol (Ilisz et al., 2002)

presence of dissolved O_2 the chlorophenoxyl radical may lead to the formation of quinonic derivatives (10)). Since the hydroxylation initiated by either •OH or a surface trapped hole can lead to chlorodihydroxycyclohexadienyl, a distinction between direct hole and •OH oxidation can hardly be accomplished by using only the product distribution. Further oxidation of the aromatic intermediates leads to ring opening and aliphatic products may occur (e.g. carboxylic acids and hydroxylated carboxylic acids). Prolonged irradiation will lead to the total mineralization, producing water, carbon dioxide and hydrochloric acid as final products. It is reported that higher pH discouraged the formation of aromatic intermediates. Moreover, when compounds undergo oxidation. they produce organochlorine may other organochlorine compounds that may be more toxic than the parent compound itself. Due to its widely use, potential pollutant, and hazardous property, 2-chlorophenol was selected as the target compound for evaluating the photocatalytic activity of the synthesized TiO₂ in this study.

18

2.2 Literature Reviews

2.2.1 Photocatalysis of Doped Titanium Dioxide

Liu, Yang and Li (2006) synthesized the visible-light responsive $TiO_2-V_2O_5$ photocatalyst by using a binary sol-gel and in-situ intercalation method. The photoactivity of the prepared catalyst under UV and visible light irradiation were evaluated by decolorization of methylene blue solution. The results showed that the composite catalyst displayed a homogeneous anatase phase, and the vanadium pentoxide species was highly dispersed in the TiO₂ phase. The composite catalyst responded to visible light because of the narrowed band gap.

Huang, Sun and Liu (2007) studied about Pt/N-codoped TiO_2 nanotubes and its photocatalytic activity under visible light by photodegradation of Rhodamine B in an aqueous solution. It has been confirmed that Pt/N-codoped TiO_2 nanotubes could be excited by visible light and the recombination rate of electron-hole pairs reduced significantly. The higher visible light activity is due to the co-doping of nitrogen and platinum.

Ishibai et al. (2008) synthesized TiO_2 photocatalyst with Pt-modification which active to visible-light. The results showed that Pt on the surface of TiO_2 increased photocatalytic activity under visible light irradiation, depending on the calcination temperature. The temperature correlated with the light absorption properties of the Pt complex on TiO_2 nanoparticles. It was found that TiO_2 surface structure plays an important role in the formation of Ti-O-Pt bonds resulting in a large visible light absorbance and high photocatalytic activity under visible light irradiation.

Xu et al. (2008) studied the low-temperature preparation of F-doped TiO₂ film and its photocatalytic activity under solar light. The photocatalytic activity was evaluated by decomposing X-3B under artificial solar light. The results showed that the crystallinity of TiO₂ was improved by F-doping. Fluoride ions could prevent the grain growth, and the transformation of anatase to rutile phase was also inhibited. F-doped TiO₂ film exhibited better photocatalytic activity. The high photocatalytic activity of F-doped TiO₂ film may due to extrinsic absorption through the creation of oxygen vacancies rather than the excitation of the intrinsic absorption band of bulk TiO₂. Lin, Wu and Onn (2008) studied the degradation of 4-chlorophenol in TiO₂, WO₃, SnO₂, TiO₂/WO₃ and TiO₂/SnO₂ systems and found that TiO₂/WO₃ increased the band edge wavelength to 475 nm, gap energy decreased and the specific surfaces area reduced to 2.61 eV. Although the specific surfaces area of TiO₂/WO₃ decreased due to its larger size as compared to either TiO₂ or WO₃, the 4-chlorophenol degradation efficiency significantly increased as compared to single TiO₂ or WO₃ system at 435 nm wavelength. The TiO₂/WO₃ degradation of 4-chlorophenol at 369 nm was inhibited. For TiO₂/SnO₂, the degradation efficiency also suffered at 369 nm, and only slightly increased compared to otherwise hardly 4-chlorophenol degraded in single TiO₂ or SnO₂ system.

2.2.2 Sol-Gel and Hydrothermal Methods

Kontos et al. (2005) prepared mixed anatase-rutile phase nanocrystalline TiO₂ powders by hydrothermal modification used Degussa P-25 as a precursor. The preparation procedure took place at 200 °C for 1-10 days in an autoclave system with water as the solvent. Thus, different degrees of modification were achieved. After that, TiO₂ water modified nanocrystalline thin films were immobilized on glass substrates by applying a doctor-blade's deposition technique. Methyl orange was used in order to evaluate the photocatalytic efficiency of the modified material. The results show that the photocatalytic activity of the modified films is improved by a two factor when the hydrothermal treatment was extended from 1 to about 4 days in the autoclave system. Scratch tests revealed favorable interconnection of the titanium nanoparticles as well as significantly higher adhesion to the glass substrate for the modified films, in comparison to the original P-25 material.

Carotta et al. (2007) synthesized TiO_2 thick films and powders by two synthetic processes, traditional sol-gel and hydrothermal route. A comparison between two synthetic processes has been performed. They found that in the hydrothermal process, the TiO_2 film was maintained the anatase phase at higher calination temperature with any introduction of foreign elements than traditional solgel process. Furthermore, hydrothermal powders show particle size much smaller than sol-gel.

Tian et al. (2009) synthesized S-doped TiO_2 nanoparticles by hydrothermal process and their photocatalytic ability was studied by degradation of methyl orange. The result showed that S-doped TiO_2 photocatalysts at a nanometer scale could be

successfully synthesized at 180°C by a hydrothermal process, which could achieve the crystalline under a mind condition. The particle size and morphology, and phase/chemical compositions of the S-doped TiO₂ photocatalysts were strongly dependent on the amount of S incorporation in TiO₂. S/TiO₂ sample at 1.5% with a spherical morphology and 30 nm in diameter has the best photocatalytic activity.

2.2.3 Photocatalysis of 2-Chlorophenol and Phenolic Compounds

Shchukin et al. (2004) synthesized nanocrystalline bicomponent $TiO_2-In_2O_3$ powder and studied the photodegradation of 2-chlorophenol in water. From the results, it found that photocatalytic activity increased with decreasing In_2O_3 . The concentration of the main aromatic intermediate products (chlorohydroquinone and catechol) was considerably lower for $TiO_2-In_2O_3$ photocatalysts than pure TiO_2 . On the basis of various characterizations of the photocatalysts, the reasons invoked to explain the photocatalytic activity enhancement due to In_2O_3 included a better separation of photogenerated charge carriers, an improved oxygen reduction and an increased surface acidity inducing a higher extent of adsorption of the aromatics.

Barakat et al. (2005) studied the photocatalytic degradation of 2-chlorophenol by nanoparticles Co-doped TiO₂. The results revealed that Co-doped TiO₂ exhibited high activity for UV-photocatalytic degradation of 2-chlorophenol. The efficiency values of the 2-chlorophenol photodegradation were 93.4% and 96.4% at solution pH of 9 and 12, respectively. The presence of Co ions in the TiO₂ structure caused a significant absorption shift towards the visible region.

Araña et al. (2007) investigated the photocatalytic behavior of different phenolic compounds (catechol, resorcinol, phenol, m-cresol and o-cresol). Their adsorption and interaction types with the TiO_2 Degussa P-25 surface were also studied. Langmuir and Freundlich isotherms were applied in the adsorption studies. The obtained results indicated that catechol adsorption was much higher than those of the other phenolics and its interaction occured preferentially through the formation of a catecholate monodentate. Resorcinol and cresols interacted by means of hydrogen bonds through the hydroxyl group, and their adsorption was much lower than that of catechol. Finally, phenol showed an intermediate behavior with a Langmuir adsorption constant (K) much lower than that of catechol, but a similar interaction. The interaction of the selected molecules with the catalyst surface was evaluated by means of FTIR experiments, which allowed the determination of the probability of •OH radical attack to the aromatic ring which found to follow the sequence of resorcinol > m-cresol > o-cresol > catechol \ge phenol.


CHAPTER III

METHODOLOGY

3.1 Materials and Chemicals

3.1.1 Chemicals

-Tetra(n-butoxyl)titanium (Ti(O-Bu)₄) from Fluka was used as the titanium precursor.

-Ethanol (C_2H_5OH) from Merck was use as a solvent to prepare the TiO_2 solution.

-Sodium tungsten dihydrate (Na₂WO₄•2H₂O) from Fluka was used as the dopant for tungsten doped TiO₂ (W/TiO₂).

-Ammonium fluorine (NH₄F) from Merck was used as the dopant for fluorine doped TiO₂ (F/TiO_2).

-Tetra-amine platinum(II) nitrate $(Pt(NH_4)_4(NO_3)_2)$ from Sigma-Aldrich was used as the dopant for platinum doped TiO₂ (Pt/TiO₂).

-Nitric acid (HNO₃), sulfuric acid (H_2SO_4) and phosphoric acid (H_3PO_4) from Merck were used as the acid catalyst to control hydrolysis rate.

-Diethanolamine ((CH₂OHCH₂)₂NH) from Carlo Erba was used as the base catalyst to control hydrolysis rate.

-Commercial TiO₂ (Degussa P-25) with the BET surface area of 59.1 m^2/g and average particle diameter of 27 nm was used as a reference for photocatalytic activity comparison.

-2-chlorophenol (C_6H_5OCl) from Fluka was used as the organic probe in phototocatalytic determination.

-Perchloric acid (HClO₄) and sodium hydroxide (NaOH) were used to adjust/control the pH during the photocatalysis process.

-All other chemicals were reagent grade.

-All reagents were prepared by using the deionized water.

3.1.2 Reactor

Photocatalytic experiments were conducted in a 1-liter Pyrex beaker placed in a circulating water bath controlled at 25 °C. Magnetic stirrer bar was used to mix the solution. Two-watt light-emitting diode (LEDs), which provide the light in the visible range, i.e., either blue (450-495 nm), green (495-570 nm) or red (620-750 nm), or 4watt low-pressure mercury UV lamp was placed above the reactor to irradiate the light. pH of the solution was controlled at appropriated value throughout the experiment by pH controller connected with cartridge pump to add acid/base as necessary. A schematic diagram of the photocatalytic reactor is shown in Figure. 3.1.

3.2 Experimental Procedures

Experimental works were divided into two parts, i.e., TiO_2 synthesis and determination of the TiO_2 activity.



Figure 3.1 Schematic diagram of the photocatalytic reactor.

3.2.1 Titanium Dioxide Synthesis

3.2.1.1 Synthesis of Titanium Dioxide by Sol-Gel Process

In this part, two types of TiO₂ were synthesized by using the sol-gel process. Undoped TiO₂ was prepared according to the procedure of Lin, Tseng and Chen (2006) with some modifications. Doped TiO₂ with tungsten, fluorine and platinum were prepared similarly to the undoped TiO₂ except the dopant at desired ratio was added to the matrix before the catalyst was added. To synthesize W/TiO₂, F/TiO₂, and Pt/TiO₂, Na₂WO₄•2H₂O, NH₄F, and Pt(NH₄)₄(NO₃)₂ were used as the sources of element dopant, respectively. Diagram for TiO₂ synthesis was illustrated in Figure 3.2 and the details were described bellows:

a. Place 70 mL anhydrous ethanol in a 250 mL flask and slowly add 0.05 mole of tetra(n-butoxyl)titanium under the vigorous stirring condition to prepare a clear tetra(n-butoxyl)titanium ethanol solution (Solution I). The flask was then placed in water bath to control the temperature at 4°C for the desired time.

b. At the same time, 20 mL of deionized water was added into 20 mL of anhydrous ethanol alcohol to make the ethanol aqueous solution. In the case of doped TiO₂, the doping compound at the desired mole ratio was added into the ethanol aqueous solution. The mixture was continuously stirred until the doping element was completely dissolved (Solution II).

c. Solution II was dropwise added into Solution I and the precipitates were immediately formed.

d. After 1 hour of continuous stirring, 4 mL of the acid or base catalyst was added into the solution. The mixed liquor was thoroughly mixed to undergo hydrolytic condensation for 3 hours.

e. Hydrolyzed solution was then placed into the oven to dry at 120°C for 2 hours to obtained Ti(OH)₄ and then pulverized into powder form.

f. Finally, $Ti(OH)_4$ powder was calcined at the desired temperature for 10 hours to obtain TiO_2 .

