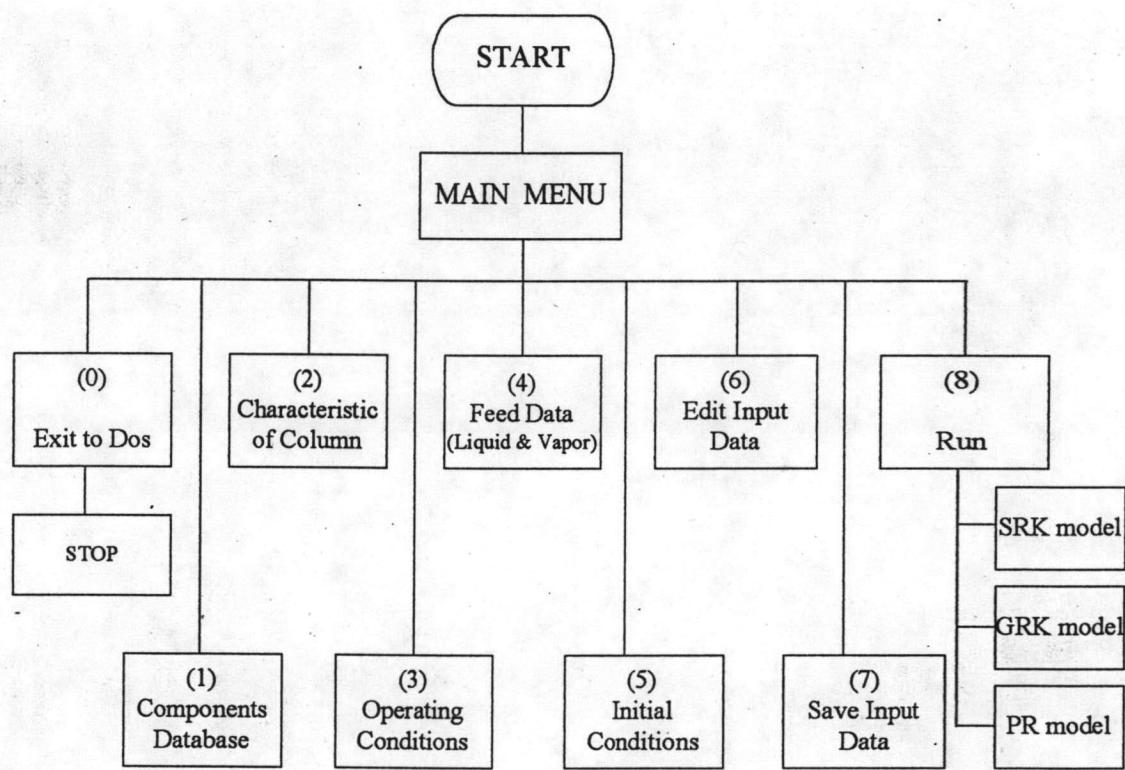


REFERENCE

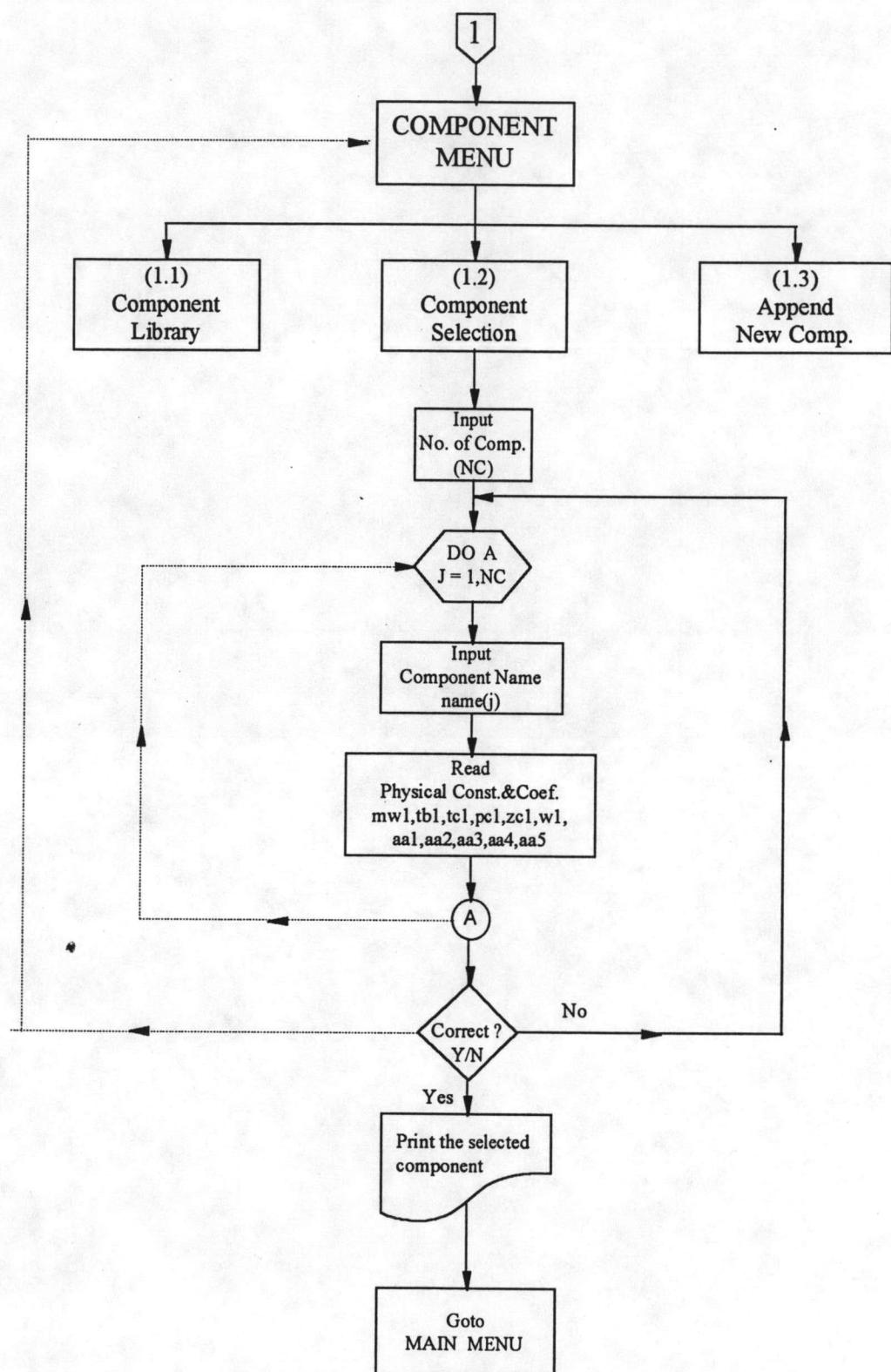
1. Aly Q gncl Ashour I. Thermodynamic Modelling for Oleochemical Industry, European Symopoum on Computer AidedProcess Engineering-2, pp 195–202
2. Dac R. Yang, Kurt V. Waller, Dale E. Sebory and Duncan A. Mellichamp, Dynamic Structural Tranformation for Distillation Control Configuration, AIChE J., vol 36, no. 9, pp 1391-1402, 1990
3. Edmister, W.C., Hydrocarbon Processing ,vol 47, no. 10, pp 145-149, 1968
4. Ernest J. Henley, J.D. Seader, Equilibrium-Stage Separation Operation in Chemical Engineering, John Wiley & sons Inc., New York, 1981
5. Hasan Orbey and J.H. Vera, Correlation for the Third Virial Coefficient Using Tc, Pc and ω As Parameters, AIChE J., vol 29, no. 1, pp 107-113,
6. Hendric C. Van Nees and Michael M. Abbott, Classical Thermodynamics of Nonelectrolyte Solutions, Mc Graw-Hill Book Company, USA, 1984
7. J. Perregard, Model simplification and Reduction for Simulation and Optimization of Chemical Processes, Computer Chem. Engng., vol 17, no. 516, pp 465-483,1993
8. L. Uric, S. Bottini, E.A. Brigde and J.RA Romarnoli, Thermodynamic Tuning in Separation process Simulation and Design, Computer chem. Engng., vol 15 no. 7, 1991
9. Marahiro Kinoshita, Simple Model for Dynamic Simulation of Stage Separation Processes with very Volatile Component, AIChE J., vol 32, no. 5, pp 872-874, 1986
10. Nelson W.L., Petroleum Refinery Engineering, Mc Graw-Hill Book Company, USA, 1982

11. Peng, D.Y., and D.B. Robinson, A new Two-constant Equation of state, Ind. Eng. Chem. Fundam, vol 15, pp 59-64, 1976
12. R. E. Fitymouis, Improving Distillation Column Design Usig Thermodnamic Availability Analysis, AIChE J., vol 26, no. 2, pp 265-273, 1980
13. Roberto De Santis and Biagio Grande, An Equation for Predicting Third Virial Coefficent of Non polar Gases, AIChE J., vol 25, no. 6, pp 931-938, 1979
14. Robert H. Perry and Don Green, Perry's Chemical Engineers, Handbook, sixth edition, McGrow-Hill International Editions, 1984
15. Tomio Umeda, Kayuo Niida and Katsuo Shiroko, Thrmodynamic Appoach to Heat Integration in Distillaion Systems, AIChE J., vol 29, no. 3, pp 423-429, 1979
16. V. R. Dhole and B. Linnhoff, Distillation Column Targets, Computer chem Engng, vol 17, no. 516, pp 549-560, 1993
17. West, E.w., and J. H. Earbar, An Evaluation of Four Methods of Predicting Thermodynamic Properties of Light Hydrocarbon System, Paper presented at the 52 nd Annual Meeting of NPGA, Dallas, Texas, March 26-28, 1973
18. William L. Luyben, Process Modeling, Simulation and Control for Chemical Engineers, Mc Graw-Hill publishing company, Second Edition, 1990
19. Yuji Naka, Masayuki Terashita and Tekuichiro Takamatsu, A Thermodynamic Approach to Multicomponent Distillation System Synthesis, AIChE J., vol 28, no. 5, pp 812-820, 1982
20. Z. T. Fidkowski, M. F. Doherty, and M. F. Malone, Feasibility of Separations for Distillation of Nonideal Ternary Mixtures, AIChE J., vol 39, no. 8, pp 1303-1321, 1993

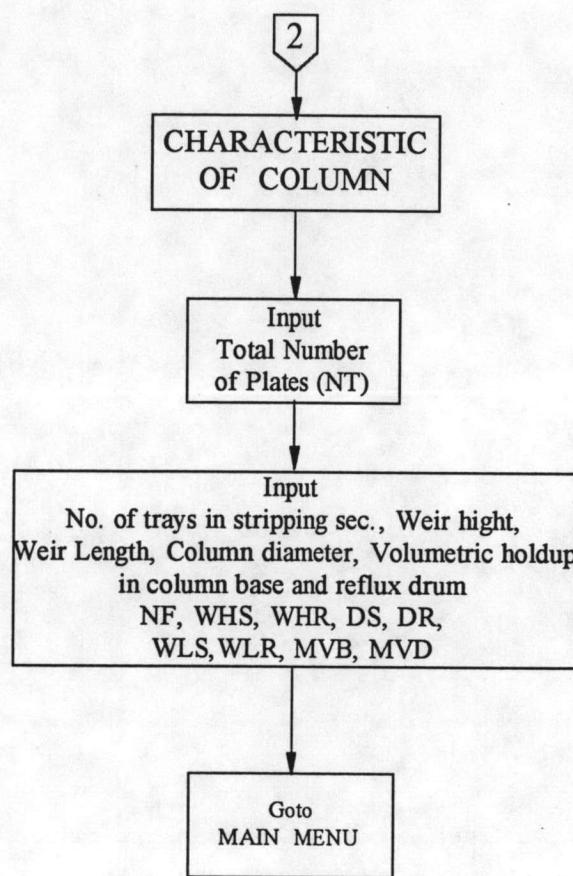
Appendix A
Computer Program Flow Chart



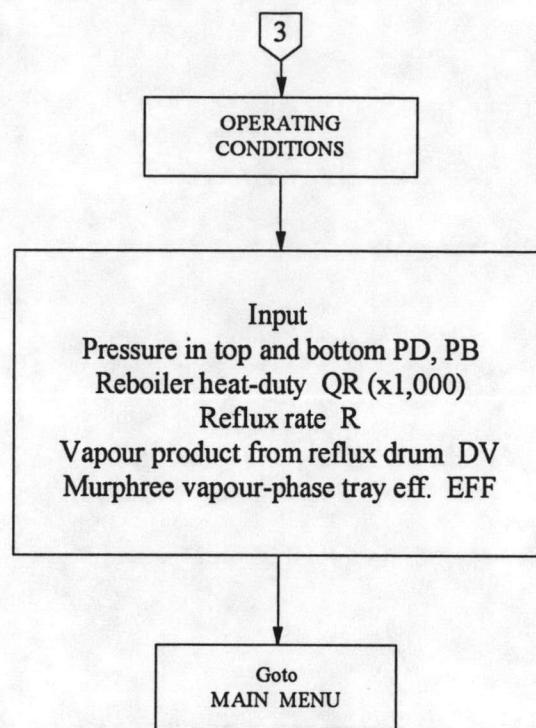
A) Program Structure



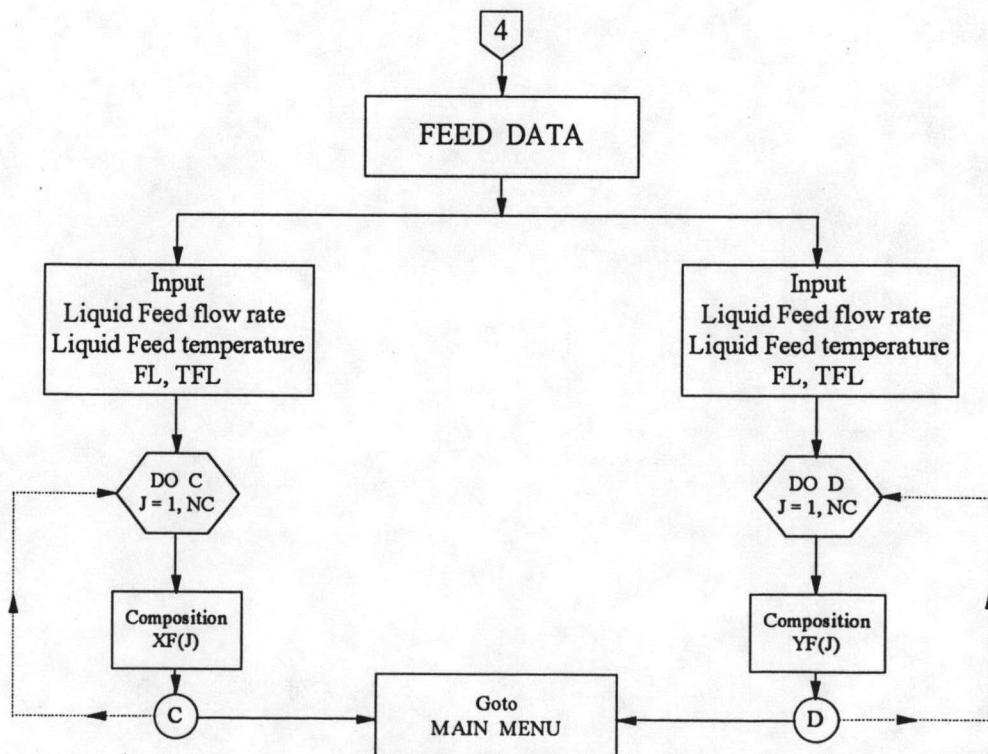
1) Component Database



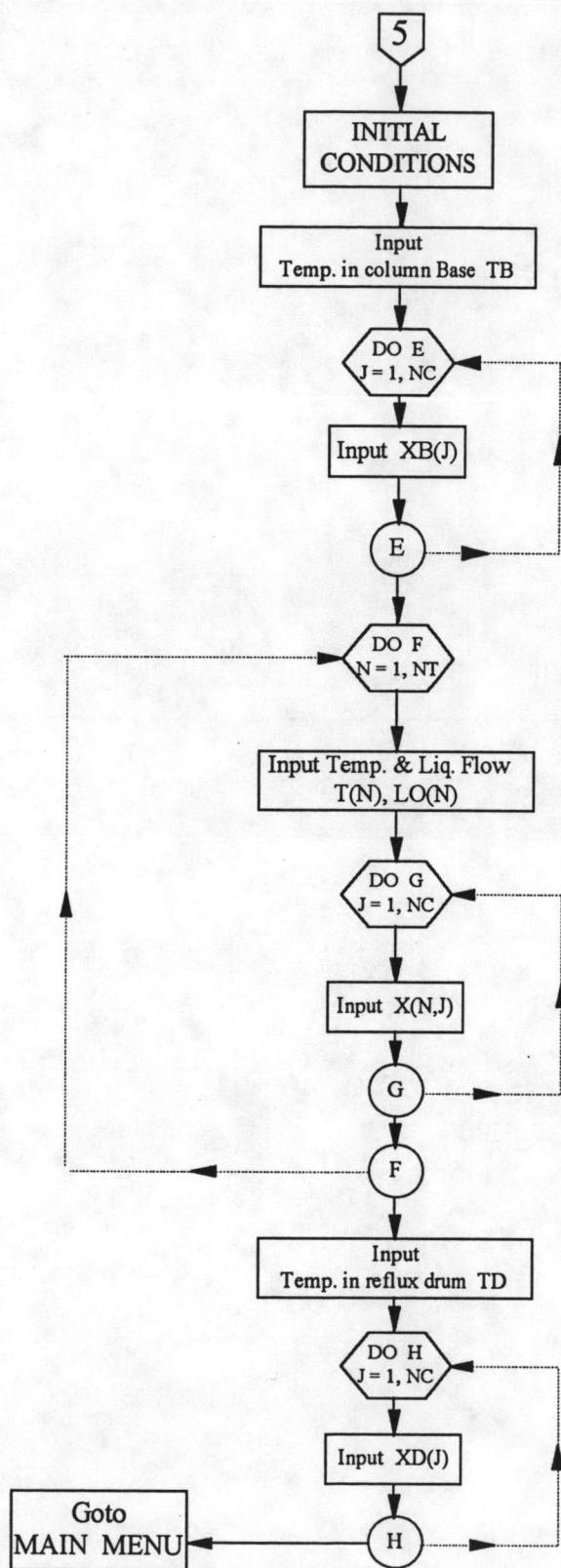
2) Characteristic of Column



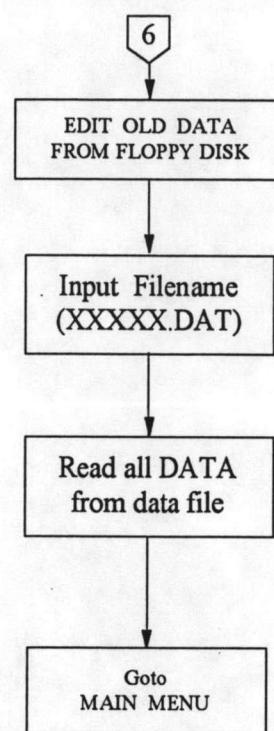
3) Operating Conditions



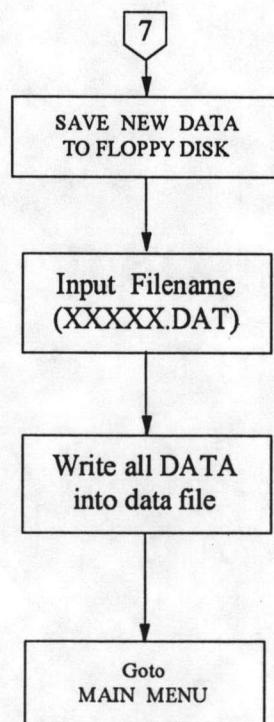
4) Feed Data



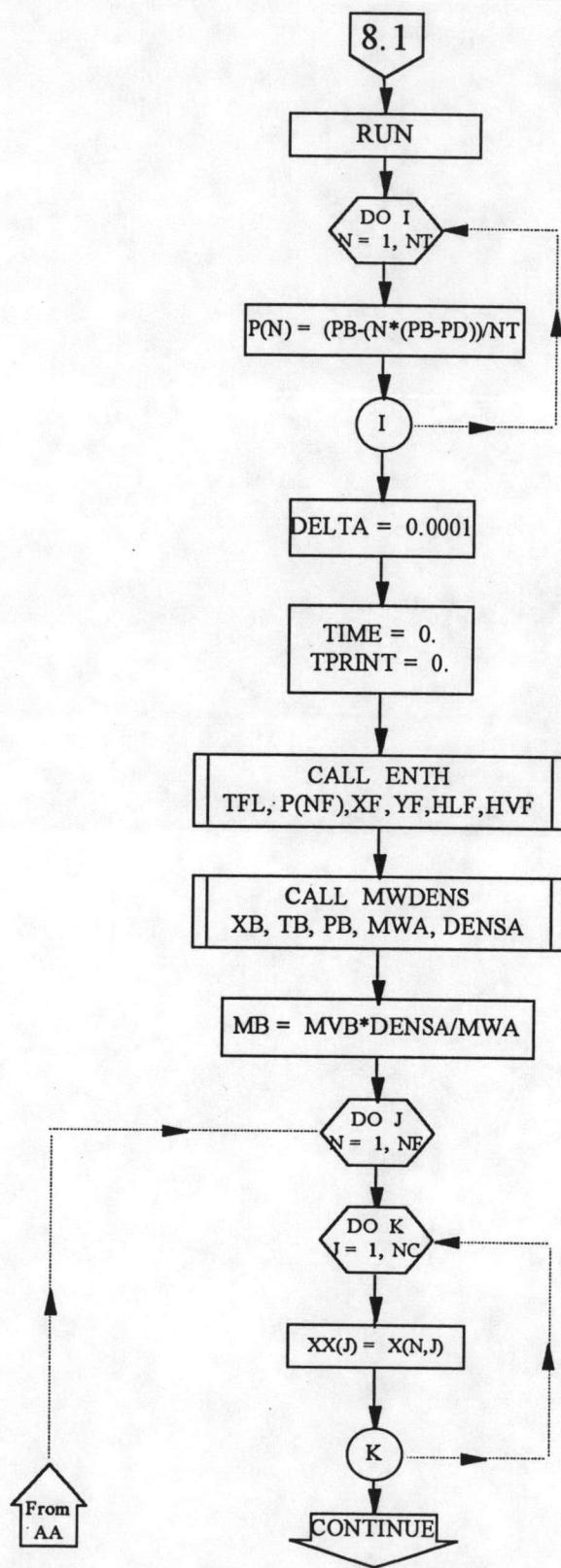
5) Initial Conditions



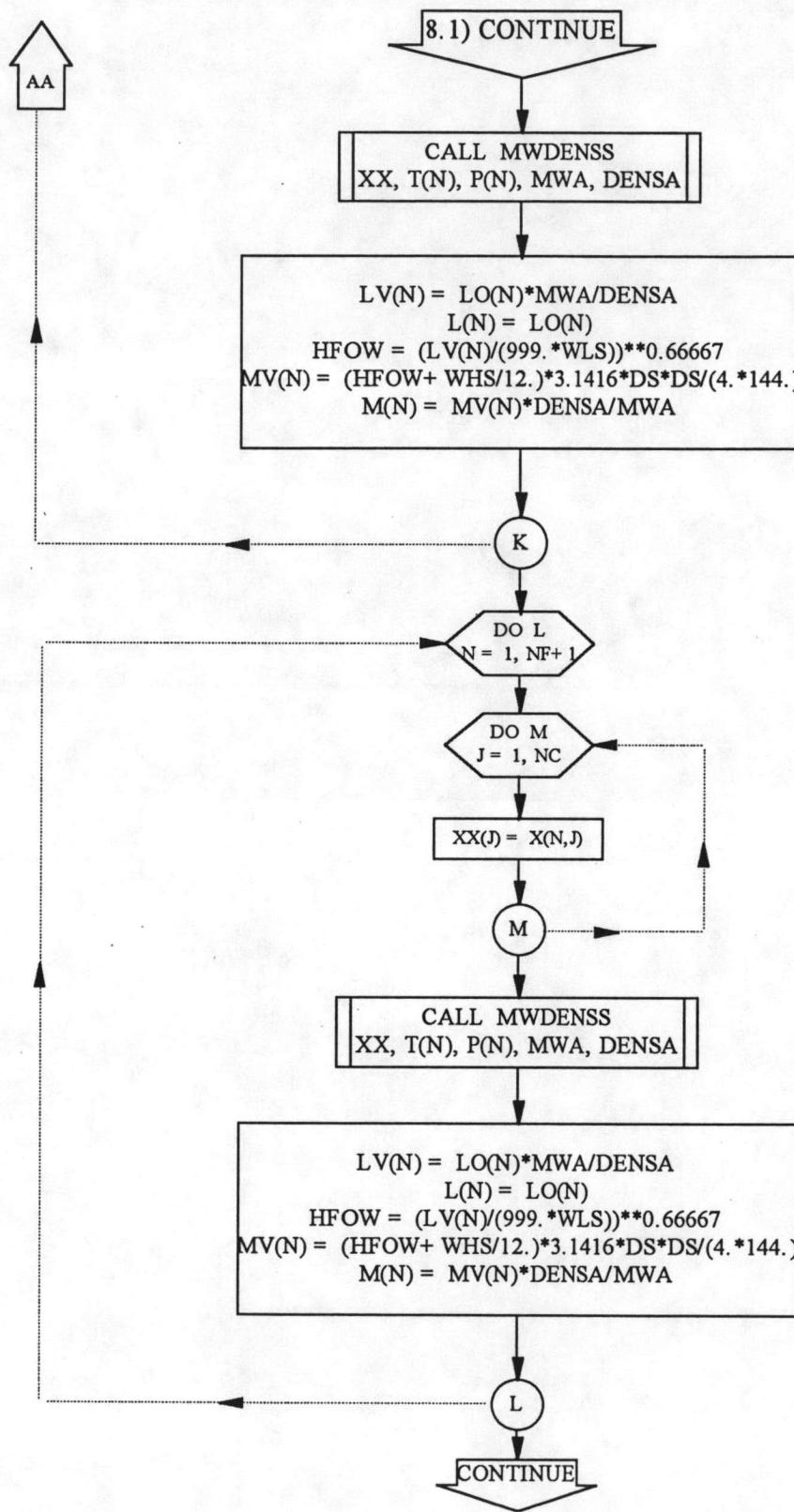
6) Edit Input Data



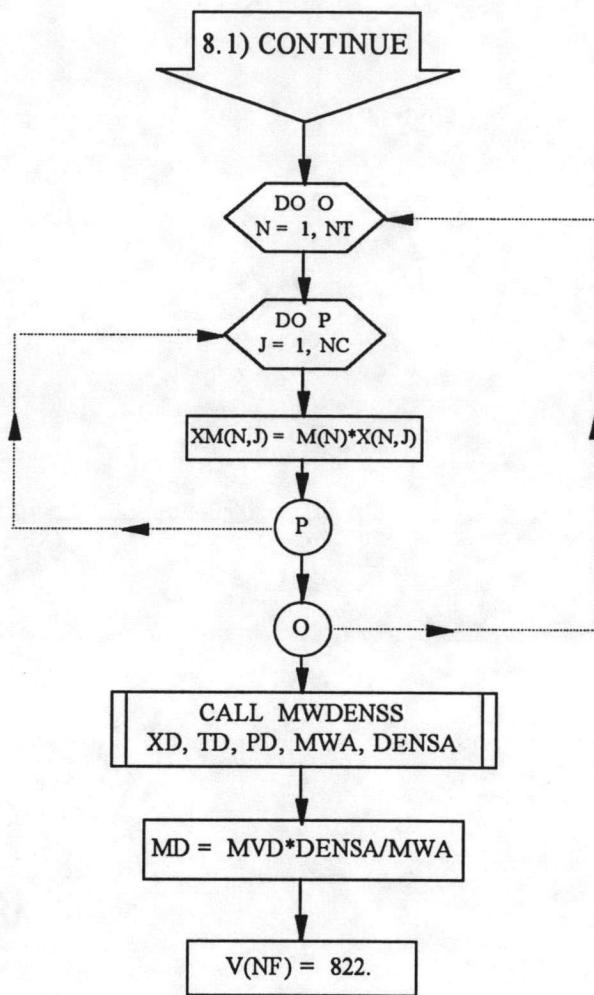
7) Save Input Data



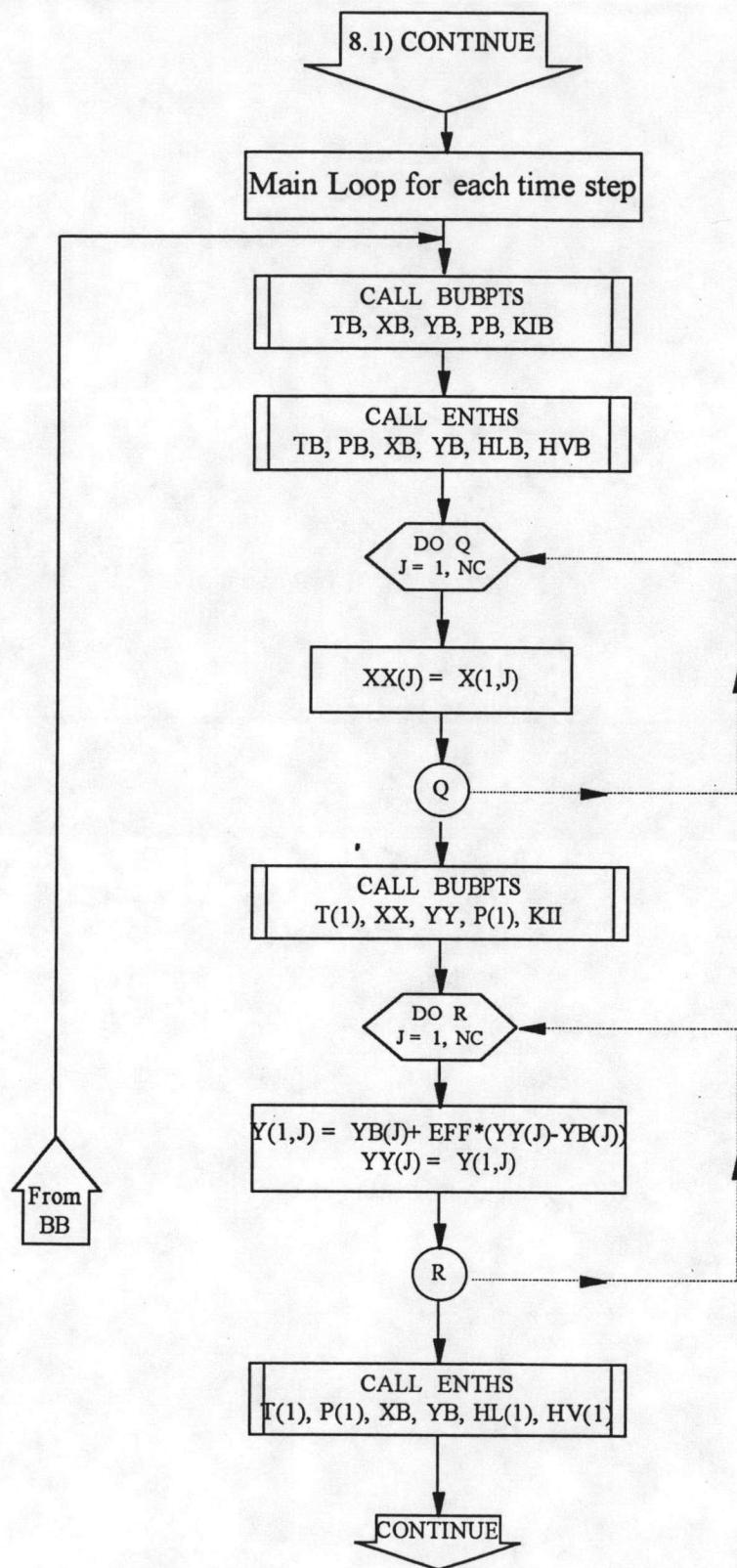
8.1) Running SRK model



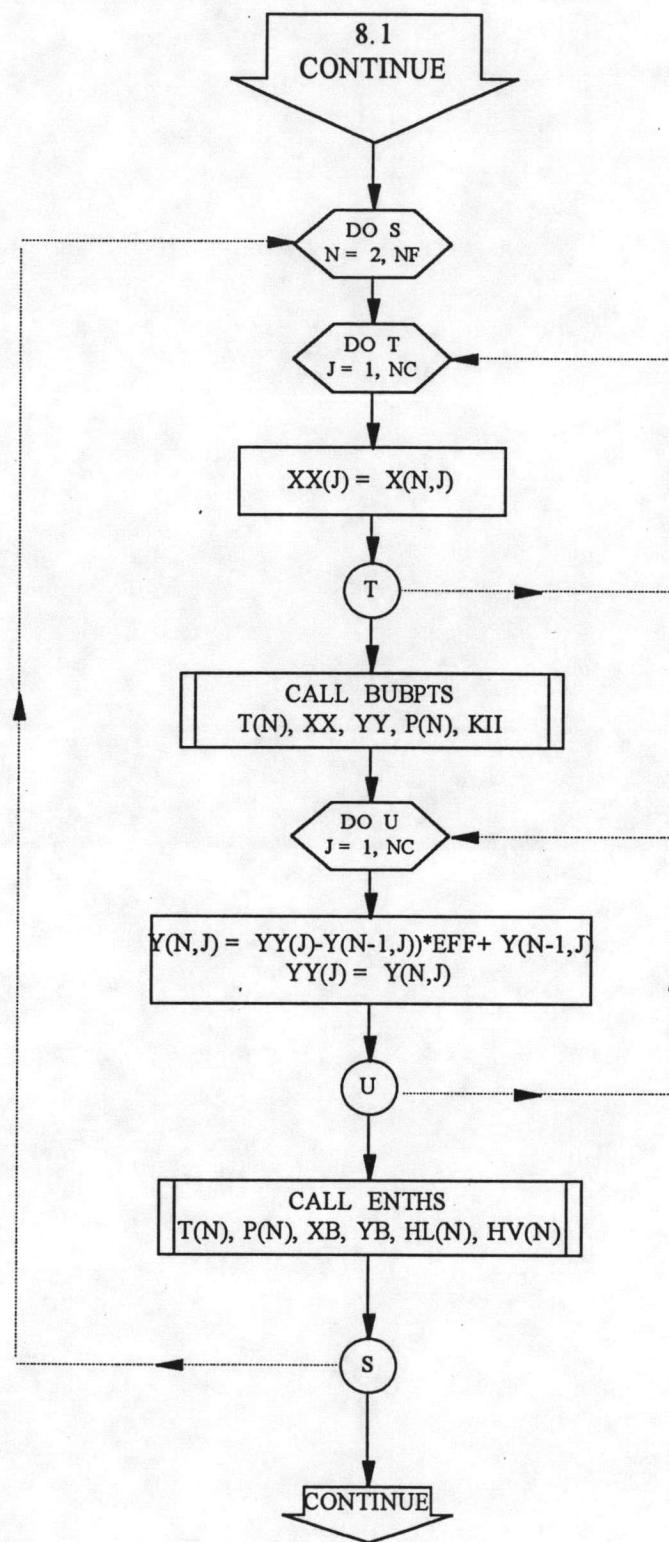
8.1) Running SRK model (Continue)



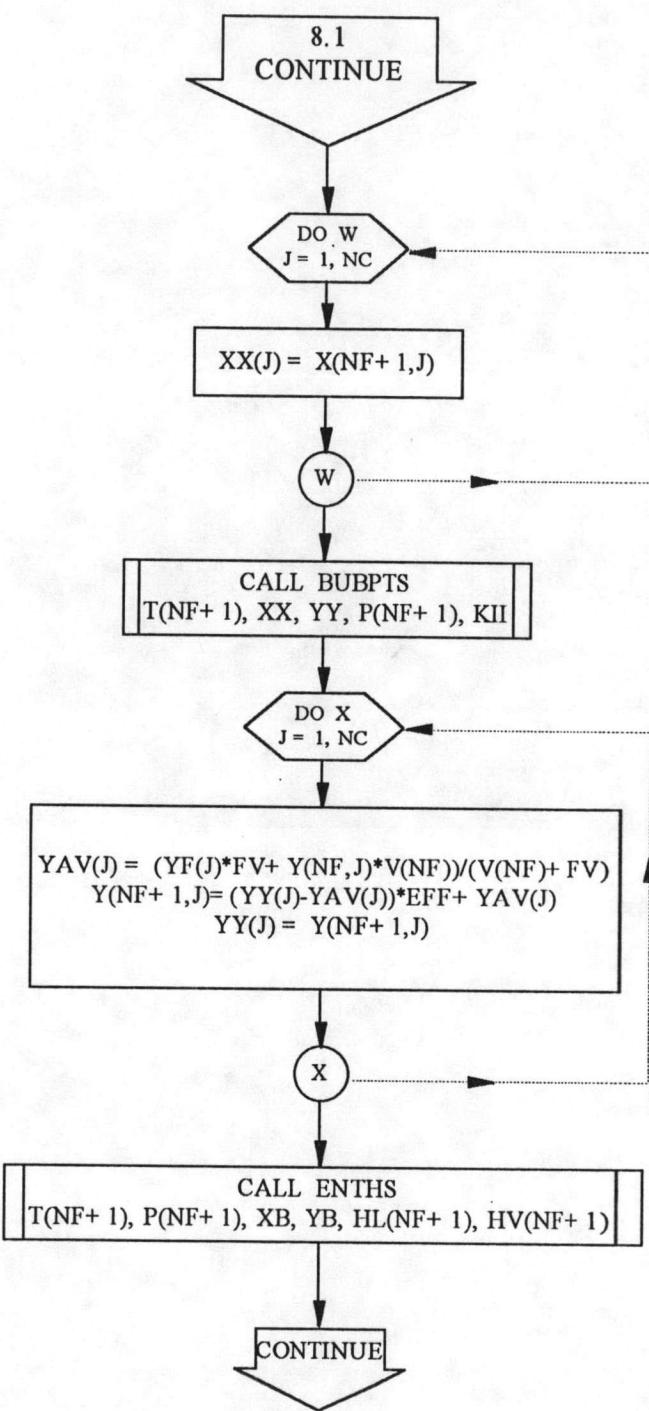
8.1) Running SRK model (Continue)



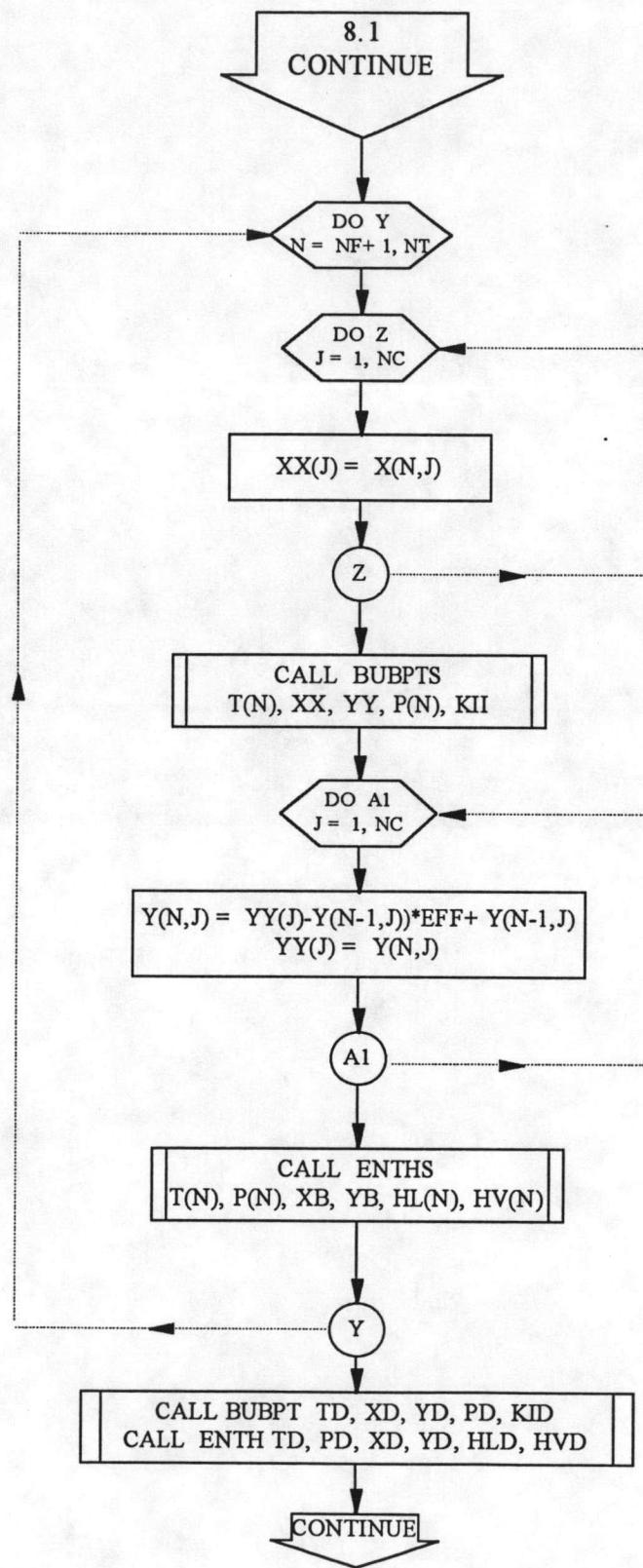
8.1) Running SRK model (Continue)



