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APPENDIX

CORRELATIONS FOR OIL AND GAS PROPERTIES

The correlations used for determining properties of oil and gas for the simulation study in this work are included in this appendix. The following is the detail of those correlation. It includes the development of each correlation and limitation to each correlation is included if available.

Bubble point pressure correlation

Standing's correlation¹⁷ for estimating bubble point pressure of oil is used in this work. His correlation was based on 105 oil samples from California. The average error of the correlation to the actual data from the samples was 4.8% and 106 psi. The correlation is as follows.

$$p_b = 18(R_{sb} / \gamma_g)^{0.83} \times 10^{y_g}$$

where

y_g = mole fraction gas

$$= 0.00091 (T_R) - 0.0125 \gamma_{API}$$

p_b = bubble point pressure, psia,

R_{sb} = solution gas oil ratio at $p \geq p_b$, SCF/STB,

γ_g = gas gravity (air = 1.0),

T_R = reservoir temperature, °F,

γ_{API} = stock-tank oil gravity, °API

Solution gas oil ratio for saturated oil

For the pressure point below initial bubble point pressure of oil in the reservoir, the correlation of Standing¹⁷ as follows is used.

$$R_s = \gamma_g (p / 18 \times 10^8)^{1.24}$$

where

R_s = solution gas oil ratio, SCF/STB,

γ_g = $0.00091(T) - 0.0125 \gamma_{API}$,

p = pressure, psia,

γ_g = gas gravity,

γ_{API} = oil gravity, °API

T = Temperature, °F

Oil Formation Volume Factor

The correlation of Standing¹⁷ is used for determining oil formation volume factor in this work. He used the same oil systems used for developing a correlation for determining bubble point pressure correlation. The correlation is of the following form.

$$B_o = 0.972 + 0.000147 F^{1.175}$$

where

$$F = R_s (\gamma_g / \gamma_o)^{0.5} + 1.25T$$

B_o = oil formation volume factor, RB/STB

R_s = solution gas oil ratio, SCF/STB

γ_g = gas gravity, air = 1.0

$$\gamma_o = \text{oil specific gravity} = 141.5/(131.5 + \gamma_{API})$$

T = Temperature, °F

Oil Viscosity

Correlation of Beggs and Robinson¹⁷ is used for determining oil viscosity. The correlation was developed in 1975. More than 2,000 measured data points from 600 oil systems were used for developing the correlation. The equation developed reproduced the measured data with an average error of -1.83% and a standard deviation of 27%. The equation for dead-oil viscosity is

$$\mu_{od} = 10^x - 1.0$$

where

$$x = T^{-1.163} \exp(6.9824 - 0.04658\gamma_{API})$$

μ_{od} = dead - oil viscosity, cp

T = Temperature, °F

γ_{API} = Stock tank oil gravity, °API

To correct for the effect of dissolved gas, the following equation is used.

$$\mu_o = A\mu_{od}^B$$

where

μ_o = saturated-oil viscosity, cp

μ_{od} = dead-oil viscosity, cp

$$A = 10.715 (R_s + 100)^{-0.515}$$

$$B = 5.44(R_s + 150)^{-0.338}$$

R_s = solution gas oil ratio, SCF/STB

Gas Viscosity

Lee, Gonzalez, and Eakin¹⁸ proposed the correlation for predicting gas viscosity as the following form.

$$\mu_g = K \exp (X \rho^Y)$$

where

$$K = (9.4 + 0.02 M) T^{1.5} / (209 + 19M + T)$$

$$X = 3.5 + 986/T + 0.01M$$

$$Y = 2.4 - 0.2 X$$

μ_g = gas viscosity, micropoise

T = absolute temperature, °R

M = molecular mass,

ρ = gas density, g / cm³



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VITAE

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