3.2.1.2 Synthesis of Titanium Dioxide with Hydrothermal Treatment This part aimed to study the effect of hydrothermal on the synthetic TiO₂ property. Optimum criteria obtained from previous part were used in this



Figure 3.2 Schematic for TiO₂ synthesis by sol-gel method.

hydrothermal section; however, after the hydrolytic condensation for 3 hours, the hydrolyzed solution was sealed and then autoclaved at 121° C and 103.4 kPa for selected time before placing into the oven to dry at 120° C. Overall procedure of TiO₂ synthesis by hydrothermal treatment is illustrated in the Figure 3.3.

3.2.2 Determination of the Titanium Dioxide Activity

Photocatalytic experiments were conducted in a 1-liter Pyrex beaker. At first, the 2-chlorophenol solution with TiO_2 was magnetically stirred in the dark until reaching an adsorption/desorption equilibrium. After that, the irradiation began to initiate the photocatalytic experiment. The disappearance of the 2-chlorophenol, which represented the activity of synthetic TiO_2 , was monitored. At a predetermined time, the sample was taken, filtered through a Millipore filter (0.22 µm pores) and analyzed by the UV-VIS spectrophotometer at 510 nm for residual 2-chlorophenol,



Figure 3.3 Schematic for TiO₂ synthesis by hydrothermal method.

according to the 4-amino-antipyrine colorimetric method (APHA, 1992). Sampling times were 0, 30, 60, 90, 120, 180, 240, 300 and 360 minutes. Solution pH was controlled throughout the experiment. Diagram for the photocatalytic activity test is described in Figure. 3.4.

3.3 Experimental Scenarios

3.3.1 Modification of Titanium Dioxide Synthesis

3.3.1.1 Sol-Gel Process

Key parameters in the sol-gel process which believed to affect the TiO_2 property were investigated including calcination temperature (150, 200, 300, 400, and



Figure 3.4 Experiment schematic for photocatalytic activity investigation

500°C) and ramp rate (1, 4, and 9°C/min), and sol catalyst type (HNO₃, H₂SO₄, H₃PO₄, and diethanolanime (DEA)). Synthetic TiO₂ under various conditions were tested for their photocatalytic activity using 2-chlorophenol as the target pollutant. Experimental conditions for each scenario are shown in Tables 3.1 to 3.3.

3.3.1.2 Element Doping

In this section, the TiO_2 was synthesized following the optimum conditions obtained from previous part; however, the target dopant (either tungsten, fluorine or platinum) was added to determine the improvement in photocatalytic property.

3.3.1.3 Hydrothermal Treatment

 TiO_2 was pretreated by hydrothermal process to further enhance the photocatalytic property. The gel prepared according to the optimum conditions obtained from previous parts was autoclaved for either 2, 3, 4 or 6 hours and the

Ramp rate (°C/min)	Catalyst type	Calcination Temp. (°C)		
1		150		
		200		
	HNO ₃	300		
		Calcination Temp. (°C) 150 200 300 400 500		
		500		

Table 3.1 Conditions for the study of calcinations temperature effect.

Table 3.2 Conditions for the study of ramp rate effect.

Ramp rate (°C/min)	Catalyst type	Calcination Temp. (°C)
1		
4	HNO ₃	Optimum from Table 3.1
9	h Tan	

Table 3.3 Conditions for the study of sol catalyst effect.

Ramp rate (°C/min)	Catalyst type	Calcination Temp. (°C)
0	HNO ₃	
Optimum from Table	H_2SO_4	Optimum from Table 3.1
3.12	H ₃ PO ₄	Optimum nom rable 5.1
	DEA	6

obtained TiO_2 were tested for their photocatalytic activity using 2-chlorophenol as the target compound.

3.3.2 Adsorption Study

It is important to determine the adsorption behavior of the synthetic TiO_2 which principally affects its photocatalytic activity. Table 3.4 shows the conditions used to determine the adsorption isotherm of the synthetic TiO_2 .

3.3.3 Photocatalytic Activity Investigation

Photocatalytic activity of the synthetic TiO_2 was investigated under several conditions. The effects of TiO_2 dose, light wavelength, light intensity and pH on 2-

chlorophenol degradation were investigated. Moreover, photocatalytic kinetics of 2chlorophenol was also determined. The experimental scenarios are shown in Tables 3.5 to 3.9.

Table 3.4 Conditions for characterizing the 2-chlorophenol adsorption onto TiO₂ surface.

TiO ₂ dose (g/L)	pH	Temp. (°C)	2-chlorophenol (mM)
4			0.005
			0.01
	1 5		0.03
1		25	0.05
			0.1
			0.2
			0.5
			1.3

 Table 3.5 Conditions for characterizing the P-25 catalytic activity under blue and UV light irradiation.

2-chlorophenol (mM)	TiO ₂ dose (g/L)	рН	Temp. (°C)	Light source
0.01	1	5	25	UV
	-		20	Blue light

Table 3.6 Conditions for determining the effect of TiO_2 dose under blue light irradiation.

	2-chlorophenol (mM)	Temp. (°C)	TiO ₂ dose (g/L)
		6	0.25
0.01	0.01	9 192	0.5
	25		
1			1.5

2-chlorophenol (mM)	Temp. (°C)	Light color	TiO ₂ dose (g/L)	рН
		1000	Ontimum	5
0.01	25	Blue light	from Table 3.3	6
				7
				8

Table 3.7 Conditions for determining the effect of pH on TiO_2 photocatalytic activity.

Table 3.8 Conditions for determining the effect of light wavelength on TiO₂ photocatalytic activity.

2-chlorophenol (mM)	Temp. (°C)	TiO ₂ dose (g/L)	рН	Light color	
		Optimum from	Optimum	Blue light	
0.01	25	25 Table 3.3	25 Table 3.3 from Table	from Table	Green light
			3.4	Red light	

Table 3.9 Conditions for determining the effect of 2-chlorophenol on TiO₂ photocatalytic activity.

Temp. (°C)	TiO ₂ dose (g/L)	рН	Light color	Light intensity (lamp)	2-chlorophenol (mM)
25	Optimum from Table 3.3	Optimum from Table 3.4	Blue light	ู่ เป็า	0.005 0.01 0.03 0.05

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3.4 Analytical Methods

3.4.1 Identification of Crystalline Structure

Crystal structure of the synthetic TiO₂ was characterized by the X-ray diffraction spectroscopy (XRD) (D8 Discovery, Bruker-AXS) with Cu K α radiation ($\lambda = 0.15406$ nm) in a 2 θ range of 20-80° and a scanning speed of 3°/min.

3.4.2 Identification of Morphology

Surface morphology of the synthetic TiO₂ was characterized by the scanning electron microscopy (SEM) (JEOL, JSM-5410LV).

3.4.3 UV-VIS Absorption Spectra Analysis

Absorption property of the synthetic TiO_2 was evaluated by using a diffuse reflectance scanning spectrophotometer (Perkin Elmer Lambda 35 Spectrophotometer) with the scanning range between 200 and 800 nm.

3.4.4 Point of Zero Charge (pzc) Analysis

Point of zero charge of synthetic TiO_2 was analyzed by using the dynamic light scattering (Malvern ZS90).

3.4.5 Surface Area Analysis

Surface area of synthetic TiO_2 was obtained from nitrogen adsorption isotherm by the Brunauer-Emmett-Teller (BET) method following the ASTM standard.

3.4.6 Laser Particle Size Distribution Analysis

Particle size distribution of synthetic TiO2 was analysed by using laser particle size distribution Analyzer model Mastersizer-S.

3.4.7 Elemental Concentration

X-ray fluorescence (XRF) analysis was used to determine the elemental concentration.

3.4.8 Measurement of 2-Chlorophenol

4-aminoantipyrine colorimetric method (APHA, 1992) was used to analyze residual concentration of 2-chlorophenol. One mL of buffer solution, 1 mL of 4amino-antipyrine solution, and 1 mL of potassium ferric cyanide solution were added into the sample and mixed together to produce a color reaction product. The color intensity representing the 2-chlorophenol concentration was measured by a UV-VIS spectrophotometer at 510 nm.



CHAPTER IV

RESULTS AND DISCUSSION

4.1 Titanium Dioxide Synthesis

4.1.1 Optimizing Sol-Gel Conditions

4.1.1.1 Effect of Calcination Temperature

This experimental part aimed to study effect of calcination temperature on TiO₂ photocatalytic property. Titanium gel was calcined at 150, 200, 300, 400 and 500°C for 10 hours. Figure 4.1 shows the X-ray diffraction (XRD) patterns of the TiO₂ obtained from different calcination temperatures as compared to the commercial TiO₂ (Degussa P-25). The diffraction angles (20) of 25.28 and 27.43 represent the crystal plane of anatase (1 0 1) and rutile (1 1 0). Crystal size can be determined from the Scherrer formula as shown in Equation (4.1):

$$D = \frac{K\lambda}{\beta\cos\theta}$$
(4.1)

where λ is the wavelength characteristic of the Cu K α radiation ($\lambda = 0.154$ nm), β is the full width at half maximum of which unit is in radians and θ is the reflecting angle. The full widths at half-maximum of the anatase, brookite, and rutile peaks could be obtained from the XRD pattern; it can be seen from Figure 4.1 that the samples calcined at 200 and 300°C contained only anatase and the crystal sizes were calculated to be 4.029 and 4.284 nm, respectively. As calcination temperature reached to 400°C, a large peak at 2 θ of 27.43° and a small peak at 2 θ of 25.28° were observed, indicating that the major crystallize phase had transformed from anatase to rutile and the crystal size has been increased to 11.302 nm. At 500°C, the peak at 2 θ of 27.43° became predominate; however, greatly reduced at 2 θ of 25.28°, suggesting that most of the crystalline had transformed to rutile and the corresponding crystal size has increased to 18.083 nm. Table 4.1 summarizes the crystal sizes of the TiO₂ obtained from this study under various calcination temperatures.



Figure 4.1 XRD patterns of sol-gel synthetic TiO₂ without doping calcined at various temperatures (A and R represents the crystal plane of anatase and rutile, respectively).

 Table 4.1 Effect of calcinations temperature on the crystallize size and weight fraction of anatase and rutile phases.

Calcination temp.	Crystallize size	% Anatase	% Rutile
(*C)	(nm)		
200	4.029	100.00	0
300	4.284	100.00	0
400	11.302	29.09	70.91
500	18.083	93.23	6.77

To quantify the effect of calcination temperature on the phase transformation of the TiO_2 , the portions of anatase and rutile were calculated from Equations (4.2), (4.3) and (4.4) by using the integrated intensities of the anatase (1 0 1), rutile (1 1 0), and brookite (1 2 1) peaks obtained from the XRD pattern (Figure 4.1):

$$W_{A} = \frac{K_{A} A_{A}}{K_{A} A_{A}^{+} A_{R}^{+} K_{B} A_{B}}$$
(4.2)

$$W_{R} = \frac{A_{R}}{K_{A}A_{A} + A_{R} + K_{B}A_{B}}$$
(4.3)

$$W_{B} = \frac{K_{B} A_{B}}{K_{A} A_{A}^{+} A_{R}^{+} K_{B} A_{B}}$$
(4.4)

where W_A , W_R , and W_B represent the weight fractions of the anatase, rutile, and brookite phases, respectively. A_A , A_R , and A_B are the integrated intensities of the anatase, rutile and brookite peaks, respectively. The variables K_A and K_B are coefficients with values 0.886 and 2.721, respectively. The summary results were also shown in Table 4.1 which is in agreement with previous discussion.