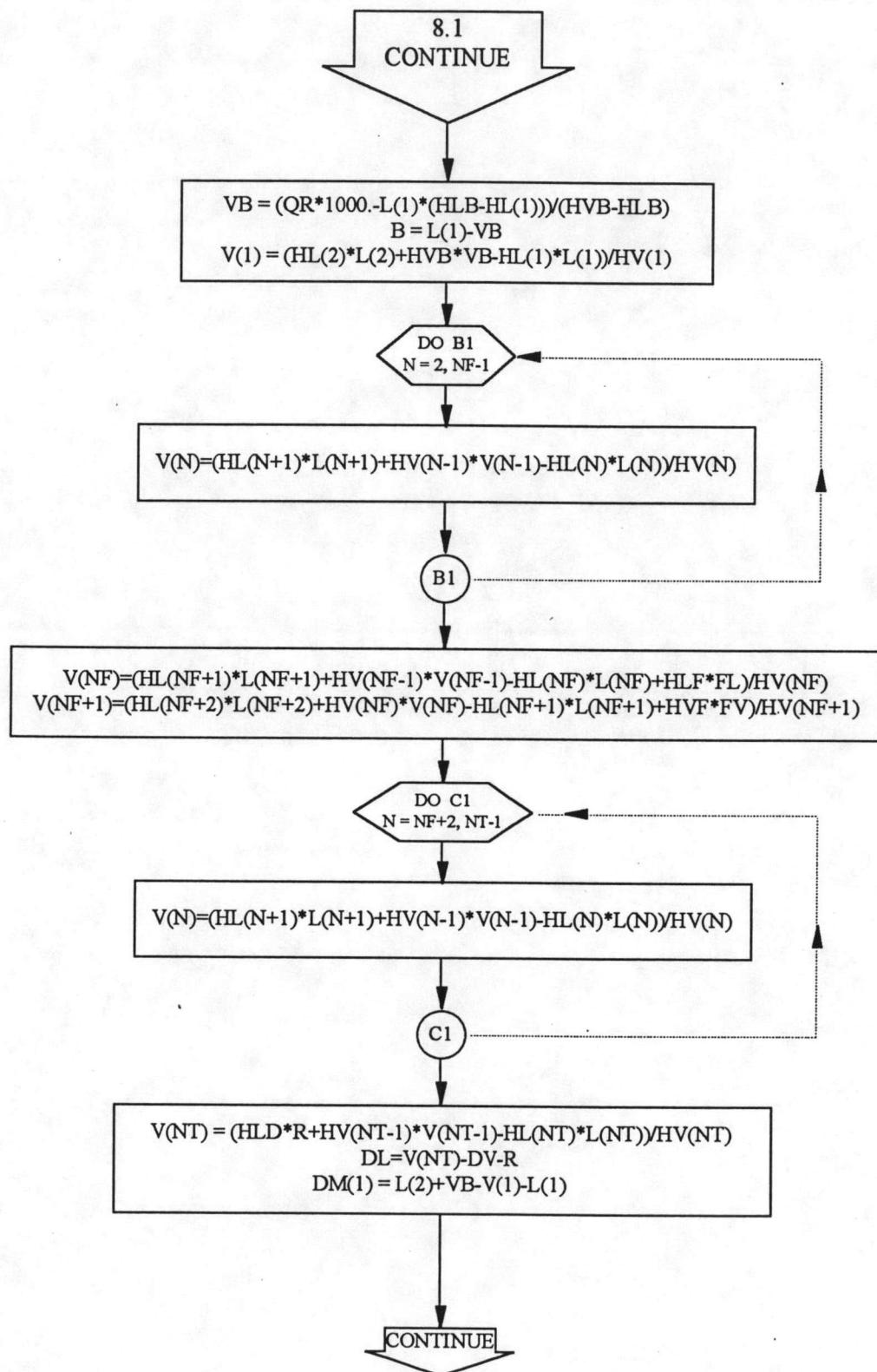
8.1) Running SRK model (Continue)



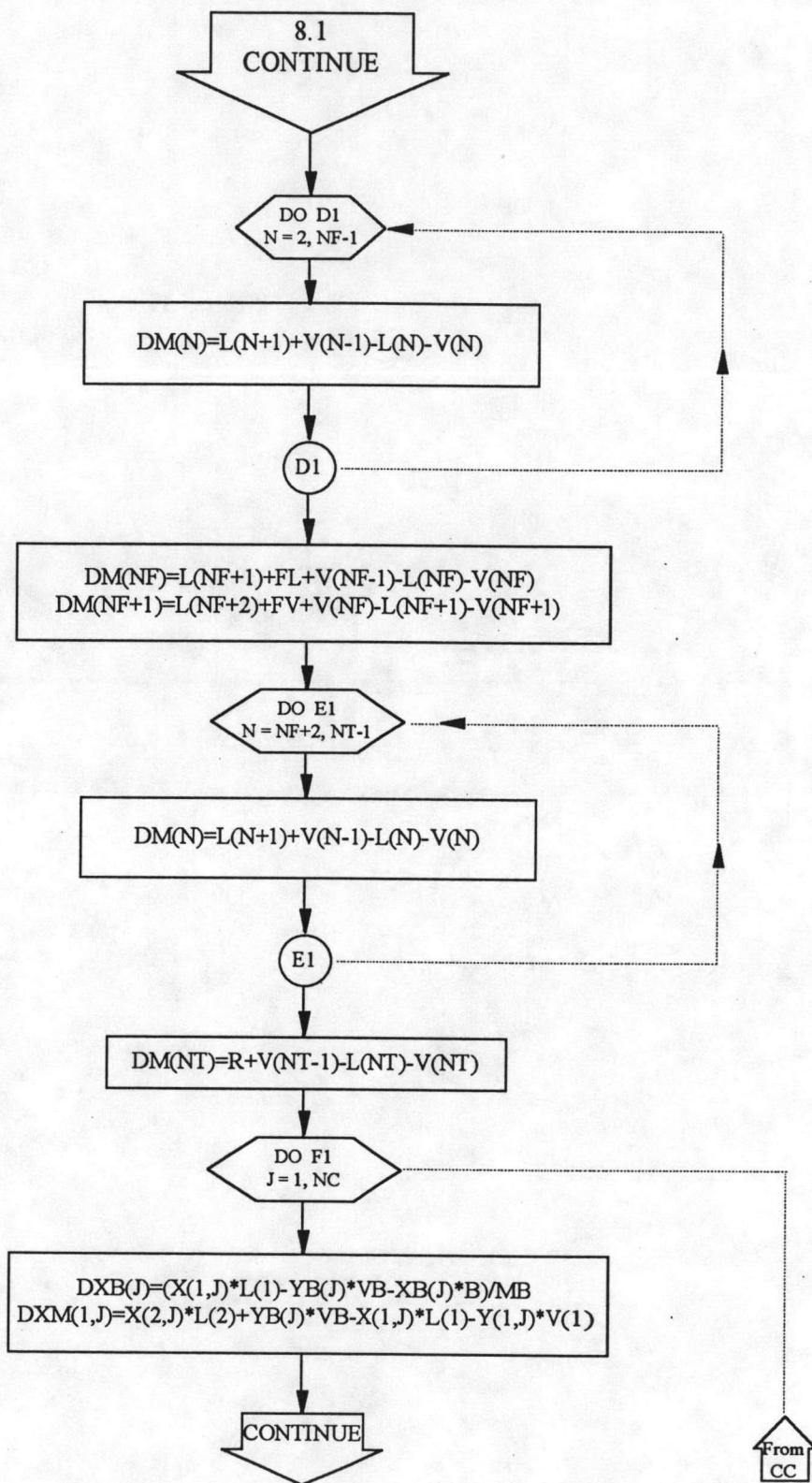
8.1) Running SRK model (Continue)



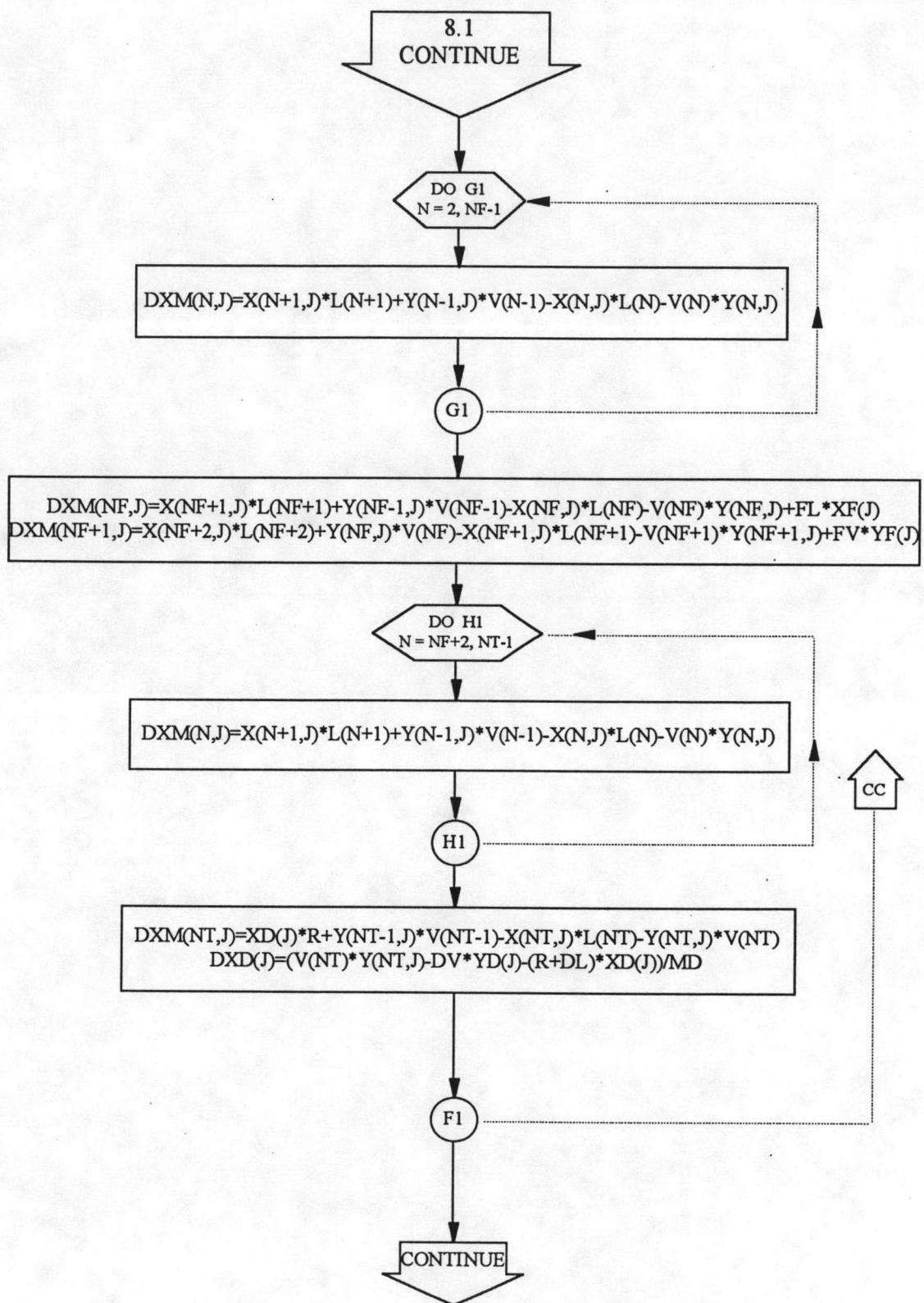
8.1) Running SRK model (Continue)



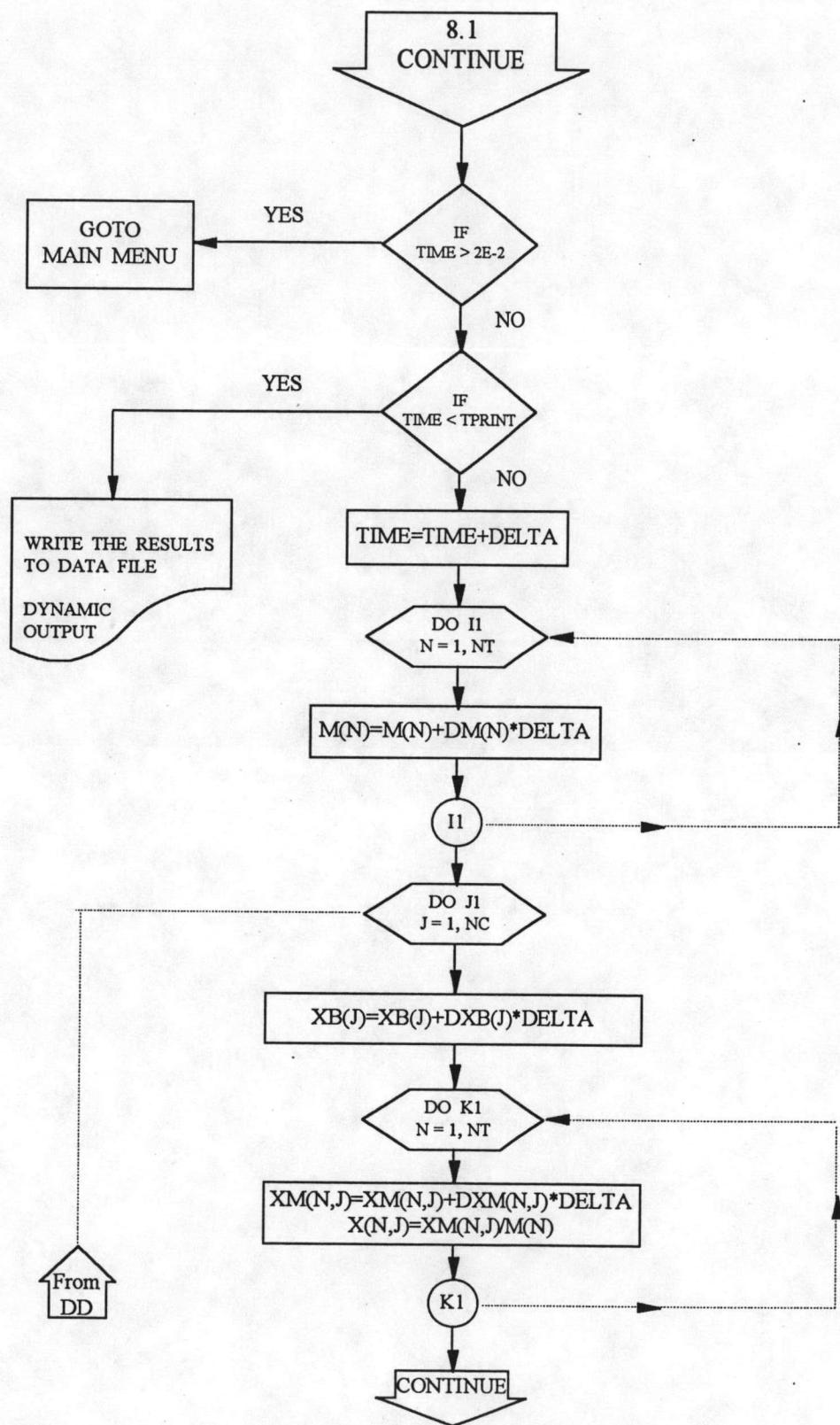
8.1) Running SRK model (Continue)



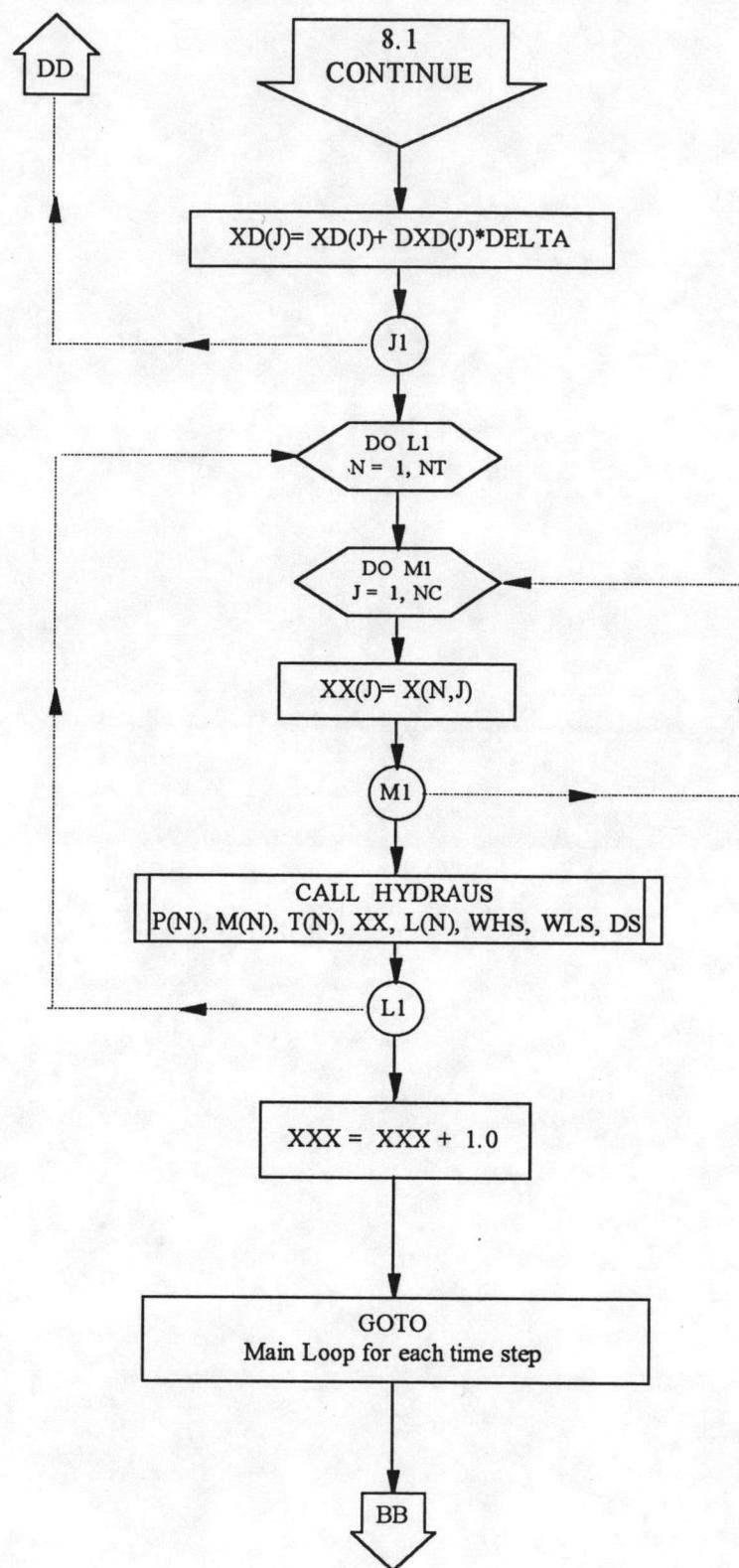
8.1) Running SRK model (Continue)



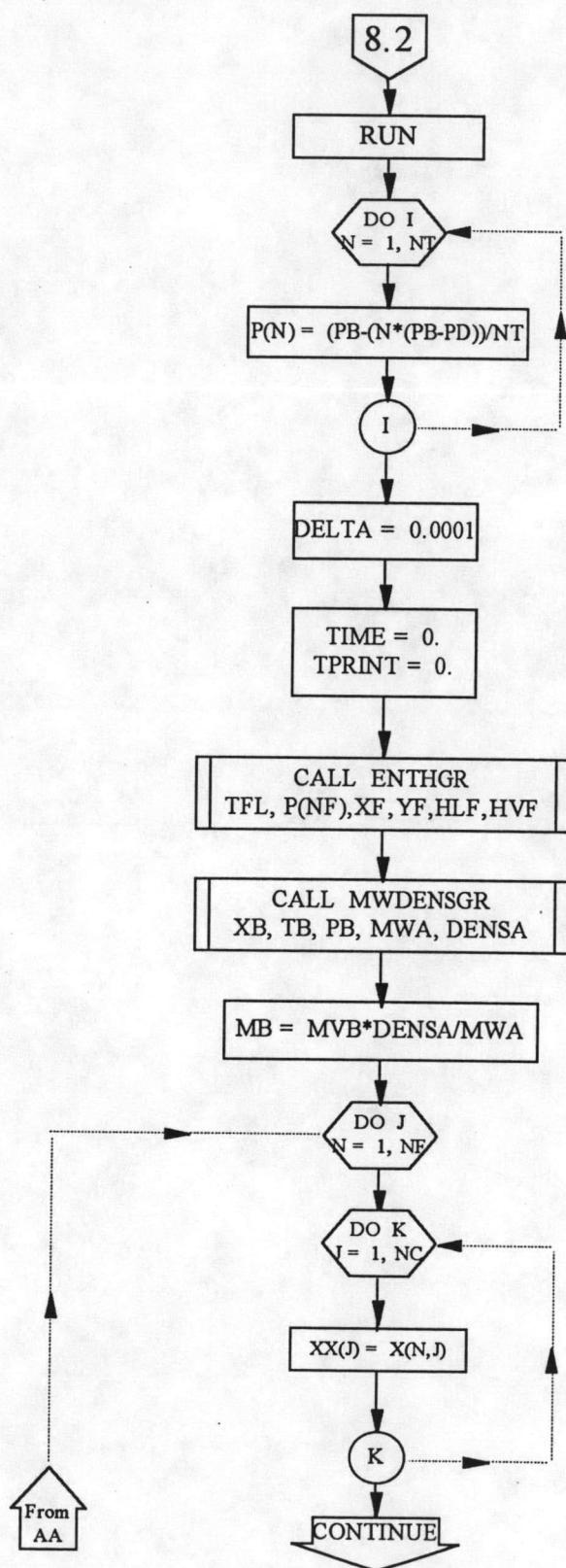
8.1) Running SRK model (Continue)



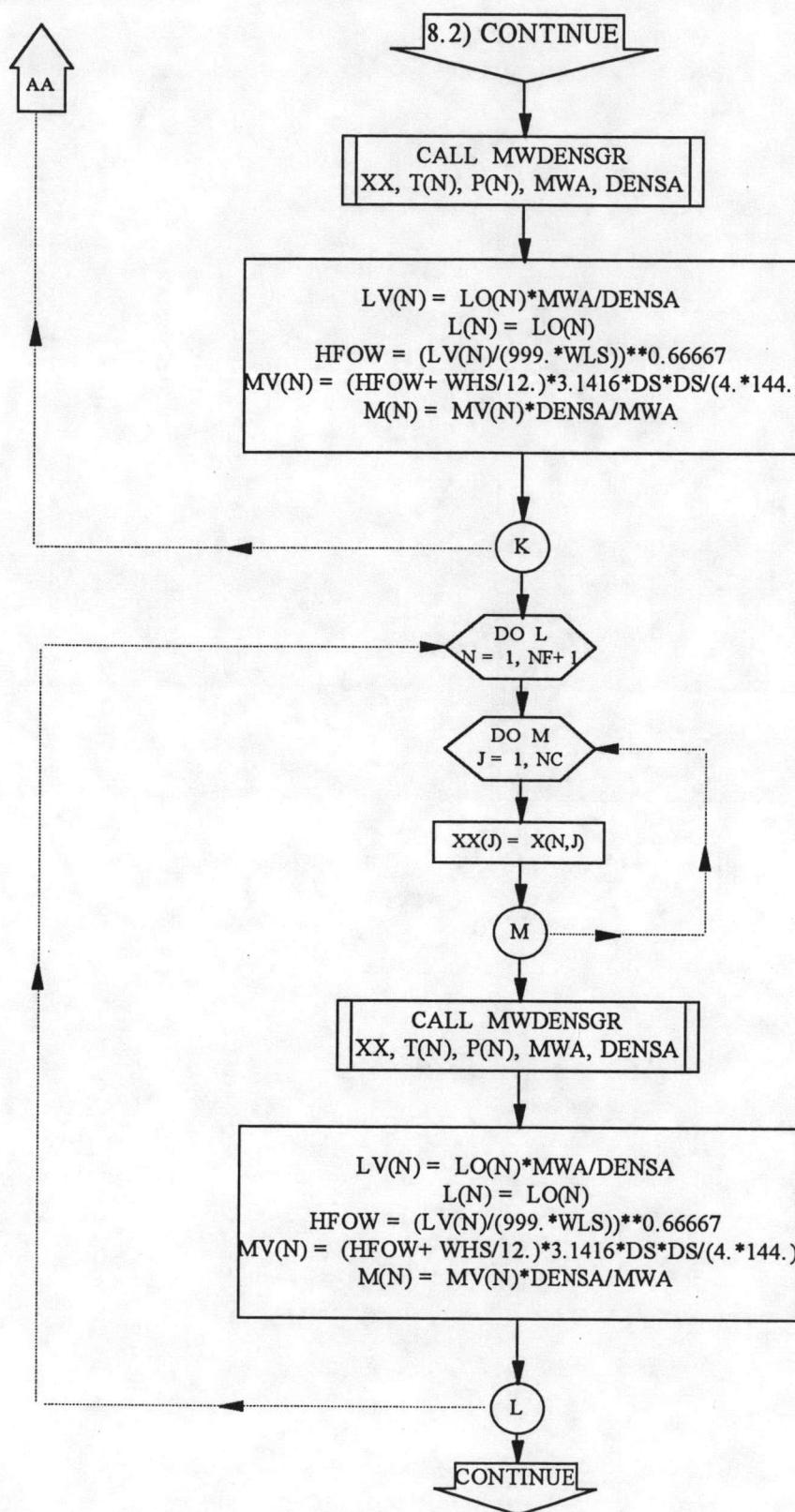
8.1) Running SRK model (Continue)



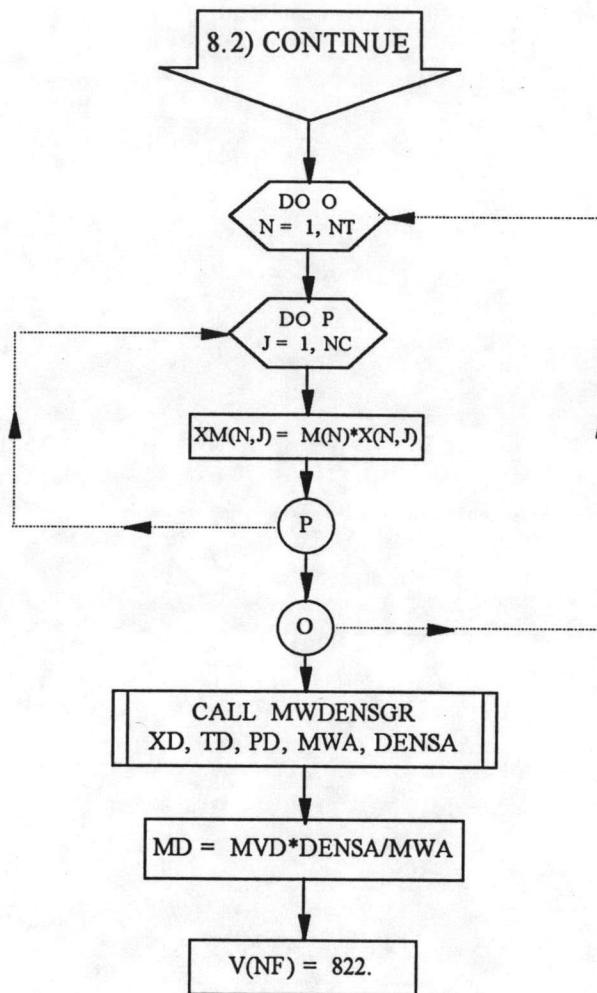
8.1) Running SRK model (Continue)



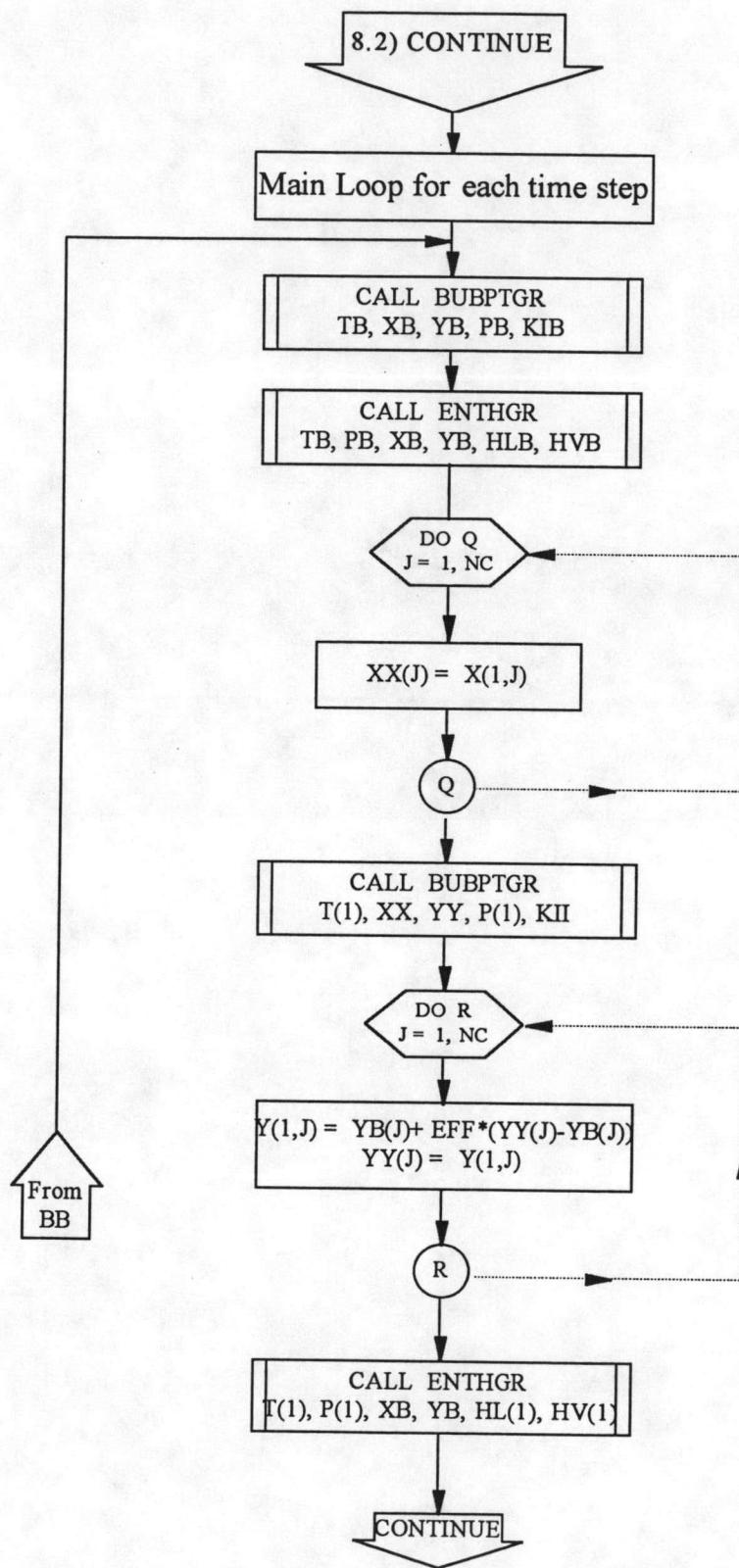
8.2) Running GRK model



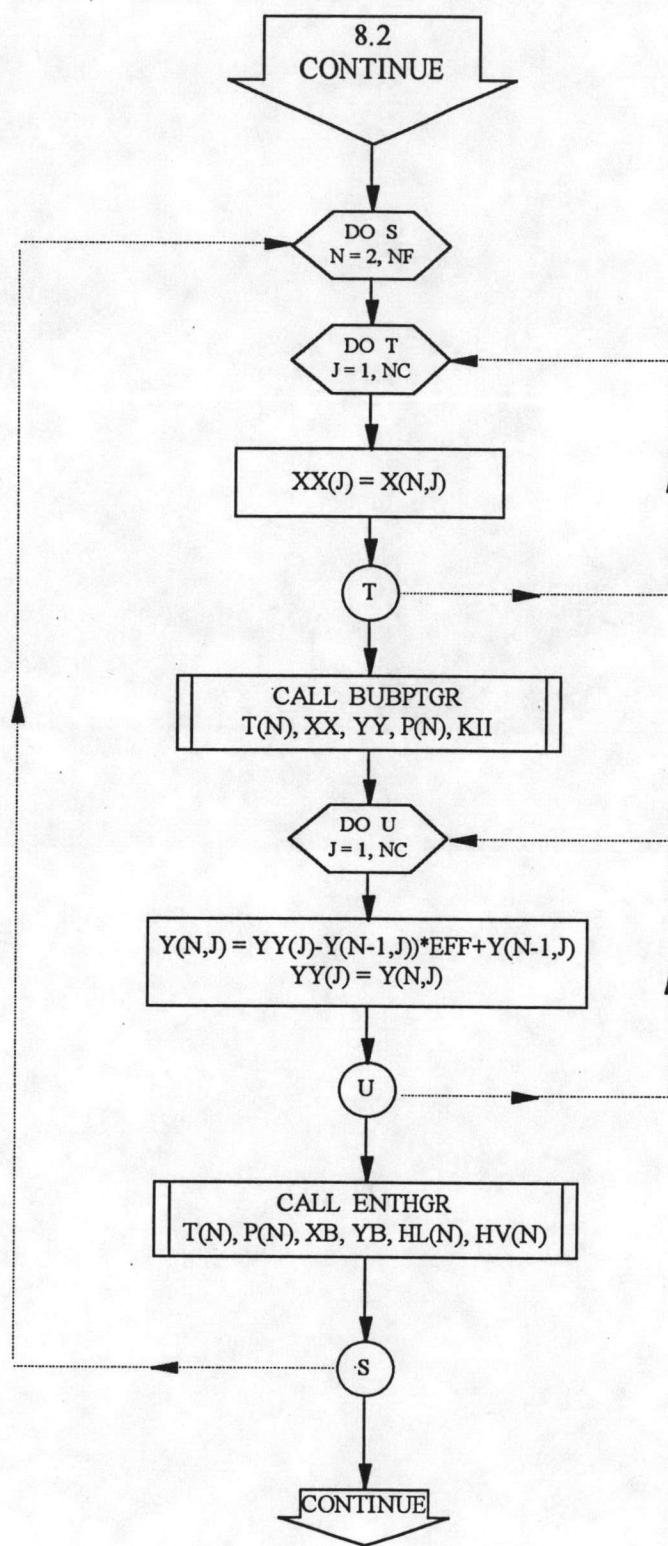
8.2) Running GRK model (Continue)



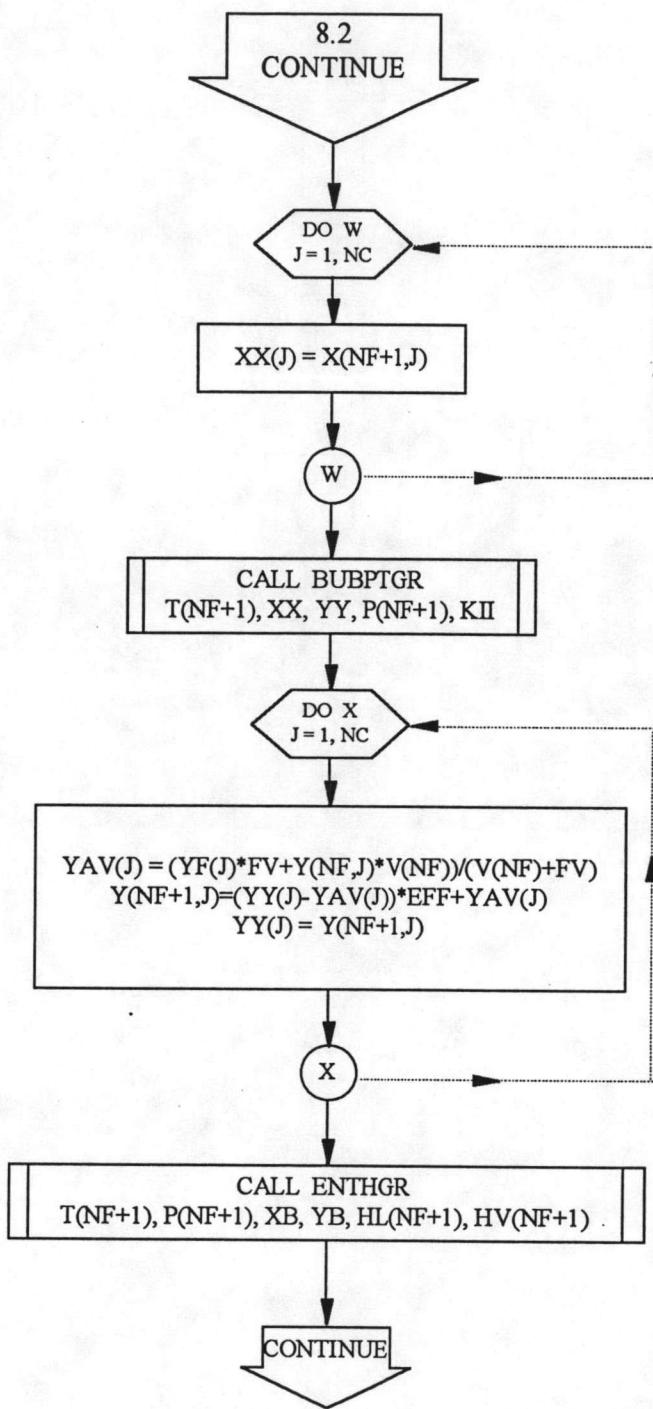
8.2) Running GRK model (Continue)



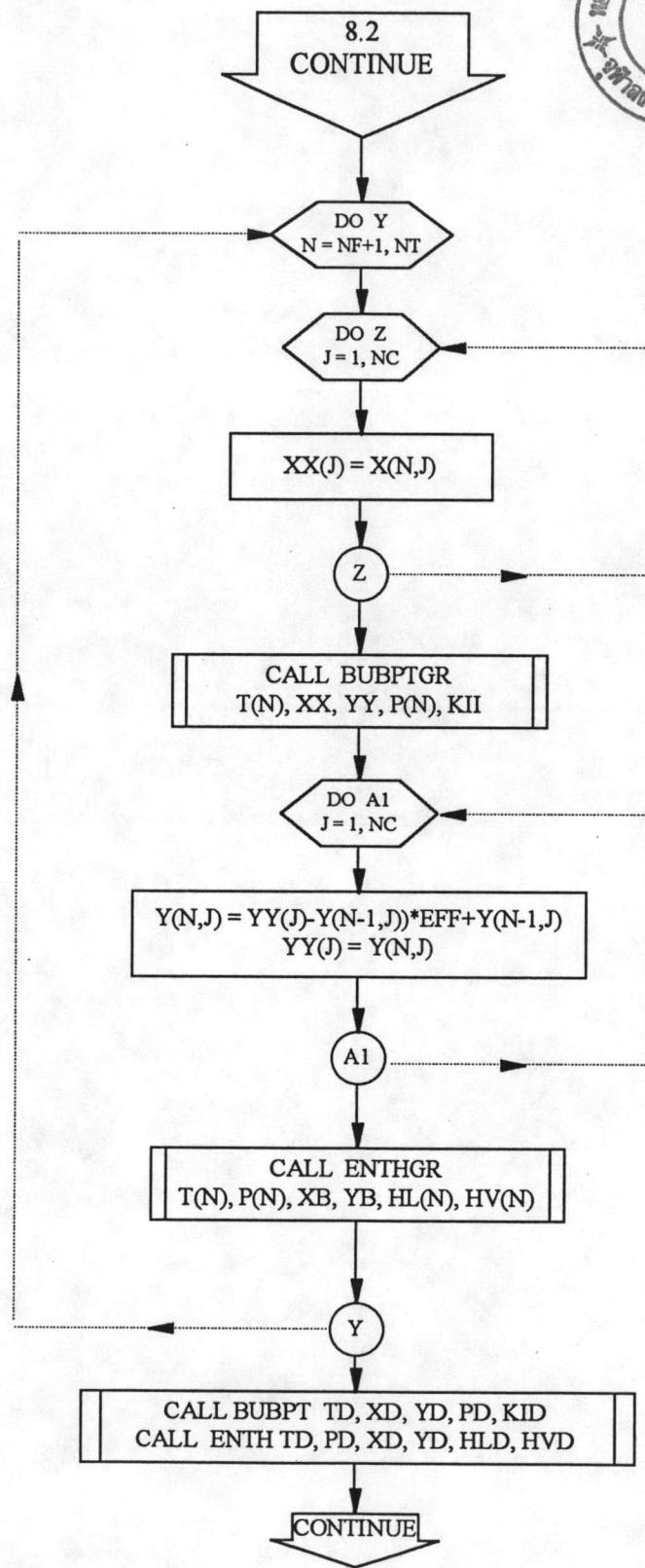
8.2) Running GRK model (Continue)