Furthermore, it was found that the synthetic method and calcined temperature also affected the light absorption ability of the TiO₂. All synthetic TiO₂ obtained in this study could absorb visible light much better than the Degussa P-25 as shown in Figure 4.2 although the Degussa P-25 absorbed better within the UV range. The visible-light absorptivity was the highest at 400 nm (violet light) and declined substantially as the wavelength increased to 800 nm. Visible light absorption ability improved as the calcined temperature increased from 150 to 200°C; however, decreased simultaneously afterward. The presence of carbonaceous species might cause the prepared TiO₂ photocatalyst to be able to respond to the visible light. These carbonaceous species are normally burnt out by the calcination at elevated temperature in typical synthetic procedures as reported by Lettmann et al. (2001) and Lin et al. (2006).

Band gap energy of the TiO₂ can be estimated from the plot of square root of Kubelka Munk function (F(R)) versus photon energy (Asahi et al., 2001). The relation of $(\alpha h\nu)^{r}$ and hv was plotted. The band gap energy of TiO₂ can be determined from the Equation (4.5).

$$\alpha h \nu = A (h \nu - E_g)^r \tag{4.5}$$

where A is a constant, hv is the photon energy, E_g represents the band gap energy of material and r is the characteristic of the type of the transition process which is 0.5 for a direct-allowed optical transition and 2.0 for an indirect-allowed optical transition (non direct in case of an amorphous semiconductor). Results are summarized in Table 4.2 which shows that the band gap energies of all synthetic TiO₂ are lower than



Figure 4.2 UV-VIS absorption spectrograph of sol-gel synthetic undoped TiO₂ calcined at various temperatures.

Calcination temperature (°C)	Band gap energy (eV)
150	1.80
200	1.20
300	1.50
400	2.80
500	2.79

Table 4.2 Band gap energy of the TiO₂ calcined at various temperatures.

Degussa P-25 which is 3.2 eV. The band gap energy was decreased from 3.2 eV to 1.80 and 1.20 eV for the TiO₂ calcined at 150 and 200°C, respectively. Nonetheless, the band gap increased again as the calcination temperature increased further. At 300°C, the band gap energy is 1.50 eV and significantly increased to 2.80 and 2.79 eV at 400 and 500 °C, respectively. This narrower band gap should better facilitate the excitation of an electron to jump from the valance band to conduction band which can result in higher photocatalytic activities. Oxidation of 2-chlorophenol also supported this band gap reduction. The TiO₂ calcined at 200°C had a higher photocatalytic activity under the blue light irradiation than those calcined at 300°C, i.e., 91.8% of 0.01 mM 2-chlorophenol was removed in 6 hours by the TiO₂ calcined at 200°C



Figure 4.3 Photodegradation of 0.01 mM 2-chlophenol at calcine temperature 200°C and 300°C under blue light irradiation (1g/L TiO₂, pH at 5 and 25°C).

compared to 48.1% of those calcined at 300°C as shown in Figure 4.3. Generally, the Degussa P-25 does not have any significant activity under the visible light irradiation. This implies that the crystal structure formation does not seriously affect the activity of TiO_2 under visible light region as in the case of UV range where anatase has higher absorptivity than rutile and brookite, respectively. According to Figure 4.1, little anatase was formed at the calcinations temperature of 200°C with no other crystal form existed; however, the photocatalytic activity was still exceptional regardless on crystal formation. As a result, the calcination temperature of 200°C was the optimum value for this synthetic method.

4.1.1.2 Effect of Ramp Rate

In this part, all TiO₂ gels were calcined at 300°C but with different ramp rates from 1 to 4 and 9°C/min. Figure 4.4 shows the XRD pattern of synthetic TiO₂ obtained from various ramp rates. At the ramp rate of 1 °C/min, the crystal phase was totally anatase whereas some rutile phase, which has lower UV-VIS photocatalytic activity than anatase, occurred when the ramp rate was increased to 4 and 9°C/min, respectively. It is interesting to observe that the intensity of the main characteristic peak of anatase phase did not change in all samples which indicating that the formation of rutile crystal phase did not from anatase transformation. It is expected



Figure 4.4 XRD pattern of undoped TiO₂ calcined at various ramp rates (A and R represents the crystal plane of anatase and rutile, respectively).



Figure 4.5 Photodegradation of 0.01 mM 2-chlophenol of the TiO₂ at various ramp rate under blue light irradiation (1g/L TiO₂, pH at 5 and 25°C).

that some amorphous TiO_2 were transformed to rutile as a result from high heating rate. Thus, the ramp rate could affect the growth behavior and phase structure of crystal phase similar to the results from Durán et al. (2001), Lei et al. (2009) and Meng et al. (2010). The formation of rutile phase was somehow weakening the photocatalytic activity of the TiO_2 as represented by the removal efficiency of 0.01 mM 2-chlorophenol, i.e., the TiO_2 calcined at 1° C/min had the highest efficiency of 48.1 as compared to 32.2 and 29.8% of those calcined at 4 and 9° C/min, respectively (Figure 4.5). Thus, the optimum ramp rate for this synthetic method was 1 °C/min.

4.1.1.3 Effect of Dissolution Temperature

This part aimed to study the effect of temperature during the dissolution stage on the photocatalytic activity of the synthetic TiO_2 . The dissolution stage included the mixing step of tetra(n-butoxyl) titanium ethanol solution (Solution I) with ethanol aqueous solution (Solution II) and the curing step before the catalyst was added. Several scenarios were performed including no control (no temperature control during the whole dissolution stage), only mixing step (control temperature at 4°C during the mixing of Solution I and Solution II), 30 minutes (control temperature at 4°C during the mixing step and 30 minutes during the curing step), and 1 hour (control temperature at 4°C during the mixing step and the whole 1-hr curing step). The obtained sol was further processed to generate TiO₂ following the optimum conditions obtained from previous sections, i.e., calcination temperature of 200 °C and ramp rate at 1 °C/min. From Figure 4.6, the TiO₂ prepared by controlling at 4°C for 30 minutes during the dissolution steps provided the best adsorption spectrum in both UV and visible light regions whereas the other conditions yielded the similar light-adsorption property. Nonetheless, when considering on the photocatalytic activity, it was found that the synthetic TiO₂ prepared by controlling at 4°C for 30 minutes and 1 hour had comparable activities, i.e., 91.8 and 90.4% of the 0.01 mM 2-chlorophenol could be removed in 6 hours, respectively, whereas the TiO₂ from other conditions had lower activity with 87.4 and 71.8% removal efficiency of mix step and no control, respectively, as revealed in Figure 4.7. These results suggested that the tetra(n-butoxyl)titanium is very sensitive to the moisture and the water vapor in the atmosphere; hence, maintaining the tetra(n-butoxyl)titanium during the dissolution stage at low temperature could significantly reduce the reaction with water vapor. By controlling the temperature at 4°C, a clear solution of TiO₂ precursor in ethanol could be achieved. If the temperature was not controlled at 4°C during the dissolution stage, the reaction between tetra(n-butoxyl)titanium and water vapor



Figure 4.6 UV-VIS absorption spectrograph of sol-gel synthetic undoped TiO₂ at temperature control in dissolution stage.



Figure 4.7 Photodegradation of 0.01 mM 2-chlophenol at various temperature and duration time control in dissolution stage under blue light irradiation (1g/L TiO₂, pH at 5 and 25°C).

would occur and white solids would precipitate out and caused failure to the synthesis. Moreover, the low temperature control during dissolution stage could slow down the hydrolysis and polymerization rates resulting in the formation of smaller particles with more uniformity. As a result from this part, it is necessary to control temperature during the dissolution stage for 30 minutes after the Solution I was completely mixed with Solution II. In conclusion, the optimum conditions for synthesizing the TiO_2 by sol-gel process were dissolution at 4°C for 30 minutes after Solution I and Solution II were completely mixed together, calcinations at 200°C with the ramp rate of 1°C/min.

4.1.2 Enhancement of Visible-Light Photocatalysis by Doping

4.1.2.1 Effect of Doping Element

In this part, the TiO₂ was synthesized by doping with several elements including tungsten (W/TiO₂), fluorine (F/TiO₂), and platinum (Pt/TiO₂) at different mole ratios to enhance their visible-light responses. The optimal conditions from previous section were used. The studied mole ratios of each dopant to Ti are shown in Table 4.3. It is important to note that in the case of Pt/TiO₂, only one mole ratio was investigated since the preliminary result showed that the very expensive platinum was not as effective as other elements in promoting the visible-light absorptivity of the TiO₂ as will be discussed later. The UV-VIS absorption spectra of W/TiO₂, F/TiO₂ and Pt/TiO₂ obtained in this study are shown in Figures 4.8, 4.9 and 4.10, respectively. From Figure 4.8, it was found that tungsten doping enhance the visible light absorptivity of the synthetic TiO₂ though no significant impact in the UV range.

Dopant	Mole ratio of dopant to Ti (%)
6910191019	0.1%W/TiO ₂
Tungsten	0.5% W/TiO ₂
	1%W/TiO ₂
900.056010	0.5%F/TiO ₂
Fluorine	1%F/TiO ₂
9	2%F/TiO ₂
Platinum	1%Pt/TiO ₂

Table 4.3 Mole ratio of dopant to titanium



Figure 4.8 Absorption spectrographs of the TiO₂ doped with tungsten under the optimum sol-gel conditions.



Figure 4.9 Absorption spectrographs of the TiO₂ doped with fluorine under the optimum sol-gel conditions.

The absorption enhancement increased as the W:Ti ratio increased from 0.1 to 0.5%; however, decreased sharply as the ratio increased to 1.0%; thus, the optimum W:Ti ratio was 0.5%. For fluorine doping, the visible light absorptivity increased as the

mole ratio of F:Ti increased from 0.5% to 1%. Nonetheless, the absorbance of visible light of the 2%F/TiO₂ was found to be lower than 1%F/TiO₂. The effect of F:Ti mole ratio was not obvious in the UV range. Therefore, the optimum F:Ti ratio was 1%. Moreover, Figure 4.10 shows the absorptivity of 1%Pt/TiO₂ indicating that 1%Pt/TiO₂ had lower absorbance in UV region but had a higher absorbance in visible light than the P-25. As a result, it can be concluded that all three elements being tested could enhance the absorptivity of the TiO₂ in the visible-light region. Nonetheless, when considering on the effect of element type, it was found that the 0.5% W/TiO₂ was the best followed by 1%TiO₂/F, undoped TiO₂, 1%Pt/TiO₂ and P-25, respectively, as shown in Table 4.4. It was found that all dopants impacted the absorptivity property of the TiO₂ and could reduce the band gap energy to be lower than the Degussa P-25 of 3.2 eV. The 0.5% W/TiO₂ had the lowest band gap energy of 1.12 eV causing it to be the easiest catalyst to be activated by visible light.







Figure 4.11 Absorption spectrographs of 0.5% W/TiO₂, 1%F/TiO₂ and 0.5% Pt/TiO₂ compare to undoped TiO₂ and Degussa P-25.

Doned TiO	Band gap energy		
Doped 1102	(eV)		
0.1%W/TiO ₂	1.20		
0.5% W/TiO ₂	1.12		
1%W/TiO ₂	2.85		
0.5%F/TiO ₂	2.80		
1%F/TiO ₂	1.13		
2% F/TiO ₂	1.15		
0.5%Pt/TiO ₂	1.70		

Table 4.4 Band gap	energy o	of the	doped	TiO ₂
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Figure 4.12(a) reveals the results from XRD analysis. It was found that the 0.5% W/TiO₂ apparently had lower the crystal formation than undoped TiO₂ and P-25, chronologically, i.e., much lower anatase peak was detected in the doped sample compared to undoped TiO₂ and P-25. In addition, the reflection peak at 20 of 25.28 which representing the anatase slightly has shifted to a higher angle of 25.40 in the case of undoped TiO₂ and 0.5% W/TiO₂ as shown in Figure 4.12(b). The reflection



Figure 4.12 XRD pattern of the 0.5% W/TiO₂ (a) 0.5% W/TiO₂ compared with undoped TiO₂ and Degussa P-25; (b) an enlargement of (a) at 2θ of 25.28 (A and R represents the crystal plane of anatase and rutile, respectively).

peak corresponds to the interlayer spacing of titanium. Thus, the peak shift means a decrease of interlayer spacing. According to Scherrer formula as shown in Equation (4.1), the crystal size was found to be 2.993 nm for 0.5% W/TiO₂. It implied that

tungsten and the sol-gel conditions used in this study retarding the phase transformation and crystal grain growth.

Photocatalytic activity of various TiO₂ synthesized in this study were investigated under the blue light irradiation and the results were illustrated in Figure 4.13. The performance in 2-chlorophenol removal could be arrayed in order of undoped TiO₂ $\approx 0.5\%$ W/TiO₂ > 1%F/TiO₂ > 1%Pt/TiO₂ > Degussa P-25 with the efficiencies of 91.8, 90.5, 51.9, 35.3 and 23.2%, respectively. The high photocatalytic activity of undoped TiO₂ probably because of the existence of carbonaceous species that act as sensitizers as suggested by Lin et al., (2006). However among synthetic TiO₂ the band gap energy of 0.5% W/TiO₂ of 1.12 eV is the lowest. Additionally, the intense absorption and red shift in the visible light range of 0.5% W/TiO₂ (Figure 4.11) implied that more electron hole pairs could be photo- generated under visiblelight irradiation. Moreover, from the XRD pattern, it was found that despite low crystalline phases were formed, the 0.5% W/TiO₂ but much better than the more crystalline formed P-25. This implies that the photoactivity under



Figure 4.13 Photodegradation of 0.01 mM 2-chlophenol at various doped TiO_2 compare to undoped TiO_2 and Degussa P-25 under blue light irradiation (1g/L TiO_2 , pH at 5 and 25°C).

visible light irradiation of the TiO_2 does not depend on crystallinity, i.e., the 0.5%W/TiO₂ with low reflection peak of anatase could effectively serve as the photocatalyst under the visible light irradiation. The lowest photocatalytic activity of the Degussa P-25 also corresponded to its lowest visible light absorption ability as shown in Figure 4.11.

4.1.2.2 Effect of Sol Catalyst on 0.5% W/TiO2

In this part, the optimum 0.5% W/TiO₂ was selected as a medium to study the effect of catalyst type being used during the sol preparation step. From literature reviews, it was found that good catalytic property under UV irradation is governed by two major opposing physical properties, i.e., crystallinity and surface area of the photocatalysts. High crystallinity helps to prolong the recombination rate; hence, strongly increases the activity of the photocatalyst. High surface area helps to facilitate adsorption of the target molecules onto the surface of the catalyst (Kanna and Wongnawa, 2008). From these reasons, 2 types of catalyst using during the sol preparation were tested, i.e., the acid group including HNO₃, H₂SO₄, and H₃PO₄, and the base group in which the diethanolanime (DEA) was used. Figure 4.14 is the adsorption spectrograph of the 0.5% W/TiO₂ powders prepared under DEA and various acid catalysts. The result shows that the acid catalyst type had no effect on the absorptivity in the UV region ($\lambda < 400$ nm) but had a strong effect to the adsorption in visible region. Among acid catalysts, phosphoric acid was the worst whereas HNO₃ and H₂SO₄ had a mixed impact. For the wavelength greater than 550 nm, the H₂SO₄catalyzed TiO₂ possessed a better absorptivity whereas the HNO₃-catalyzed TiO₂ was better as the wavelength below 550 nm. On the other hand, the basic DEA showed the lowest absorptivity both in the UV and visible light region. Normally, DEA is used as an inhibitor for the precipitation of oxides and a stabilizing agent on the hydrolysis of the metal alkoxides. Thus, the sol was stable for a long period before it transformed into a gel; hence, aging time should be extended. This application of base catalyst is generally suitable for the preparation of the immobilized TiO₂ but not in this study. The XRD analysis for different acid catalyst types is shown in Figure 4.15 indicating that only the HNO_3 -catalyzed TiO_2 had a clear crystal structure (anatase) whereas the H₃PO₄ and H₂SO₄ could not detect any crystal structure since their spectra became broaden. It could be concluded that acid catalyst played an important role during the formation of TiO₂ crystal. Additionally, the photodegradation of 0.05 mM of



Figure 4.14 Absorption spectrographs of 0.5%W/TiO₂ with different catalyst prepared under optimum conditions.



Figure 4.15 Effect of acid catalyst on XRD patterns of the 0.5%W/TiO₂ prepared under the optimum sol-gel conditions (A and R represents the crystal plane of anatase and rutile, respectively).

2-chlorophenol showed that the HNO_3 -catalyst TiO_2 had the highest efficiency while H_3PO_4 - and H_2SO_4 -catalyst TiO_2 were not significantly different as shown in Figure 4.16. Thus, the optimum sol catalyst for this condition was HNO_3 .

4.1.2.3 Effect of Hydrothermal Treatment

In this part, hydrothermal treatment was applied by autoclaving the hydrolized mixture before dehydration and calcination to modifies TiO_2 structure rather than sol-gel process only. The sol-gel method is most widely used due to its possible capability in controlling the textural and surface properties of composite oxides. But the calcination process frequently lead to serious particle agglomeration, grain growth, small surface area and phase transformation from anatase to rutile, which all decrease the photocatalytic activity of titanium. The hydrothermal processing represents an alternative to high-temperature calcination for crystallization of titanium hydroxide under mild temperatures. It has been widely applied in the synthesis of zeolites and in the production of advanced ceramic powders with ultrafine particle size. In the hydrothermal treatment, grain size, particle morphology, crystalline phase, and surface chemistry can be controlled via processing variables such as hydrothermal temperature, pressure and time. In this research, the autoclaving



Figure 4.16 Photodegradation of 0.05 mM 2-chlophenol by 0.5%W/TiO₂ with different acid catalysts under blue light irradiation (1 g/L TiO₂, pH 5 and 25°C).

time was varied between 2 and 6 hours. It was found that the hydrothermal treatment could significantly intensify the absorptivity of the 0.5% W/TiO₂ particularly at high wavelengths as shown in Figure 4.17. The improvement increased as the treatment period increased from 2 to 4 hours; however, diminished when extended to 6 hours. Activity test with 2-chlorophenol indicated the 0.5% W/TiO₂ with 4 hours of hydrothermal treatment was more active than others (Figure 4.18). Hence, hydrothermal treatment of 4 hours was considered to be the optimum period. The XRD pattern of 0.5% W/TiO₂ autoclaved for 4 hours compare to 0.5% W/TiO₂ in Figure 4.19. It can be seen that for 0.5% W/TiO₂ without hydrothermal treatment, the TiO_2 sample had low anatase peak. This is because the precursor of TiO_2 was hydrolyzed at lower temperature, the rate of hydrolysis reaction is relative low and the hydrolysis was not completed, there was a large amount of un-hydrolyzed sols still remaining in the xerogel powders. These un-hydrolyzed sols prevented the phase transformation of amorphous to anatase by adsorbing sols on the surface of TiO_2 particles. Consequently, the as-prepared TiO₂ powders were amorphous or low crystallinity as reported by Yu et al (2005). In contrast, the TiO₂ samples after hydrothermal treatment appeared to have higher anatase peak. Hence, it can be concluded that hydrothermal treatment enhanced the phase transformation of the TiO₂ powders from amorphous to anatase at a low temperature and increased peak intensity



Figure 4.17 Absorption spectrographs of 0.5%W/TiO₂ prepared at the optimum sol-gel conditions with different hydrothermal treatment time.



Figure 4.18 Effect of hydrothermal treatment time on the photodegradation of 0.01 mM 2-chlorophenol under blue light irradiation (1 g/L TiO₂, pH 5 and 25°C).



Figure 4.19 XRD pattern of TiO₂ synthesized under various conditions.

which was also reported by Mahata and Kundu (2009). It is important to note that, after hydrothermal treatment, the shift in anatase peak was not observed as in case of 0.5% W/TiO₂ synthesized by sol-gel process. This could be understood because the radius of Wⁿ⁺ (4<n<6) of 62-70 pm is virtually the same as Ti⁴⁺ atom of 62 pm. Thus, it could be concluded that some Ti⁴⁺ in the lattice of TiO₂ were substituted by Wⁿ⁺.

The hydrothermal treatment also improved the catalytic property of undoped TiO_2 as shown in Figure 4.20; however, the improvement was less evident than those in the case of 0.5% W/TiO₂. In addition, the performance of hydrothermal-treated 0.5% W/TiO₂ was better than undoped TiO₂ and hydrothermal-treated undoped TiO₂ as shown in Figure 4.20. Furthermore, it is very interesting to observe that the photocatalysis activity of the 4 hours hydrothermal-treated 0.5% W/TiO₂ under blue light irradiation was nearly comparable to those of the P-25 under UV irradiation at 253.7 nm, i.e., 0.01 mM of 2-chlorophenol could be removed completely in 120 and 90 minutes, respectively. It is implied that the presence of transition metals and hydrothermal process increases the photocatalytic activity either by scavenging electrons that reduce the recombination of charges and therefore favors the •OH formation, or by modifying the surface properties of the material regarding the active sites, presence of defects etc., which could increase the adsorption and favor the interfacial reactions. This can significantly reduce the treatment cost of the photocatalytic process as the expensive UV irradiation can be replaced by the cheaper blue light irradiation.



Figure 4.20 Photodegradation of 0.01 mM 2-chlophenol by TiO₂ synthesized under various conditions under blue-light irradiation as compared to Degussa P-25 under blue-light and UV irradiations (1 g/L TiO₂, pH 5 and 25°C).

The X-ray fluorescence (XRF) analysis was used to determine the elemental concentration of tungsten in the 0.5% W/TiO₂ with 4-hour hydrothermal treatment. The structure analysis result of XRF shows that 1.78% (w/w) tungsten was presented in the sample which was reasonable and corresponding very well with the doped mole ratio of 1.92% (w/w) (equivalent to 0.5% by mole).

4.1.3 Physical Properties of Synthetic Titanium Dioxide

Crystal size, band gap energy and weight fraction of anatase and rutile phase of the synthetic TiO_2 were calculated and summarized in Table 4.5. The crystal size estimated from Scherrer formula showed that tungsten had an effect on the crystal size, i.e., the crystal size decreased as compared to the undoped TiO_2 . On the other hand, the hydrothermal treatment could significantly increase the crystal size. However, all synthetic TiO_2 samples had the crystal sizes smaller than the Degussa P-25. In addition, no rutile was found in the TiO_2 synthesized under the conditions used in this study, only the anatase phase was identified.

Morphologies of the undoped TiO_2 and 0.5% W/TiO₂ both with and without hydrothermal treatment were revealed by the SEM micrographs as shown in Figure 4.21. It reveals that the Degussa P-25 (Figure 4.21(a)) had better uniformity than the TiO₂ obtained from this study all of which exhibited nanogranular and rough surface. The morphologies of undoped TiO₂ and hydrothermal-treated 0.5% W/TiO₂ showed no significant difference as demonstrated in Figures 4.21(b) and 4.21(d). The nanoparticle size of the 0.5% W/TiO₂ was significantly larger than that estimated by the XRD measurements. This is due to the agglomeration of the nanocrystallines on the surface to form larger grains as shown by the SEM image in Figure 4.21(c). Formation of more aggregates could be related to the change of surface properties of the TiO_2 crystallites. The values of surface area, pore volume, and pore size are shown in Table 4.6. Among the synthetic TiO_2 , the undoped TiO_2 had the high surface area (251.30 m^2/g). After doped with tungsten, the TiO₂ surface reduced to 201.50 m^2/g due to the agglomeration of the nanocrystallites as shown in the SEM image. It is very interesting to observe that the surface area became the highest after hydrothermal treatment. Moreover, it can be seen that all the samples had much higher surface area and pore volume whereas lower pore size than the Degussa P-25. In fact, Degussa P-25 powder, produced through hydrolysis of TiCl₄ in a hydrogen flame (Datye et al., 1995), does not contain pore in each TiO_2 crystallites. Therefore,

TiO ₂	Crystal size (nm)	Band gap energy (eV)	% Anatase	% Rutile
Degussa P-25	34.426	3.20	69.55	30.45
Undoped TiO ₂	4.209	1.20	100	0
0.5%W/TiO2	2.993	1.18	100	0
Hydrothermal-treated	8.032	0.90	100	0
0.5% W/TiO ₂				

Table 4.5 Crystal size, band gap energy, and weight fraction of anatase and rutile phase of the synthetic TiO₂ compared to the Degussa P-25.