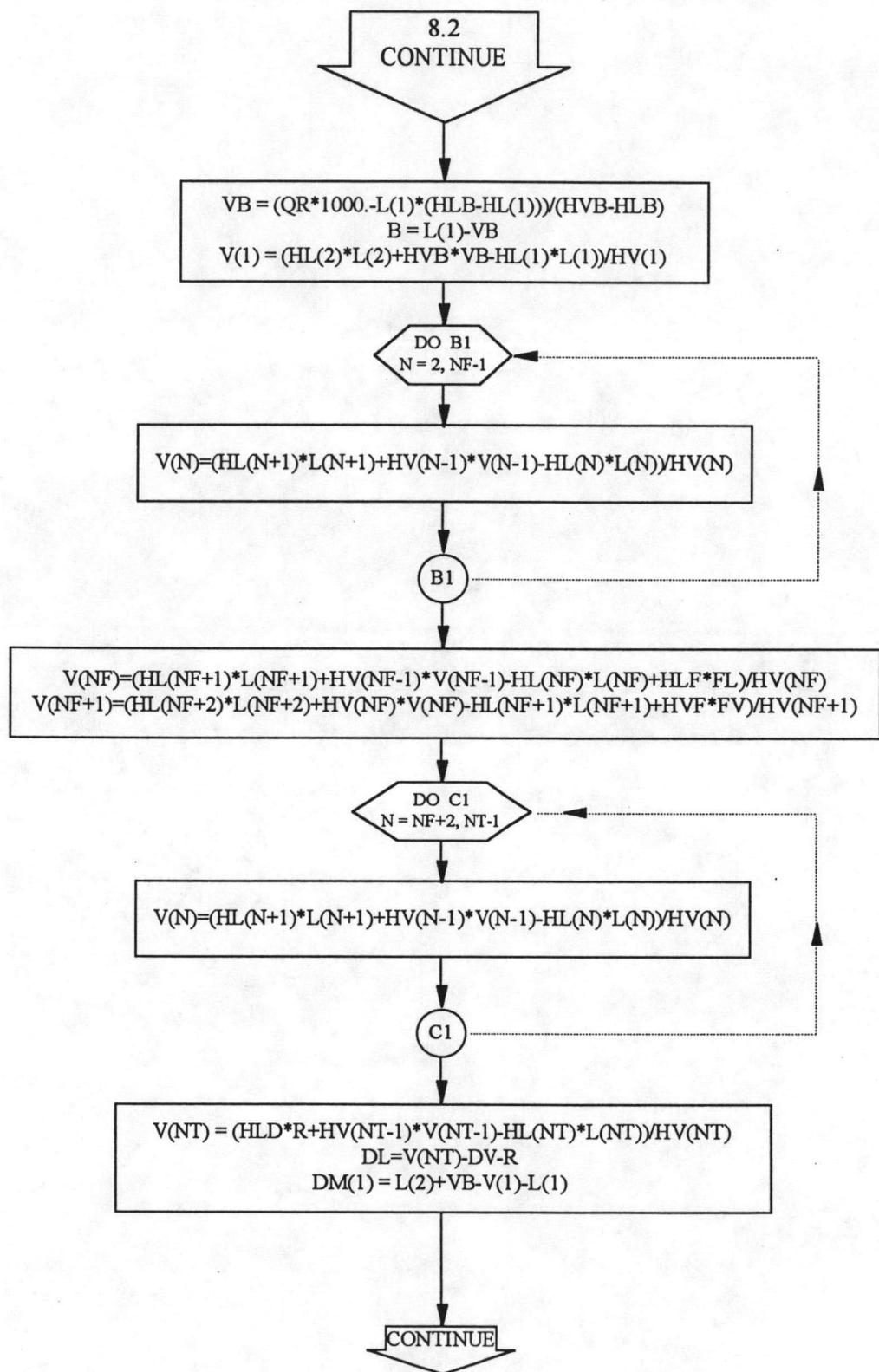
8.2) Running GRK model (Continue)



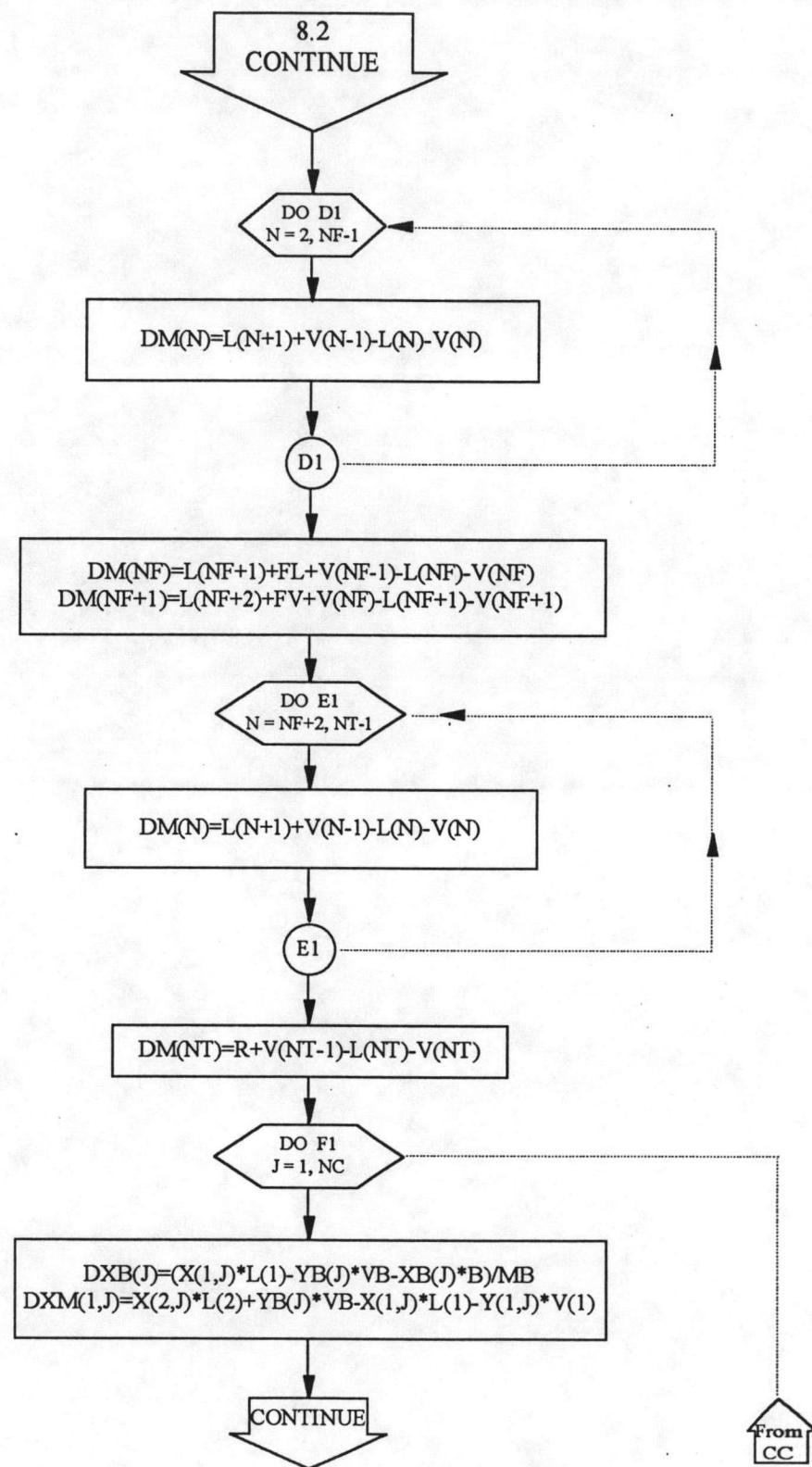
8.2) Running GRK model (Continue)



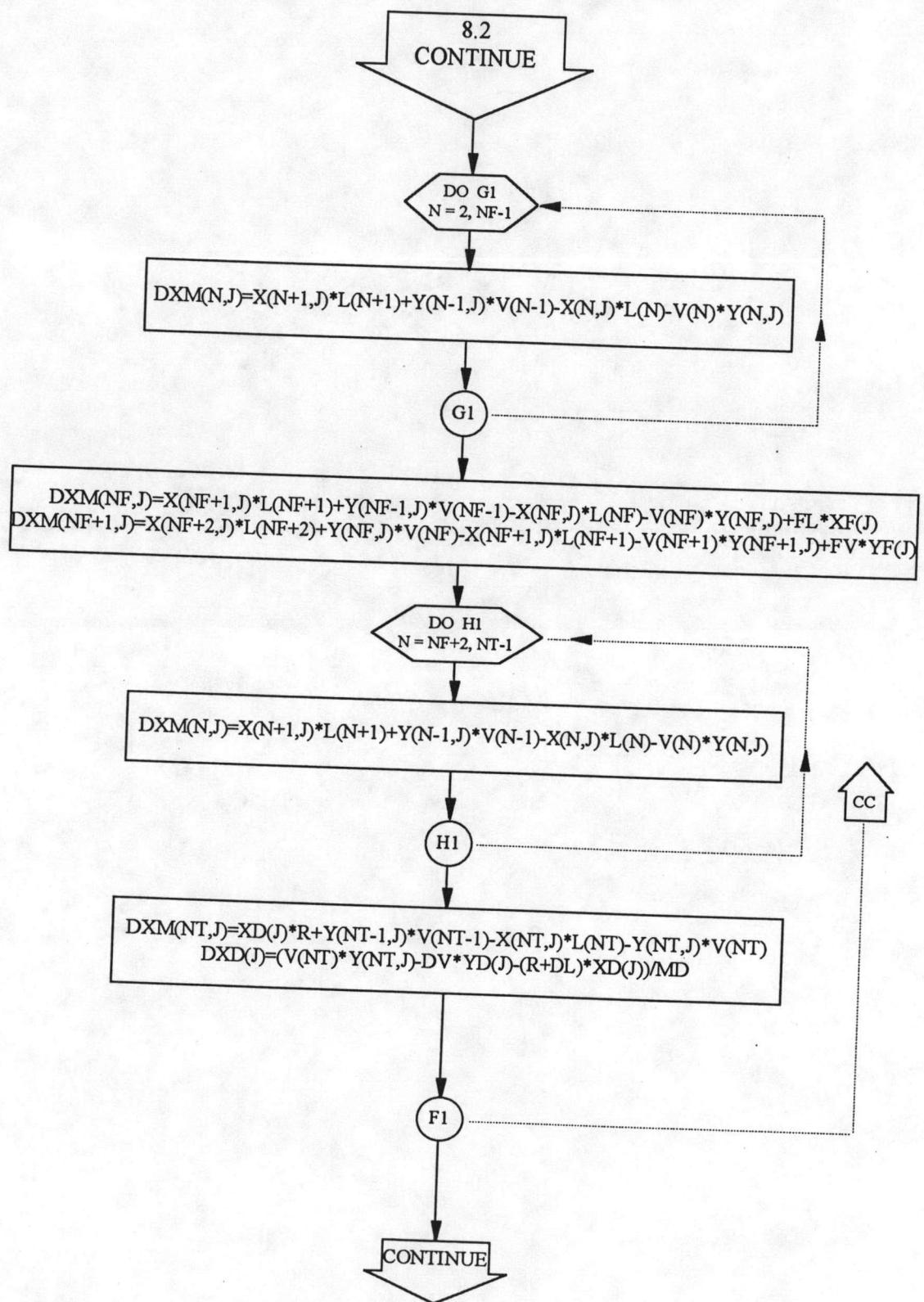
8.2) Running GRK model (Continue)



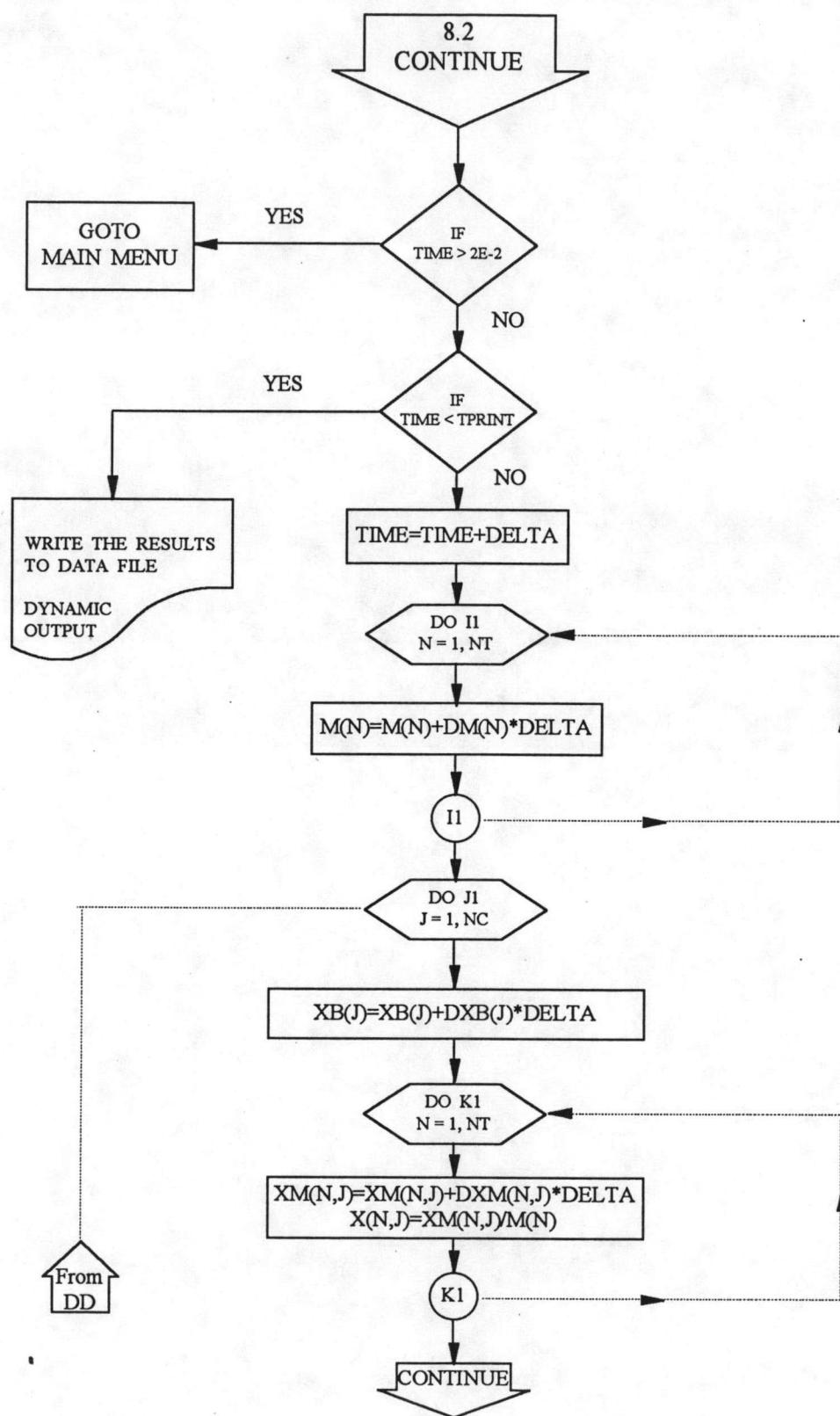
8.2) Running GRK model (Continue)



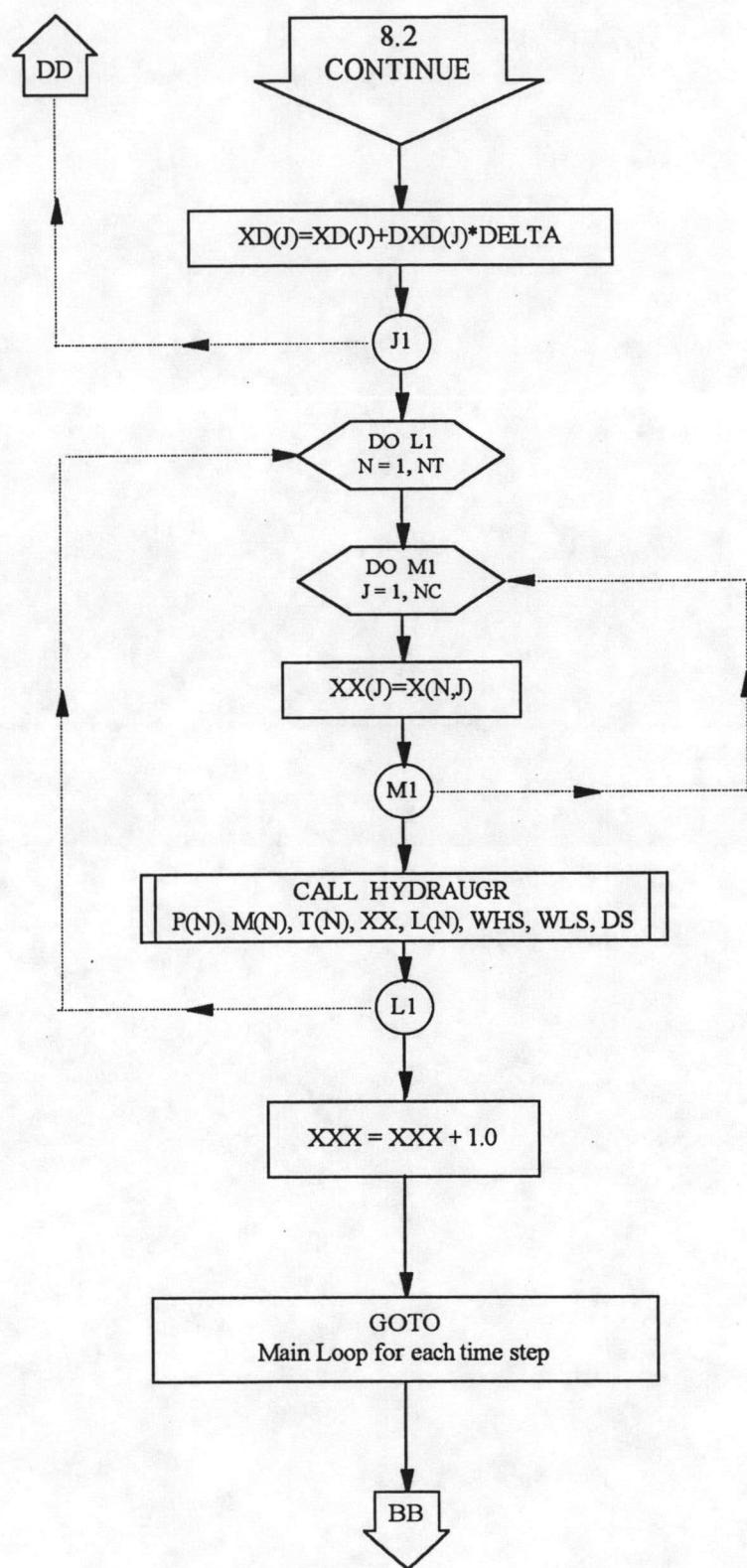
8.2) Running GRK model (Continue)



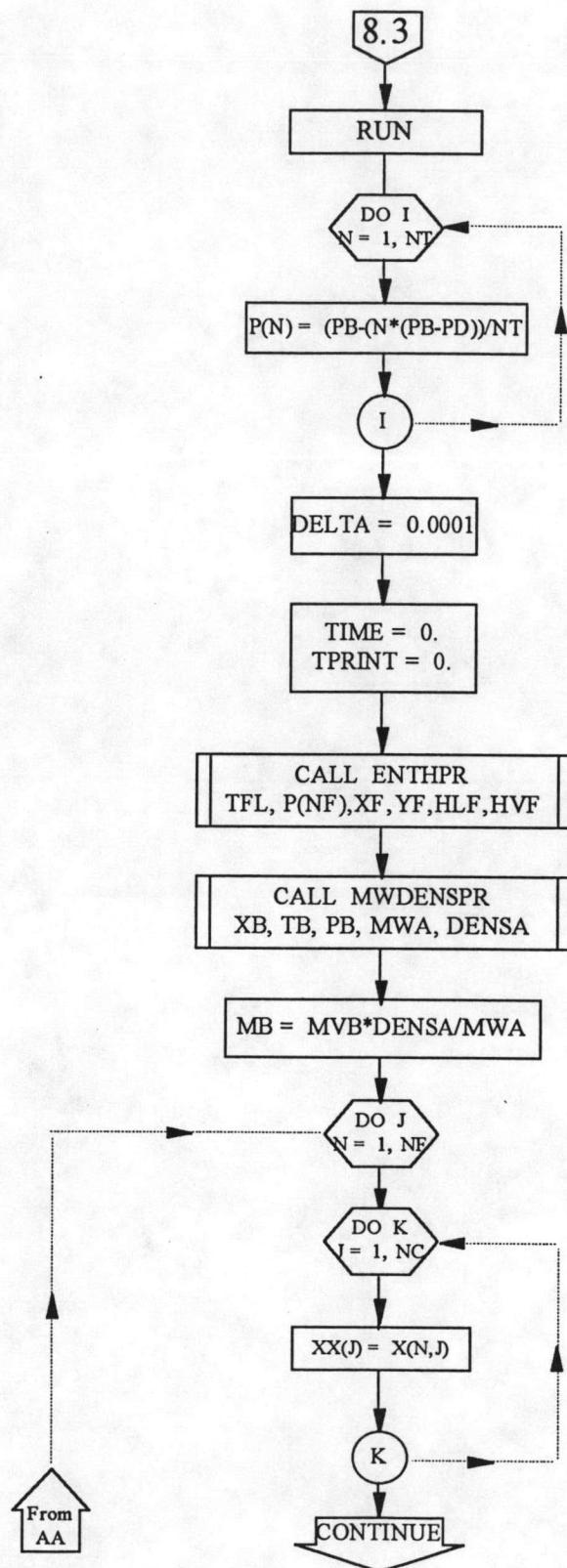
8.2) Running GRK model (Continue)



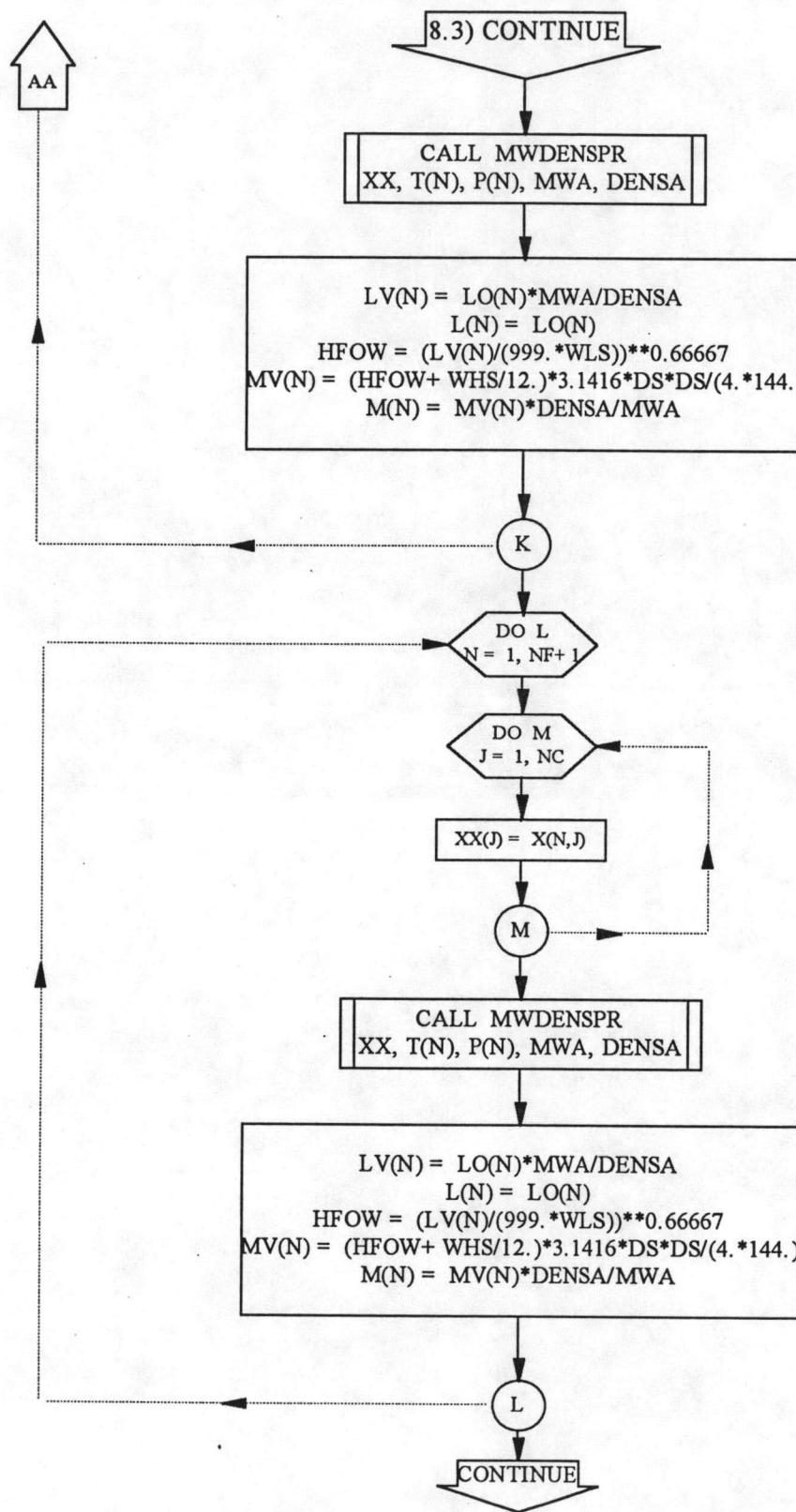
8.2) Running GRK model (Continue)



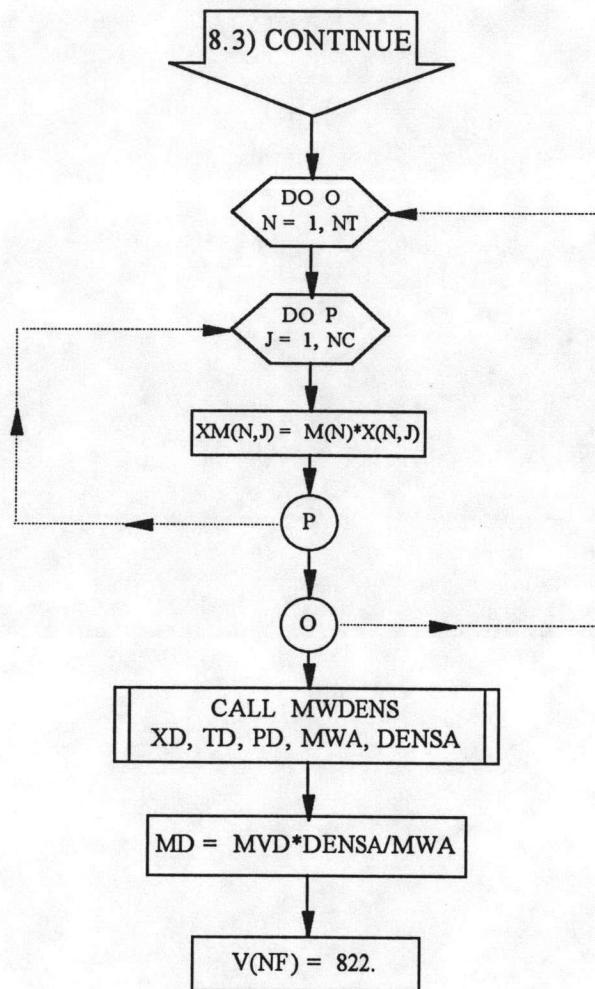
8.2) Running GRK model (Continue)



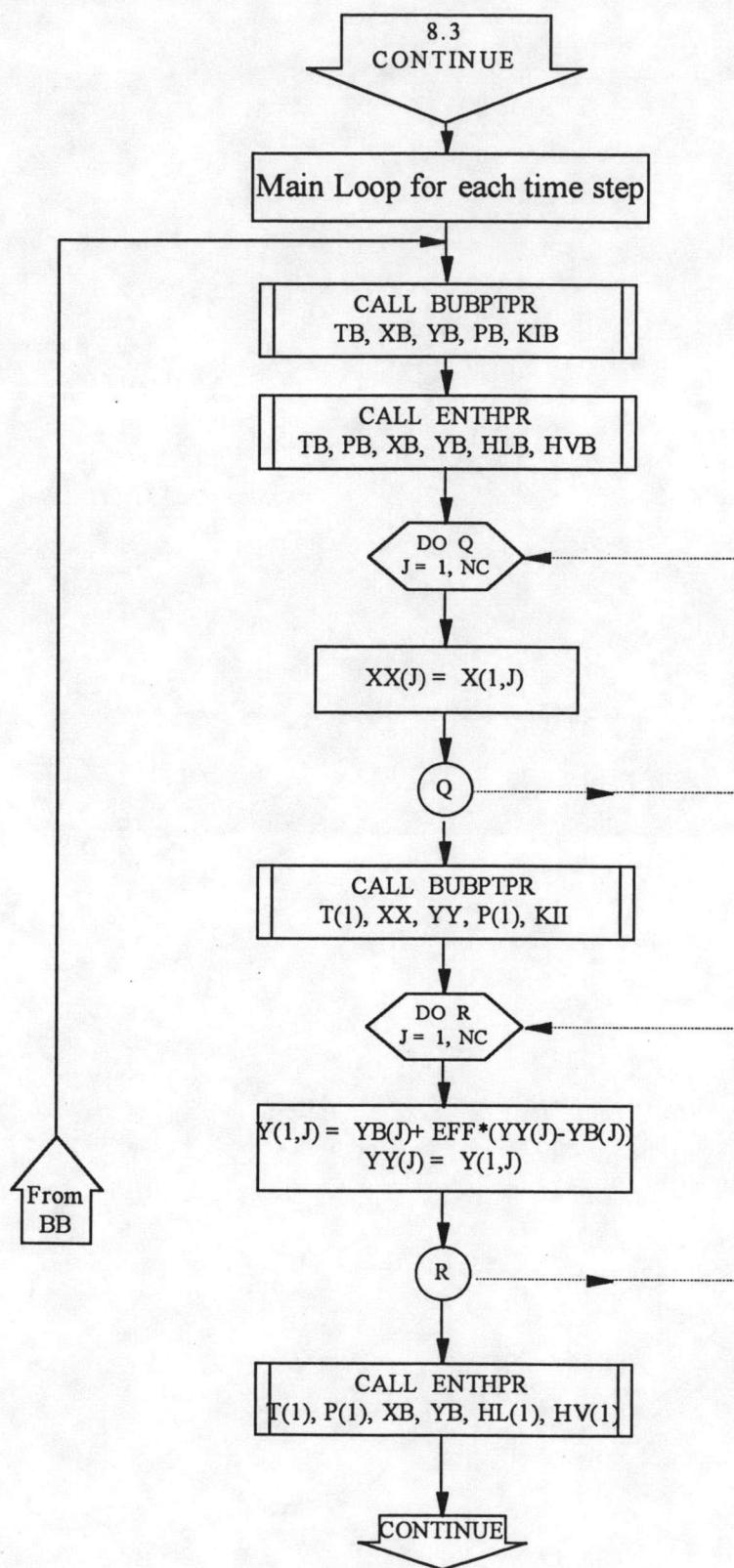
8.3) Running PR model



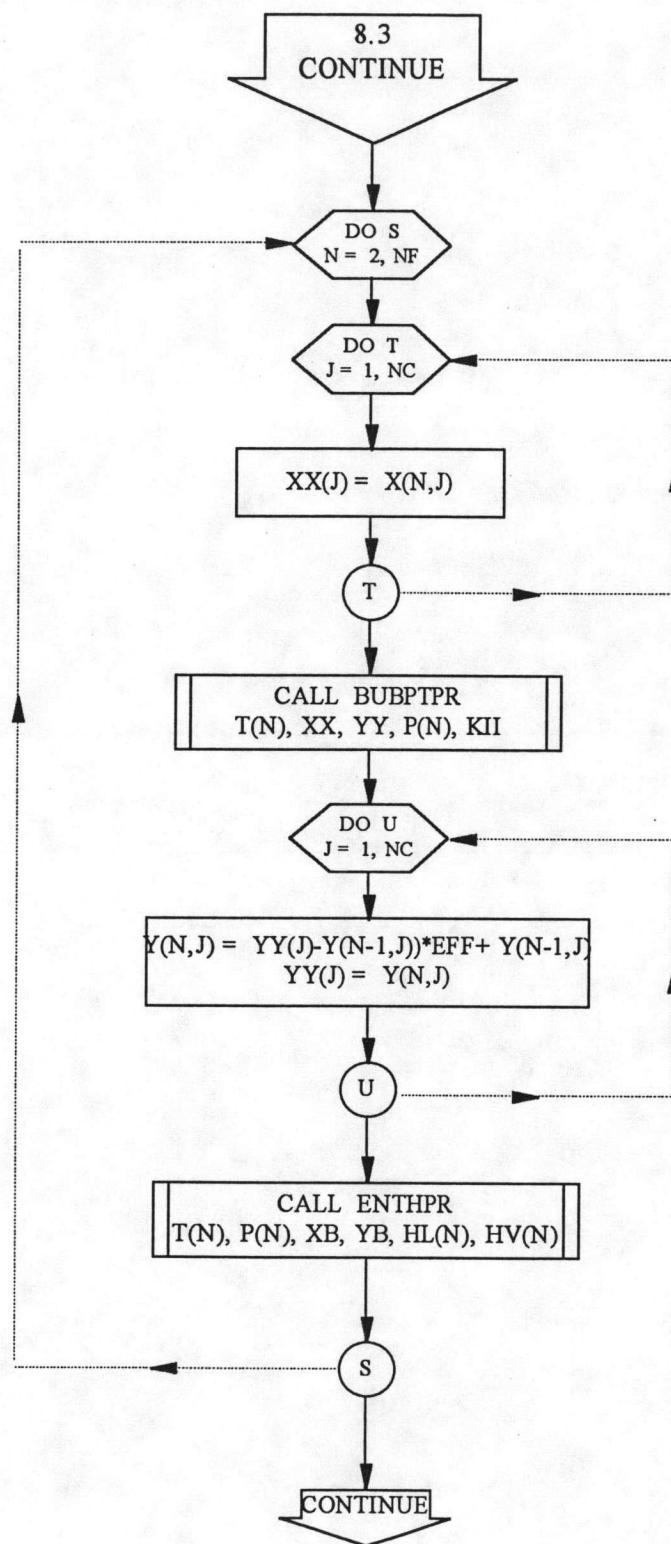
8.3) Running PR model (Continue)



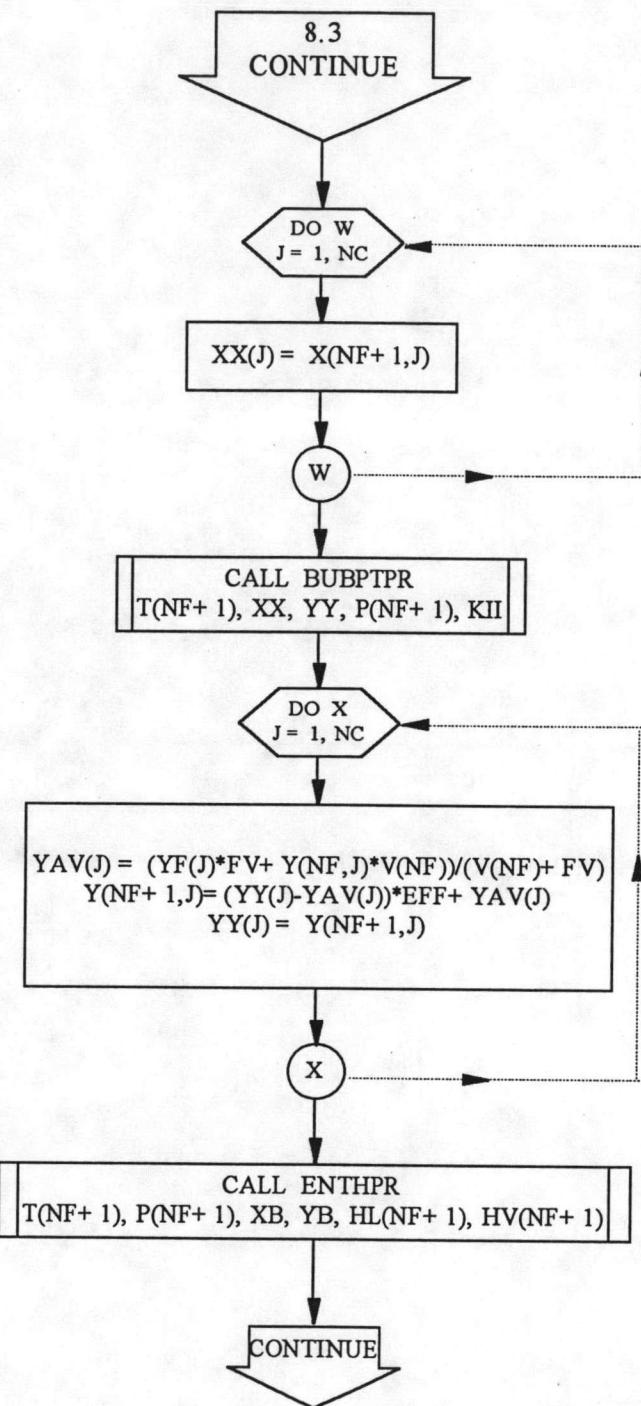
8.3) Running PR model (Continue)



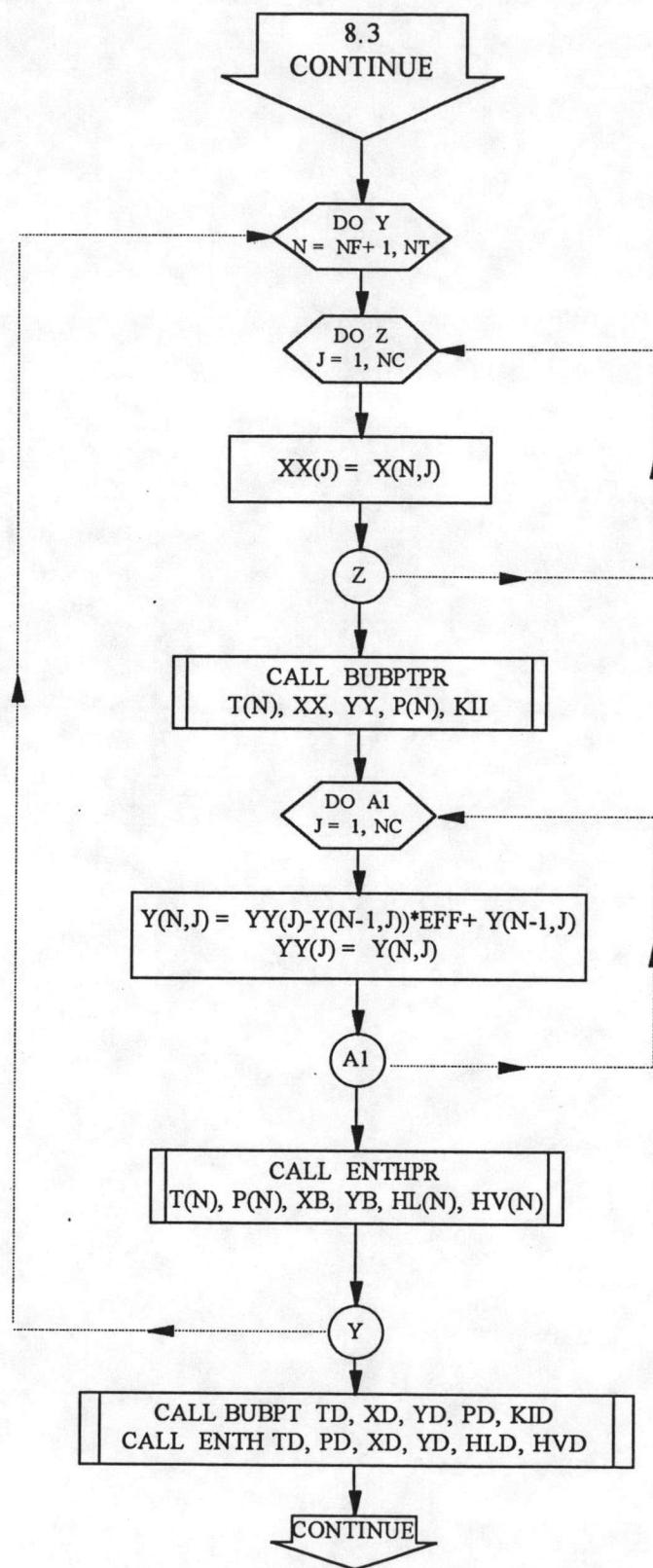
8.3) Running PR model (Continue)



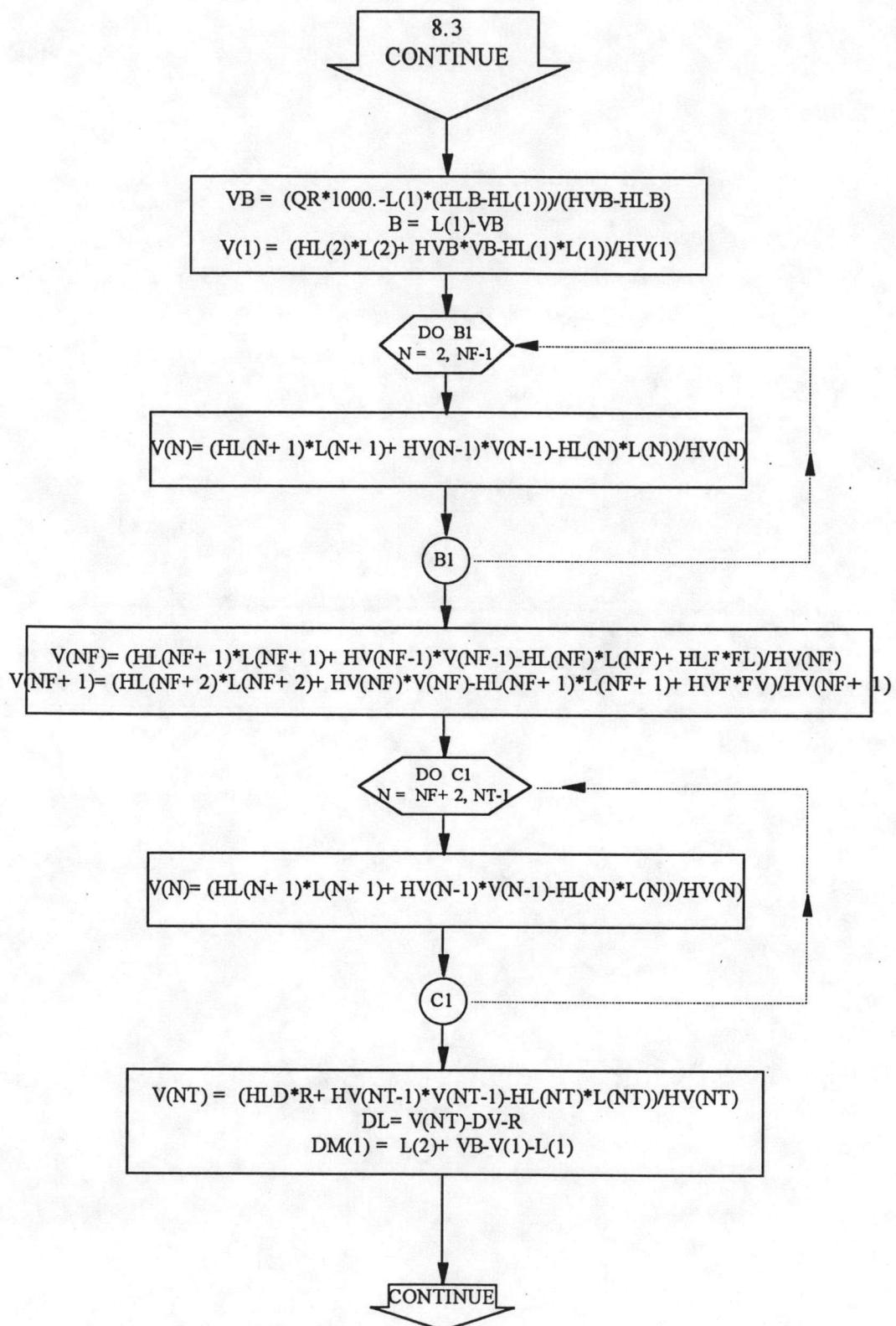
8.3) Running PR model (Continue)



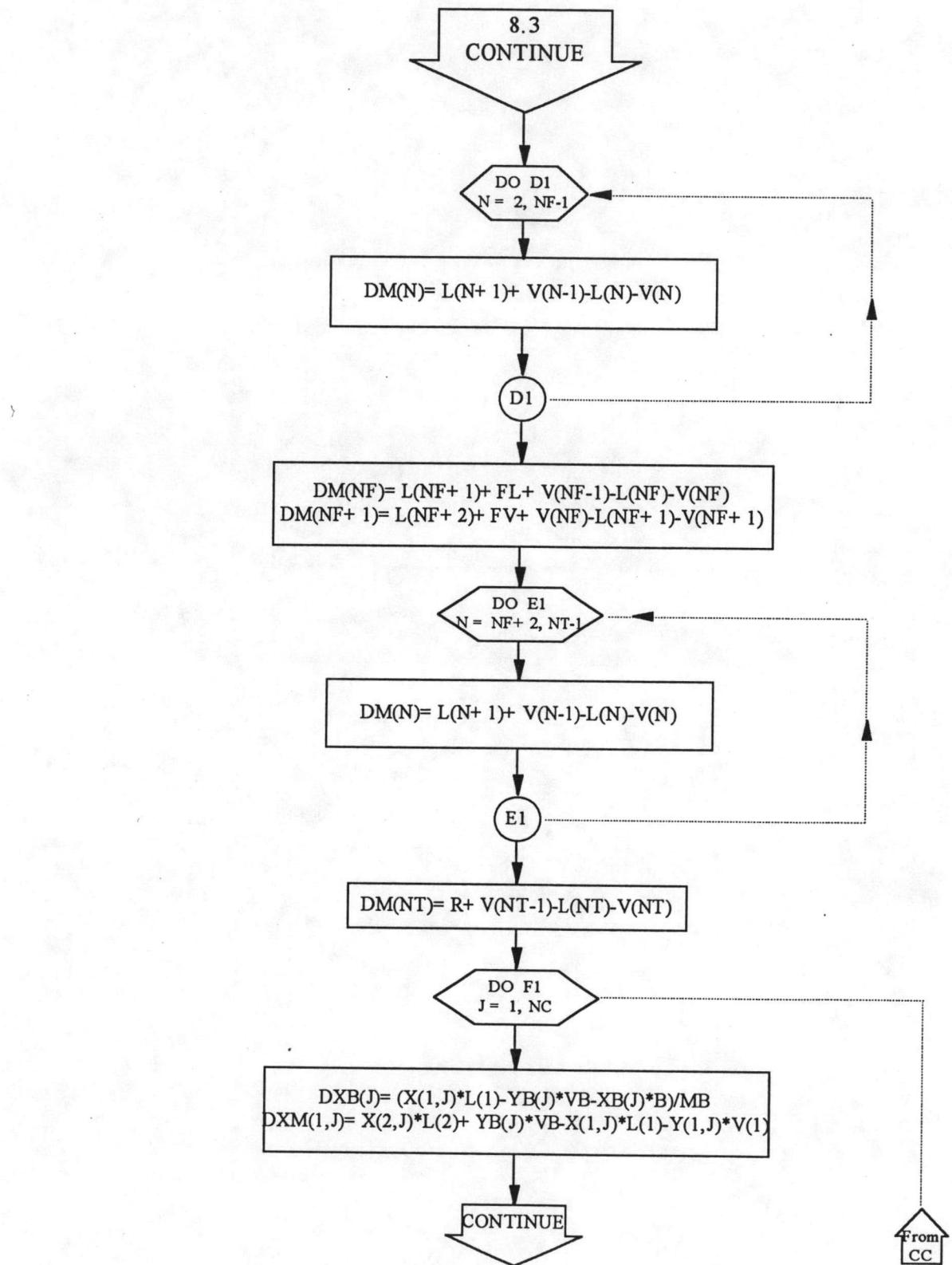
8.3) Running PR model (Continue)



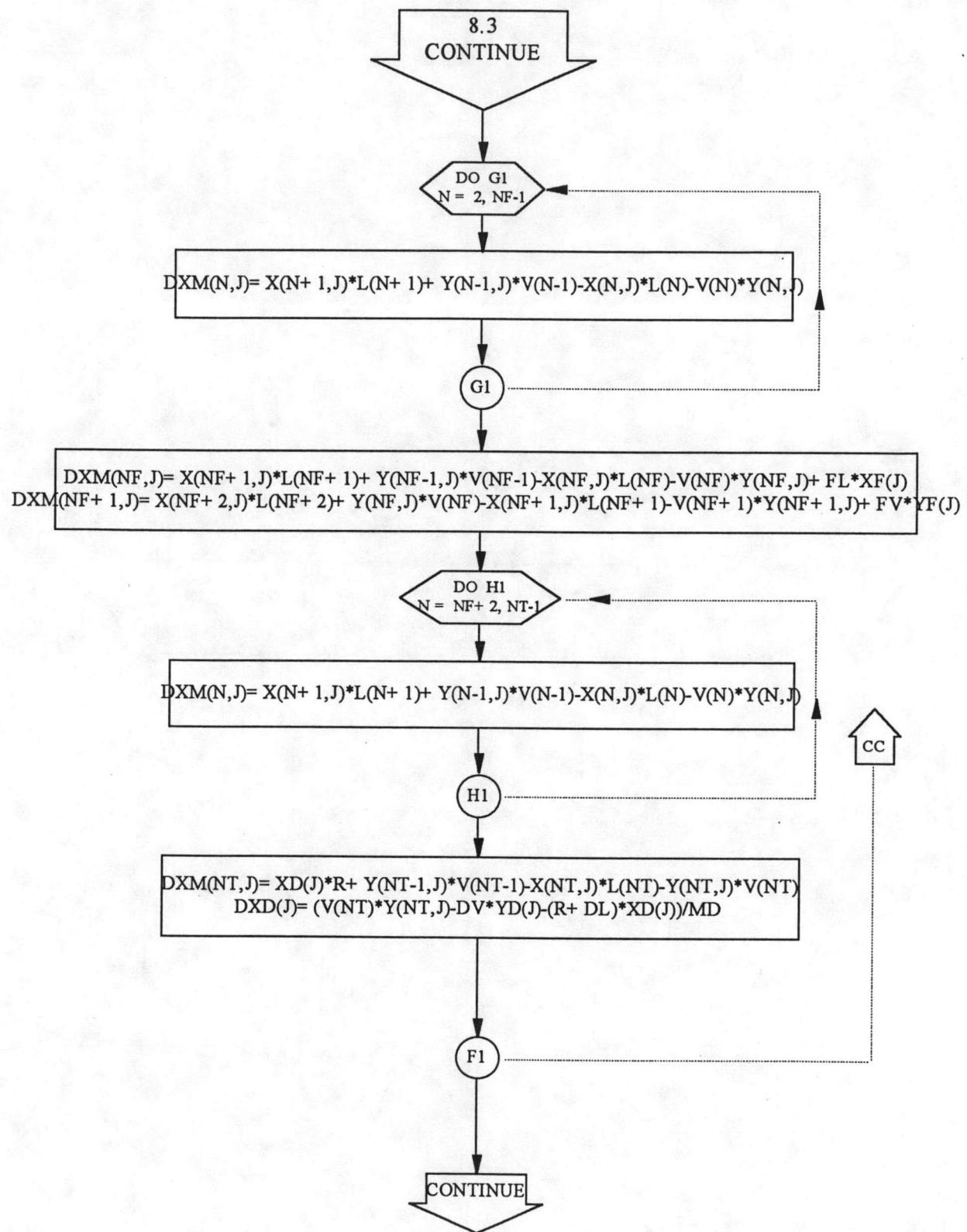
8.3) Running PR model (Continue)



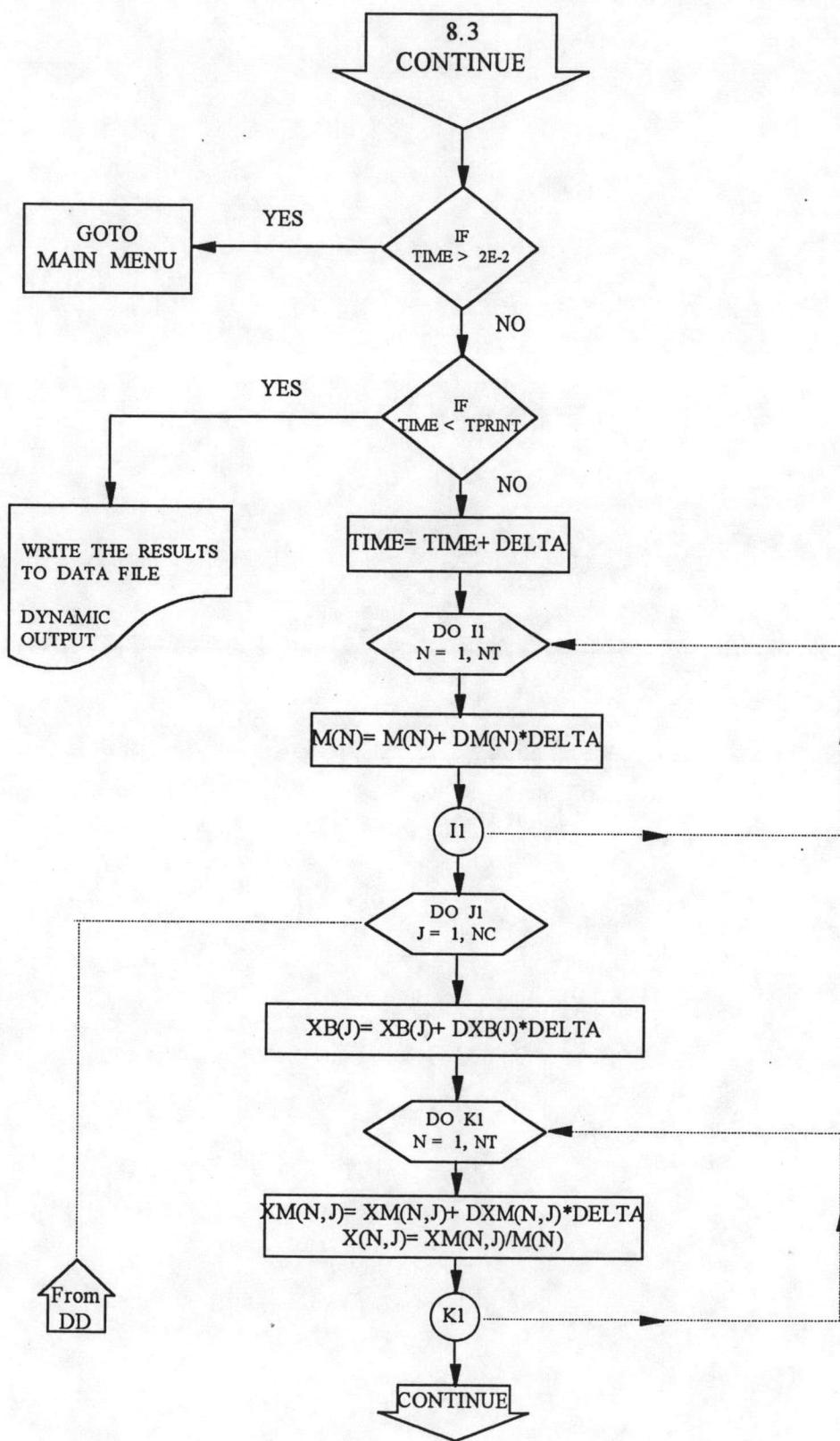
8.3) Running PR model (Continue)



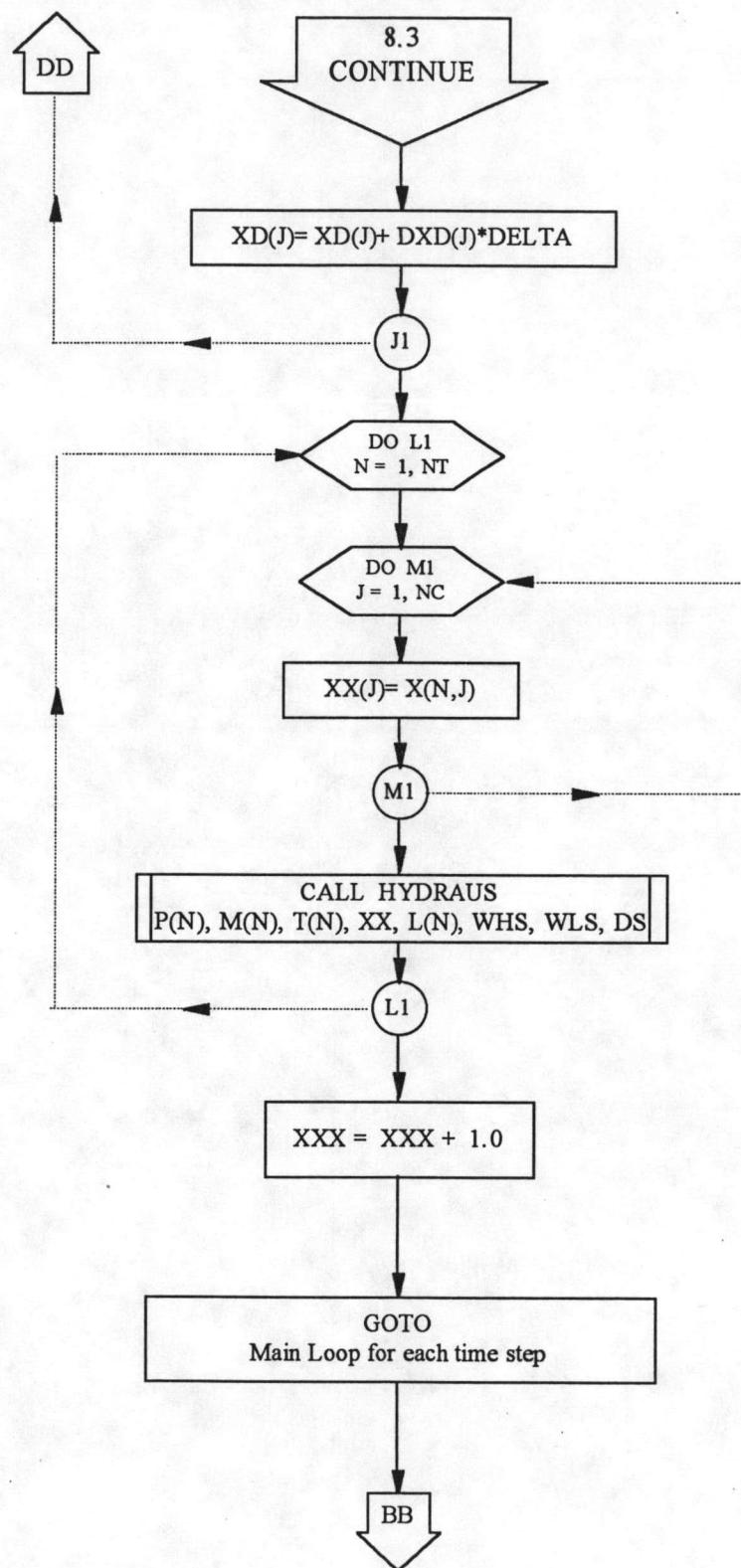
8.3) Running PR model (Continue)



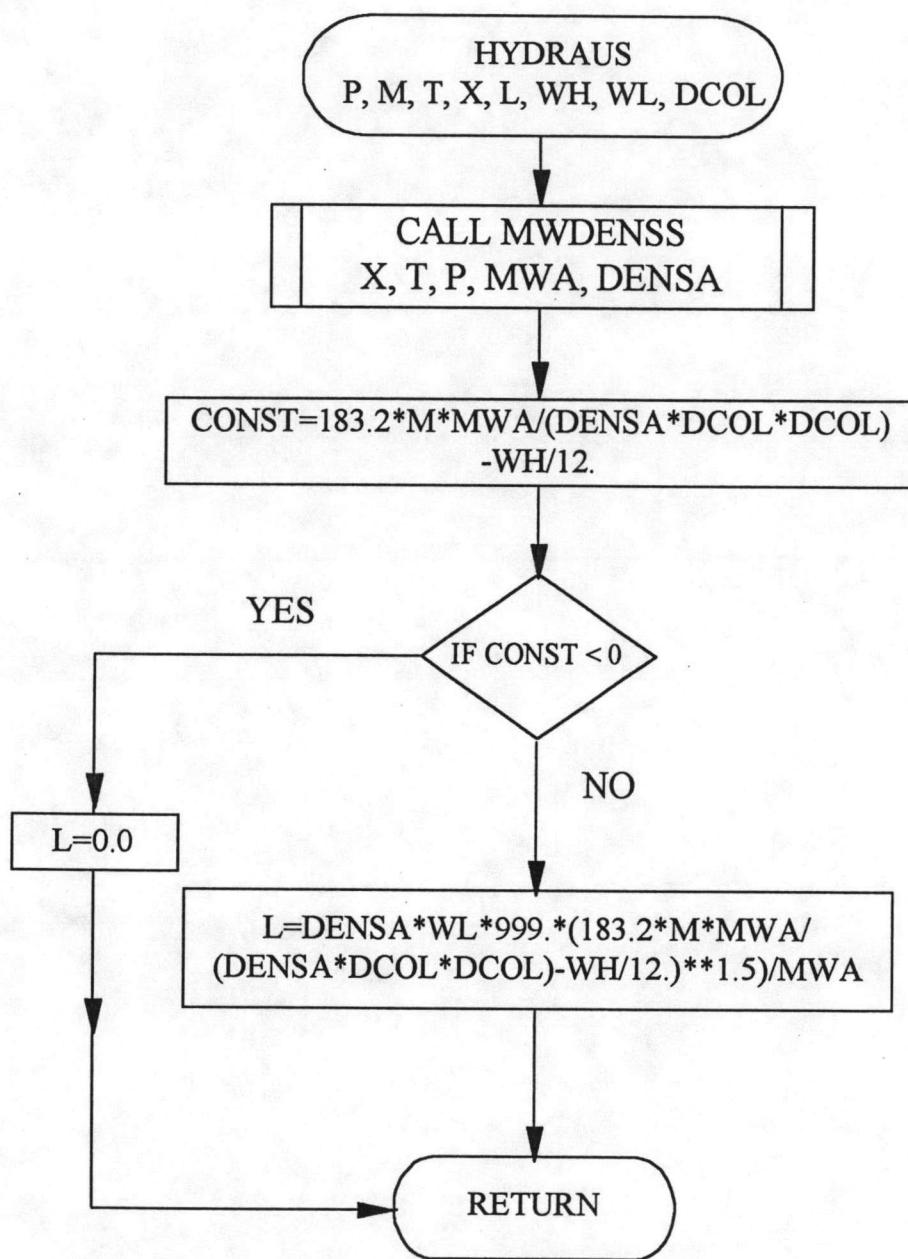
8.3) Running PR model (Continue)

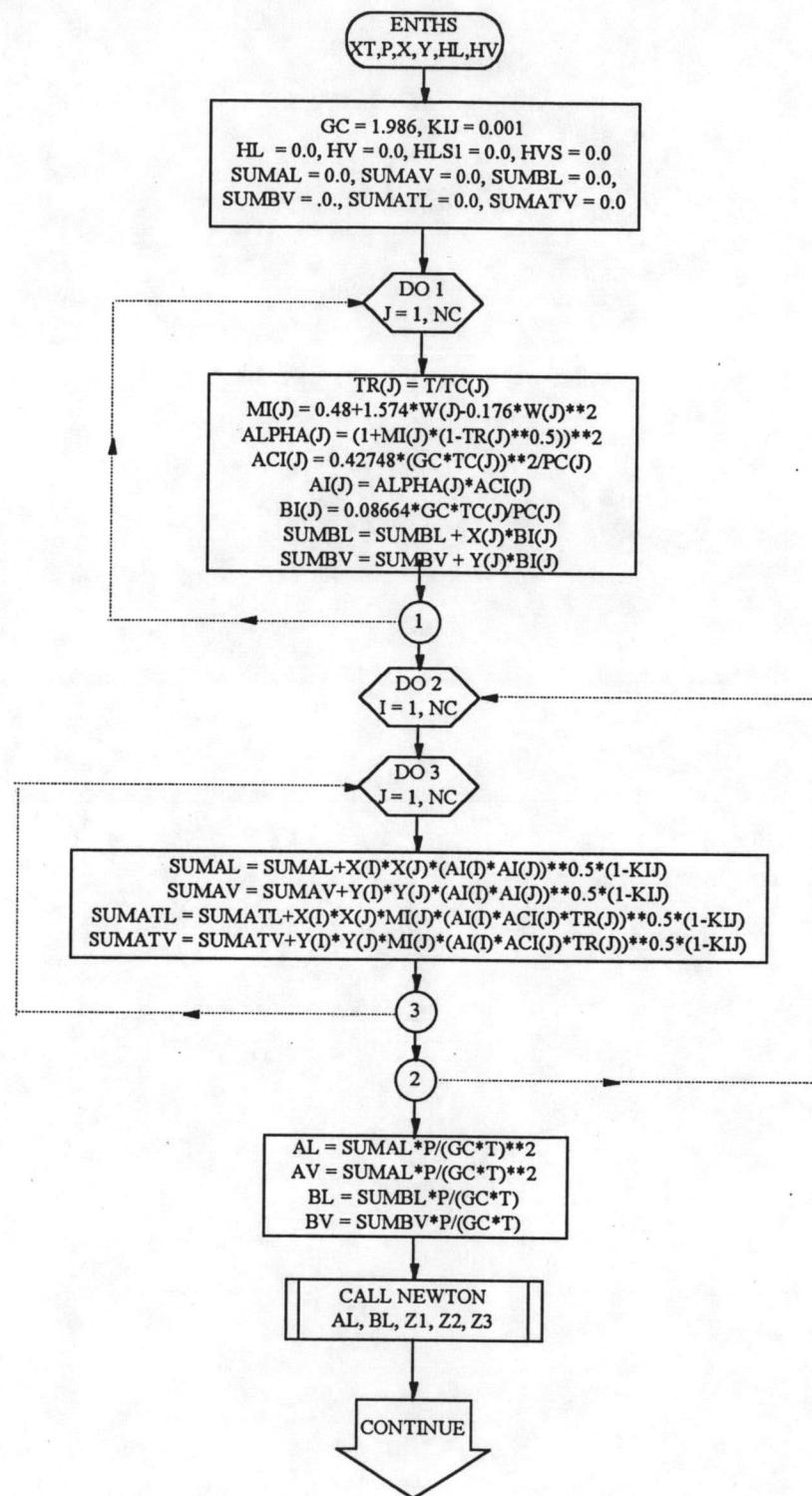


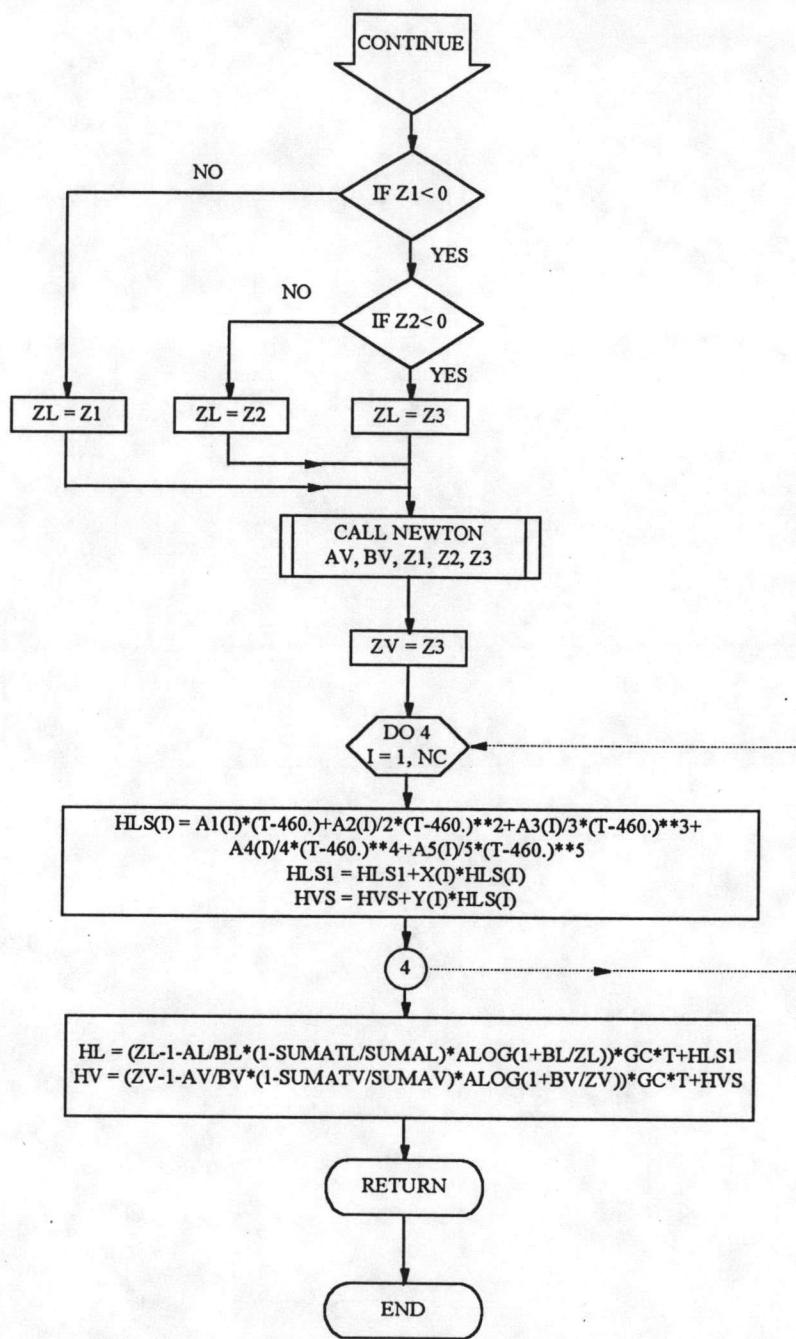
8.3) Running PR model (Continue)



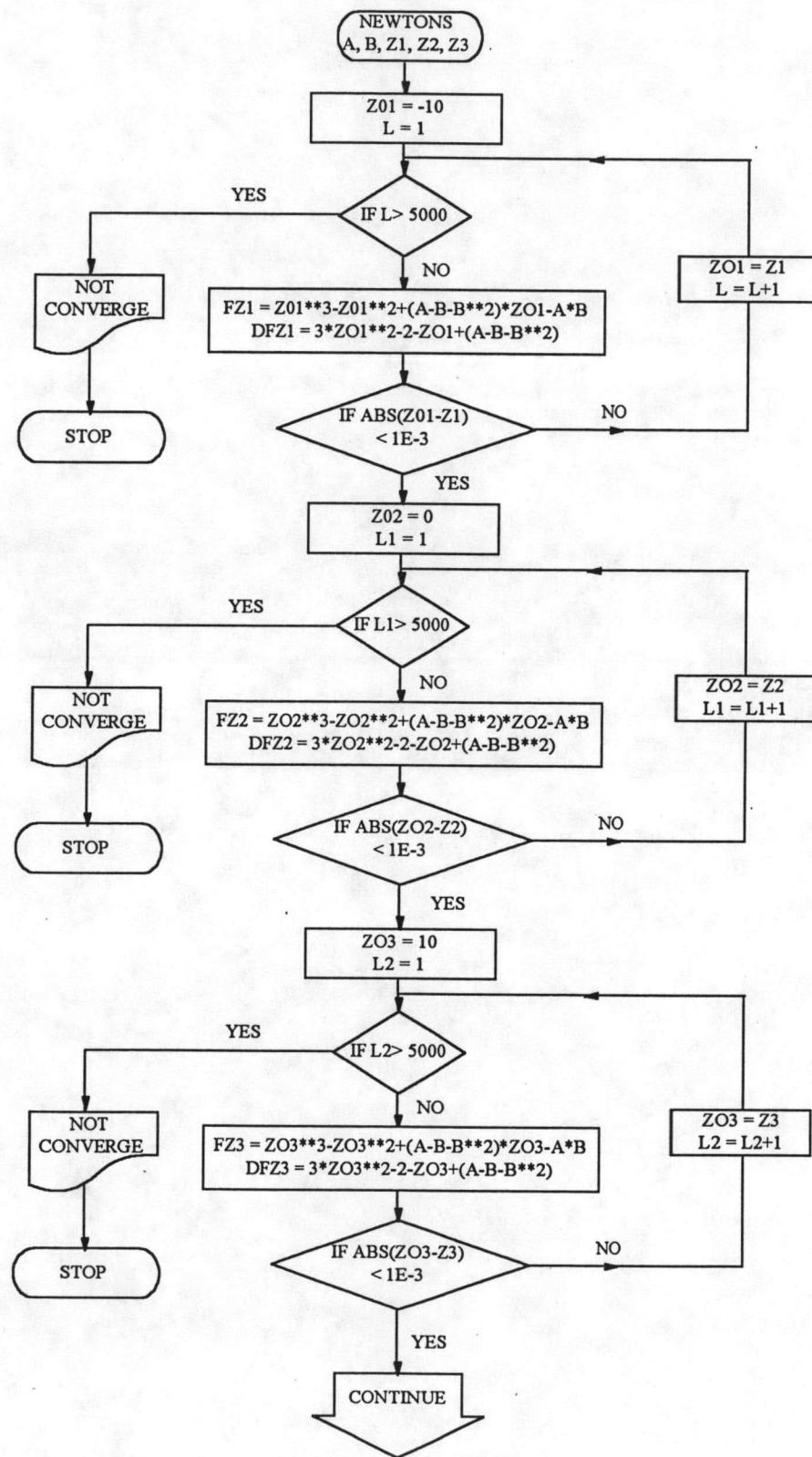
8.3) Running PR model (Continue)

**SUBPROGRAM HYDRAUS**

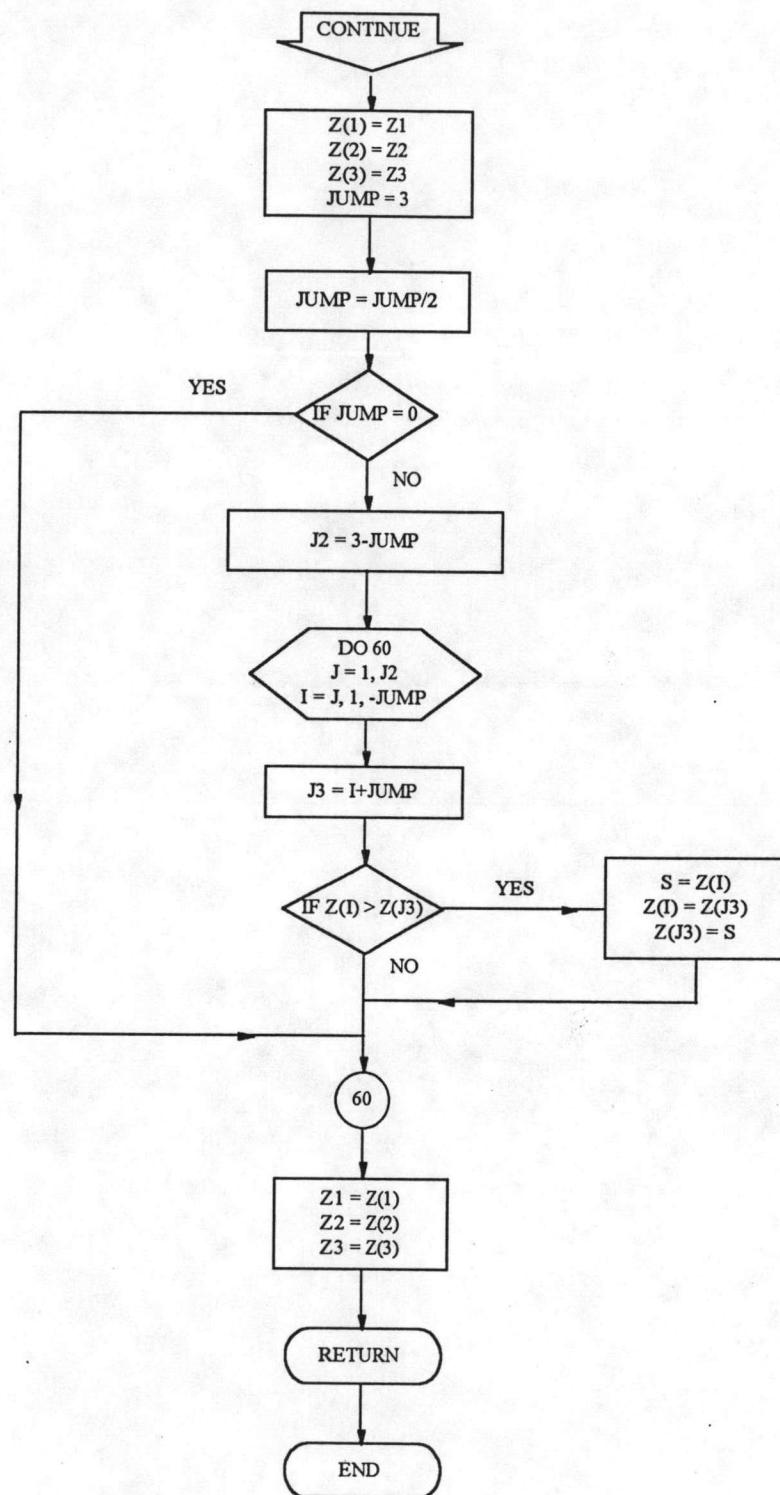
**SUBROUTINE ENTHS**



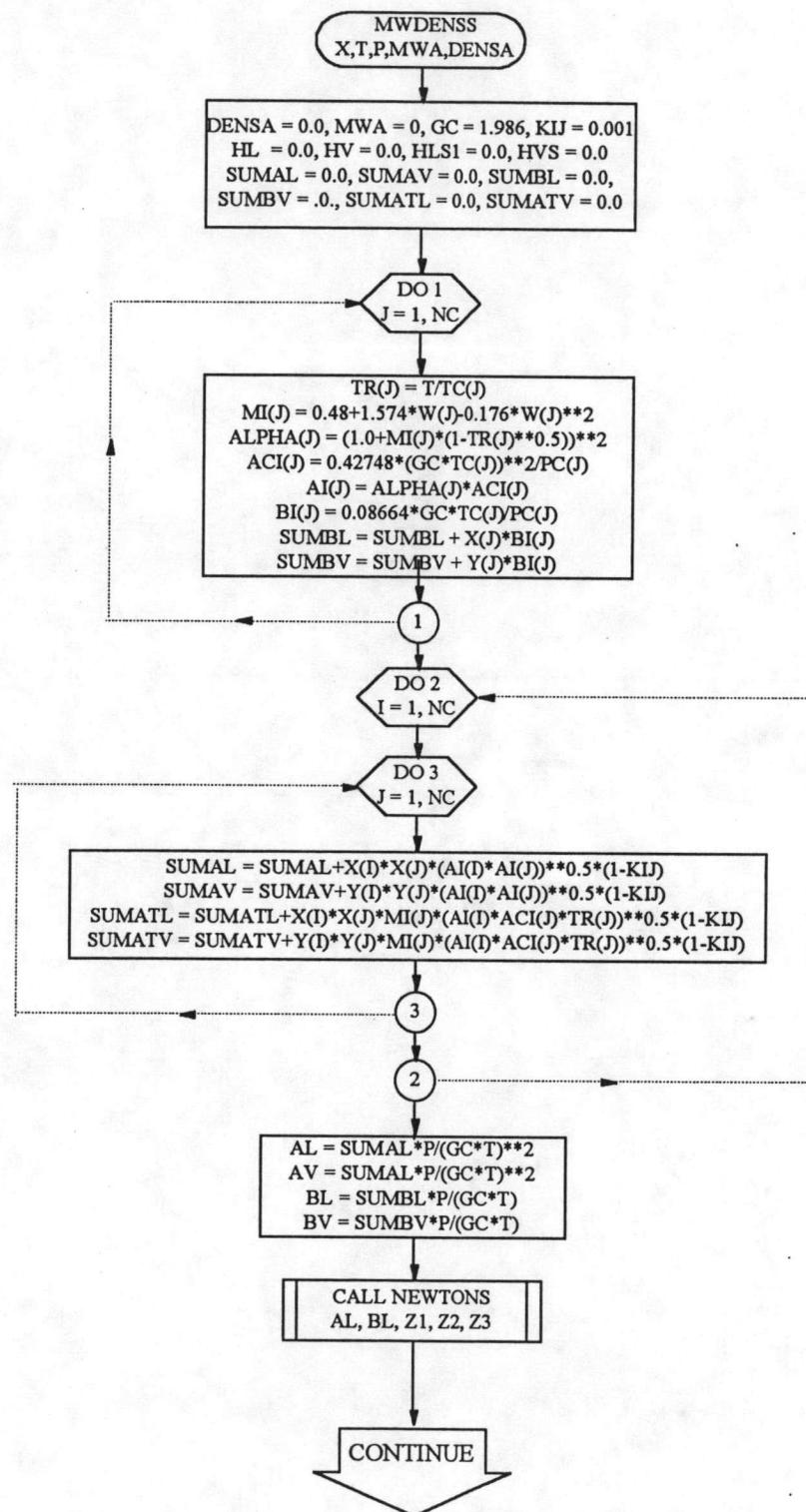
SUBROUTINE ENTHS (Continue)