Figure 4.21 SEM micrographs of synthetic TiO₂ and Degussa P-25. (a) Degussa P-25, (b) undoped TiO₂, (c) 0.5%W/TiO₂, and (d) 0.5%W/TiO₂ with hydrothermal treatment.

T:O somela	Surface area	Pore volume	Pore size
110_2 sample	(m ² /g)	(cc./g)	(Å)
Degussa P-25 ^a	49.30	0.0900	83.00
Undoped TiO ₂	251.30	0.1832	29.16
0.5% W/TiO ₂	201.50	0.1245	24.72
Hydrothermal-treated 0.5% W/TiO ₂	313.70	0.3337	42.56

Table 4.6 BET specific surface area, pore volume and size of the synthetic TiO₂ compared to Degussa P-25.

^a from Yu et al. (2006)

the formation of the pore structures in the samples could be attributed to the aggregations of TiO_2 crystallites. Finally, the synthetic TiO_2 was analyzed for their particle size distribution. From the particle size analysis as shown in Table 4.7 and Figure 4.22, it was found that the size distributions of all TiO_2 synthesized in this study were not significantly different. Particle sizes measured from this analysis were quite large due to the crystallite agglomeration. Nonetheless, it is believed that most particles would disperse into their primary sizes in aqueous suspension with sufficient mixing.

4.2 Adsorption of 2-Chlorophenol

This part aimed to characterize the adsorption behavior of 2-chlorophenol onto the TiO₂ surface. Different types of synthetic TiO₂ as well as the Degussa P-25 were used in this part. It was found that the contact time to reach adsorption equilibrium was approximately 20 minutes for all synthetic TiO₂ and approximately 30 minutes for Degussa P-25 as shown in Figure 4.23. The results revealed that Degussa P-25

Table 4.7 Comparison the particle size distribution between synthetic TiO₂ and Degussa P-25.

	TiO ₂ sample	Particle size distribution (µm)			
		D(v,0.1)	D(v,0.5)	D(v,0.9)	
	Undoped TiO ₂	7.25	81.25	253.57	
	0.5% W/TiO ₂	13.80	68.63	237.48	
	Hydrothermal-treated 0.5% W/TiO ₂	6.85	93.44	290.77	



Figure 4.22 Particle size distribution of the synthetic TiO₂: (a) undoped TiO₂, (b) 0.5%W/TiO₂, and (c) hydrothermal-treated 0.5%W/TiO₂.



Figure 4.23 Adsorption of 2-chlorophenol on synthetic TiO₂ and Degussa P-25.

provided the lowest adsorption capacity for 2-chlorophenol whereas the 0.5% W/TiO₂ with hydrothermal treatment had the highest capacity followed by undoped TiO₂ and 0.5% W/TiO₂, respectively. In addition, there was no significant difference in adsorption ability between fresh and used undoped TiO₂. This behavior might be explained by surface area and pore structure as shown previously in Table 4.6 and SEM morphology (Figure 4.21). Low surface area of 0.5% W/TiO₂ (201.5 m^2/g) resulted in a low active surface site to adsorb 2-chlorophenol as compared to 313.7 m²/g for the 0.5% W/TiO₂ with autoclaving. Since the 0.5% W/TiO₂ with hydrothermal treatment had the highest photocatalytic activity (as will be discussed later), it's adsorption isotherm was investigated with the initial 2-chlorophenol ranging from 0.005 to 1.5 mM. The results were shown in Figure 4.24. It is obvious that the amount of 2-chlorophenol adsorbed on titanium surface increased with increasing initial concentration of 2-chlorophenol in water. Figure 4.25 shows the isotherm plot and indicates that 2-chlorophenol adsorbed on titanium surface increased with increasing of the equilibrium concentration of 2-chlorophenol in aqueous phase until reaching a plateau. Further analysis using the linearized forms of Langmuir and Freundlich adsorption isotherms following Equations 2.9 and 2.11 in Chapter 2 as shown in Figures 4.26 and 4.27, respectively.


Figure 4.24 Adsorption of 2-chlorophenol onto the surface of 0.5%W/TiO₂ with hydrothermal treatment.



Figure 4.25 Isotherm plot of the 2-chlorophenol adsorption onto 0.5%W/TiO₂ with hydrothermal treatment.



Figure 4.26 Langmuir adsorption isotherm plot for hydrothermal-treated



Figure 4.27 Freundlich adsorption isotherm plot for hydrothermal-treated 0.5%W/TiO₂.

The Langmuir parameters, q_{max} and b, and R^2 were 0.046 mmole of 2-chlorophenol/ g of TiO₂ and 3.309 L/mmole, and 0.9947, respectively, whereas the Freundlich parameters, K_F and n, and R^2 were 16.501 and 1.271, and 0.9563, respectively. From the R^2 values, it revealed that the Langmuir isotherm could describe the experimental data better than the Freundlich isotherm.

4.3 Kinetics Study

4.3.1 Direct Photolysis and Volatilization

In this part, Degussa P-25 was used to study the photodegradation of 2-chlorophenol at the initial concentration of 0.01 mM. The results in Figure 4.28 reveal that 2-chlorophenol had a low volatilization rate (1.5% in 6 hours); hence, its volatilization to the atmosphere could be neglected. In addition, direct photolysis with blue light irradiation was also minimal and could be neglected as well. Photodegradation of 2-chlorophenol in the presence of Degussa P-25 under UV and blue light irradiations were also investigated and shown in Figure 4.28. It was found that P-25 was very active under UV irradiation whereas much less active in blue light, i.e., 0.01 mM of 2-chlorophenol was completely removed in 90 minutes under UV irradiation whereas only 23.2% removal efficiency was obtained in 6 hours under blue light irradiation. It is important to mention that the initial concentration of 2-chlorophenol in the case of photocatalytic oxidation was the concentration after 30 minutes of dark adsorption to allow the 2-chlorophenol equilibrated between aqueous phase and solid surface.



Figure 4.28 Volatilization, photolysis and photocatalytic oxidation of 2-chlorophenol irradiated by blue light or UV in present of Degussa P-25 (1 g/L TiO₂, 0.01 mM 2-chlorophenol, pH 5 and 25°C).

4.3.2 Effect of Titanium Dioxide Dose

To obtain the optimum TiO_2 dose on photodegradation under the study conditions, undoped TiO_2 was selected. The effect of TiO_2 dose on the photocatalysis of 2-chlorophenol is demonstrated in Figure 4.29. The results showed that the degradeation of 2-chlorophenol increased as a TiO_2 dose increased from 0.25 up to 1 g/L, i.e., from 43.5% at 0.25 g/L to 76.0 and 91.8% at 0.5 and 1.0 g/L, respectively. However, further increased to 1.5 g/L slightly decreased the efficiency of 2-chlorophenol degradation to 87.6%. This suggested that the degradation increased with increasing catalyst concentration, which is the characteristic of heterogeneous photocatalysis. An increase in catalyst amount actually increases the number of active sites on the photocatalyst surface thus causing an increase in the number of •OH radicals which can take part in actual degradation of 2-chlorophenol in solution. Beyond a certain limit of catalyst amount, the solution becomes turbid and thus blocks the light penetration into the mixture resulting in limiting the reaction and therefore percentage degradation starts decreasing (Macedo et al., 2007; Wang et al., 2008).



Figure 4.29 Effect of undoped TiO_2 dose on photocatalytic degradation of 2-chlorophenol irradiated by blue light (0.01 mM 2-chlorophenol, pH 5 and $25^{\circ}C$).

4.3.3 Effect of pH

In this part aimed to characterize the photocatalytic activity of synthetic TiO_2 under different pH under blue light irradiation. It was found that pH had a great effect on the photodegradation efficiency of 2-chlorophenol. Variation of solution pH changed the surface charge of TiO₂ particles and shifted the potentials of catalytic reactions. Point of zero charge (pzc) of the synthetic TiO₂ was shown in Figure 4.30 showing that the pzc of undoped TiO_2 was 4.5 and decreasing to 3.6 and 3.4 for 0.5% W/TiO₂ and hydrothermal-treated 0.5% W/TiO₂, respectively. Figure 4.31 summarizes the effect of pH on the photocatalytic oxidation of 2-chlorophenol in present of undoped TiO₂. It revealed that as the pH decreased sequentially from 8 to 7, 6 and 5, the oxidation of 2-chlorophenol became more efficient, i.e., the removal efficiencies increased from 49.4% to 59.0, 67.3 and 91.8%, respectively. This observation may be due to the electrical interaction between charged surface and ionic adsorbates. Since the pzc of the synthetic TiO_2 was 4.5, the TiO_2 surface was positively charged as the pH was less than 4.5 whereas became negatively charged when the pH was greater than 4.5. Additionally, since the pK_a of 2-chlorophenol is 8.53, 2-chlorophenols transform to 2-chlorophenol anion when the pH is greater than 8.53. Therefore, adsorption of 2-chlorophenol onto the TiO₂ surface is likely to be maximized at pH 4.5 where both species have no charge. As a result, the degradation became better as the solution pH decreasing toward the pzc of the TiO₂.



Figure 4.30 Point of zero charge of the synthetic TiO₂.



Figure 4.31 Effect of pH on photocatalytic degradation of 2-chlorophenol irradiated by blue light (1 g/L TiO₂, 2-chlorophenol 0.01 mM and 25°C).

This results agreed with Drzewicz et al (1999) who studied degradation of 2,4-dichlorophenol and found that the most efficient decomposition of 2,4-dichlorophenol occurred at pH 5 whereas the least efficient happened at the most alkaline solution which was pH 10.7.

4.3.4 Effect of Light Wavelength

It is interesting to determine the photo-respond of synthetic TiO_2 to the light at other wavelength rather than blue light because its absorption spectra also showed a superior trend to Degussa P-25. In this part, the blue, green and red lights were used to activate the synthetic TiO_2 to evaluate its photocatalytic activity and the results were summarized in Table 4.8 and Figure 4.32. For undoped TiO_2 , it was found that the removal efficiencies in 6 hours of 0.01 mM of 2-chlorophenol were 91.8, 52.9,

Table 4.8 Effect of light color on the photocatalytic activity of the synthetic TiO₂.

TiO, sample	6-hour	removal efficien	ncy (%)
110 ² sample	Blue light	Green light	Red light
Undoped TiO ₂	91.8	52.9	20.9
0.5% W/TiO ₂	90.5	33.8	17.4
Hydrothermal-treated 0.5% W/TiO ₂	100.0	43.4	20.0





and 20.9% under the blue, green and red lights, respectively. The 0.5% W/TiO₂ showed the lowest photocatalytic activity in every light wavelength. It is note that the nanocrystalline 0.5% W/TiO₂ had the highest degree of agglomeration as compared to other types. Interestingly, 0.5% W/TiO₂ with hydrothermal treatment could completely removed 2-chlorophenol in 120 minutes under blue light activation however the photocatalytic activity under green light activation was less than undoped TiO₂ while providing similar result in red light irradiation.

4.3.5 Kinetics Determination

TiO₂ photocatalytic reaction is known to be a heterogeneous reaction, and the oxidation reaction can be mainly achieved by •OH. Langmuir-Hinshelwood model as shown in equation 2.13 in Chapter 2 can be applied to determine the contribution of adsorption and oxidation in the reaction. In this experimental part, the photocatalytic activities of the undoped TiO₂ and 0.5% W/TiO₂ with hydrothermal treatment under blue light irradiation were investigated and compared. Figures 4.33 and 4.34 illustrate the degradation of 2-chlorophenol under different concentrations for undoped and 0.5% W/TiO₂ with hydrothermal treatment, respectively.