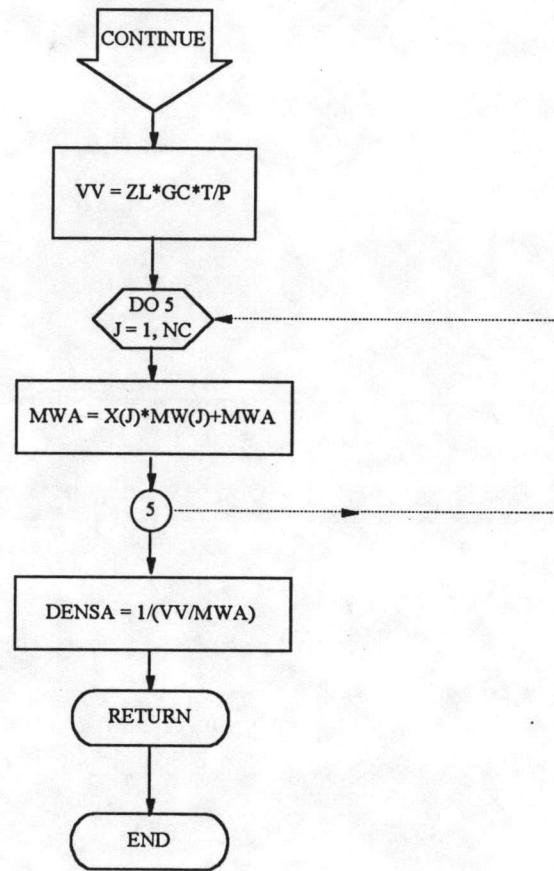
SUBROUTINE NEWTONS

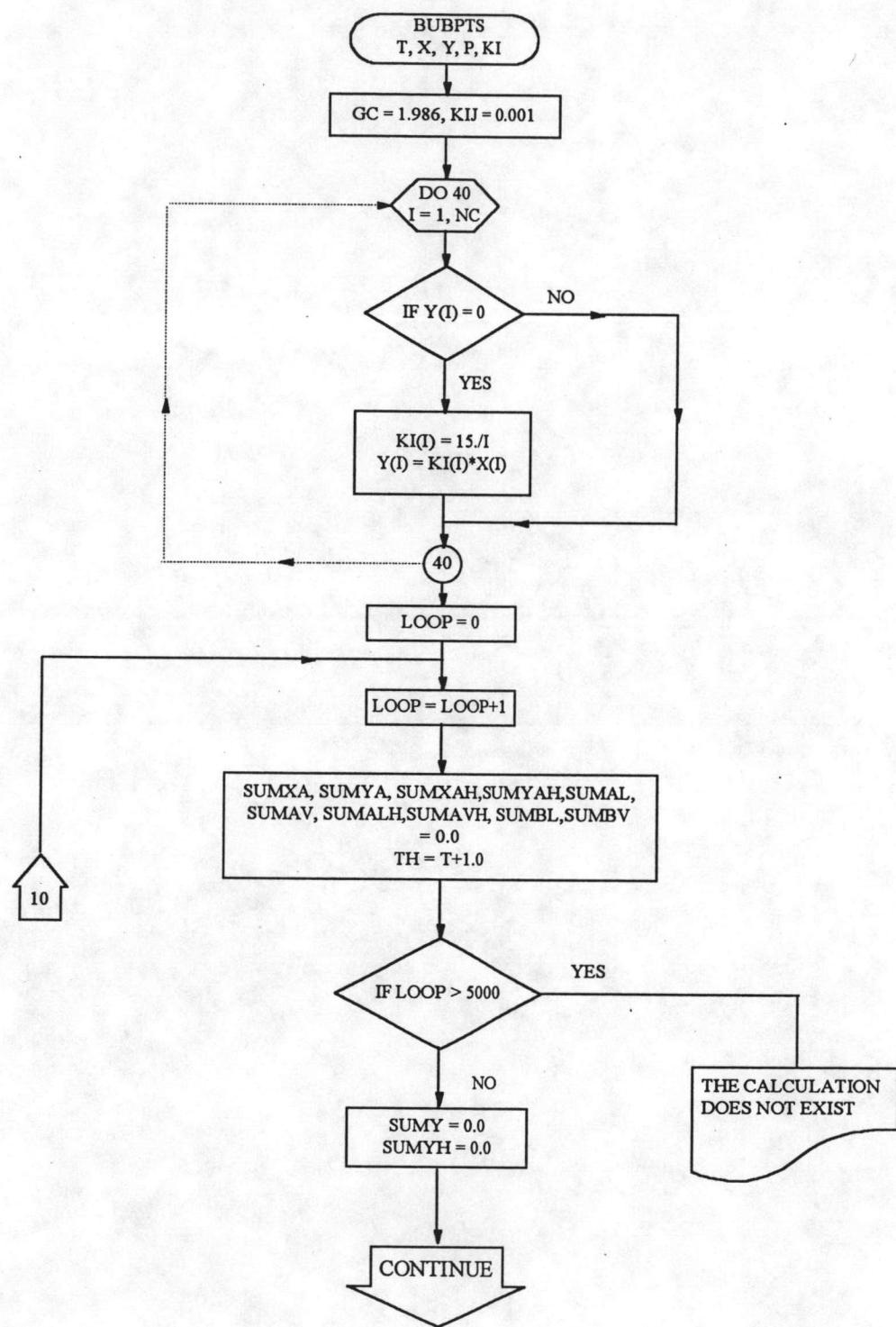


SUBROUTINE NEWTONS (Continue)

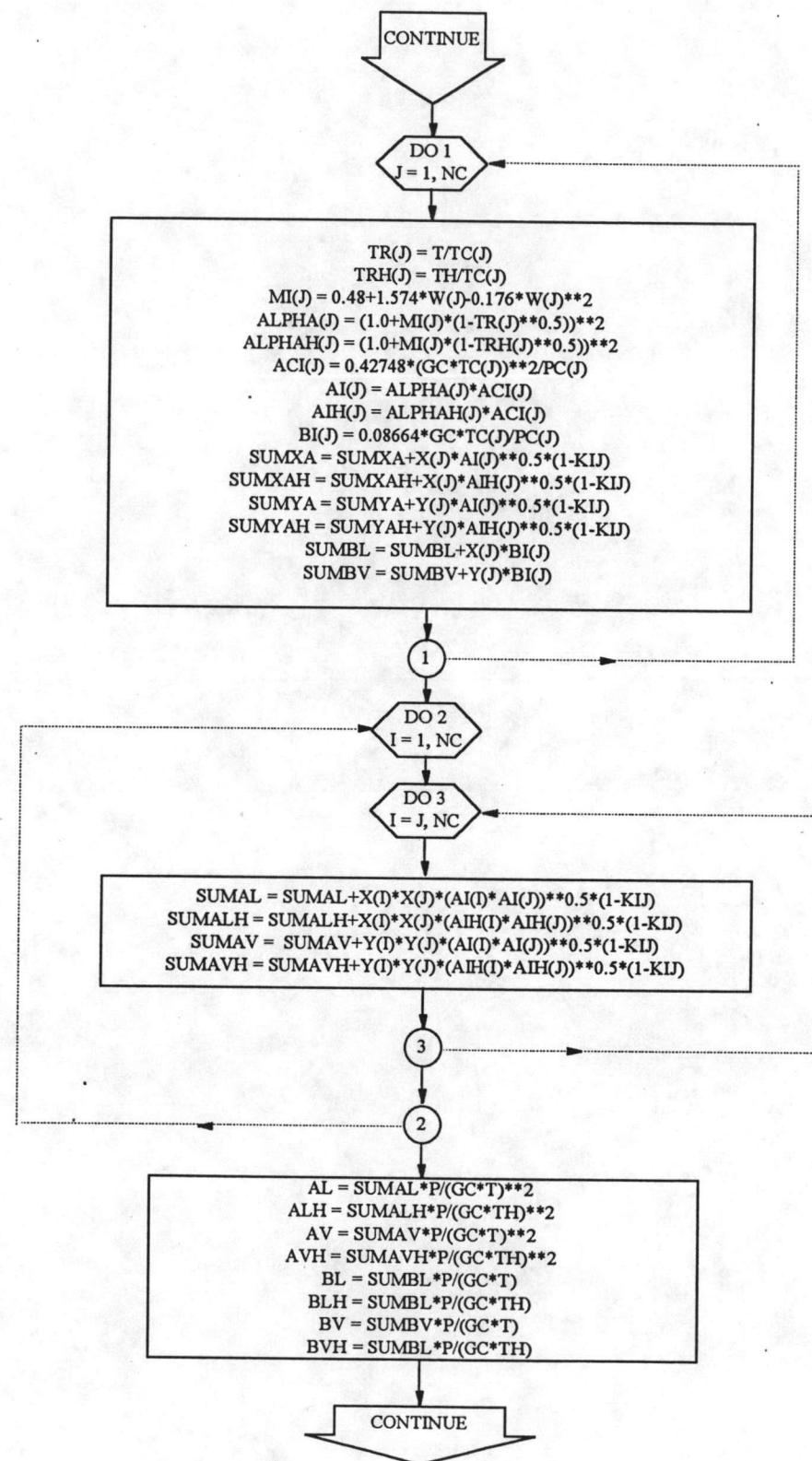


SUBROUTINE MWDENSS

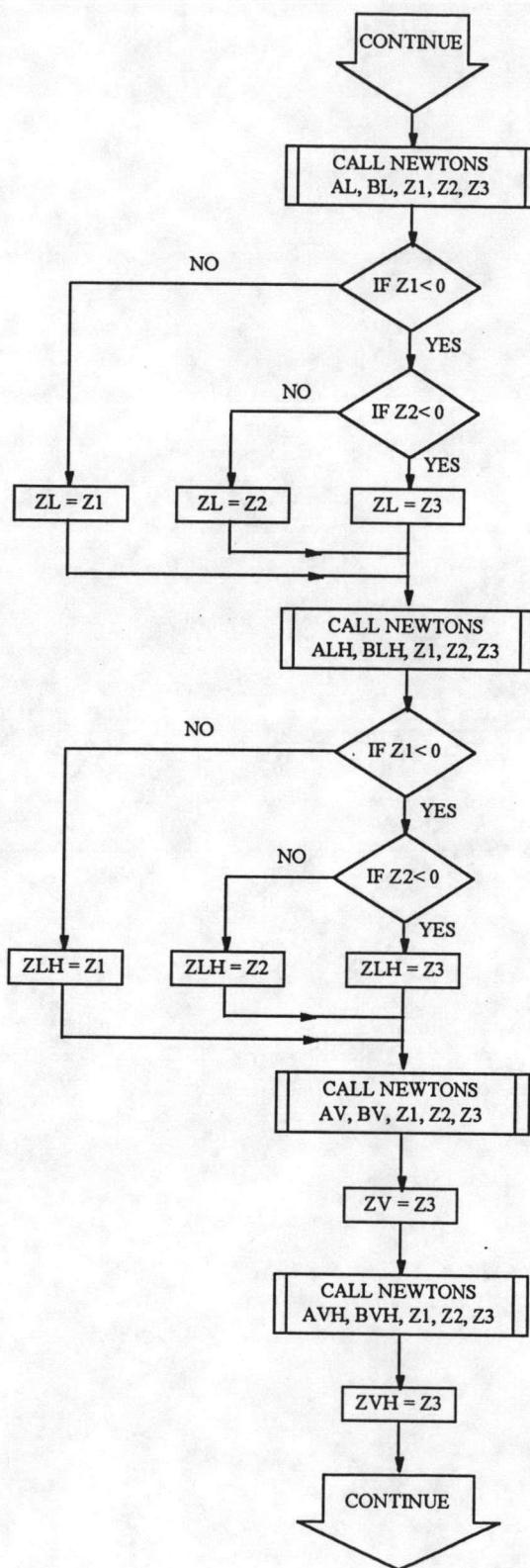
**SUBROUTINE MWDENSS (Continue)**



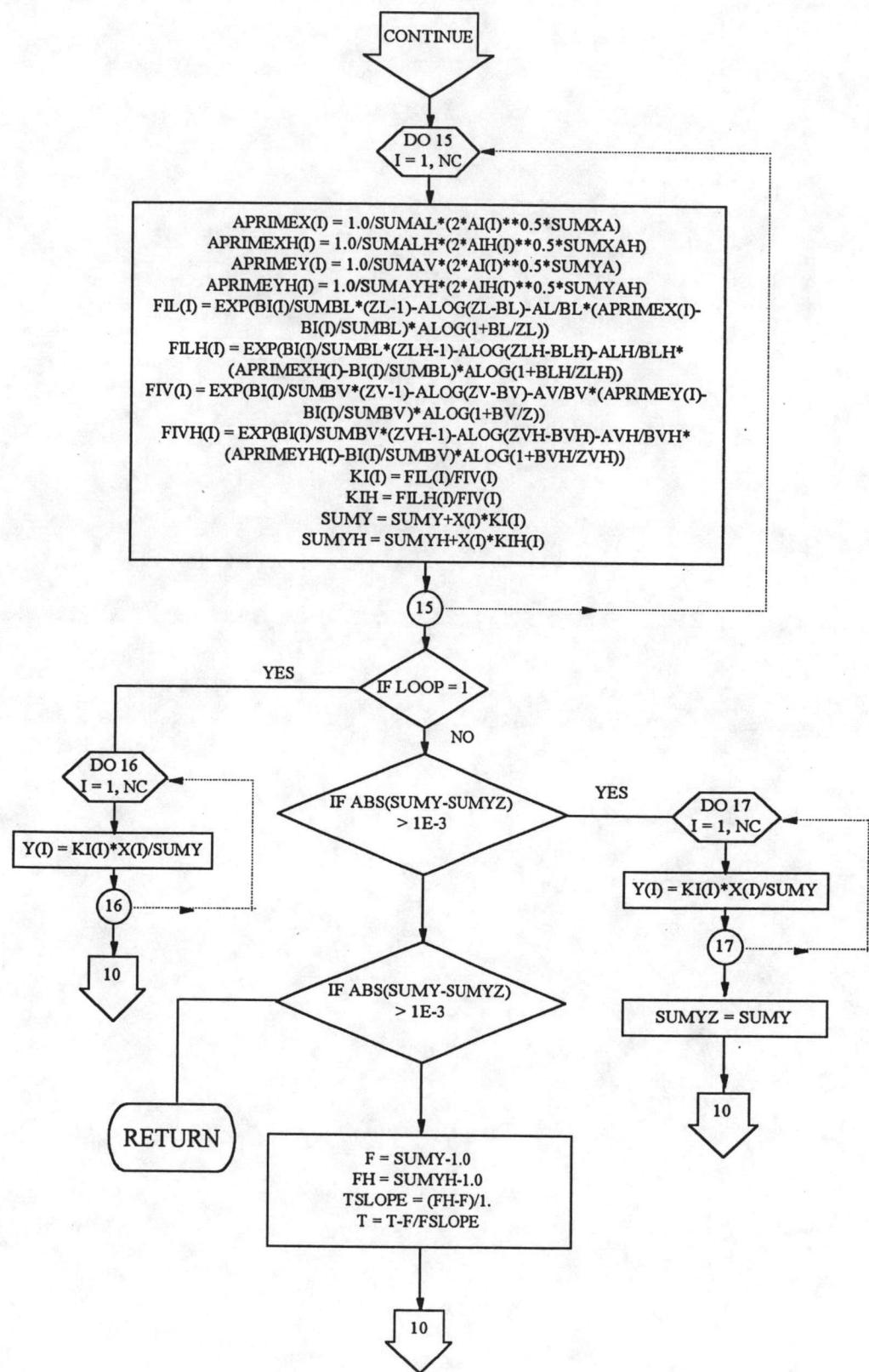
SUBROUTINE BUBPTS



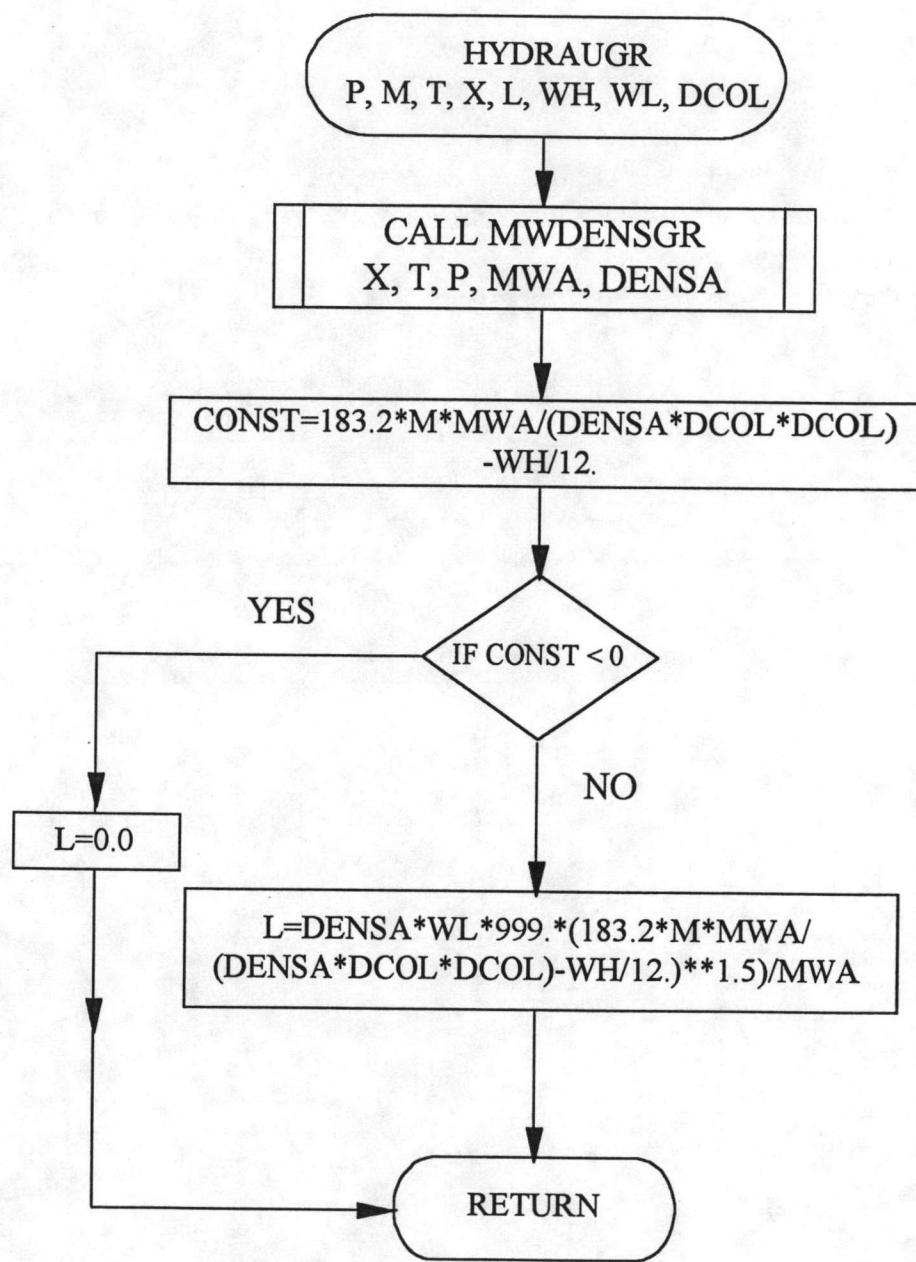
SUBROUTINE BUBPTS (Continue)



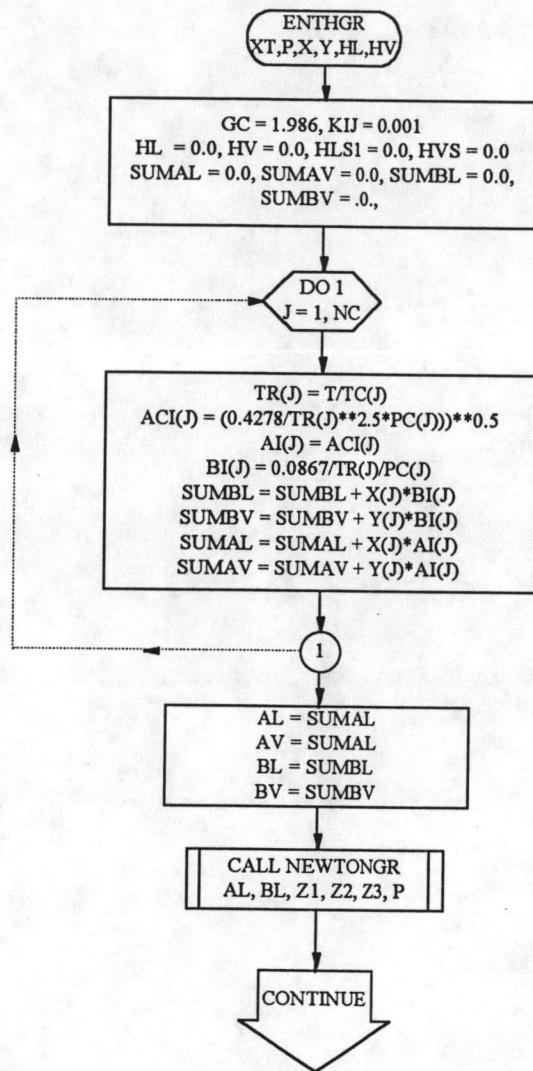
SUBROUTINE BUBPTS (Continue)



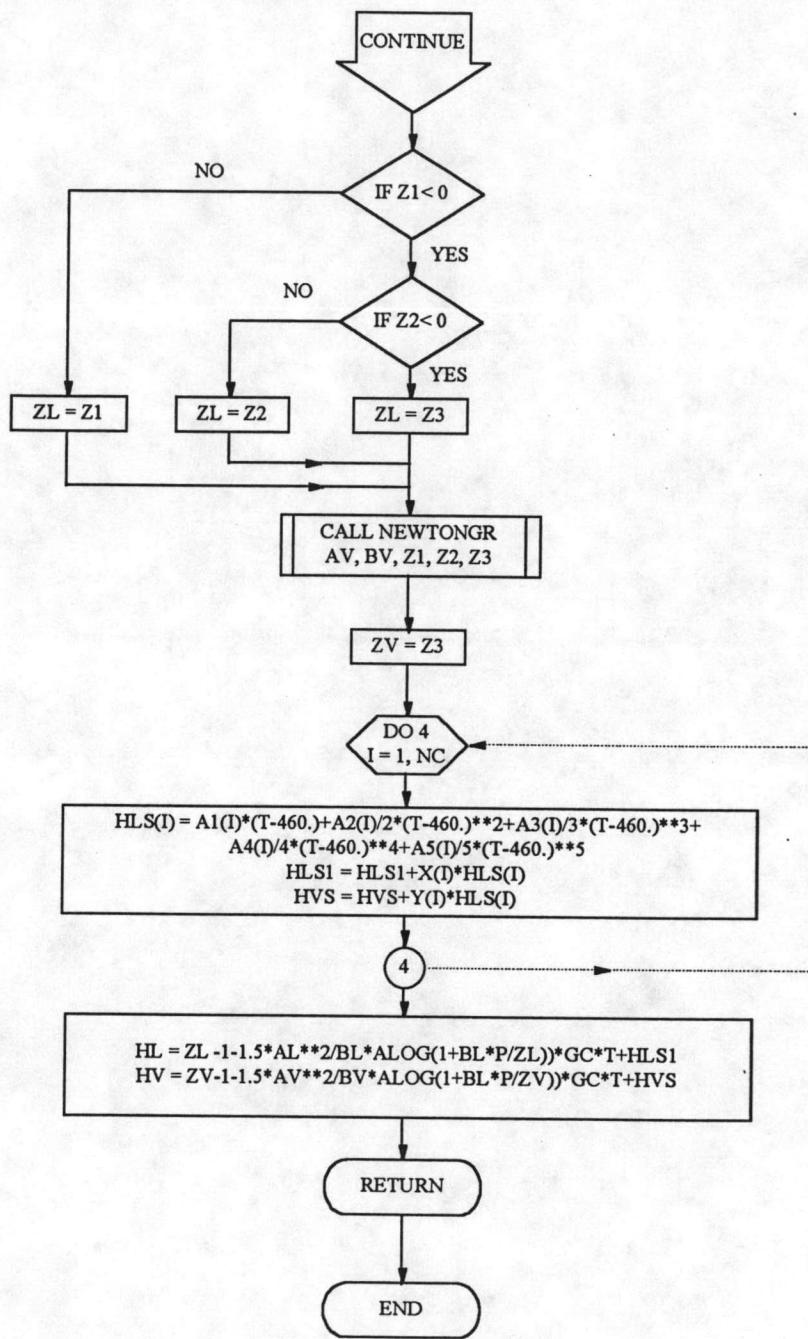
SUBROUTINE BUBPTS (Continue)



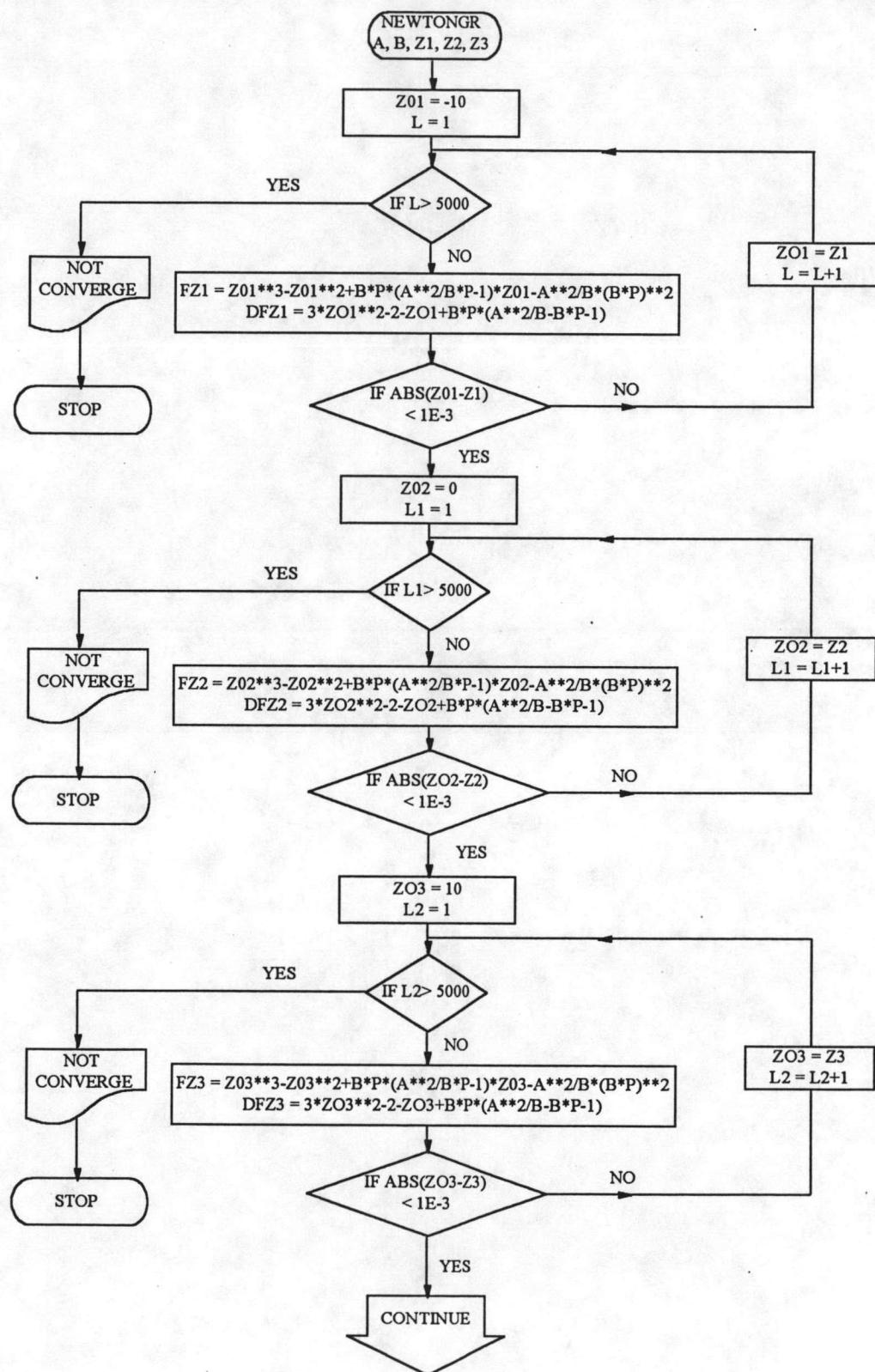
SUBPROGRAM HYDRAUGR



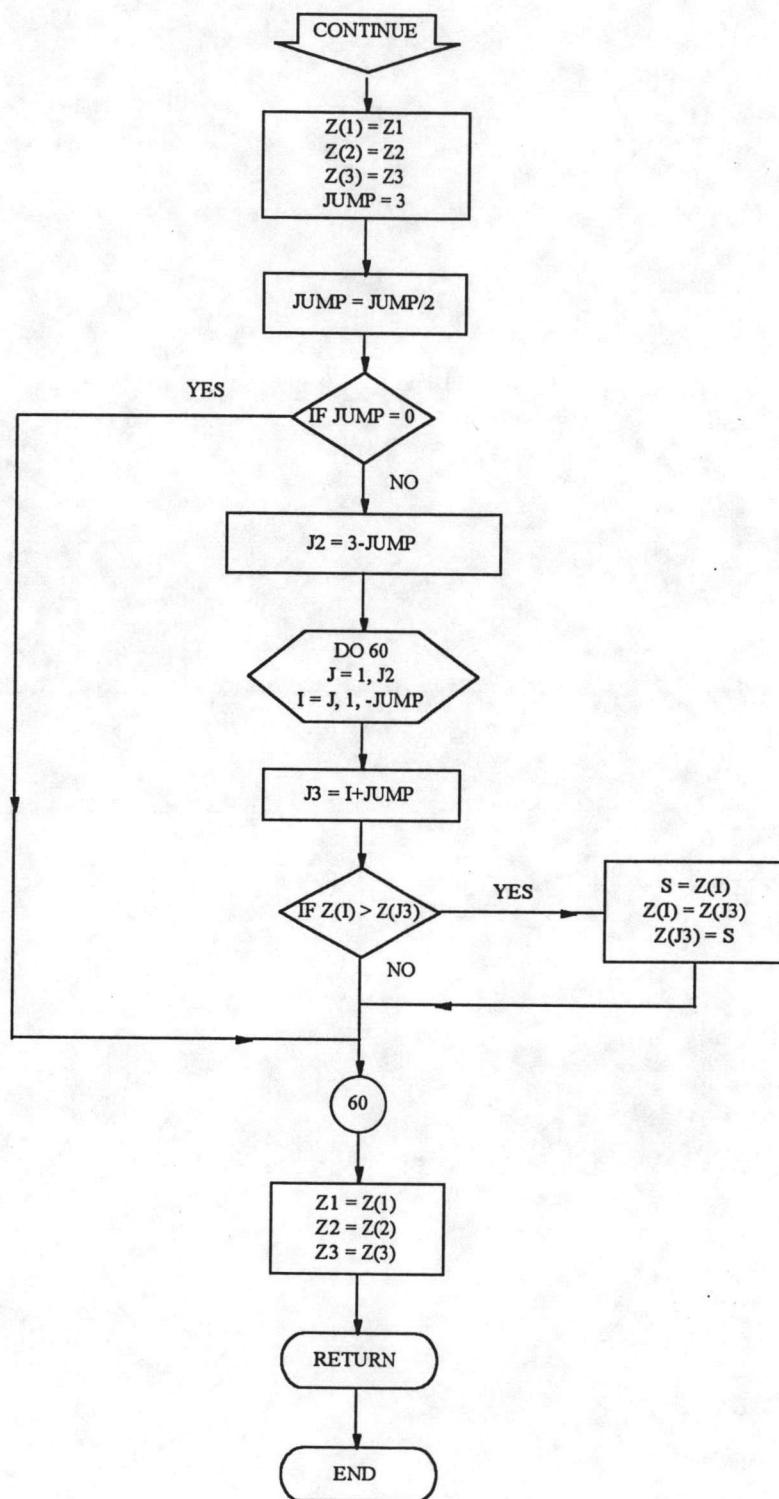
SUBROUTINE ENTHGR



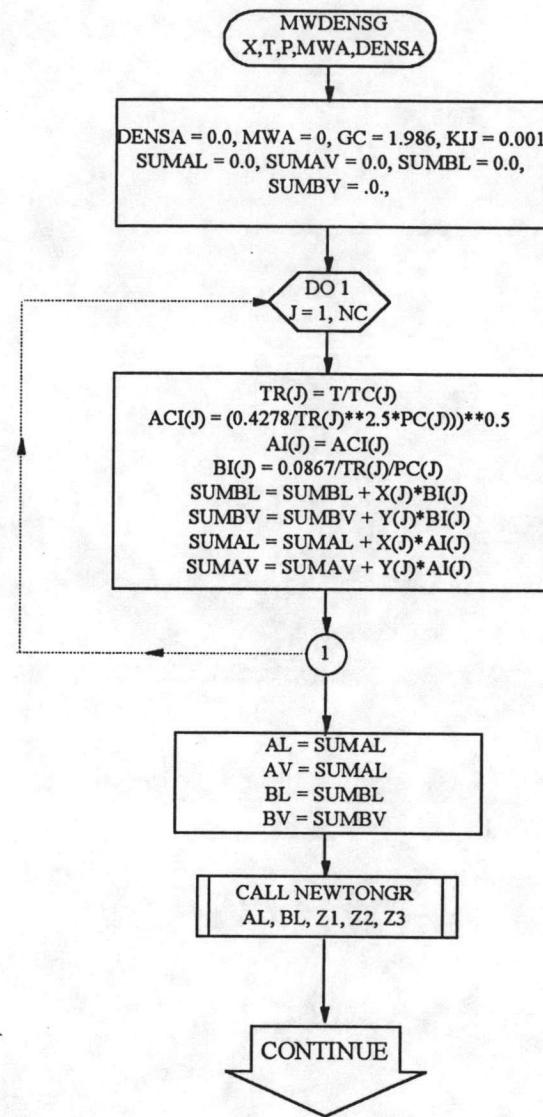
SUBROUTINE ENTHGR (Continue)

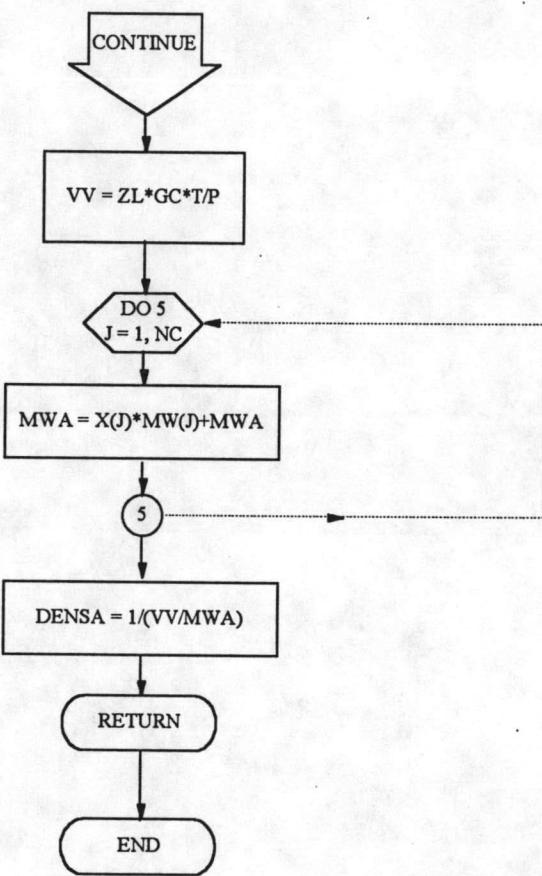


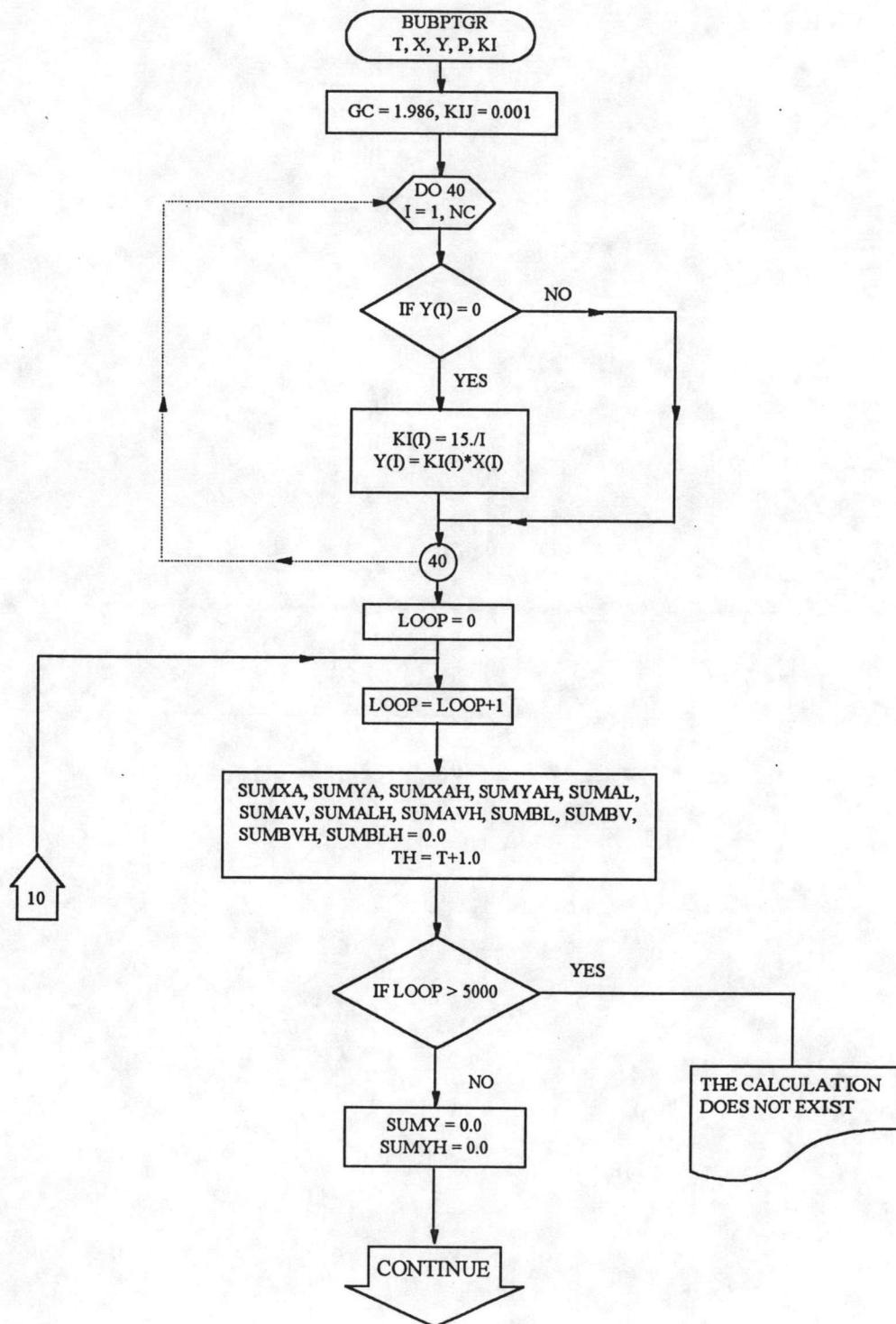
SUBROUTINE NEWTONGR



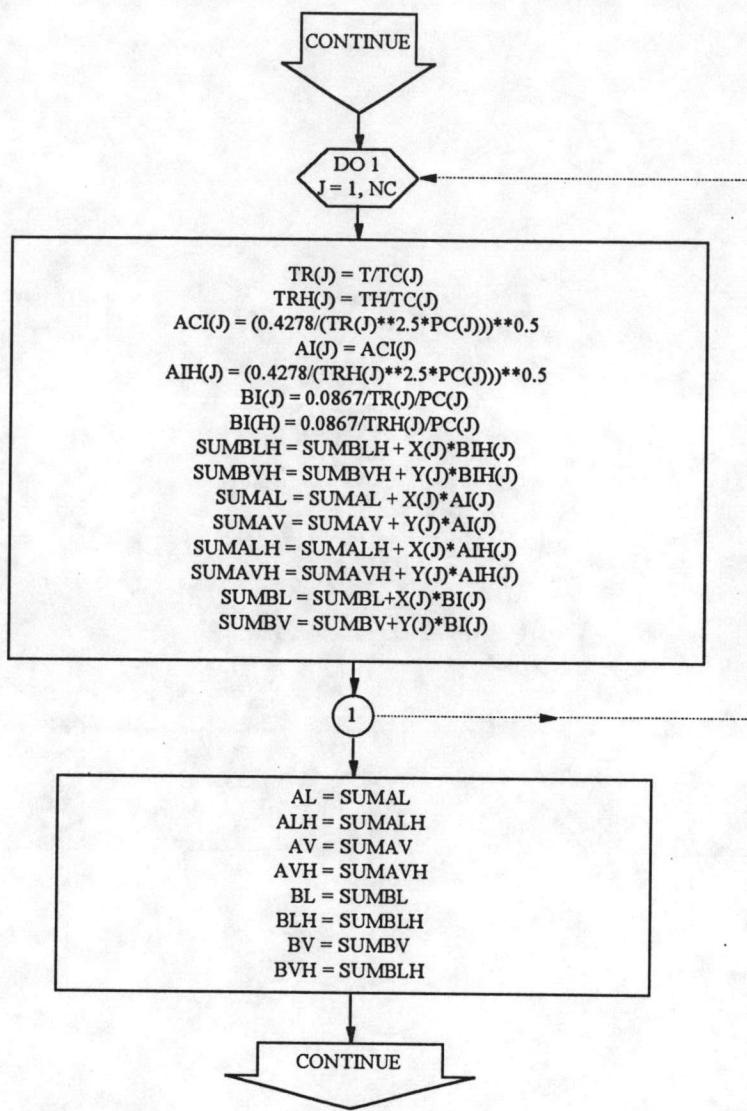
SUBROUTINE NEWTONGR (Continue)

**SUBROUTINE MWDENSG**

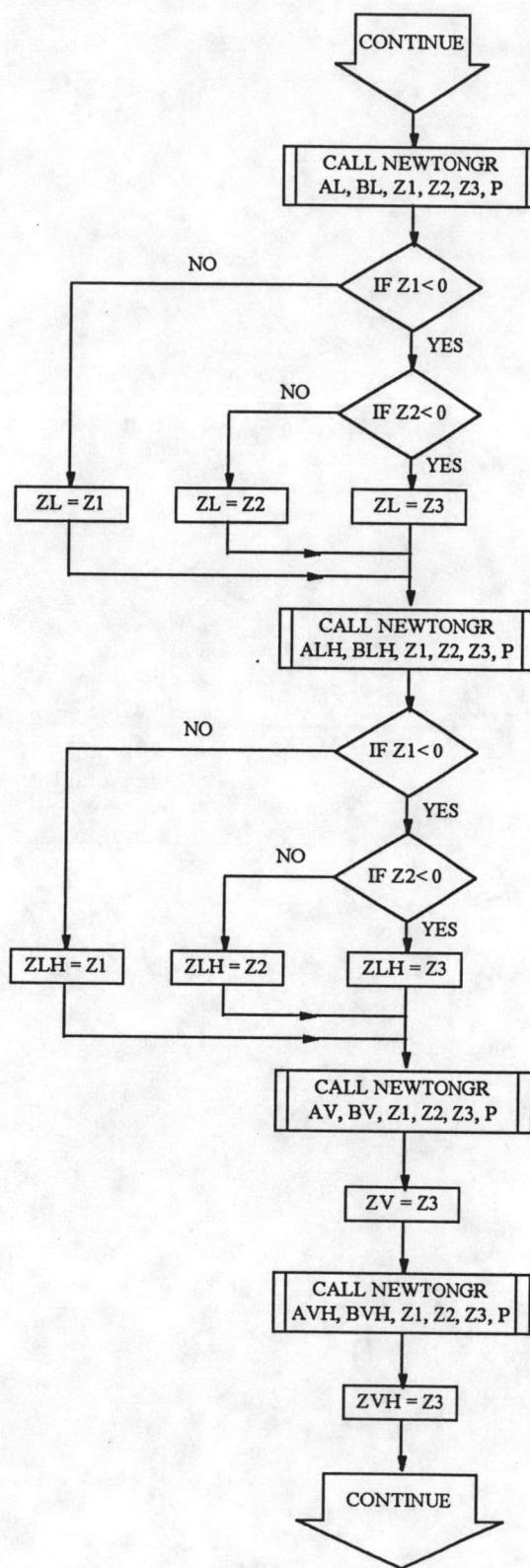
**SUBROUTINE MWDENSG (Continue)**



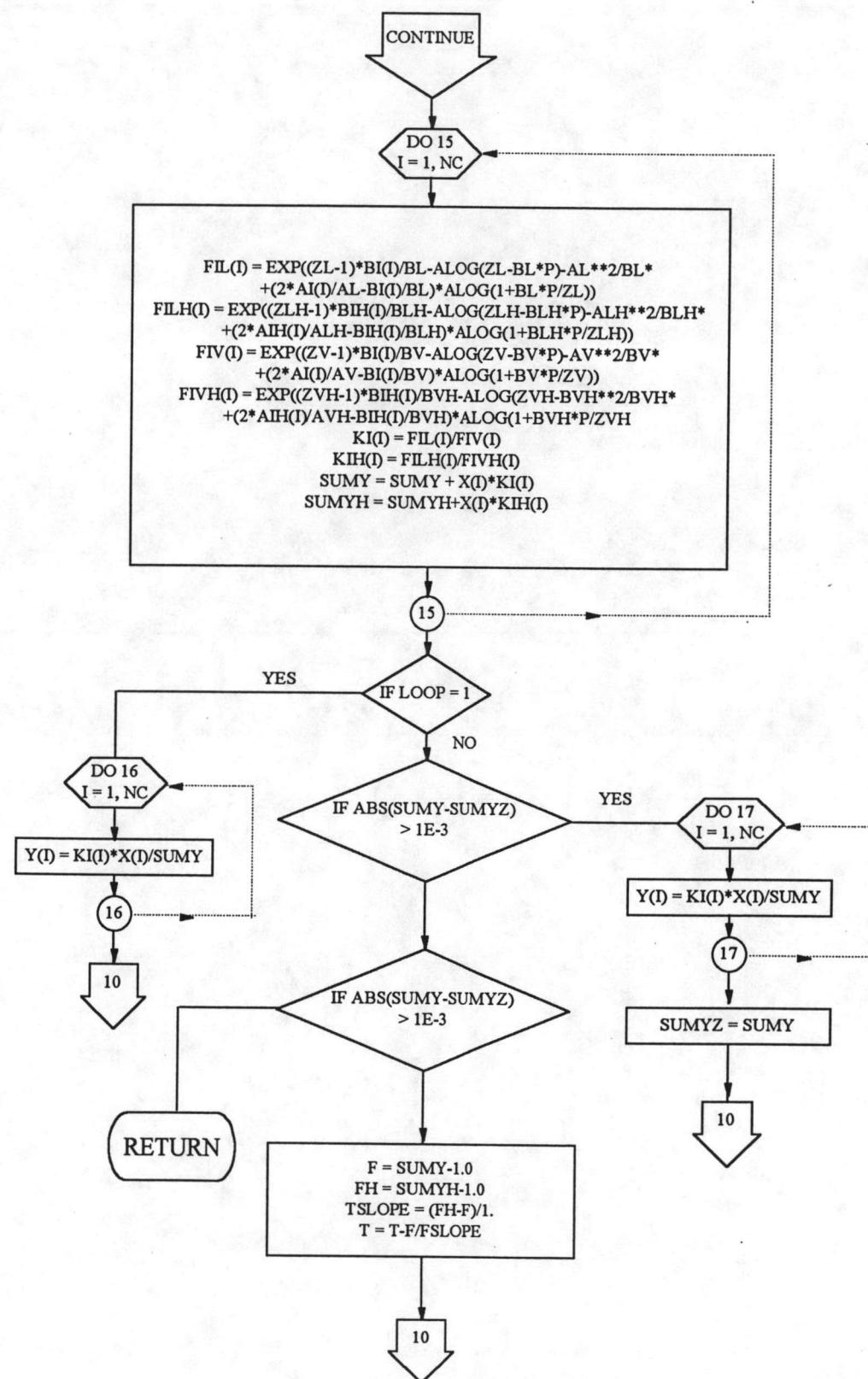
SUBROUTINE BUBPTGR



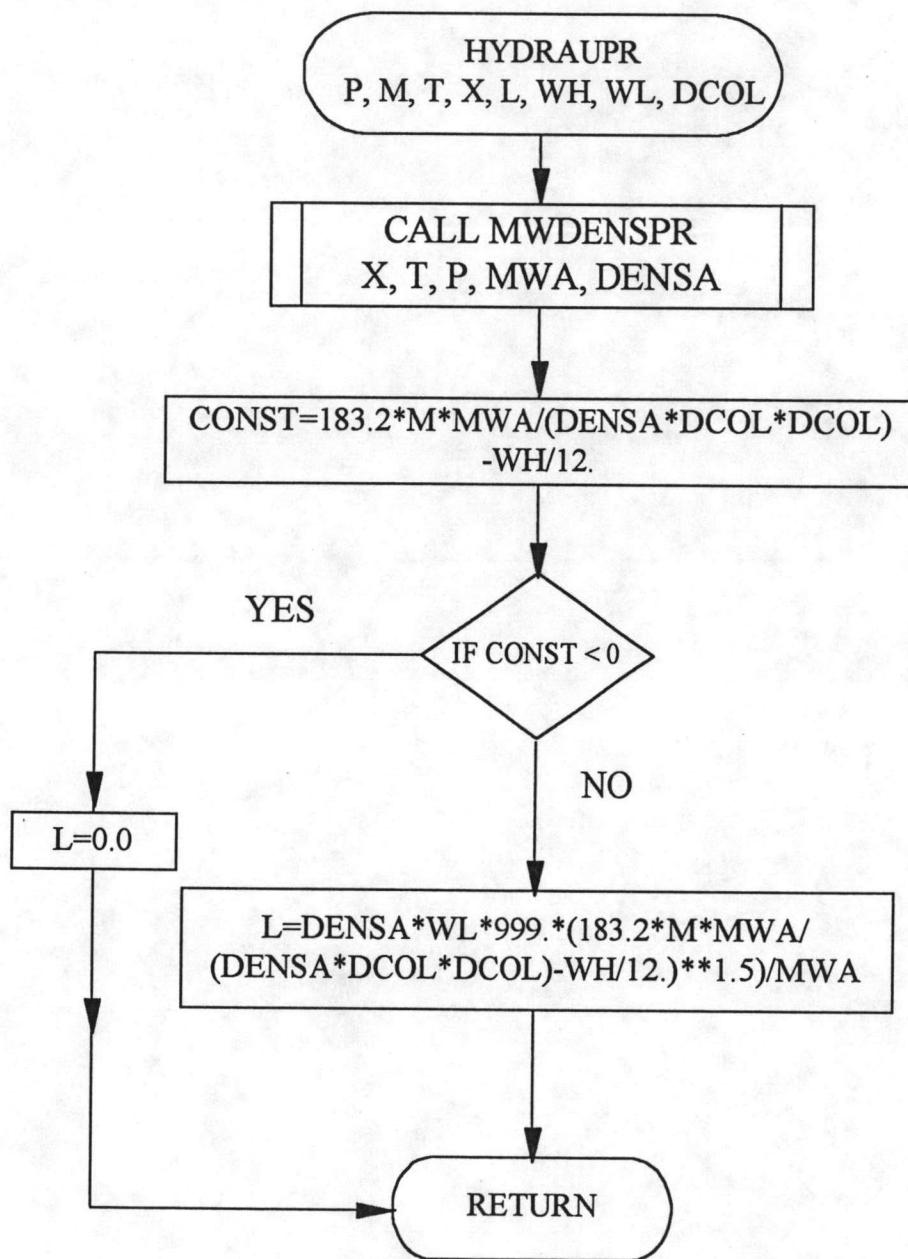
SUBROUTINE BUBPTGR (Continue)



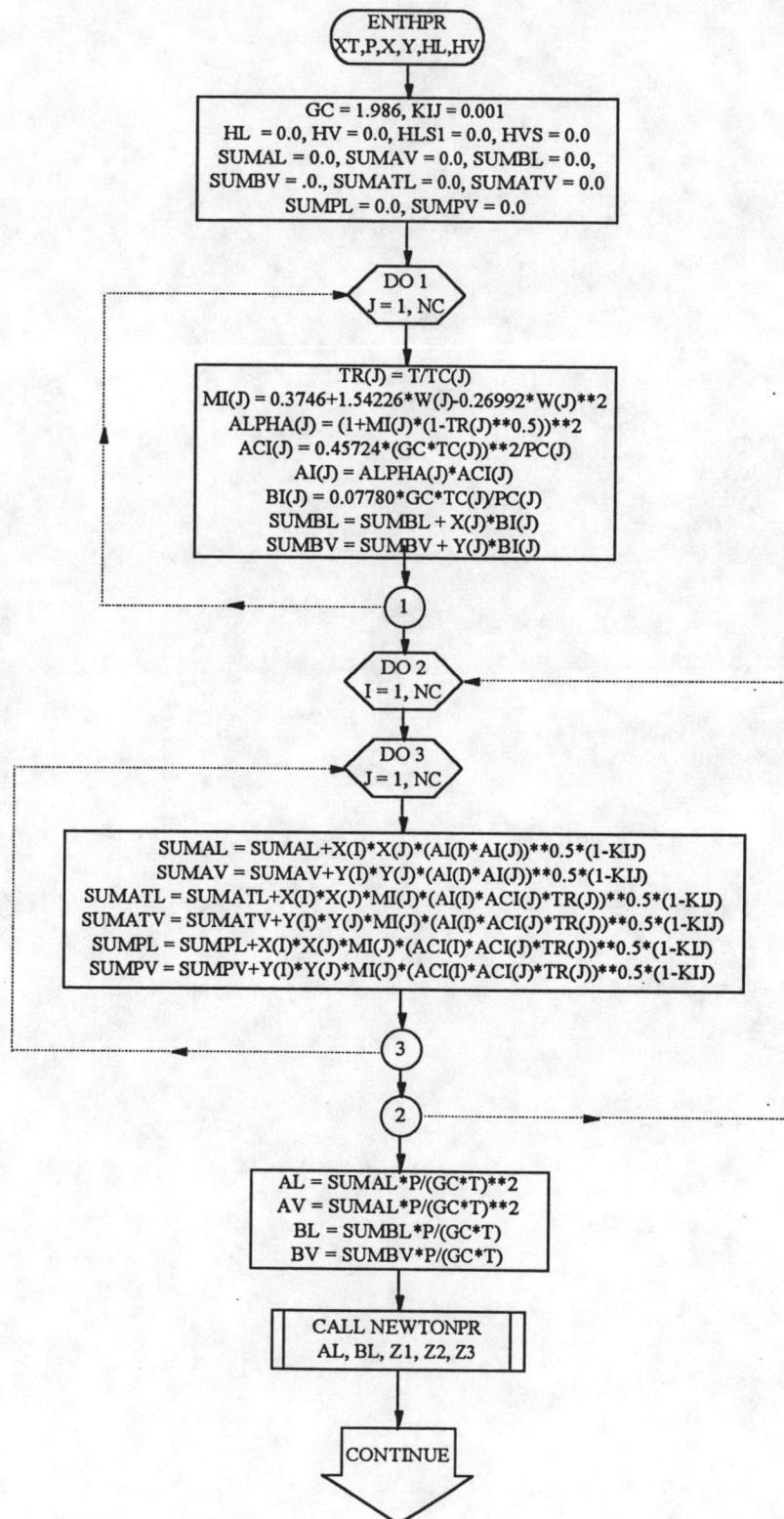
SUBROUTINE BUBPTGR (Continue)



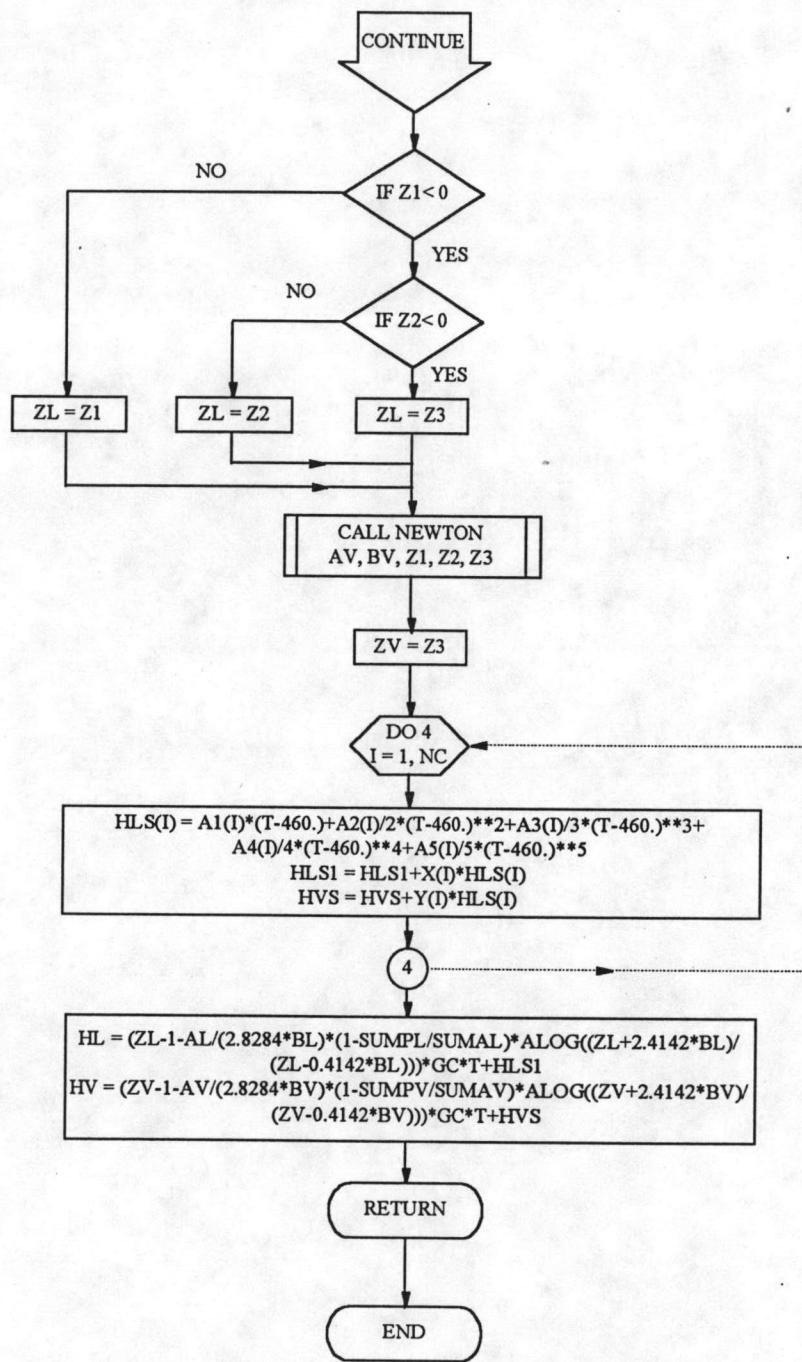
SUBROUTINE BUBPTGR (Continue)



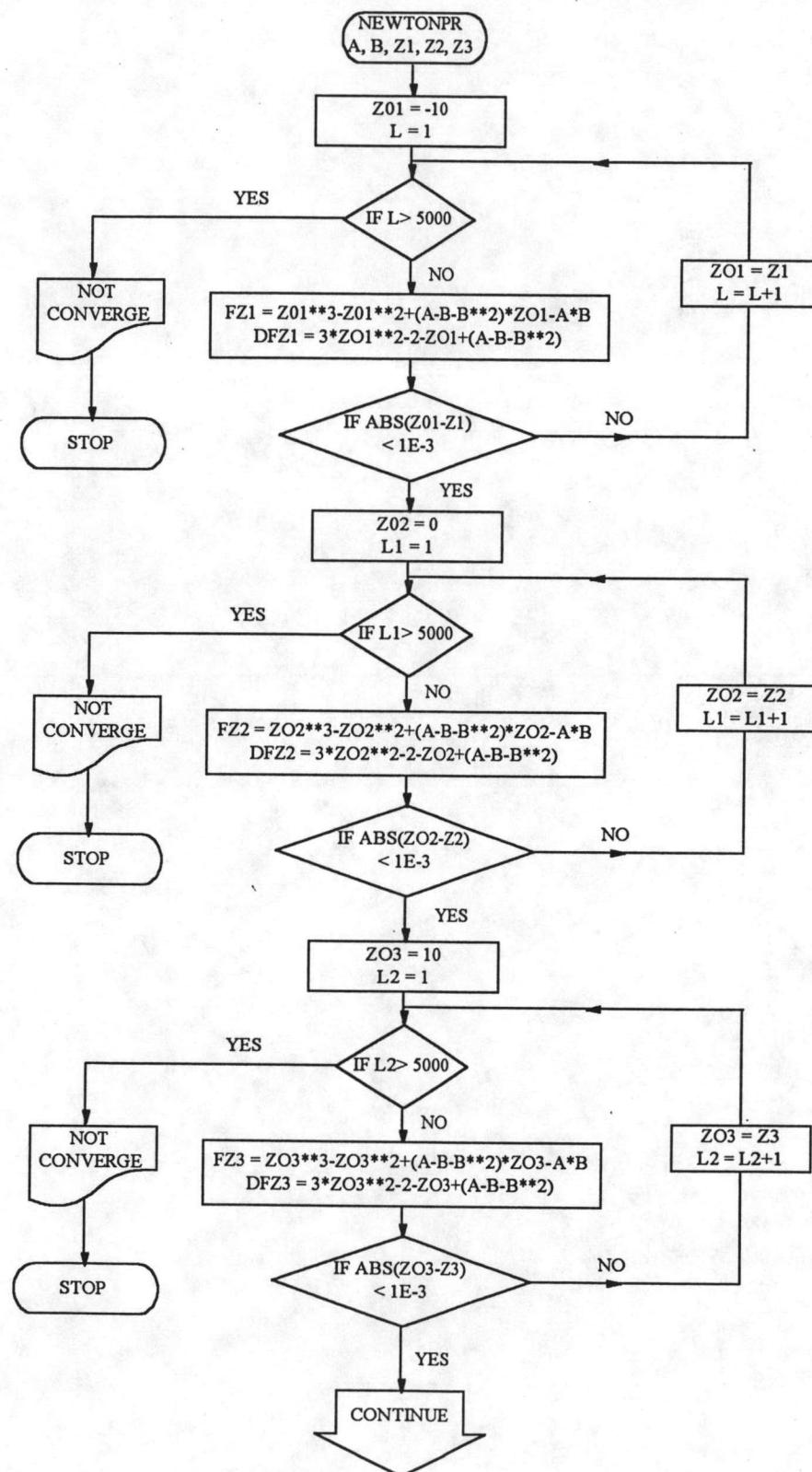
SUBPROGRAM HYDRAUPR



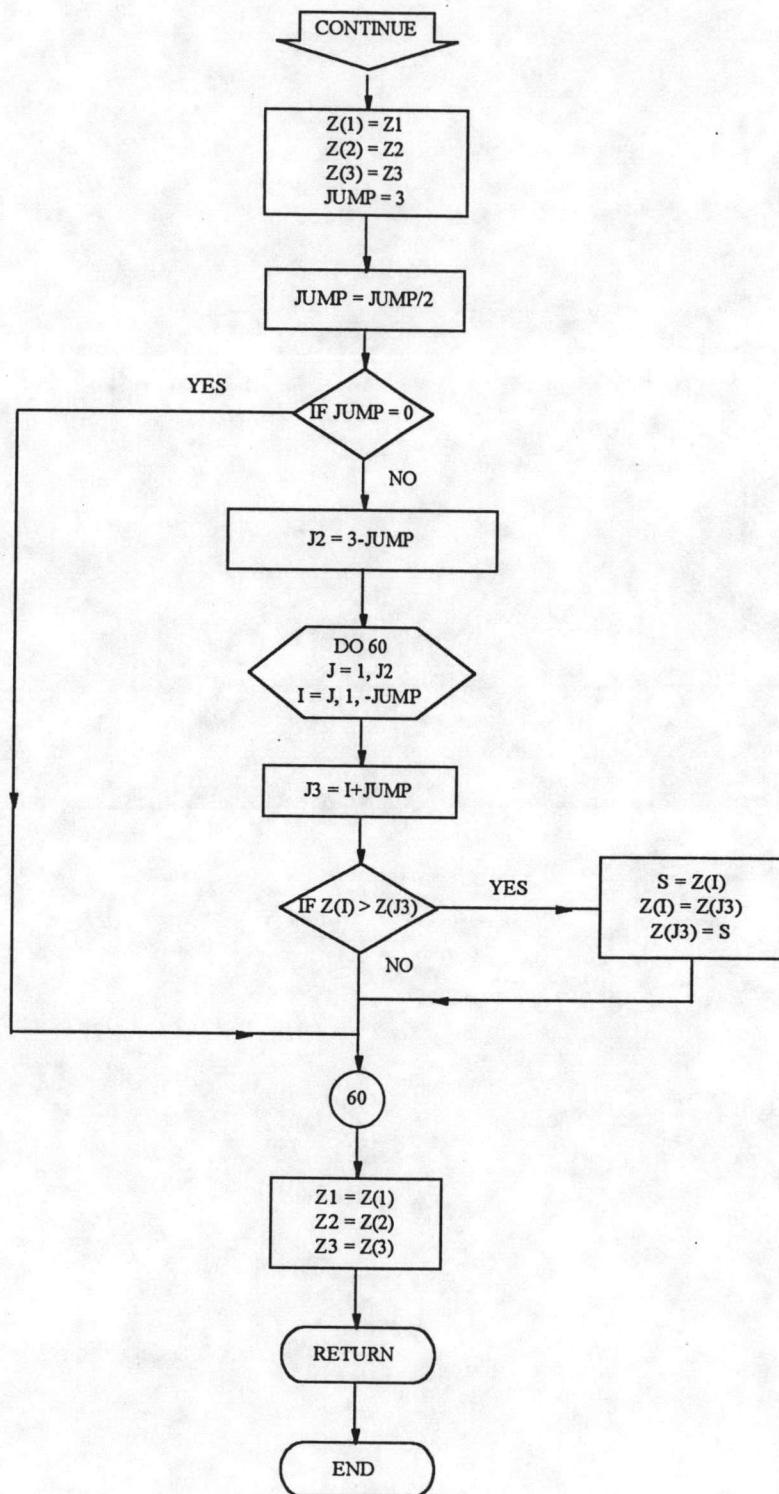
SUBROUTINE ENTHPR



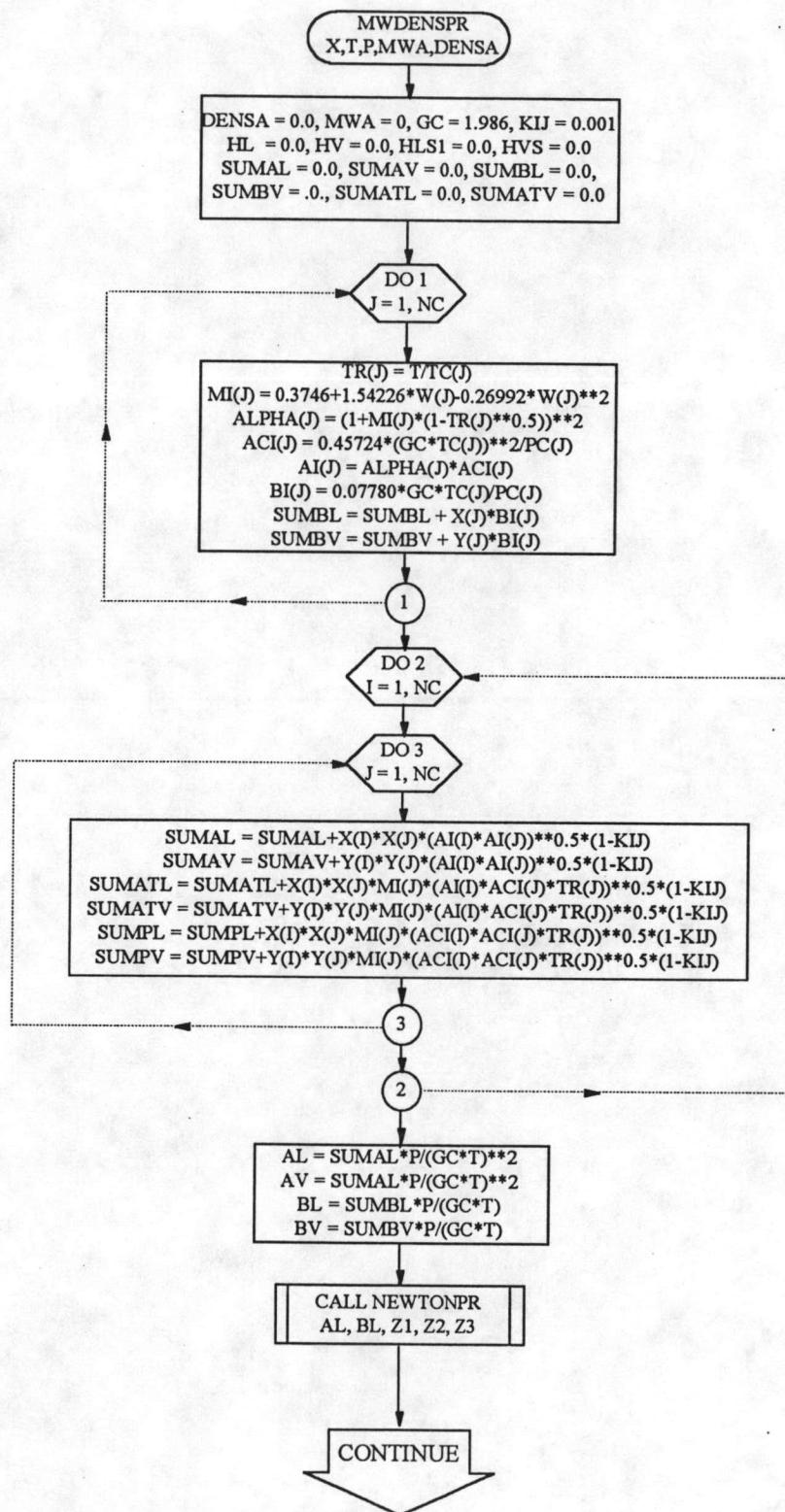
SUBROUTINE ENTHPR (Continue)

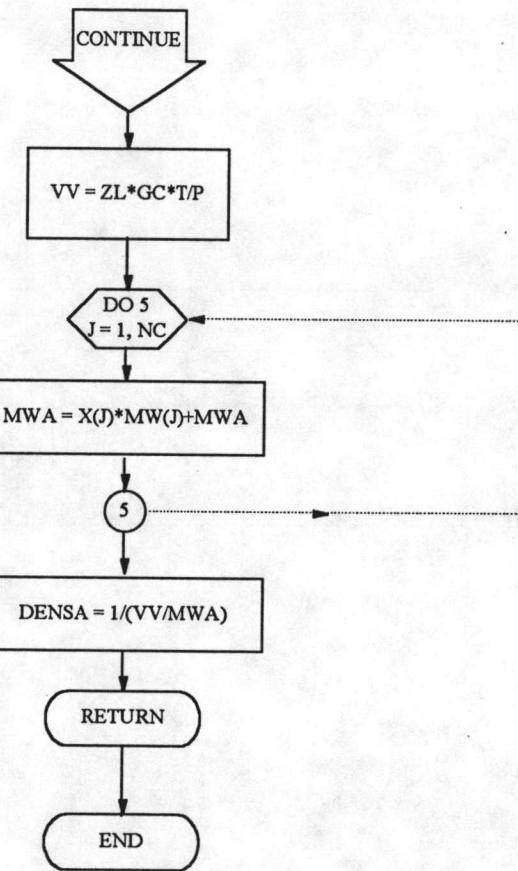


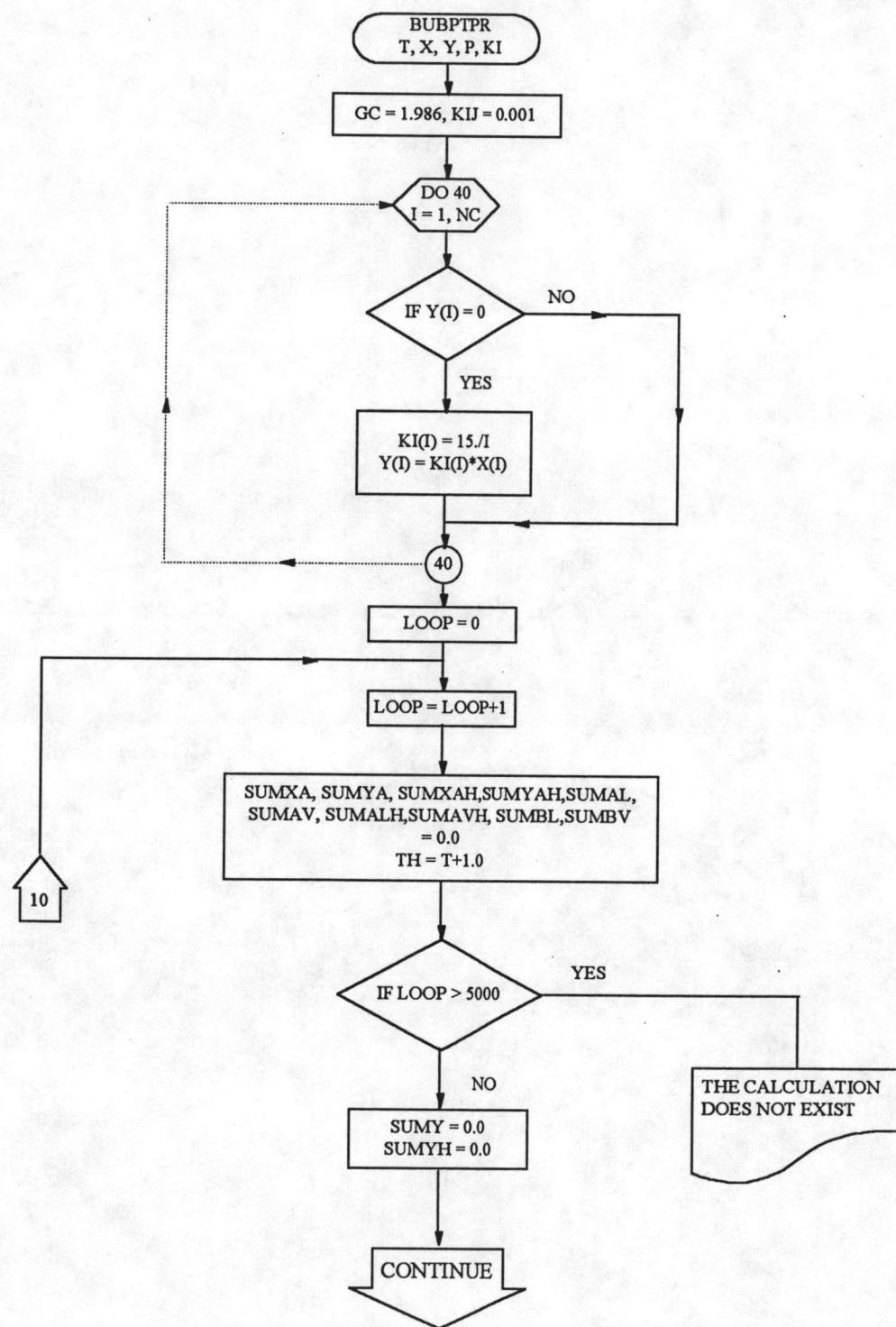
SUBROUTINE NEWTONPR



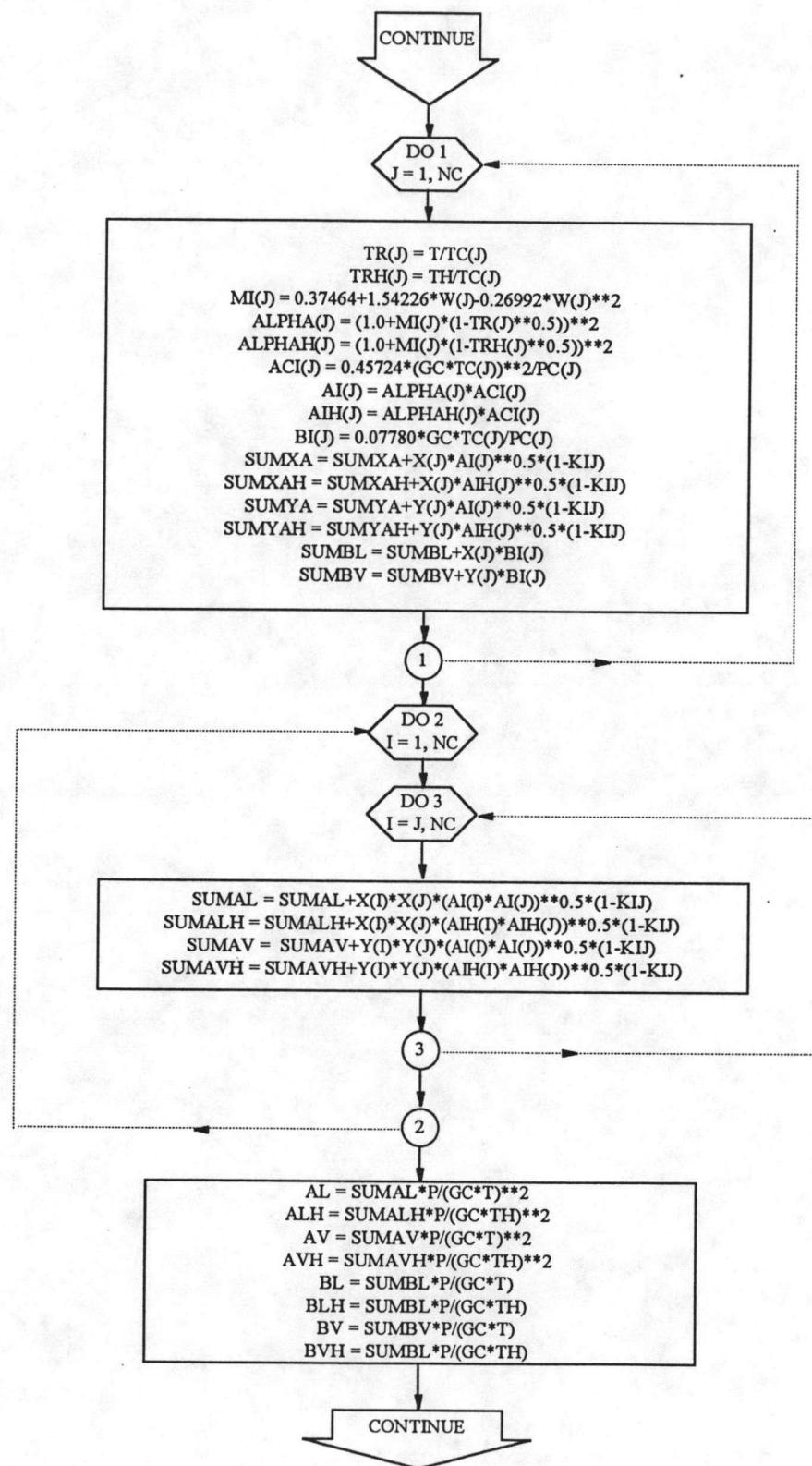
SUBROUTINE NEWTONPR (Continue)