In order to determine the kinetics of 2-chlorophenol oxidation by photocatalytic oxidation by TiO₂, it is important to eliminate the competitive reaction from several intermediates being formed from 2-chlorophenol oxidation. This study decided to use the initial rate technique to determine the oxidation rate of 2-chlorophenol since there was no intermediate present at the initial stage. In practice, it is very difficult to obtain an accurate initial rate if the reaction does not follow zero-order reaction (as in this study) where the initial slope can be drawn easily and directly from the profile plot. This study tried to overcome this problem by fitting the experimental data with either pseudo-first or pseudo-second order to obtain the reaction rate constant and then calculated the initial rate. It was found that the degradation data at the initial stage of 120 minutes could be characterized better by pseudo-1st-order reaction as shown in Figures 4.33 and 4.34 (plots for pseudo-2ndorder reaction were not shown). The y-intercept and slope which represent "1/kr" and "1/krK" were summarized in Table 4.9. Further analysis following the Langmuir-Hinshelwood model as shown in Figure 4.35 provided the k_r and K of 1.65×10^{-4} mM/min and 85.03 1/mM for undoped TiO₂ and 3.00×10^{-4} mM/min and



Figure 4.33 Photocatalysis of various initial concentration of 2-chlorophenol under blue light irradiation in present of undoped TiO₂: (a) degradation timeprofile and (b) 1st-order plot (1 g/L TiO₂, pH 5 and 25°C).



Figure 4.34 Photocatalysis of various initial concentration of 2-chlorophenol under blue light irradiation in present of 0.5% W/TiO₂ with hydrothermal treatment: (a) degradation time-profile and (b) 1st-order plot (1 g/L TiO₂, pH 5 and 25°C).

Initial	τ	Undoped Ti	\mathbf{D}_2	0.5%W/TiO ₂ with hydrothermal- treated		
(mM)	k _{observed} (min ⁻¹)	R ²	Rate _{ini} (mM/min)	k _{observed} (min ⁻¹)	\mathbf{R}^2	Rate _{ini} (mM/min)
0.005	0.0109	0.9798	4.93×10 ⁻⁵	0.0375	0.9534	1.55×10 ⁻⁴
0.01	0.0095	0.9930	8.12×10 ⁻⁵	0.0204	0.9783	1.76×10 ⁻⁴
0.03	0.0036	0.9439	9.97×10 ⁻⁵	0.0097	0.9170	2.65×10 ⁻⁴
0.05	0.0029	0.9765	1.37×10 ⁻⁴	0.0074	0.9517	2.88×10 ⁻⁴

 Table 4.9 Pseudo-first order rate constant for 2-chlorophenol photocatalytic

 oxidation under different initial concentrations.



Figure 4.35 Langmuir-Hinshelwood plot of Table 4.9.

239.13 1/mM for hydrothermal-treated 0.5% W/TiO₂, respectively. It is obviously seen that the tungsten doping and hydrothermal treatment could significantly improve both photocatalytic activity and adsorption property of the TiO₂.

4.3.6 Reusability of Synthetic Titanium Dioxide

This part aimed to determine the reusability of the hydrothermal-treated 0.5% W/TiO₂ as the photocatalyst in the visible light region. After the catalysts were used to treat 2-chlorophenol for 6 hours, they were washed with the deionized water

several times and re-suspended in the 2-chlorophenol wastewater under blue-light irradiation. The experiment results revealed that the removal rate and efficiency of reused hydrothermal-treated 0.5% W/TiO₂ were almost the same as in the first cycle as shown in Figure 4.36. This implied that the photoactivity of hydrothermal-treated 0.5% W/TiO₂ could possible be sustained for a long period of time.



Figure 4.36 Photocatalysis of 2-chlorophenol under blue light irradiation in present of fresh and used hydrothermal-treated 0.5%W/TiO₂. (1g/L TiO₂, 2-chlorophenol 0.01 mM, at pH 5 and 25°C).



CHAPTER V

CONCLUSION

5.1 Conclusions

In this study, a new TiO_2 photocatalyst, which can be effectively activated by the blue light, has been synthesized and tested for its photocatalytic activity using 2-chlorophenol as the target compound. Important findings from this study can be summarized as follows:

- Optimum conditions for visible-light activated TiO₂ were:

a) Placing 70 mL anhydrous ethanol in a 250 mL flask and slowly adding 0.05 mole of tetra(n-butoxyl)titanium under the vigorous stirring condition to prepare a clear tetra(n-butoxyl)titanium ethanol solution (Solution I). The flask was then placed in a water bath controlled at 4°C.

b) At the same time, 20 mL of deionized water was mixed with 20 mL anhydrous ethanol to make an ethanol aqueous solution. Tungsten in the form of $Na_2WO_4.2H_2O$ at the W:Ti ratio of 0.5% on the mole basis was added and the mixture was continuously stirred until the doping chemical was completely dissolved (Solution II).

c) Solution II was dropwise added into Solution I under vigorous stirring condition and the precipitates would be formed. The mixture was control at 4°C through out the dropwise addition step and maintaining at 4°C for another 30 minutes during the following curing step.

d) Mixture was continuous stirred in the water bath for another 30 minutes without temperature control, i.e., allowed the temperature to gradually increase to room condition. The mixture was then added with 4 mL of concentrated HNO_3 and underwent hydrolytic condensation for 3 hours under vigorous stirred condition.

e) Hydrolyzed solution was then treated by hydrothermal process by autoclaving at 121°C and 103.4 kPa for 4 hours before placing into an oven to dry at 120°C for 2 hours to obtain solid titanium hydroxide.

f) Titanium hydroxide was pulverized into a powder form and calcined at 200°C with the ramp rate of 1°C/minute for 10 hours to become titanium dioxide doped with tungsten.

- Hydrothermal-treated 0.5% W/TiO₂ prepared under the optimum conditions had the photocatalytic activity under blue light irradiation almost comparable to those of the commercial Degussa P-25 under UV irradiation, i.e., 0.01 mM of 2-chlorophenol could be completely removed in 120 and 90 minutes by the hydrothermal-treated 0.5% W/TiO₂ under blue light irradiation and the Degussa P-25 under UV irradiation, respectively.

- Crystalline structure, a very important factor affecting the photoactivity of the TiO_2 under the UV irradiation, did not directly involve in the photocatalytic behavior of the TiO_2 under visible light irradiation.

- Photo-oxidation kinetics of 2-chlorophenol could be explained by the Langmuir-Hinshelwood model with k_r and K of 1.65×10^{-4} mM/min and 85.03 1/mM for undoped TiO₂ and 3.00×10^{-4} mM/min and 239.13 1/mM for hydrothermal-treated 0.5% W/TiO₂, respectively.

5.2 Recommendations for Future Study

- Investigate into more details of the chemical structure and phase composition of the hydrothermal-treated 0.5% W/TiO₂ to determine the causes which make this catalyst so active under the blue light irradiation.

- Study the photoactivity of the hydrothermal-treated 0.5% W/TiO₂ by using other target pollutants and compared the results to 2-chlorophenol case.

- Investigate the photoactivity of the hydrothermal-treated 0.5% W/TiO₂ under sunlight irradiation.

- Immobilize the hydrothermal-treated 0.5% W/TiO₂ on fixed surface for possible field applications both in air and water treatment.

จุฬาลงกรณ่มหาวิทยาลัย

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APPENDIX A

Experimental Setup



Figure A.1 Reactor setup (outside)



Figure A.2 Reactor setup (inside)





Figure A.3 The color of undoped TiO₂ calcined at different temperature

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82



Figure A.4 The color of W/TiO₂ synthesized by sol-gel process



Figure A.5 The color of F/TiO_2 synthesized by sol-gel process



Figure A.6 The color of Pt/TiO₂ synthesized by sol-gel process



Figure A.7 The color of hydrothermal-treated 0.5%W/TiO₂ (autoclaved 4 hours)



APPENDIX B

Experimental Data

Time	Residual of 2-ch	lorophenol (mM)
(min)	200°C	300°C
Adsorption 0	0.009	0.012
15	0.009	0.011
30	0.009	0.011
Irradiation 0	0.009	0.011
30	0.006	0.010
60	0.005	0.010
90	0.004	0.009
120	0.003	0.009
180	0.002	0.008
240	0.001	0.007
300	0.001	0.007
360	0.001	0.006

Table B.1 Photodegradation of 0.01 mM 2-chlorophenol by TiO₂ calcined at 200°C and 300°C under blue light irradiation.



Time		Residual of 2-chlorophenol (mM)				
(min)		1°C/min	4°C/min	9°C/min		
Adsorption 0		0.012	0.014	0.014		
15	5	0.011	0.012	0.011		
30)	0.011	0.012	0.012		
Irradiation ()	0.011	0.012	0.012		
30)	0.010	0.011	0.011		
60)	0.010	0.011	0.011		
90)	0.009	0.010	0.011		
120)	0.009	0.010	0.010		
180)	0.008	0.009	0.009		
240)	0.007	0.009	0.009		
300)	0.007	0.008	0.008		
360)	0.006	0.008	0.008		

Table B.2 Photodegradation of 0.01 mM 2-chlorophenol of undoped TiO_2 at various ramp rate under blue light irradiation.



Time		R	Residual of 2-ch	lorophenol (mN	I)
(min))	No control	Mix step	4 °C, 30 min	4 °C, 1 hour
Adsorption	0	0.009	0.011	0.009	0.009
	15	0.009	0.011	0.009	0.008
	30	0.008	0.010	0.009	0.009
Irradiation	0	0.008	0.010	0.009	0.009
	30	0.007	0.007	0.006	0.006
	60	0.006	0.006	0.005	0.005
	90	0.006	0.005	0.004	0.004
	120	0.005	0.004	0.003	0.003
	180	0.004	0.003	0.002	0.002
	240	0.003	0.003	0.001	0.001
	300	0.003	0.002	0.001	0.001
	360	0.002	0.001	0.001	0.001

Table B.3 The photodegradation of 0.01 mM 2-chlorophenol at various temperature and duration time control in dissolution stage under blue light irradiation.

Time (min)		Residual of 2-chlorophenol (mM)						
		0.5%W/TiO ₂	1%F/TiO ₂	1%Pt/TiO ₂	Undoped TiO ₂	Degussa P-25		
Adsorption	0	0.009	0.010	0.009	0.009	0.009		
	15	0.008	0.010	0.009	0.009	0.008		
	30	0.009	0.010	0.009	0.009	0.008		
Irradiation	0	0.009	0.010	0.009	0.009	0.008		
	30	0.006	0.008	0.008	0.006	0.008		
	60	0.005	0.008	0.008	0.005	0.008		
	90	0.004	0.007	0.007	0.004	0.008		
	120	0.003	0.007	0.007	0.003	0.007		
	180	0.002	0.006	0.006	0.002	0.007		
	240	0.0 <mark>0</mark> 1	0.005	0.006	0.001	0.007		
	300	0.001	0.005	0.006	0.001	0.007		
	360	0.001	0.005	0.006	0.001	0.006		

Table B.4 The photodegradation of 0.01 mM 2-chlorophenol at various doped TiO₂ compare to undoped TiO₂ and Degussa P-25 under blue light irradiation.

Time	Residu	Residual of 2-chlorophenol (mM)				
(min)	H ₂ SO ₄	H ₃ PO ₄	HNO ₃			
Adsorption 0	0.039	0.045	0.059			
15	0.037	0.042	0.057			
30	0.037	0.042	0.057			
Irradiation 0	0.037	0.042	0.004			
30	0.036	0.042	0.003			
60	0.035	0.041	0.003			
90	0.034	0.037	0.003			
120	0.034	0.038	0.003			
180	0.033	0.037	0.003			
240	0.032	0.036	0.003			
300	0.032	0.036	0.003			
360	0.030	0.035	0.003			

Table B.5 The photodegradation of 0.05 mM 2-chlorophenol of 0.5%W/TiO₂ at acid catalyst under blue light irradiation.