**SUBROUTINE MWDENSPR**

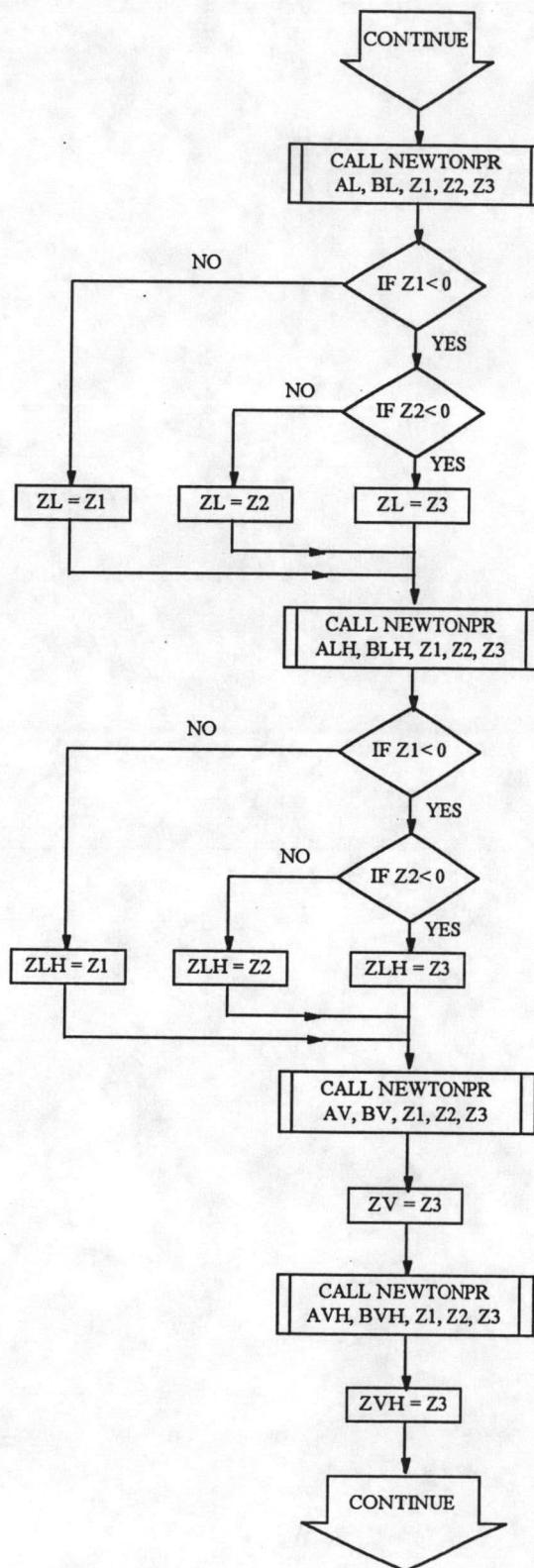
**SUBROUTINE MWDENSPR (Continue)**



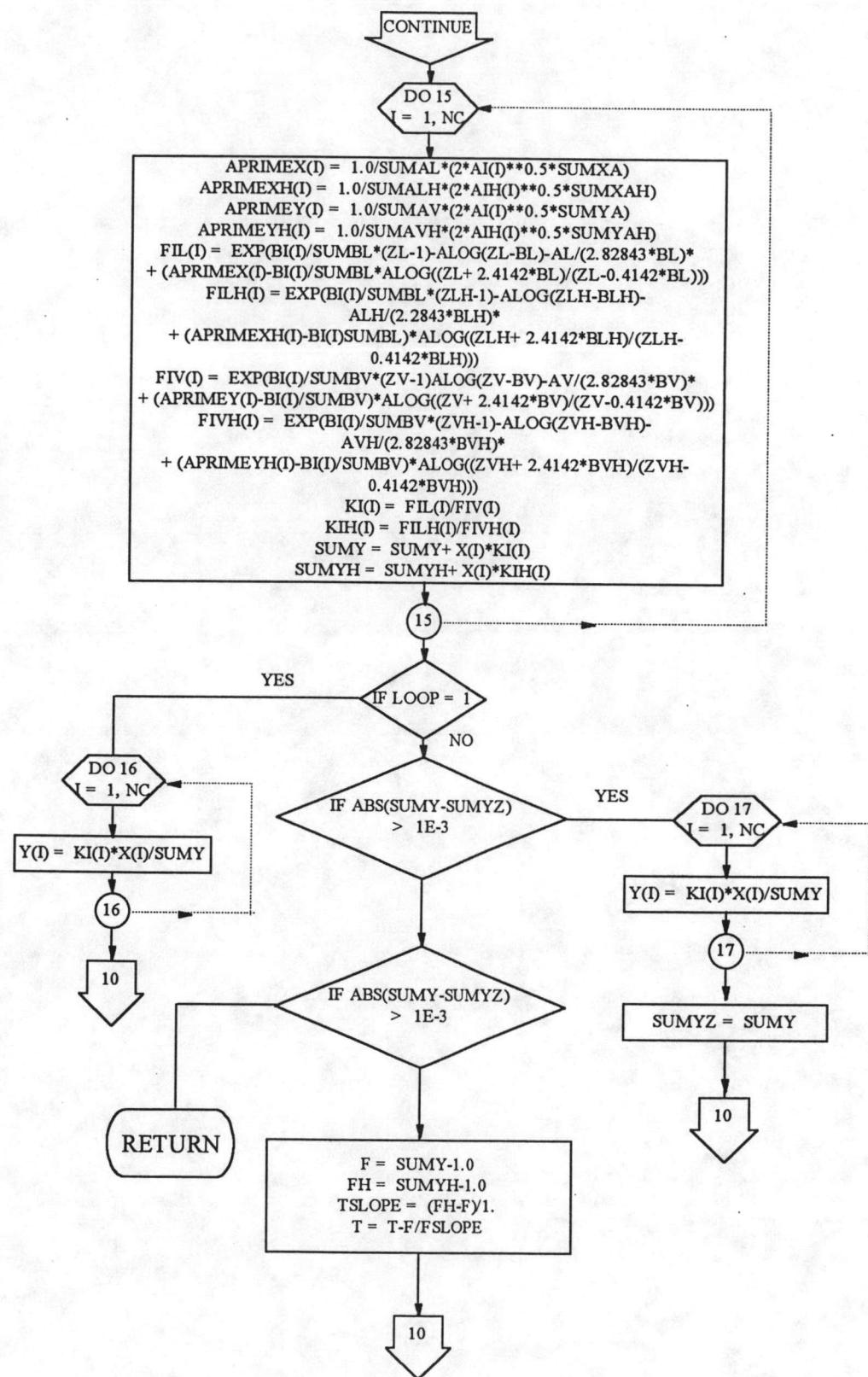
SUBROUTINE BUBPTPR



SUBROUTINE BUBPTPR (Continue)



SUBROUTINE BUBPTPR (Continue)



SUBROUTINE BUBPTPR (Continue)

Appendix B

List of computer program

CC Dynamics Simulation Program for Multicomponent Distillation
CC Created by Miss Kallaya Klaithong C 517152
CC Chemical Engineering Department
CC Chulalongkorn University @1994

INCLUDE 'FGRAPH.FI'

INCLUDE 'FGRAPH.FD'

CC

CC Declare all variables

CC

CC

CC INPUTS R, QR AND DV ARE FIXED

CC

REAL MW,LO,MVB,MVD,MWA,MV,LV,M,L,MB,MD,MW1,TB,TC,PC,ZC,W,
+A1,A2,A3,A4,A5

CHARACTER*15 NAME,NAMEX,name1

CHARACTER str*2

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION LV(50),L(50),P(50),XF(20),YF(20),DXD(20),YAV(20),
+YY(20),HL(50),HV(50),V(50),DM(50),DXM(50,20),XM(50,20),DXB(20)

DIMENSION NAME(20),T(50),XB(20),X(50,20),Y(50,20),LO(50),XD(20),
+YB(20),YD(20),XX(20),MV(50),M(50)

```

INTEGER*2 dummy2, key
EXTERNAL printmenu
RECORD / rccoord / curpos

OPEN( 1, FILE = 'physical.dat' )
OPEN( 2, FILE = 'phytemp.dat' )
OPEN( 5, FILE = 'result.dat')

CC
CC
CC

CALL drawlines()
CALL drawlines2()
dummy2 = settextcolor(15)
CALL settextposition( 3, 28, curpos )
CALL outtext( 'Chulalongkorn University' )
CALL settextposition( 4, 25, curpos )
CALL outtext( 'Chemical Engineering Department' )

dummy2 = settextcolor( 14 )
CALL settextposition( 11, 27, curpos )
CALL outtext( 'Dynamics Simulation Program' )
CALL settextposition(13, 38, curpos )
CALL outtext( 'for' )
CALL settextposition(15, 27, curpos )
CALL outtext( 'Multicomponent Distillation' )

dummy2 = settextcolor( 15 )
CALL settextposition(21, 35, curpos )
CALL outtext( 'Created by' )
CALL settextposition( 22, 24, curpos )
CALL outtext( 'Miss Kallaya Klaithong C 517152' )
CALL settextposition( 23, 32, curpos )
CALL outtext( 'M.Eng. Thesis @ 1994' )

```

```
READ (*,*)  
  
CALL clearscreen( $VIEWPORT )  
  
CC  
CC MENU  
CC  
  
9000 key = -1  
DO WHILE( (key .LT. 0) .OR. (key .GT. 9) )  
    CALL drawlines()  
    CALL drawlines1()  
  
    dummy2 = settextcolor( 14 )  
    CALL settextposition( 4, 30, curpos )  
    CALL outtext( '**** MAIN MENU ****' )  
    dummy2 = settextcolor( 15 )  
    CALL settextposition( 8, 25, curpos )  
    CALL outtext( '0) Exit to Dos' )  
    CALL settextposition( 9, 25, curpos )  
    CALL outtext( '1) Components Database' )  
    CALL settextposition( 10, 25, curpos )  
    CALL outtext( '2) Characteristic of Column' )  
    CALL settextposition( 11, 25, curpos )  
    CALL outtext( '3) Operating Conditions' )  
    CALL settextposition( 12, 25, curpos )  
    CALL outtext( '4) Feed Data' )  
    CALL settextposition( 13, 25, curpos )  
    CALL outtext( '5) Initial Conditions' )  
    CALL settextposition( 14, 25, curpos )  
    CALL outtext( '6) Edit Input Data' )  
    CALL settextposition( 15, 25, curpos )  
    CALL outtext( '7) Save Input Data' )  
    CALL settextposition( 16, 25, curpos )
```

```
CALL outtext( '8) Run' )
CALL settextposition( 17, 25, curpos )
CALL outtext( '9) Reporting & Reviewing the results' )
dummy2 = settextcolor(14)
CALL settextposition( 22, 25, curpos )
CALL outtext ( 'Please ENTER your selection : ' )
READ (*,* ,ERR = 9000) key
END DO
dummy2 = setvideomode( $DEFAULTMODE )

DO WHILE ( key .EQ. 0 )
    GOTO 400
END DO

DO WHILE ( key .EQ. 1 )
    GOTO 9100
END DO

DO WHILE ( key .EQ. 2 )
    GOTO 9200
END DO

DO WHILE ( key .EQ. 3 )
    GOTO 9300
END DO

DO WHILE ( key .EQ. 4 )
    GOTO 9400
END DO

DO WHILE ( key .EQ. 5 )
    GOTO 9500
END DO

DO WHILE ( key .EQ. 6 )
```

```
GOTO 9600
END DO

DO WHILE ( key .EQ. 7 )
    GOTO 9700
END DO

DO WHILE ( key .EQ. 8 )
    GOTO 9800
END DO

CC      DO WHILE ( key .EQ. 9 )
CC      GOTO 9900
CC      END DO

CC
CC      key = 1
CC

CC
CC      Component Database
CC

9100 keyc = -1
DO WHILE( (keyc .LT. 0) .OR. (keyc .GT. 3) )
    CALL drawlines()
    CALL drawlines1()

    dummy2 = settextcolor( 14 )
    CALL settextposition( 4, 30, curpos )
    CALL outtext( '**** COMPONENT MENU ****' )
    dummy2 = settextcolor( 15 )
    CALL settextposition( 10, 25, curpos )
    CALL outtext( '0) Return to Main Menu' )
    CALL settextposition( 12, 25, curpos )
```

```
CALL outtext( '1) List for All Components Database' )
CALL settextposition( 14, 25, curpos )
CALL outtext( '2) Select Component in your system ' )
CALL settextposition( 16, 25, curpos )
CALL outtext( '3) Append New Component Record' )
dummy2 = settextcolor(14)
CALL settextposition( 22, 25, curpos )
CALL outtext ( 'Please ENTER your selection : ' )
READ (*,* ,ERR = 9100) keyc
END DO
dummy2 = setvideomode( $DEFAULTMODE )

DO WHILE ( keyc .EQ. 0 )
    GOTO 9000
END DO

DO WHILE ( keyc .EQ. 1 )
    GOTO 9101
END DO

DO WHILE ( keyc .EQ. 2 )
    GOTO 9102
END DO

DO WHILE ( keyc .EQ. 3 )
    GOTO 9103
END DO

CC
CC      keyc = 1
CC

CC
CC      1) List for All Component
CC
```

```

9101 CALL drawlines()
      CALL drawlines3()
      REWIND( UNIT = 1 )

9111 kk = 0
      dummy2 = settextcolor( 14 )
      CALL settextposition( 3, 27, curpos )
      CALL outtext( '*** Component Library ***' )
      dummy2 = settextcolor( 15 )
      kk1 = 0

9105 READ( 1, 9110, END = 9107 ) NAME1
      CALL settextposition( 6+kk, 10+kk1, curpos )
      CALL outtext( name1 )
      kk1 = kk1+16
      IF ( kk .GE. 16 ) THEN
          dummy2 = settextcolor( 14 )
          CALL settextposition( 23, 4, curpos )
          CALL outtext( ' Press any key to continue ...' )
          READ(*,*)
          CALL drawlines()
          GOTO 9111
      END IF
      IF ( kk1 .GE. 50 ) THEN
          kk = kk + 1
          kk1 = 0
      END IF
      GOTO 9105

9110 FORMAT(3X,A15)
9120 FORMAT(A15)

9107 dummy2 = settextcolor( 14 )
      CALL settextposition( 23, 4, curpos )
      CALL outtext( ' Press any key to continue ...' )
      READ(*,*)
      GOTO 9100

```

CC

CC keyc = 2

CC

CC

CC 2) Select Component

CC

9102 CALL drawlines()

CALL drawlines1()

dummy2 = settextcolor(14)

CALL settextposition(4, 27, curpos)

CALL outtext('*** Component Selection ***')

dummy2 = settextcolor(15)

CALL settextposition(5, 20, curpos)

CALL outtext('The name must be typed in CAPITAL LETTER')

dummy2 = settextcolor(14)

CALL settextposition(9, 18, curpos)

CALL outtext(' Total number of component (NC) = ')

READ(*,*) NC

2220 DO 9130 j = 1, NC

CALL settextposition(10+j, 22, curpos)

WRITE(str, '(I2)') j

CALL outtext('Component Name no.'// str // ' = ')

READ(*,9120) name(j)

REWIND(UNIT = 1)

2200 READ(1, 2070, END = 2210) NAME1

IF (name1 .EQ. name(j)) THEN

BACKSPACE(UNIT = 1)

READ(1, 2080) mw1,tb1,tc1,pc1,zc1,w1,aa1,aa2,aa3,aa4,aa5

mw(j) = mw1

bpt(j) = tb1

tc(j) = tc1

pc(j) = pc1

```

zc(j)      = zc1
w(j)       = w1
a1(j)      = aa1
a2(j)      = aa2
a3(j)      = aa3
a4(j)      = aa4
a5(j)      = aa5
GOTO 9130

END IF

GOTO 2200

2210 CALL settextposition( 24, 5, curpos )
CALL outtext( 'Component not exist !! ... Press ENTER' )
READ(*,*)
CALL drawlines()
CALL drawlines1()
dummy2 = settextcolor( 14 )
CALL settextposition( 4, 27, curpos )
CALL outtext( '*** Component Selection ***' )
dummy2 = settextcolor( 15 )
CALL settextposition( 5, 20, curpos )
CALL outtext( 'The name must be typed in CAPITAL LETTER' )
dummy2 = settextcolor( 14 )
CALL settextposition( 9, 18, curpos )
WRITE( str, '(I2)' ) NC
CALL outtext( ' Total number of component ( NC ) = '// str )
GOTO 2220

9130 CONTINUE
CALL settextposition( 24, 5, curpos )
CALL outtext( 'Press ENTER to continue ...' )
READ(*,*)

2095 kk2 = 0
CALL drawlines()
CALL drawlines3()
dummy2 = settextcolor( 14 )
CALL settextposition( 3, 10, curpos )

```

```

      WRITE( str,(I2) ) NC
      CALL outtext( 'Your system has '//str// components : ' )
      dummy2 = settextcolor( 15 )
      kk3 = 0
      DO 2090 j = 1,NC
      CALL settextposition( 6+kk2, 10+kk3, curpos )
      namex = name(j)
      CALL outtext( namex )
      kk3 = kk3+16
      IF ( kk2 .GE. 16 ) THEN
          dummy2 = settextcolor( 14 )
          CALL settextposition( 23, 4, curpos )
          CALL outtext( ' Press any key to continue ...' )
          READ(*,*)
          CALL drawlines()
          GOTO 2095
      END IF
      IF ( kk3 .GE. 50 ) THEN
          kk2 = kk2 + 1
          kk3 = 0
      END IF
      2090 CONTINUE
      dummy2 = settextcolor( 14 )
      CALL settextposition( 23, 4, curpos )
      CALL outtext( ' Press any key to continue ...' )
      READ(*,*)
      GOTO 9100
      2070 FORMAT(3X,A15)
      2080 FORMAT(18X,F8.3,3F7.1,F6.3,F8.4,F10.6,4E16.7)

```

CC

CC keyc = 3

CC

CC

CC 3) Append New Component Record
 CC

9103 REWIND(UNIT = 1)
 3001 READ(1, 3070, END = 3000) ID,NAME1,MW1,TB1,TC1,PC1,ZC1,W1,AA1,
 +AA2,AA3,AA4,AA5
 WRITE(2,3070) ID,NAME1,MW1,TB1,TC1,PC1,ZC1,W1,AA1,AA2,AA3,AA4,AA5
 GOTO 3001
 3000 CALL drawlines()
 dummy2 = settextcolor(14)
 CALL settextposition(4, 22, curpos)
 CALL outtext('**** APPEND NEW COMPONENT RECORD ****')
 dummy2 = settextcolor(15)
 CALL settextposition(6, 4, curpos)
 CALL outtext('Physical Property')
 dummy2 = settextcolor(14)
 CALL settextposition(10, 4, curpos)
 CALL outtext('ID no. (0 to terminate) = ')
 READ(*,3080) ID
 IF (id .EQ. 0) THEN
 GOTO 3040
 END IF
 CALL settextposition(12, 6, curpos)
 CALL outtext('Component Name = ')
 READ(*,3087) NAME1
 CALL settextposition(13, 6, curpos)
 CALL outtext('Molecular Weight = ')
 READ(*,*) MW1
 CALL settextposition(14, 6, curpos)
 CALL outtext('Boiling Point (R) = ')
 READ(*,*) TB1
 CALL settextposition(15, 6, curpos)
 CALL outtext('Critical Temp.(R) = ')
 READ(*,*) TC1
 CALL settextposition(16, 6, curpos)



```

CALL outtext( 'Critical Press.(psia) = ' )
READ(*,*) PC1

CALL settextposition( 17, 6, curpos )
CALL outtext( 'Critical Z-factor      = ' )
READ(*,*) ZC1

CALL settextposition( 18, 6, curpos )
CALL outtext( 'Acentric Factor      = ' )
READ(*,*) W1

dummy2 = settextcolor( 15 )

CALL settextposition( 6, 45, curpos )
CALL outtext( 'Heat Capacity Coefficients' )

dummy2 = settextcolor( 14 )

CALL settextposition( 12, 47, curpos )
CALL outtext( ' a1   = ' )
READ(*,*) AA1

CALL settextposition( 13, 47, curpos )
CALL outtext( ' a2   = ' )
READ(*,*) AA2

CALL settextposition( 14, 47, curpos )
CALL outtext( ' a3   = ' )
READ(*,*) AA3

CALL settextposition( 15, 47, curpos )
CALL outtext( ' a4   = ' )
READ(*,*) AA4

CALL settextposition( 16, 47, curpos )
CALL outtext( ' a5   = ' )
READ(*,*) AA5

WRITE(2,3070) ID,NAME1,MW1,TB1,TC1,PC1,ZC1,W1,AA1,AA2,AA3,AA4,AA5
GOTO 3000

3040 END FILE(UNIT = 2)

3070 FORMAT(I3,A15,F8.3,3F7.1,F6.3,F8.4,F10.6,4E16.7)
3080 FORMAT(I3)
3087 FORMAT(A15)
3090 FORMAT(F4.1)

```

3095 FORMAT(F5.3)

3097 FORMAT(F5.4)

GOTO 9100

CC

CC key = 2

CC

CC

CC READ COLUMN DATA

CC

9200 CALL drawlines()

CALL drawlines2()

dummy2 = settextcolor(15)

CALL settextposition(4, 23, curpos)

CALL outtext('**** Characteristic of Column ****')

2000 dummy2 = settextcolor(14)

CALL settextposition(8, 14, curpos)

CALL outtext('Total number of plates (NT) = ')

READ(*,*) NT

CALL settextposition(10, 14, curpos)

CALL outtext('Number of trays in stripping section (NF) = ')

READ(*,*) NF

CALL settextposition(11, 14, curpos)

CALL outtext('Weir height in stripping section (WHS) = ')

READ(*,*) WHS

CALL settextposition(12, 14, curpos)

CALL outtext('Weir height in rectifying section (WHR) = ')

READ(*,*) WHR

CALL settextposition(13, 14, curpos)

CALL outtext('Column diameter in stripping section (DS) = ')

READ(*,*) DS

CALL settextposition(14, 14, curpos)

CALL outtext('Column diameter in rectifying section (DR) = ')

```

READ(*,*) DR
CALL settextposition( 15, 14, curpos )
CALL outtext( 'Weir length in stripping section    (WLS) = ' )
READ(*,*) WLS
CALL settextposition( 16, 14, curpos )
CALL outtext( 'Weir length in rectifying section   (WLR) = ' )
READ(*,*) WLR
CALL settextposition( 17, 14, curpos )
CALL outtext( 'Volumetric holdup in column base   (MVB) = ' )
READ(*,*) MVB
CALL settextposition( 18, 14, curpos )
CALL outtext( 'Volumetric holdup in reflux drum   (MVD) = ' )
READ(*,*) MVD
301 FORMAT(A)
13 FORMAT( 3I3 )
14 FORMAT( 8F6.2 )
CALL settextposition( 24, 5, curpos )
CALL outtext( 'Press ENTER to continue ...' )
READ(*,*)
GOTO 9000

```

```

CC
CC      key = 3
CC

```

```

CC
CC      READ CONDITIONS
CC

```

```

9300 CALL drawlines()
CALL drawlines2()
dummy2 = settextcolor( 15 )
CALL settextposition( 4, 25, curpos )
CALL outtext( '**** Operating Conditions ****' )
dummy2 = settextcolor( 14 )

```

```

CALL settextposition( 8, 14, curpos )
CALL outtext( 'Pressure in top of column PD, (psia) = ' )
READ(*,*) PD

CALL settextposition( 10, 14, curpos )
CALL outtext( 'Pressure in bottom of column PB, (psia) = ' )
READ(*,*) PB

CALL settextposition( 12, 14, curpos )
CALL outtext( 'Reboiler heat-duty QR, (x 1,000 Btu/hr) = ' )
READ(*,*) QR

CALL settextposition( 14, 14, curpos )
CALL outtext( 'Reflux rate R, (moles/hr) = ' )
READ(*,*) R

CALL settextposition( 16, 14, curpos )
CALL outtext( 'Vapor product from reflux drum DV, (moles/hr) = ' )
READ(*,*) DV

CALL settextposition( 18, 14, curpos )
CALL outtext( 'Murphree vapor-phase tray efficiency EFF = ' )
READ(*,*) EFF

CALL settextposition( 24, 5, curpos )
CALL outtext( 'Press ENTER to continue ...' )
READ(*,*)

GOTO 9000

```

```

CC
CC      key = 4
CC

```

```

CC
CC  READ FEED
CC

```

```

9400 CALL drawlines()
CALL drawlines2()
dummy2 = settextcolor( 15 )
CALL settextposition( 4, 29, curpos )

```

```

CALL outtext( '**** Feed Data ****' )
dummy2 = settextcolor( 14 )
CALL settextposition( 8, 14, curpos )
CALL outtext( 'Liquid Feed flow rate (moles/hr) = ' )
READ(*,*) FL
CALL settextposition( 9, 14, curpos )
CALL outtext( 'Liquid Feed temperature (F) = ' )
READ(*,*) TFL
CALL settextposition( 11, 14, curpos )
CALL outtext( 'Composition (mole fraction) : ' )
DO 310 J = 1,NC
CALL settextposition( 11+J, 17, curpos )
namex = name(j)
CALL outtext( namex // ' = ' )
READ(*,*) XF(J)

310 CONTINUE
CALL drawlines()
CALL drawlines2()
dummy2 = settextcolor( 15 )
CALL settextposition( 4, 29, curpos )
CALL outtext( '**** Feed Data ****' )
dummy2 = settextcolor( 14 )
CALL settextposition( 8, 14, curpos )
CALL outtext( 'Vapor Feed flow rate (moles/hr) = ' )
READ(*,*) FV
CALL settextposition( 9, 14, curpos )
CALL outtext( 'Vapor Feed temperature (F) = ' )
READ(*,*) TFV
CALL settextposition( 11, 14, curpos )
CALL outtext( 'Composition (mole fraction) : ' )
DO 320 J = 1,NC
CALL settextposition( 11+J, 17, curpos )
namex = name(j)
CALL outtext( namex // ' = ' )
READ(*,*) YF(J)

```

320 CONTINUE

```
CC      CALL ENTHS(TFL,P(NF),XF,YF,HLF,HVF)
       8 FORMAT(1X,2F8.2,10E10.2)
       CALL settextposition( 24, 5, curpos )
       CALL outtext( 'Press ENTER to continue ...' )
       READ(*,*)
       GOTO 9000
```

CC

```
CC      key = 5
CC
```

CC

```
CC      READ INITIAL CONDITIONS
CC
```

9500 CALL drawlines()

```
CALL drawlines2()
dummy2 = settextcolor( 15 )
CALL settextposition( 4, 25, curpos )
CALL outtext( '**** Initial Conditions ****' )
dummy2 = settextcolor( 14 )
CALL settextposition( 8, 14, curpos )
CALL outtext( 'Temperature in column base TB, (F) = ' )
READ(*,*) TB
CALL settextposition( 10, 14, curpos )
CALL outtext( 'Composition in Column base :')
DO 510 J = 1,NC
CALL settextposition( 11+J, 17, curpos )
namex = name(j)
CALL outtext( namex // ' = ' )
READ(*,*) XB(J)
```

510 CONTINUE

```
DO 15 N = 1,NT
CALL drawlines()
```

```

CALL drawlines2()
dummy2 = settextcolor( 15 )
CALL settextposition( 4, 25, curpos )
CALL outtext( '**** Initial Conditions ****' )
dummy2 = settextcolor( 14 )
WRITE( str, '(I2)' ) N
CALL settextposition( 8, 14, curpos )
CALL outtext( 'Temperature in tray no.'//str//'(F) = ' )
READ(*,*) T(N)
CALL settextposition( 9, 14, curpos )
CALL outtext( 'Liquid flow rate in tray no.'//str//'(moles/hr) =
+ ' )
READ(*,*) LO(N)
DO 520 J = 1,NC
CALL settextposition( 10, 14, curpos )
CALL outtext( 'Composition in tray no.'//str//': ' )
CALL settextposition( 11+J, 17, curpos )
namex = name(j)
CALL outtext( namex // ' = ' )
READ(*,*) X(N,J)
520 CONTINUE
BLANK=0.
CALL settextposition( 24, 5, curpos )
CALL outtext( 'Press ENTER to continue ...' )
READ(*,*)

15 CONTINUE
CALL drawlines()
CALL drawlines2()
dummy2 = settextcolor( 15 )
CALL settextposition( 4, 25, curpos )
CALL outtext( '**** Initial Conditions ****' )
dummy2 = settextcolor( 14 )
CALL settextposition( 8, 14, curpos )
CALL outtext( 'Temperature in reflux drum TD, (F) = ' )
READ(*,*) TD

```

```

CALL settextposition( 10, 14, curpos )
CALL outtext( 'Composition in reflux drum :' )
DO 530 J = 1,NC
CALL settextposition( 11+J, 17, curpos )
namex = name(j)
CALL outtext( namex // '=' )
READ(*,*) XD(J)
530 CONTINUE
    CALL settextposition( 24, 5, curpos )
    CALL outtext( 'Press ENTER to continue ...' )
    READ(*,*)
    GOTO 9000

```

```

CC
CC      Read old data from floppy disk
CC

```

```

CC
CC      key = 6
CC

```

```

9600 CALL old()
    REWIND(UNIT = 3)
    READ(3,9610) NC
    DO 9615 j = 1,NC
    READ(3,9625) name(j),mw(j),bpt(j),tc(j),pc(j),zc(j),w(j),a1(j),
    +a2(j),a3(j),a4(j),a5(j)
9615 CONTINUE
    READ(3,9630) NT,NF,WHS,WHR,DS,DR,WLS,WLR,MVB,MVD
    READ(3,9640) PD,PB,QR,R,DV,EFF
    READ(3,9645) FL,TFL,(XF(J), J = 1,NC)
    READ(3,9645) FV,TFV,(YF(J), J = 1,NC)
    BLANK = 0.
    READ(3,9650) TB,BLANK,(XB(J), J = 1,NC)
    DO 9660 N = 1,NT

```

NN = N
 READ(3,9655) NN,T(N),LO(N),(X(N,J),J=1,NC)
 9660 CONTINUE
 READ(3,9650) TB,R,(XD(J), J = 1,NC)
 9610 FORMAT(I3)
 9625 FORMAT(A15,F8.3,3F7.1,F6.3,F8.4,F10.6,4E16.7)
 9630 FORMAT(2I3,8F6.2)
 9640 FORMAT(6F8.2)
 9645 FORMAT(2F12.2,20E16.7)
 9650 FORMAT(5X,2F8.2,20E16.7)
 9655 FORMAT(1X,I3,1X,2F8.2,20E16.7)
 GOTO 9000

CC
 CC Save data into floppy disk
 CC
 CC
 CC key = 7
 CC

9700 CALL save()
 WRITE(4,9610) NC
 DO 9715 j = 1,NC
 WRITE(4,9625) name(j),mw(j),bpt(j),tc(j),pc(j),zc(j),w(j),a1(j),
 +a2(j),a3(j),a4(j),a5(j)
 9715 CONTINUE
 WRITE(4,9630) NT,NF,WHS,WHR,DS,DR,WLS,WLR,MVB,MVD
 WRITE(4,9640) PD,PB,QR,R,DV,EFF
 WRITE(4,9645) FL,TFL,(XF(J), J = 1,NC)
 WRITE(4,9645) FV,TFV,(YF(J), J = 1,NC)
 WRITE(4,9650) TB,BLANK,(XB(J), J = 1,NC)
 DO 9760 N = 1,NT
 NN = N
 WRITE(4,9655) NN,T(N),LO(N),(X(N,J),J=1,NC)

9760 CONTINUE

WRITE(4,9650) TB,R,(XD(J), J = 1,NC)

GOTO 9000

CC RUN SRK MODEL

CC

CC key = 8.1

CC

CC

CC Assign temperature in Degree Rangin

CC

9800 TFL = TFL + 460.

TFV = TFV + 460.

TB = TB + 460.

TD = TD + 460.+125.0

DO 18 N = 1,NT

T(N) = T(N) + 460.

18 CONTINUE

CC

CC CALCULATE PRESSURE PROFILE

CC

CALL drawlines()

DO 35 N=1,NT

35 P(N)=(PB-(N*(PB-PD))/NT)

DELTA = 0.0001

WRITE(*,37) DELTA

37 FORMAT(1X,' DELTA = ', F8.5)

TIME = 0.

TPRINT = 0.

CALL ENTHS(TFL,P(NF),XF,YF,HLF,HVF)

CC

CC CALL INTITIAL HOLDUPS

CC

CALL MWDENSS(XB,TB,PB,MWA,DENSA)

MB=MVB*DENSA/MWA

DO 20 N=1,NF

DO 21 J=1,NC

21 XX(J) = X(N,J)

CALL MWDENSS(XX,T(N),P(N),MWA,DENSA)

LV(N) = LO(N)*MWA/DENSA

L(N) = LO(N)

HFLOW = (LV(N)/(999.*WLS))**.66667

MV(N) = (HFLOW+WHS/12.)*3.1416*DS*DS/(4.*144.)

M(N) = MV(N)*DENSA/MWA

20 CONTINUE

DO 25 N = NF+1,NT

DO 26 J = 1,NC

26 XX(J) = X(N,J)

CALL MWDENSS(XX,T(N),P(N),MWA,DENSA)

LV(N) = LO(N)*MWA/DENSA

L(N) = LO(N)

HFLOW = (LV(N)/(999.*WLR))**.66667

MV(N) = (HFLOW+WHR/12.)*3.1416*DR*DR/(4.*144.)

M(N) = MV(N)*DENSA/MWA

25 CONTINUE

DO 30 N=1,NT

DO 31 J=1,NC

XM(N,J)=M(N)*X(N,J)

31 CONTINUE

30 CONTINUE

```
CALL MWDENSS(XD,TD,PD,MWA,DENSA)
MD=MVD*DENSA/MWA
```

CC

CC Initial Guess of V(5) for first efficiency calculation

CC

V(NF) = 822.

CC

CC Main Loop for each time step

CC

xxx=0

100 CONTINUE

write(*,*) xxx

CALL BUBPTS (TB,XB,YB,PB)

CALL ENTHS (TB,PB,XB,YB,HLB,HVB)

DO 105 J=1,NC

105 XX(J)=X(1,J)

CALL BUBPTS (T(1),XX,YY,P(1))

DO 106 J=1,NC

Y(1,J)=YB(J)+EFF*(YY(J)-YB(J))

106 YY(J)=Y(1,J)

CALL ENTHS(T(1),P(1),XX,YY,HL(1),HV(1))

DO 110 N=2,NF

DO 111 J=1,NC

111 XX(J)=X(N,J)

CALL BUBPTS(T(N),XX,YY,P(N))

DO 112 J = 1,NC

$Y(N,J) = (YY(J) - Y(N-1,J)) * EFF + Y(N-1,J)$
 112 YY(J)=Y(N,J)
 CALL ENTHS(T(N),P(N),XX,YY,HL(N),HV(N))

110 CONTINUE

DO 113 J=1,NC
 113 XX(J)=X(NF+1,J)
 CALL BUBPTS(T(NF+1),XX,YY,P(NF+1))
 DO 114 J=1,NC
 $YAV(J) = (YF(J)*FV + Y(NF,J)*V(NF)) / (V(NF) + FV)$
 $Y(NF+1,J) = (YY(J) - YAV(J)) * EFF + YAV(J)$
 114 YY(J)=Y(NF+1,J)
 CALL ENTHS(T(NF+1),P(NF+1),XX,YY,HL(NF+1),HV(NF+1))
 DO 115 N=NF+2,NT
 DO 116 J=1,NC
 116 XX(J)=X(N,J)
 CALL BUBPTS(T(N),XX,YY,P(N))
 DO 117 J=1,NC
 $Y(N,J) = (YY(J) - Y(N-1,J)) * EFF + Y(N-1,J)$
 117 YY(J)=Y(N,J)
 CALL ENTHS (T(N),P(N),XX,YY,HL(N),HV(N))

115 CONTINUE

CALL BUBPTS (TD,XD,YD,PD)
 CALL ENTHS(TD,PD,XD,YD,HLD,HVD)

CC

CC CALCULATE VAPOR RATES

CC

$VB = (QR * 1000. - L(1) * (HLB - HL(1))) / (HVB - HLB)$

$B = L(1) - VB$

CC IF (B .LT. 0.) THEN

CC WRITE(*,*) ' ***** B IS LESS THAN 0 *****'

CC STOP

CC END IF

$$V(1) = (HL(2)*L(2) + HVB*VB - HL(1)*L(1)) / HV(1)$$

DO 120 N=2,NF-1

$$V(N) = (HL(N+1)*L(N+1) + HV(N-1)*V(N-1) - HL(N)*L(N)) / HV(N)$$

120 CONTINUE

$$V(NF) = (HL(NF+1)*L(NF+1) + HV(NF-1)*V(NF-1) - HL(NF)*L(NF) + HLF*FL) / HV(NF)$$

$$V(NF+1) = (HL(NF+2)*L(NF+2) + HV(NF)*V(NF) + HV*FV - HL(NF+1)*L(NF+1)) / HV(NF+1)$$

DO 130 N=NF+2,NT-1

$$130 V(N) = (HL(N+1)*L(N+1) + HV(N-1)*V(N-1) - HL(N)*L(N)) / HV(N)$$

$$V(NT) = (HLD*R + HV(NT-1)*V(NT-1) - HL(NT)*L(NT)) / HV(NT)$$

$$DL = V(NT) - DV - R$$

CC IF (DL .LT. 0) THEN

CC WRITE(*,*) ' ***** DL IS LESS THAN 0 *****'

CC STOP

CC END IF

CC

CC EVALUATE DERIVATIVES

CC

$$DM(1) = L(2) + VB - V(1) - L(1)$$

DO 140 N=2,NF-1

$$140 DM(N) = L(N+1) + V(N-1) - L(N) - V(N)$$

$$DM(NF) = L(NF+1) + FL + V(NF-1) - L(NF) - V(NF)$$

$$DM(NF+1) = L(NF+2) + FV + V(NF) - L(NF+1) - V(NF+1)$$

DO 150 N=NF+2,NT-1

$$150 DM(N) = L(N+1) + V(N-1) - L(N) - V(N)$$

$$DM(NT) = R + V(NT-1) - L(NT) - V(NT)$$

DO 160 J=1,NC

$$DXB(J) = (X(1,J)*L(1) - YB(J)*VB - XB(J)*B) / MB$$

$$DXM(1,J) = X(2,J)*L(2) + YB(J)*VB - X(1,J)*L(1) - Y(1,J)*V(1)$$

DO 165 N=2,NF-1

```

165 DXM(N,J)=X(N+1,J)*L(N+1)+Y(N-1,J)*V(N-1)-X(N,J)*L(N)-V(N)*
+Y(N,J)

DXM(NF,J)=X(NF+1,J)*L(NF+1)+Y(NF-1,J)*V(NF-1)-X(NF,J)*L(NF)-
+V(NF)*Y(NF,J)+FL*XF(J)

DXM(NF+1,J)=X(NF+2,J)*L(NF+2)+Y(NF,J)*V(NF)-X(NF+1,J)*L(NF+1)
+V(NF+1)*Y(NF+1,J)+FV*YF(J)

DO 170 N=NF+2,NT-1

170 DXM(N,J)=X(N+1,J)*L(N+1)+Y(N-1,J)*V(N-1)-X(N,J)*L(N)-V(N)*Y(N,J)
DXM(NT,J)=XD(J)*R+Y(NT-1,J)*V(NT-1)-X(NT,J)*L(NT)-Y(NT,J)*V(NT)
DXD(J)=(V(NT)*Y(NT,J)-DV*YD(J)-(R+DL)*XD(J))/MD

160 CONTINUE

IF (TIME .GT. 4e-2) GOTO 9000
IF (TIME .LT. TPRINT) GOTO 210

CALL drawlines()
WRITE(5,201)

201 FORMAT (5X,'TIME      T      X1      X2      X3      X4
+      X5      L')
WRITE(5,202) TIME,TB,(XB(J),J=1,NC),B

202 FORMAT (1X,F5.4,3X,F7.2,8F14.6,F10.1)

DO 203 N=1,NT

203 WRITE(5,204) N,T(N),(X(N,J),J=1,NC),L(N)
204 FORMAT (3X,I3,3X,F7.2,8F14.6,F10.1)
WRITE(5,205) TD,(XD(J),J=1,NC),R

205 FORMAT (9X,F7.2,8F14.6,F10.1)
WRITE(5,206) (YD(J),J=1,NC),DL

206 FORMAT(16X,8F14.6,F10.1)

TPRINT = TPRINT + .001

cc   CALL settextposition( 24, 5, curpos )
cc   CALL outtext( 'Press ENTER to continue ...' )
cc   READ(*,*)

CC
CC      INTEGRATION ALA EULER
CC

```



210 TIME = TIME + DELTA

cc WRITE(*,*) TIME

cc READ(*,*)

DO 215 N=1,NT

215 M(N)=M(N)+DM(N)*DELTA

DO 220 J = 1,NC

XB(J)=XB(J)+DXB(J)*DELTA

IF (XB(J) .LT. 0.) XB(J) = 0.0

IF (XB(J) .GT. 1.) XB(J) = 1.