Time		Residual of 2-chlorophenol (mM)					
(min)		2 hours	3 hours	4 hours	6 hours		
Adsorption	0	0.010	0.010	0.010	0.012		
	15	0.008	0.010	0.006	0.008		
	30	0.007	0.009	0.006	0.008		
Irradiation	0	0.007	0.009	0.006	0.008		
	30	0.005	0.004	0.004	0.005		
	60	0.003	0.002	0.002	0.003		
	90	0.002	0.001	0.001	0.002		
	120	0.001	0.000	0.000	0.002		
	180	0.000	0.000	0.000	0.000		
	240	0.000	0.000	0.000	0.000		
	300	0.000	0.000	0.000	0.000		
	360	0.000	0.000	0.000	0.000		

Table B.6 Effect of autoclave time on the photodegradation of 0.01 mM2-chlorophenol under blue light irradiation.



Time (min)		Residual of 2-chlorophenol (mM)			
		hydrothermal-treated Undoped TiO ₂	hydrothermal-treated 0.5%W/TiO ₂		
Adsorption	0	0.012	0.010		
1.	5	0.011	0.007		
3	0	0.011	0.007		
Irradiation	0	0.011	0.007		
1.	5	0.009	0.005		
3	0	0.007	0.004		
6	0	0.005	0.002		
9	0	0.004	0.001		
12	0	0.003	0.000		
18	0	0.002	0.000		
24	0	0.001	0.000		
30	0	0.000	0.000		
36	0	0.000	0.000		

Table B.7 the photodegradation of 0.01 mM 2-chlorophenol on undoped TiO_2 and 0.5%W/TiO₂ with 4hours hydrothermal treatment under blue light irradiation.

Note: 1g/L TiO₂, pH 5, 25°C, 2W (72 W/m²) blue light, using NaOH and HClO₄ for pH adjustment

Adsorption		qe (mmole of 2-chlorophenol/g of TiO ₂)				
Time (min)	Undoped TiO ₂	Used undoped TiO ₂	0.5%W/TiO ₂	0.5%W/TiO ₂ hydrothermal- treated	Degussa P-25	
0	0.0000	0.0000	0.0000	0.0000	0.0000	
5	0.0004	0.0006	0.0008	0.0004	0.0011	
10	0.0006	0.0012	0.0010	0.0007	0.0013	
15	0.0006	0.0012	0.0012	0.0011	0.0014	
20	0.0006	0.0012	0.0012	0.0011	0.0014	
30	0.0008	0.0012	0.0012	0.0011	0.0014	
45	0.0008	0.0012	0.0012	0.0011	0.0014	
60	0.0008	0.0012	0.0012	0.0011	0.0014	

Table B.8 Adsorption of 2-chlorophenol on synthetic TiO₂ and Degussa P-25.

Note: 1g/L TiO₂, pH 5, 25°C, using NaOH and HClO₄ for pH adjustment

Adsorption	q _e (mmole of 2-chlorophenol/g of TiO ₂)						
Time (min)	0.0054 mM	0.009 mM	0.034 mM	0.056 mM	0.86 mM		
0	0	0	0	0	0		
5	0.0004	0.0004	0.0011	0.0043	0.0108		
10	0.0004	0.0011	0.0011	0.0059	0.0119		
15	0.0005	0.0011	0.0014	0.0059	0.0119		
20	0.0007	0.0011	0.0032	0.0070	0.0119		
30	0.0007	0.0011	0.0032	0.0070	0.0119		
45	0.0007	0.0011	0.0036	0.0075	0.0130		
60	0.0007	0.0011	0.0036	0.0070	0.0119		
Adsorption		q _e (mmole of	2-chloropher	nol/g of TiO ₂)			
Time	0.22 mM	0.59 mM	1.27 mM				
(min)		63297					
0	0	0	0				
5	0. <mark>01</mark> 51	0.0281	0.0324				
10	<mark>0.0</mark> 194	0.0356	0.0410				
15	0.0194	0.0367	0.0432				
20	0.0216	0.0378	0.0453				
30	0.0248	0.0367	0.0432				
45	0.0259	0.0367	0.0453	21			
60	0.0259	0.0367	0.0432				

Table B.9 Adsorption of 2-chlorophenol on hydrothermal-treated 0.5%W/TiO₂.

Note: 1g/L TiO₂, pH 5, 25°C, using NaOH and HClO₄ for pH adjustment

94
Time	Residual of 2-chlorophenol (mM)			
(min)	Voltilization	Photolysis		
0	0.0067	0.0099		
30		0.0097		
60	0.0068	0.0098		
90		0.0099		
120	0.0068	0.0099		
180	0.0067	0.0094		
240	0.0068	0.0091		
300	0.0065	0.0089		
360	0.0066	0.0088		

Table B.10 Volitilization and photolysis photodegradation of 2-chlorophenol.

Time		Residual of 2-chlorophenol (mM)
(min)		Degussa P-25/UV
Adsorption	0	0.011
3	30	0.010
6	50	0.010
Irradiation	0	0.010
	5	0.008
1	10	0.007
1	15	0.006
2	20	0.005
3	30	0.004
	45	0.003
6	5 <mark>0</mark>	0.001
ç	90	0.000
12	20	0.000
18	80	0.000
24	40	0.000
30	00	0.000
36	50	0.000

Table B.11 Photodegradation of 2-chlorophenol irradiated by UV in present ofDegussa P-25.

Note: 1g/L TiO₂, pH 5, 25°C, 4W UV light, using NaOH and HClO₄ for pH adjustment

Time	lorophenol (mN	()			
(min	l)	0.25 g/L	0.5 g/L	1.0 g/L	1.5 g/L
Adsorption	0	0.014	0.008	0.009	0.009
	15	0.014	0.008	0.009	0.009
	30	0.014	0.008	0.009	0.009
Irradiation	0	0.014	0.008	0.009	0.009
	30	0.013	0.006	0.006	0.007
60		0.012	0.006	0.005	0.005
	90		0.005	0.004	0.004
	120	0.011	0.005	0.003	0.004
	180	0.011	0.004	0.002	0.003
	240	0.010	0.003	0.001	0.002
	300	0.009	0.002	0.001	0.002
	360	0.008	0.002	0.001	0.001

Table B.12 Effect of undoped TiO_2 dose on photocatalytic degradation of 2-chlorophenol irradiated by blue light.



Time	R	Residual of 2-chlorophenol (mM)				
(min)	рН 5	pH 6	pH 7	pH 8		
Adsorption 0	0.009	0.012	0.012	0.009		
15	0.009	0.011	0.011	0.009		
30	0.009	0.011	0.011	0.008		
Irradiation 0	0.009	0.011	0.011	0.008		
30	0.006	0.009	0.009	0.007		
60	0.005	0.007	0.008	0.007		
90	0.004	0.007	0.007	0.006		
120	0.003	0.006	0.007	0.005		
180	0.002	0.005	0.006	0.005		
240	0.001	0.004	0.005	0.005		
300	0.001	0.004	0.005	0.004		
360	0.001	0.004	0.004	0.004		

Table B.13 Effect of pH on photocatalytic degradation of 2-chlorophenolirradiated by blue light.



Time	Resid	Residual of 2-chlorophenol (mM)			
(min)	Blue	Green	Red		
Adsorption 0	0.009	0.009	0.015		
15	0.009	0.009	0.014		
30	0.009	0.009	0.014		
Irradiation 0	0.009	0.009	0.014		
30	0.006	0.009	0.014		
60	0.005	0.008	0.014		
90	0.004	0.008	0.014		
120	0.003	0.008	0.013		
180	0.002	0.006	0.013		
240	0.001	0.005	0.012		
300	0.001	0.005	0.011		
360	0.001	0.004	0.011		

Table B.14 Photocatalysis of 0.01 mM 2-chlorophenol under different light irradiation in present of undoped TiO₂.

Note: 1g/L TiO₂, pH 5, 25°C, 2W (72 W/m² for blue light, 22 W/m² for green light and 34 W/m² for red light) using NaOH and HClO₄ for pH adjustment



Tin	ne	Residual of 2-chlorophenol (mM)				
(mi	n)	Blue	Green	Red		
Adsorption	0	0.009	0.007	0.009		
	15	0.008	0.008	0.009		
	30	0.009	0.008	0.009		
Irradiation	0	0.009	0.008	0.009		
	30	0.006	0.008	0.009		
	60	0.005	0.007	0.008		
	90	0.004	0.007	0.008		
	120	0.003	0.007	0.008		
	180	0.002	0.006	0.008		
	240	0.001	0.006	0.008		
	300	0.001	0.006	0.008		
	360	0.001	0.005	0.007		

Table B.15 Photocatalysis of 0.01 mM 2-chlorophenol under different light irradiation in present of 0.5%W/TiO₂.

Note: 1g/L TiO₂, pH 5, 25°C, 2W (72 W/m² for blue light, 22 W/m² for green light and 34 W/m² for red light) using NaOH and HClO₄ for pH adjustment



Time (min)		Resid	ual of 2-chloropheno	l (mM)
		Blue	Green	Red
Adsorption ()	0.010	0.010	0.011
15	5	0.007	0.010	0.010
30)	0.007	0.010	0.010
Irradiation ()	0.007	0.010	0.010
15	5	0.005	0.009	0.010
30)	0.004	0.008	0.009
60)	0.002	0.008	0.009
90)	0.001	0.007	0.009
120		0.000	0.007	0.009
180)	0.000	0.006	0.009
240)	0.000	0.006	0.008
300)	0.000	0.006	0.008
360		0.000	0.005	0.008

Table B.16 Photocatalysis of 0.01 mM 2-chlorophenol under different light irradiation in present of hydrothermal-treated 0.5%W/TiO₂.

Note: 1g/L TiO₂, pH 5, 25°C, 2W (72 W/m² for blue light, 22 W/m² for green light and 34 W/m² for red light) using NaOH and HClO₄ for pH adjustment



Time	e	Residual of 2-chlorophenol (mM)				
(min)	0.005 mM	0.01 mM	0.03 mM	0.05 mM	
Adsorption	0	0.005	0.009	0.031	0.051	
	15	0.004	0.009	0.028	0.048	
	30	0.004	0.009	0.028	0.047	
Irradiation	0	0.004	0.009	0.028	0.047	
30		0.003	0.006	0.024	0.043	
60		0.002	0.005	0.021	0.040	
	90		0.004	0.020	0.035	
120		0.001	0.003	0.019	0.034	
	180	0.001	0.002	0.016	0.032	
	240	0.001	0.001	0.014	0.030	
	300	0.000	0.001	0.013	0.025	
	360	0.000	0.001	0.012	0.023	

Table B.17 Photocatalysis of various initial concentration of 2-chlorophenol under blue light irradiation in present of undoped TiO₂.



Tim	e	R	Residual of 2-chlorophenol (mM)				
(min)		0.005 mM	0.01 mM	0.03 mM	0.05 mM		
Adsorption	0	0.005	0.010	0.030	0.050		
	15	0.004	0.008	0.027	0.043		
	30	0.004	0.008	0.027	0.039		
Irradiation	0	0.004	0.008	0.027	0.039		
	15	0.003	0.006	0.020	-		
	30	0.002	0.004	0.018	0.028		
	60	0.000	0.003	0.014	0.024		
	90	0.000	0.001	0.012	0.019		
	120	0.000	0.000	0.009	0.017		
	180	0.000	0.000	0.007	0.012		
	24 <mark>0</mark>	0.000	0.000	0.005	0.010		
	300	0.000	0.000	0.004	0.008		
	360	0.000	0.000	0.003	0.006		

Table B.18 Photocatalysis of various initial concentration of 2-chlorophenol under blue light irradiation in present of hydrothermal-treated 0.5%W/TiO₂.

Time	Residual of 2-ch	Residual of 2-chlorophenol (mM)			
(min)	Fresh	Used			
Adsorption 0	0.010	0.010			
15	0.007	0.010			
30	0.007	0.010			
Irradiation 0	0.007	0.010			
15	0.005	0.007			
30	0.004	0.006			
60	0.002	0.003			
90	0.001	0.001			
120	0.000	0.000			
180	0.000	0.000			
240	0.000	0.000			
300	0.000	0.000			
360	0.000	0.000			

Table B.19 the photodegradation of 0.01 mM 2-chlorophenol on fresh and used hydrothermal-treated 0.5%W/TiO₂ under blue light irradiation



		Residual of 2-chlorophenol (mM)				
Time (min)		Undoped TiO ₂	Hydrothermal- treated undoped	0.5%W/TiO ₂	Hydrothermal- treated 0.5%W/TiO ₂	
Adsorption	0	0.009	0.010	0.009	0.009	
	15	0.008	0.010	0.007	0.005	
	30	0.007	0.009	0.008	0.005	
Irradiation	0	0.007	0.009	0.008	0.005	
	15		0.009	-	-	
	30	0.005	0.008	0.005	0.005	
	60	0.004	0.007	0.005	0.004	
	90	0.003	0.006	0.004	-	
	120	0.002	0.005	0.002	0.002	
	180	0.002	0.004	0.001	0.002	
	240	0.001	0.003	0.000	0.001	
	300	0.000	0.002	0.000	0.001	
	360	0.000	0.002	0.000	0.001	

Table B.20 Photocatalysis of 0.01 mM 2-chlorophenol on synthetic TiO₂ under UV irradiation.

Time		Residual of 2-ch	lorophenol (mM)
(min)		Run 1	Run 2
Adsorption 0		0.009	0.009
15	_	0.009	0.008
30		0.009	0.008
Irradiation 0		0.009	0.008
30		0.006	0.006
60		0.005	0.005
90		0.004	0.004
120		0.003	0.003
180		0.002	0.003
240		0.001	0.002
300		0.001	0.001
360		0.001	0.001

Table B.21 The photodegradation of 0.01 mM 2-chlorophenol on undoped underblue light irradiation.



Time	Residual of 2-ch	lorophenol (mM)
(min)	Run 1	Run 2
Adsorption 0	0.009	0.009
15	0.008	0.008
30	0.009	0.008
Irradiation 0	0.009	0.008
30	0.006	0.006
60	0.005	0.005
90	0.004	0.004
120	0.003	0.003
180	0.002	0.002
240	0.001	0.002
300	0.001	0.001
360	0.001	0.001

Table B.22 The photodegradation of 0.01 mM 2-chlorophenol on 0.5%W/TiO₂ under blue light irradiation.



Time		Residual of 2-chlorophenol (mM)	
(min)		Run 1	Run 2
Adsorption 0		0.012	0.012
15		0.011	0.011
30		0.011	0.011
Irradiation 0		0.011	0.011
30		0.010	0.009
60		0.007	0.007
90	Z/11	0.006	0.005
120		0.005	0.004
180		0.004	0.003
240	1/1/16.	0.002	0.002
300		0.001	0.001
360	2.4	0.000	0.000

Table B.23 The photodegradation of 0.01 mM 2-chlorophenol on hydrothermaltreated undoped TiO₂ under blue light irradiation.



Tin	ne	Residual of 2-chlorophenol (mM)		
(mi	n)	Run 1	Run 2	Run 3
Adsorption	0	0.010	0.010	0.010
	15	0.007	0.008	0.009
	30	0.007	0.007	0.008
Irradiation	0	0.007	0.007	0.008
	15	0.005	0.005	-
	30	0.004	0.003	0.004
	60	0.002	0.002	0.002
	90	0.001	0.001	-
	120	0.000	0.000	0.000
	180	0.000	0.000	0.000
	<mark>24</mark> 0	0.000	0.000	0.000
	300	0.000	0.000	0.000
	3 <mark>6</mark> 0	0.000	0.000	0.008

Table B.24 Photocatalysis of various initial concentration of 2-chlorophenol under blue light irradiation in present of hydrothermal-treated 0.5%W/TiO₂.



Size (µm)	Intensity (%)	Size (µm)	Intensity (%)
0.05	0.00	6.63	1.24
0.06	0.00	7.72	1.34
0.07	0.00	9.00	1.44
0.08	0.00	10.48	1.55
0.09	0.00	12.21	1.68
0.11	0.00	14.22	1.83
0.13	0.00	16.57	2.00
0.15	0.00	19.31	2.20
0.17	0.00	22.49	2.43
0.20	0.00	26.20	2.67
0.23	0.00	30.53	2.91
0.27	0.04	35.56	3.14
0.31	0.09	41.43	3.36
0.36	0.14	48.27	3.55
0.42	0.19	56.23	3.74
0.49	0.23	65.51	3.95
0.58	0.26	76.32	4.20
0.67	0.28	88.91	4.51
0.78	0.27	103.58	4.89
0.91	0.28	120.67	5.30
1.06	0.28	140.58	5.71
1.24	0.30	163.77	6.04
1.44	0.33	190.80	6.09
1.68	0.37	222.28	5.67
1.95	0.43	258.95	4.67
2.28	0.52	301.68	3.09
2.65	0.61	351.46	1.51
3.09	0.71	409.45	0.00
3.60	0.82	477.01	0.00
4.19	0.94	555.71	0.00
4.88	1.04	647.41	0.00
5.69	1.15	754.23	0.00

Table B.25 Particle size distribution of undoped TiO₂.

Size (µm)	Intensity (%)	Size (µm)	Intensity (%)
0.05	0.00	6.63	0.81
0.06	0.00	7.72	1.02
0.07	0.00	9.00	1.28
0.08	0.00	10.48	1.59
0.09	0.00	12.21	1.93
0.11	0.00	14.22	2.31
0.13	0.00	16.57	2.71
0.15	0.00	19.31	3.12
0.17	0.00	22.49	3.51
0.20	0.00	26.20	3.87
0.23	0.00	30.53	4.18
0.27	0.02	35.56	4.42
0.31	0.04	41.43	4.53
0.36	0.07	48.27	4.69
0.42	0.09	56.23	4.74
0.49	0.11	65.51	4.77
0.58	0.12	76.32	4.81
0.67	0.12	88.91	4.87
0.78	0.12	103.58	4.95
0.91	0.11	120.67	5.05
1.06	0.10	140.58	5.12
1.24	0.10	163.77	5.07
1.44	0.11	190.80	4.84
1.68	0.11	222.28	4.37
1.95	0.13	258.95	3.60
2.28	0.16	301.68	2.56
2.65	0.19	351.46	1.33
3.09	0.24	409.45	0.10
3.60	0.31	477.01	0.00
4.19	0.39	555.71	0.00
4.88	0.50	647.41	0.00
5.69	0.64	754.23	0.00

Table B.26 Particle size distribution of 0.5%W/TiO₂.

Size (µm)	Intensity (%)	Size (µm)	Intensity (%)
0.05	0.00	6.63	1.18
0.06	0.00	7.72	1.27
0.07	0.00	9.00	1.38
0.08	0.00	10.48	1.49
0.09	0.00	12.21	1.61
0.11	0.00	14.22	1.75
0.13	0.00	16.57	1.90
0.15	0.00	19.31	2.07
0.17	0.00	22.49	2.25
0.20	0.00	26.20	2.43
0.23	0.00	30.53	2.61
0.27	0.03	35.56	2.79
0.31	0.09	41.43	2.94
0.36	0.15	48.27	3.08
0.42	0.21	56.23	3.23
0.49	0.27	65.51	3.41
0.58	0.31	76.32	3.63
0.67	0.33	88.91	3.94
0.78	0.34	103.58	4.34
0.91	0.35	120.67	4.81
1.06	0.35	140.58	5.32
1.24	0.37	163.77	5.86
1.44	0.39	190.80	6.25
1.68	0.43	222.28	6.28
1.95	0.48	258.95	5.76
2.28	0.55	301.68	4.61
2.65	0.62	351.46	2.90
3.09	0.71	409.45	1.19
3.60	0.80	477.01	0.00
4.19	0.89	555.71	0.00
4.88	0.99	647.41	0.00
5.69	1.08	754.23	0.00

Table B.27 Particle size distribution of hydrothermal-treated 0.5% W/TiO₂.

рН	Zeta potential
2	29.50
3	23.70
3.5	-4.03
4	-19.00
5	-25.80
6	-27.70
7	-27.90
8	-26.80
9	-30.50
10	-29.10
11	-30.30
12	-27.60

Table B.28 Point of zero charge determination by zeta potential method of undoped TiO₂.

рН	Zeta potential
2	13
3	16.7
3.5	5.9
3.84	-10.9
4	-11.1
5	-22.9
6	-23.9
7	-26.2
8	-28.9
9	-26.9
10	-36.1
11	-37.4

Table B.29 Point of zero charge determination by zeta potential method of 0.5%W/TiO₂.

рН	Zeta potential
2	29.5
3	23.7
3.5	-4.03
4	-19
5	-25.8
6	-27.7
7	-27.9
8	-26.8
9	-30.5
10	-29.1
11	-30.3
12	-27.6

Table B.30 Point of zero charge determination by zeta potential method of hydrothermal-treated 0.5%W/TiO₂.

Undoped TiO ₂				
P/P ₀	Volume	P/P ₀	Volume	
Adsorption		Deso	rption	
0.0577	53.6081	0.8995	114.7889	
0.0792	57.1624	0.7920	113.6731	
0.1043	60.6064	0.6914	112.7534	
0.1501	65.8068	0.5920	111.5669	
0.2008	70.5686	0.4984	107.9111	
0.2515	74.8686	0.3994	86.5709	
0.3021	78.8553	0.2922	78.0865	
0.4077	86.7019	0.1917	69.7797	
0.5074	94.0329	0.0932	59.2656	
0.6074	101.3778			
0.7074	108.1806	1		
0.7997	112.5729			
0.9054	114.7032			
0.9939	119.1955	24		

Table B.31 Adsorption and desorption isotherm of undoped TiO₂.





0.5%W/TiO ₂				
P/P ₀	Volume	P/P ₀	Volume	
Adsorption		Desor	rption	
0.0584	48 <mark>.4500</mark>	0.8912	72.1616	
0.0809	51.0233	0.7907	71.7073	
0.1062	53.3616	0.6905	71.3053	
0.1537 🛁	56.7333	0.5903	70.8165	
0.2049	59.4814	0.4912	69.9118	
0.2564	61.6584	0.3999	65.9122	
0.3074	63.3747	0.2958	62.9700	
0.4052	6 <mark>5.8</mark> 904	0.1980	59.1343	
0.5065	67.7624	0.0909	52.0524	
0.6070	<mark>6</mark> 9.3688			
0.7075	70.7484			
0.8083	71.6806			
0.9089	72.2882			
0.9967	80.9749			

Table B.32 Adsorption and desorption isotherm of 0.5%W/TiO₂.



Figure B.2 Adsorption and desorption isotherm of 0.5%W/TiO2.

hydrothermal-treated 0.5%W/TiO ₂				
P/P ₀	Volume	P/P ₀	Volume	
Adsorption		Deso	rption	
0.0510	58.0385	0.9005	211.0169	
0.0771	63.7190	0.7931	208.8683	
0.1032	68.6185	0.6930	206.9103	
0.1580	77.6586	0.5947	204.1074	
0.1999	83.9810	0.5038	149.9670	
0.2577	92.4298	0.3961	113.6686	
0.2995	98.5467	0.2975	98.1910	
0.3992	114.2499	0.1954	83.2356	
0.5038	133.7554	0.0949	67.0282	
0.5994	155.9137			
0.7014	184.0976			
0.8015	206.0261			
0.9013	210.9596			
0.9928	217.0818			

Table B.33 Adsorption and desorption isotherm of hydrothermal-treated 0.5%W/TiO₂.



Figure B.3 Adsorption and desorption isotherm of hydrothermal-treated 0.5%W/TiO₂.

BIOGHAPHY

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