DO 225 N=1,NT

XM(N,J)=XM(N,J)+DXM(N,J)*DELTA

X(N,J)=XM(N,J)/M(N)

IF (X(N,J) .GT. 1.) X(N,J) = 1.

IF (X(N,J) .LT. 0.) X(N,J) = 0.0

225 CONTINUE

XD(J)=XD(J)+DXD(J)*DELTA

IF (XD(J) .LT. 0.) XD(J)=0.

IF (XD(J) .GT. 1.) XD(J)=1.

220 CONTINUE

CC

CC CALCULATE NEW LIQUID RATES

CC

DO 270 N=1,NF

DO 271 J=1,NC

XX(J)=X(N,J)

271 CONTINUE

CALL HYDRAUS(P(N),M(N),T(N),XX,L(N),WHS,WLS,DS)

270 CONTINUE

DO 273 N=NF+1,NT

DO 275 J=1,NC

275 XX(J)=X(N,J)

```

CALL HYDRAUS(P(N),M(N),T(N),XX,L(N),WHR,WLR,DR)
273 CONTINUE
xxx=xxx+1.0
GOTO 100
400 STOP
END

```

```

CC
CC      Calculate Liquid tray holdup by Francis Wier equation
CC

```

SUBROUTINE HYDRAUS(P,M,T,X,L,WH,WL,DCOL)

REAL M,L,MW,MWA

```

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

```

DIMENSION X(20)

```

CALL MWDENSS(X,T,P,MWA,DENSA)
CONST=183.2*M*MWA/(DENSA*DCOL*DCOL)-WH/12.
IF (CONST .LE. 0.) GOTO 10
L=DENSA*WL*999.*((183.2*M*MWA/(DENSA*DCOL*DCOL)-WH/12.)**1.5)/MWA
RETURN
10 L=0.
RETURN
END

```

```

CC
CC      ENTHSalpy calculation
CC

```

SUBROUTINE ENTHS(T,P,X,Y,HL,HV)

REAL GC,MI

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BV(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION X(20),Y(20),TR(20),MI(20),ALPHA(20),ACI(20),AI(20),
+BI(20),HLS(20)

CC

CC Define constant value

CC

GC = 1.986

KIJ = 0.001

HL = 0.0

HV = 0.0

HLS1 = 0.0

HVS = 0.0

SUMAL = 0.0

SUMAV = 0.0

SUMBBL = 0.0

SUMBV = 0.0

SUMATL = 0.0

SUMATV = 0.0

DO 1 J=1,NC

TR(J) = T/TC(J)

MI(J) = 0.48+1.574*W(J)-0.176*W(J)**2

ALPHA(J) = (1.0+MI(J)*(1-TR(J)**(0.5)))**2

ACI(J) = 0.42748*(GC*TC(J))**2/PC(J)

AI(J) = ALPHA(J)*ACI(J)

BI(J) = 0.08664*GC*TC(J)/PC(J)

SUMBL = SUMBL + X(J)*BI(J)

SUMBV = SUMBV + Y(J)*BI(J)

1 CONTINUE

DO 2 I = 1,NC

DO 3 J = 1,NC

SUMAL = SUMAL+X(I)*X(J)*(AI(I)*AI(J))**0.5*(1-KIJ)

SUMAV = SUMAV+Y(I)*Y(J)*(AI(I)*AI(J))**0.5*(1-KIJ)

SUMATL = SUMATL+X(I)*X(J)*MI(J)*(AI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)

SUMATV = SUMATV+Y(I)*Y(J)*MI(J)*(AI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)

3 CONTINUE

2 CONTINUE

AL = SUMAL*P/(GC*T)**2

AV = SUMAV*P/(GC*T)**2

BL = SUMBL*P/(GC*T)

BV = SUMBV*P/(GC*T)

CALL NEWTONS(AL,BL,Z1,Z2,Z3)

IF (Z1 .LE. 0) THEN

 IF (Z2 .LE. 0) THEN

 ZL = Z3

 ELSE

 ZL = Z2

 END IF

ELSE

 ZL = Z1

END IF

CALL NEWTONS(AV,BV,Z1,Z2,Z3)

ZV = Z3

DO 4 I = 1,NC

HLS(I) = A1(I)*(T-460.)+A2(I)/2*(T-460.)**2+A3(I)/3*(T-460.)**3+
+A4(I)/4*(T-460.)**4+A5(I)/5*(T-460.)**5

HLS1 = HLS1+X(I)*HLS(I)

HVS = HVS +Y(I)*HLS(I)

4 CONTINUE

$$\begin{aligned} \text{HL} &= (\text{ZL}-1-\text{AL}/\text{BL}*(1-\text{SUMATL}/\text{SUMAL})*\text{ALOG}(1+\text{BL}/\text{ZL}))*\text{GC}*\text{T}+\text{HLS1} \\ \text{HV} &= (\text{ZV}-1-\text{AV}/\text{BV}*(1-\text{SUMATV}/\text{SUMAV})*\text{ALOG}(1+\text{BV}/\text{ZV}))*\text{GC}*\text{T}+\text{HVS} \end{aligned}$$

RETURN

END

CC

CC Calculate the root of Z by NEWTONS's technique

CC

SUBROUTINE NEWTONS(A,B,Z1,Z2,Z3)

DIMENSION Z(3)

ZO1 = -10

L = 1

10 IF (L .GT. 8000) THEN

WRITE(*,*) ' ***** NOT CONVERGE !! *****'

STOP

END IF

FZ1 = ZO1**3-ZO1**2+(A-B-B**2)*ZO1-A*B

DFZ1 = 3*ZO1**2-2*ZO1+(A-B-B**2)

Z1 = ZO1-FZ1/DFZ1

IF (ABS(ZO1-Z1) .LT. 1E-3) THEN

GOTO 20

END IF

ZO1 = Z1

L = L+1

GOTO 10

20 ZO2 = 0

L1 = 1

25 IF (L1 .GT. 8000) THEN

```
      WRITE(*,*) ' ***** NOT CONVERGE !! *****'  
      STOP  
      END IF  
  
      FZ2 = ZO2**3-ZO2**2+(A-B-B**2)*ZO2-A*B  
      DFZ2 = 3*ZO2**2-2*ZO2+(A-B-B**2)  
      Z2 = ZO2-FZ2/DFZ2  
      IF (ABS(ZO2-Z2) .LT. 1E-3) THEN  
      GOTO 30  
      END IF  
      ZO2 = Z2  
      L1 = L1+1  
      GOTO 25  
  
30 ZO3 = 10  
      L2 = 1  
      35 IF ( L2 .GT. 8000 ) THEN  
          WRITE(*,*) ' ***** NOT CONVERGE !! *****'  
          STOP  
          END IF  
          FZ3 = ZO3**3-ZO3**2+(A-B-B**2)*ZO3-A*B  
          DFZ3 = 3*ZO3**2-2*ZO3+(A-B-B**2)  
          Z3 = ZO3-FZ3/DFZ3  
          IF (ABS(ZO3-Z3) .LT. 1E-3) THEN  
          GOTO 40  
          END IF  
          ZO3 = Z3  
          L2 = L2+1  
          GOTO 35  
  
      Z(1) = Z1  
      Z(2) = Z2  
      Z(3) = Z3  
  
      jump = 3  
50 jump = jump/2
```

```

IF ( jump .NE. 0 ) THEN
    j2 = 3-jump
    DO 60 j = 1,j2
        DO 60 i = j,1,-jump
            j3 = i+jump
            IF ( Z(i) .GT. Z(j3) ) THEN
                s = Z(i)
                Z(i) = Z(j3)
                Z(j3) = s
            END IF
60      CONTINUE
        GOTO 50
    END IF

```

Z1 = Z(1)

Z2 = Z(2)

Z3 = Z(3)

40 RETURN

END

CC

CC Calculate average density

CC

SUBROUTINE MWDENSS(X,T,P,MWA,DENSA)

```

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

```

DIMENSION X(20),TR(20),MI(20),ALPHA(20),ACI(20),AI(20),BI(20)

REAL MW,MWA,MI,GC

DENSA=0.0

MWA=0.

CC
 CC Define constant value
 CC

GC = 10.731

KIJ = 0.001

SUMAL = 0.0
 SUMBL = 0.0
 SUMATL = 0.0

DO 1 J=1,NC
 TR(J) = T/TC(J)
 MI(J) = 0.48+1.574*W(J)-0.176*W(J)**2
 ALPHA(J) = (1.0+MI(J)*(1-TR(J)**(0.5)))**2
 ACI(J) = 0.42748*(GC*TC(J))**2/PC(J)
 AI(J) = ALPHA(J)*ACI(J)
 BI(J) = 0.08664*GC*TC(J)/PC(J)
 SUMBL = SUMBL + X(J)*BI(J)

1 CONTINUE

DO 2 I = 1,NC
 DO 3 J = 1,NC
 SUMAL = SUMAL+X(I)*X(J)*(AI(I)*AI(J))**0.5*(1-KIJ)
 SUMATL = SUMATL+X(I)*X(J)*MI(J)*(AI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)

3 CONTINUE

2 CONTINUE

AL = SUMAL*P/(GC*T)**2
 BL = SUMBL*P/(GC*T)

CALL NEWTONS(AL,BL,Z1,Z2,Z3)
 IF (Z1 .LE. 0) THEN



```

IF ( Z2 .LE. 0 ) THEN
  ZL = Z3
ELSE
  ZL = Z2
END IF
ELSE
  ZL = Z1
END IF

```

VV = ZL*GC*T/P

```

DO 5 J=1,NC
5 MWA=X(J)*MW(J)+MWA
DENSA=1/(VV/MWA)

```

RETURN

END

```

CC
CC      Buble point Calculation
CC

```

SUBROUTINE BUBPTS(T,X,Y,P)

```

REAL GC,MI,KI, APRIMEX,APRIMEY,PRIMEXH,PRIMEYH,KIH,
+FSLOPE,F,y

```

```

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

```

```

DIMENSION X(20),Y(20),TR(20),MI(20),ALPHA(20),ACI(20),
+AI(20),BI(20),FIL(20),FIV(20),KI(20),APRIMEX(20),APRIMEY(20)

```

DIMENSION FILH(20),FIVH(20),PRIMEXH(20),PRIMEYH(20),KIH(20),

+ALPHAH(20),AIH(20),TRH(20)

CC

CC Define constant value

CC

GC = 1.986

KIJ = 0.001

DO 40 I = 1,NC

IF (Y(I) .EQ. 0.) THEN

ki(i) = 1.

Y(I) = KI(I)*X(I)

END IF

40 continue

LOOP = 0

10 LOOP=LOOP+1

SUMXA = 0.0

SUMYA = 0.0

SUMXAH = 0.0

SUMYAH = 0.0

SUMAL = 0.0

SUMAV = 0.0

SUMALH = 0.0

SUMAVH = 0.0

SUMBL = 0.0

SUMBV = 0.0

TH = T+1.0

IF(LOOP .GT. 8000) GOTO 30

SUMY=0.0

SUMYH = 0.0

DO 1 J=1,NC

TR(J) = T/TC(J)

TRH(J) = TH/TC(J)

MI(J) = 0.48+1.574*W(J)-0.176*W(J)**2

ALPHA(J) = (1.0+MI(J)*(1-TR(J)**(0.5)))**2

ALPHAH(J) = (1.0+MI(J)*(1-TRH(J)**(0.5)))**2

ACI(J) = 0.42748*(GC*TC(J))**2/PC(J)

AI(J) = ALPHA(J)*ACI(J)

AIH(J) = ALPHAH(J)*ACI(J)

BI(J) = 0.08664*GC*TC(J)/PC(J)

SUMXA = SUMXA+X(J)*AI(J)**0.5*(1-KIJ)

SUMXAH = SUMXAH+X(J)*AIH(J)**0.5*(1-KIJ)

SUMYA = SUMYA+Y(J)*AI(J)**0.5*(1-KIJ)

SUMYAH = SUMYAH+Y(J)*AIH(J)**0.5*(1-KIJ)

SUMBL = SUMBL + X(J)*BI(J)

SUMBV = SUMBV + Y(J)*BI(J)

1 CONTINUE

DO 2 I = 1,NC

DO 3 J = 1,NC

SUMAL = SUMAL+X(I)*X(J)*(AI(I)*AI(J))**0.5*(1-KIJ)

SUMALH = SUMALH + X(I)*X(J)*(AIH(I)*AIH(J))**0.5*(1-KIJ)

SUMAV = SUMAV+Y(I)*Y(J)*(AI(I)*AI(J))**0.5*(1-KIJ)

SUMAVH = SUMAVH + Y(I)*Y(J)*(AIH(I)*AIH(J))**0.5*(1-KIJ)

3 CONTINUE

2 CONTINUE

AL = SUMAL*P/(GC*T)**2

ALH = SUMALH*P/(GC*TH)**2

AV = SUMAV*P/(GC*T)**2

AVH = SUMAVH*P/(GC*TH)**2

BL = SUMBL*P/(GC*T)

BLH = SUMBL*P/(GC*TH)

```

BV = SUMBV*P/(GC*T)
BVH = SUMBL*P/(GC*TH)

CALL NEWTONS(AL,BL,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN
  IF ( Z2 .LE. 0 ) THEN
    ZL = Z3
  ELSE
    ZL = Z2
  END IF
ELSE
  ZL = Z1
END IF

CALL NEWTONS(ALH,BLH,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN
  IF ( Z2 .LE. 0 ) THEN
    ZLH = Z3
  ELSE
    ZLH = Z2
  END IF
ELSE
  ZLH = Z1
END IF

CALL NEWTONS(AV,BV,Z1,Z2,Z3)
ZV = Z3

CALL NEWTONS(AVH,BVH,Z1,Z2,Z3)
ZVH = Z3

DO 15 I=1,NC
APRIMEX(I) = 1.0/SUMAL*(2*AI(I)**0.5*SUMXA)
APRIMEXH(I) = 1.0/SUMALH*(2*AIH(I)**0.5*SUMXAH)
APRIMEY(I) = 1.0/SUMAV*(2*AI(I)**0.5*SUMYA)
APRIMEYH(I) = 1.0/SUMAVH*(2*AIH(I)**0.5*SUMYAH)
FIL(I) = EXP(BI(I)/SUMBL*(ZL-1)- ALOG(ZL-BL)-AL/BL*(APRIMEX(I)-
+BI(I)/SUMBL)*ALOG(1+BL/ZL))

```

```

FILH(I) = EXP(BI(I)/SUMBL*(ZLH-1)-ALOG(ZLH-BLH)-ALH/BLH*
+(APRIMEXH(I)-BI(I)/SUMBL)* ALOG(1+BLH/ZLH))

FIV(I) = EXP(BI(I)/SUMBV*(ZV-1)-ALOG(ZV-BV)-AV/BV*(APRIMEY(I)-
+BI(I)/SUMBV)* ALOG(1+BV/ZV))

FIVH(I) = EXP(BI(I)/SUMBV*(ZVH-1)-ALOG(ZVH-BVH)-AVH/BVH*
+(APRIMEYH(I)-BI(I)/SUMBV)* ALOG(1+BVH/ZVH))

KI(I) = FIL(I)/FIV(I)

KIH(I) = FILH(I)/FIVH(I)

SUMY = SUMY +X(I)*KI(I)

SUMYH = SUMYH +X(I)*KIH(I)

```

15 CONTINUE

```

IF(LOOP .EQ. 1) THEN
DO 16 I = 1,NC
Y(I) = KI(I)*X(I)/SUMY

```

16 CONTINUE

```

GOTO 10
END IF

```

```

IF (ABS(SUMY-SUMYZ) .GE. 1E-3) THEN

```

```

DO 17 I = 1,NC
Y(I) = KI(I)*X(I)/SUMY

```

17 CONTINUE

```

SUMYZ = SUMY
GOTO 10
END IF

```

```

IF ( ABS(SUMY-1.) .LT. 1E-3) RETURN
F=SUMY-1.0
FH = SUMYH-1.0
FSLOPE=(FH-F)/1.
T=T-F/FSLOPE
GOTO 10

```

```

1000 WRITE(*,*)' ***** Converged !'
read(*,*)  

WRITE(*,*)'      TEMP      SUMY      LOOP '  

WRITE(*,*)  

WRITE(*,*) T, SUMY, LOOP  

READ(*,*)  

WRITE(*,*)  

WRITE(*,*)'    yi        ki'  

write(*,*)  

DO 1010 I = 1,NC  

WRITE(*,*) Y(I),KI(I)  

READ(*,*)  

1010 CONTINUE  

stop

```

30 WRITE(*,*) 'The calculation does not converge !!'

STOP

END

CC
CC Draw Large Border lines
CC

SUBROUTINE drawlines()

INCLUDE 'FGRAPH.FD'
RECORD / rccord / curpos

dummy = setvideomode(\$ERESCOLOR)
CALL clearscreen(\$GCLEARSCREEN)
dummy2 = setcolor(3)
CALL moveto(5, 5, curpos)
dummy2 = lineto(5, 340)
dummy2 = lineto(635,340)

```

dummy2 = lineto( 635,5 )
dummy2 = lineto( 5, 5 )
CALL      moveto( 7, 7, curpos )
dummy2 = lineto( 7, 338)
dummy2 = lineto( 633, 338)
dummy2 = lineto( 633, 7 )
dummy2 = lineto( 7, 7 )

```

RETURN

END

CC

CC Draw Small Border lines

CC

SUBROUTINE drawlines1()

INCLUDE 'FGRAPH.FD'

RECORD / rccoord / curpos

```

dummy2 = setcolor( 4 )
CALL      moveto( 120, 80, curpos )
dummy2 = lineto( 120, 270 )
dummy2 = lineto( 520, 270 )
dummy2 = lineto( 520, 80 )
dummy2 = lineto( 120,80 )
CALL      moveto( 122, 82, curpos )
dummy2 = lineto( 122, 268 )
dummy2 = lineto( 518, 268 )
dummy2 = lineto( 518, 82 )
dummy2 = lineto( 122, 82 )

```

RETURN

END

CC
CC Draw Middle Border lines
CC

SUBROUTINE drawlines2()

INCLUDE 'FGRAPH.FD'
RECORD / rccoord / curpos

dummy2 = setcolor(4)
CALL moveto(80, 80, curpos)
dummy2 = lineto(80, 270)
dummy2 = lineto(560, 270)
dummy2 = lineto(560, 80)
dummy2 = lineto(80,80)
CALL moveto(82, 82, curpos)
dummy2 = lineto(82, 268)
dummy2 = lineto(558, 268)
dummy2 = lineto(558, 82)
dummy2 = lineto(82, 82)

RETURN

END

CC
CC Draw Component Border lines
CC

SUBROUTINE drawlines3()

INCLUDE 'FGRAPH.FD'
RECORD / rccoord / curpos

dummy2 = setcolor(4)
CALL moveto(60, 60, curpos)

```

dummy2 = lineto( 60, 290 )
dummy2 = lineto( 580, 290 )
dummy2 = lineto( 580, 60 )
dummy2 = lineto( 60,60 )
CALL      moveto( 62, 62, curpos )
dummy2 = lineto( 62, 288 )
dummy2 = lineto( 578, 288 )
dummy2 = lineto( 578, 62 )
dummy2 = lineto( 62, 62 )

```

RETURN

END

CC

CC Data Menu

CC

SUBROUTINE datamenu(dat)

INCLUDE 'FGRAPH.FD'

RECORD / rccoord / curpos

100 key2 = -1

DO WHILE ((key2 .LT. 0) .OR. (key2 .GT. 4))

CALL drawlines()

CALL drawlines1()

dummy2 = settextcolor(14)

CALL settextposition(4, 30, curpos)

CALL outtext('**** Data Menu ****')

dummy2 = settextcolor(15)

CALL settextposition(10, 25, curpos)

CALL outtext('0) Return to Main Menu')

CALL settextposition(12, 25, curpos)

CALL outtext('1) New Data')

CALL settextposition(14, 25, curpos)

```
CALL outtext( '2) Old Data' )
CALL settextposition( 16, 25, curpos )
CALL outtext( '3) Save Data' )
dummy2 = settextcolor( 14 )
CALL settextposition( 22, 25, curpos )
CALL outtext( 'Please ENTER your selection : ' )
READ(*,*ERR = 100) key2
dat = key2
END DO
dummy2 = setvideomode( $DEFAULTMODE )

DO WHILE (key2 .EQ. 0)
    RETURN
END DO

DO WHILE (key2 .EQ. 1)
    RETURN
END DO

DO WHILE (key2 .EQ. 2)
    CALL old()
    RETURN
END DO

DO WHILE (key2 .EQ. 3)
    CALL save()
    RETURN
END DO

END

CC
CC      Edit old data
CC
```

SUBROUTINE old()

INCLUDE 'FGRAPH.FD'

RECORD / rccoord / curpos

CHARACTER*20 fname

100 CALL drawlines()

CALL drawlines1()

dummy2 = settextcolor(14)

CALL settextposition(4, 28, curpos)

CALL outtext('*** Edit Old Data ***')

CALL settextposition(13, 18, curpos)

CALL outtext('Please type data filename : ')

READ(*,120) fname

OPEN(3, FILE = fname, ERR = 100)

120 FORMAT(A)

RETURN

END

CC

CC Save data

CC

SUBROUTINE save()

INCLUDE 'FGRAPH.FD'

RECORD / rccoord / curpos

CHARACTER*20 filename

100 CALL drawlines()

CALL drawlines1()

dummy2 = settextcolor(14)

CALL settextposition(4, 28, curpos)

CALL outtext('*** Save Data ***')

```
CALL settextposition( 13, 18, curpos )
CALL outtext( 'Please type data filename : ' )
READ(*,120) filename
OPEN( 4, FILE = filename, ERR = 100)
120 FORMAT(A)
```

```
RETURN
```

```
END
```

CC RUN GRK MODEL

CC

CC key = 8.2

CC

CC

CC Assign temperature in Degree Rangin

CC

9800 TFL = TFL + 460.

TFV = TFV + 460.

TB = TB + 460.

TD = TD + 460.+125.0

DO 18 N = 1,NT

T(N) = T(N) + 460.

18 CONTINUE

CC

CC CALCULATE PRESSURE PROFILE

CC

CALL drawlines()

DO 35 N=1,NT

35 P(N)=(PB-(N*(PB-PD))/NT)

DELTA = 0.0001

WRITE(*,37) DELTA

37 FORMAT(1X,' DELTA = ', F8.5)

TIME = 0.

TPRINT = 0.

CALL ENTHGR(TFL,P(NF),XF,YF,HLF,HVF)

CC

CC CALL INTITIAL HOLDUPS

CC

CALL MWDENSG(XB,TB,PB,MWA,DENSA)

MB=MVB*DENSA/MWA

DO 20 N=1,NF

DO 21 J=1,NC

21 XX(J) = X(N,J)

CALL MWDENSG(XX,T(N),P(N),MWA,DENSA)

LV(N) = LO(N)*MWA/DENSA

L(N) = LO(N)

HFOW = (LV(N)/(999.*WLS))**.66667

MV(N) = (HFOW+WHS/12.)*3.1416*DS*DS/(4.*144.)

M(N) = MV(N)*DENSA/MWA

20 CONTINUE

DO 25 N = NF+1,NT

DO 26 J = 1,NC

26 XX(J) = X(N,J)

CALL MWDENSG(XX,T(N),P(N),MWA,DENSA)

LV(N) = LO(N)*MWA/DENSA

L(N) = LO(N)

HFOW = (LV(N)/(999.*WLR))**.66667

MV(N) = (HFOW+WHR/12.)*3.1416*DR*DR/(4.*144.)

M(N) = MV(N)*DENSA/MWA

25 CONTINUE

DO 30 N=1,NT

DO 31 J=1,NC

XM(N,J)=M(N)*X(N,J)

31 CONTINUE

30 CONTINUE

CALL MWDENSG(XD,TD,PD,MWA,DENSA)

MD=MVD*DENSA/MWA

CC
 CC Initial Guess of V(5) for first efficiency calculation
 CC

V(NF) = 822.

CC
 CC Main Loop for each time step
 CC
 xxx=0

100 CONTINUE

write(*,*) xxx
 CALL BUBPTGR (TB,XB,YB,PB)
 CALL ENTHGR (TB,PB,XB,YB,HLB,HVB)
 DO 105 J=1,NC

105 XX(J)=X(1,J)
 CALL BUBPTGR (T(1),XX,YY,P(1))
 DO 106 J=1,NC

Y(1,J)=YB(J)+EFF*(YY(J)-YB(J))
 106 YY(J)=Y(1,J)
 CALL ENTHGR (T(1),P(1),XX,YY,HL(1),HV(1))

DO 110 N=2,NF
 DO 111 J=1,NC
 111 XX(J)=X(N,J)
 CALL BUBPTGR (T(N),XX,YY,P(N))
 DO 112 J = 1,NC

Y(N,J)=(YY(J)-Y(N-1,J))*EFF+Y(N-1,J)
 112 YY(J)=Y(N,J)
 CALL ENTHGR(T(N),P(N),XX,YY,HL(N),HV(N))

110 CONTINUE

DO 113 J=1,NC

113 XX(J)=X(NF+1,J)

CALL BUBPTGR(T(NF+1),XX,YY,P(NF+1))

DO 114 J=1,NC

YAV(J)=(YF(J)*FV+Y(NF,J)*V(NF))/(V(NF)+FV)

Y(NF+1,J)=(YY(J)-YAV(J))*EFF+YAV(J)

114 YY(J)=Y(NF+1,J)

CALL ENTHGR(T(NF+1),P(NF+1),XX,YY,HL(NF+1),HV(NF+1))

DO 115 N=NF+2,NT

DO 116 J=1,NC

116 XX(J)=X(N,J)

CALL BUBPTGR(T(N),XX,YY,P(N))

DO 117 J=1,NC

Y(N,J)=(YY(J)-Y(N-1,J))*EFF+Y(N-1,J)

117 YY(J)=Y(N,J)

CALL ENTHGR (T(N),P(N),XX,YY,HL(N),HV(N))

115 CONTINUE

CALL BUBPTGR (TD,XD,YD,PD)

CALL ENTHGR(TD,PD,XD,YD,HLD,HVD)

CC

CC CALCULATE VAPOR RATES

CC

VB=(QR*1000.-L(1)*(HLB-HL(1)))/(HV(B)-HLB)

B = L(1)-VB

CC IF (B .LT. 0.) THEN

CC WRITE(*,*) ' ***** B IS LESS THAN 0 *****'

CC STOP

CC END IF

V(1)=(HL(2)*L(2)+HV(B)*VB-HL(1)*L(1))/HV(1)

DO 120 N=2,NF-1



$$V(N) = (HL(N+1)*L(N+1) + HV(N-1)*V(N-1) - HL(N)*L(N)) / HV(N)$$

120 CONTINUE

$$V(NF) = (HL(NF+1)*L(NF+1) + HV(NF-1)*V(NF-1) - HL(NF)*L(NF) + HLF*FL) / HV(NF)$$

$$V(NF+1) = (HL(NF+2)*L(NF+2) + HV(NF)*V(NF) + HV*FV - HL(NF+1)*L(NF+1)) / HV(NF+1)$$

DO 130 N=NF+2,NT-1

$$130 \quad V(N) = (HL(N+1)*L(N+1) + HV(N-1)*V(N-1) - HL(N)*L(N)) / HV(N)$$

$$V(NT) = (HLD*R + HV(NT-1)*V(NT-1) - HL(NT)*L(NT)) / HV(NT)$$

$$DL = V(NT) - DV - R$$

CC IF (DL .LT. 0) THEN

CC WRITE(*,*) '***** DL IS LESS THAN 0 *****'

CC STOP

CC END IF

CC

CC EVALUATE DERIVATIVES

CC

$$DM(1) = L(2) + VB - V(1) - L(1)$$

DO 140 N=2,NF-1

$$140 \quad DM(N) = L(N+1) + V(N-1) - L(N) - V(N)$$

$$DM(NF) = L(NF+1) + FL + V(NF-1) - L(NF) - V(NF)$$

$$DM(NF+1) = L(NF+2) + FV + V(NF) - L(NF+1) - V(NF+1)$$

DO 150 N=NF+2,NT-1

$$150 \quad DM(N) = L(N+1) + V(N-1) - L(N) - V(N)$$

$$DM(NT) = R + V(NT-1) - L(NT) - V(NT)$$

DO 160 J=1,NC

$$DXB(J) = (X(1,J)*L(1) - YB(J)*VB - XB(J)*B) / MB$$

$$DXM(1,J) = X(2,J)*L(2) + YB(J)*VB - X(1,J)*L(1) - Y(1,J)*V(1)$$

DO 165 N=2,NF-1

$$165 \quad DXM(N,J) = X(N+1,J)*L(N+1) + Y(N-1,J)*V(N-1) - X(N,J)*L(N) - V(N)*Y(N,J)$$

$$DXM(NF,J) = X(NF+1,J)*L(NF+1) + Y(NF-1,J)*V(NF-1) - X(NF,J)*L(NF) - V(NF)*Y(NF,J) + FL*XF(J)$$

```

DXM(NF+1,J)=X(NF+2,J)*L(NF+2)+Y(NF,J)*V(NF)-X(NF+1,J)*L(NF+1)
+V(NF+1)*Y(NF+1,J)+FV*YF(J)
DO 170 N=NF+2,NT-1

170 DXM(N,J)=X(N+1,J)*L(N+1)+Y(N-1,J)*V(N-1)-X(N,J)*L(N)-V(N)*Y(N,J)
DXM(NT,J)=XD(J)*R+Y(NT-1,J)*V(NT-1)-X(NT,J)*L(NT)-Y(NT,J)*V(NT)
DXD(J)=(V(NT)*Y(NT,J)-DV*YD(J)-(R+DL)*XD(J))/MD

160 CONTINUE
IF (TIME .GT. 3e-2) GOTO 9000
IF (TIME .LT. TPRINT) GOTO 210

CALL drawlines()
WRITE(5,201)

201 FORMAT (5X,'TIME      T      X1      X2      X3      X4
+      X5      L')
WRITE(5,202) TIME,TB,(XB(J),J=1,NC),B

202 FORMAT (1X,F5.4,3X,F7.2,8F14.6,F10.1)
DO 203 N=1,NT

203 WRITE(5,204) N,T(N),(X(N,J),J=1,NC),L(N)
204 FORMAT (3X,I3,3X,F7.2,8F14.6,F10.1)
WRITE(5,205) TD,(XD(J),J=1,NC),R
205 FORMAT (9X,F7.2,8F14.6,F10.1)
WRITE(5,206) (YD(J),J=1,NC),DL
206 FORMAT(16X,8F14.6,F10.1)

TPRINT = TPRINT + .001
cc   CALL settextposition( 24, 5, curpos )
cc   CALL outtext( 'Press ENTER to continue ...' )
cc   READ(*,*)

CC
CC     INTEGRATION ALA EULER
CC

210 TIME = TIME + DELTA
cc   WRITE(*,*) TIME
cc   READ(*,*)
```

```

DO 215 N=1,NT
215 M(N)=M(N)+DM(N)*DELTA
DO 220 J = 1,NC
XB(J)=XB(J)+DXB(J)*DELTA
IF (XB(J) .LT. 0.) XB(J) = 0.0
IF (XB(J) .GT. 1.) XB(J) = 1.
DO 225 N=1,NT
XM(N,J)=XM(N,J)+DXM(N,J)*DELTA
X(N,J)=XM(N,J)/M(N)
IF (X(N,J) .GT. 1.) X(N,J) = 1.
IF (X(N,J) .LT. 0.) X(N,J) = 0.0
225 CONTINUE
XD(J)=XD(J)+DXD(J)*DELTA
IF (XD(J) .LT. 0.) XD(J)=0.
IF (XD(J) .GT. 1.) XD(J)=1.
220 CONTINUE

```

```

CC
CC  CALCULATE NEW LIQUID RATES
CC

```

```

DO 270 N=1,NF
DO 271 J=1,NC
XX(J)=X(N,J)
271 CONTINUE
CALL HYDRAU(P(N),M(N),T(N),XX,L(N),WHS,WLS,DS)
270 CONTINUE
DO 273 N=NF+1,NT
DO 275 J=1,NC
275 XX(J)=X(N,J)
CALL HYDRAU(P(N),M(N),T(N),XX,L(N),WHR,WLR,DR)
273 CONTINUE
xxx=xxx+1.0
GOTO 100

```

400 STOP

END

CC

CC Calculate Liquid tray holdup by Francis Wier equation

CC

SUBROUTINE HYDRAU(P,M,T,X,L,WH,WL,DCOL)

REAL M,L,MW,MWA

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION X(20)

CALL MWDENSG(X,T,P,MWA,DENSA)

CONST=183.2*M*MWA/(DENSA*DCOL*DCOL)-WH/12.

IF (CONST .LE. 0.) GOTO 10

L=DENSA*WL*999.*((183.2*M*MWA/(DENSA*DCOL*DCOL)-WH/12.)**1.5)/MWA

RETURN

10 L=0.

RETURN

END

CC

CC Enthalpy calculation

CC

SUBROUTINE ENTHGR(T,P,X,Y,HL,HV)

REAL GC,MI

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),

```
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)
```

```
DIMENSION X(20),Y(20),TR(20),MI(20),ALPHA(20),ACI(20),AI(20),
+BI(20),HLS(20)
```

CC

CC Define constant value

CC

GC = 1.986

KIJ = 0.001

HL = 0.0

HV = 0.0

HLS1 = 0.0

HVS = 0.0

SUMAL = 0.0

SUMAV = 0.0

SUMBL = 0.0

SUMBV = 0.0

SUMATL = 0.0

SUMATV = 0.0

DO 1 J=1,NC

TR(J) = T/TC(J)

ACI(J) = (0.4278/(TR(J)**2.5*PC(J)))**0.5

AI(J) = ACI(J)

BI(J) = 0.0867/TR(J)/PC(J)

SUMBL = SUMBL + X(J)*BI(J)

SUMBV = SUMBV + Y(J)*BI(J)

SUMAL = SUMAL + X(J)*AI(J)

SUMAV = SUMAV + Y(J)*AI(J)

1 CONTINUE

```

AL = SUMAL
AV = SUMAV
BL = SUMBL
BV = SUMBV
CALL NEWTON(AL,BL,P,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN
  IF ( Z2 .LE. 0 ) THEN
    ZL = Z3
  ELSE
    ZL = Z2
  END IF
ELSE
  ZL = Z1
END IF
CALL NEWTON(AV,BV,P,Z1,Z2,Z3)
ZV = Z3

DO 4 I = 1,NC
HLS(I) = A1(I)*(T-460.)+A2(I)/2*(T-460.)**2+A3(I)/3*(T-460.)**3+
+A4(I)/4*(T-460.)**4+A5(I)/5*(T-460.)**5
HLS1 = HLS1+X(I)*HLS(I)
HVS = HVS +Y(I)*HLS(I)
4 CONTINUE

HL = (ZL-1.5*AL**2/BL* ALOG(1+BL*P/ZL))*GC*T+HLS1
HV = (ZV-1.5*AV**2/BV* ALOG(1+BV*P/ZV))*GC*T+HVS
RETURN
END

CC
CC      Calculate the root of Z by newton's technique
CC

SUBROUTINE NEWTON(A,B,P,Z1,Z2,Z3)

```

DIMENSION Z(3)

```

ZO1 = -10
L = 1
10 IF ( L .GT. 8000 ) THEN
    WRITE(*,*) ' ***** NOT CONVERGE !! *****'
    STOP
END IF
FZ1 = ZO1**3-ZO1**2+B*P*(A**2/B-B*P-1)*ZO1-A**2/B*(B*P)**2
DFZ1 = 3*ZO1**2-2*ZO1+B*P*(A**2/B-B*P-1)
Z1 = ZO1-FZ1/DFZ1
IF (ABS(ZO1-Z1) .LT. 1E-3) THEN
    GOTO 20
END IF
ZO1 = Z1
L = L+1
GOTO 10

20 ZO2 = 0
L1 = 1
25 IF ( L1 .GT. 8000 ) THEN
    WRITE(*,*) ' ***** NOT CONVERGE !! *****'
    STOP
END IF
FZ2 = ZO2**3-ZO2**2+B*P*(A**2/B-B*P-1)*ZO2-A**2/B*(B*P)**2
DFZ2 = 3*ZO2**2-2*ZO2+B*P*(A**2/B-B*P-1)
Z2 = ZO2-FZ2/DFZ2
IF (ABS(ZO2-Z2) .LT. 1E-3) THEN
    GOTO 30
END IF
ZO2 = Z2
L1 = L1+1
GOTO 25

```

```

30 ZO3 = 10
L2 = 1
35 IF ( L2 .GT. 8000 ) THEN
  WRITE(*,*) ' ***** NOT CONVERGE !! *****'
  STOP
END IF
FZ3 = ZO3**3-ZO3**2+B*P*(A**2/B-B*P-1)*ZO3-A**2/B*(B*P)**2
DFZ3 = 3*ZO3**2-2*ZO3+B*P*(A**2/B-B*P-1)
Z3 = ZO3-FZ3/DFZ3
IF (ABS(ZO3-Z3) .LT. 1E-3) THEN
  GOTO 40
END IF
ZO3 = Z3
L2 = L2+1
GOTO 35

```

```

Z(1) = Z1
Z(2) = Z2
Z(3) = Z3

```

```

jump = 3
50 jump = jump/2
IF ( jump .NE. 0 ) THEN
  j2 = 3-jump
  DO 60 j = 1,j2
    DO 60 i = j,1,-jump
      j3 = i+jump
      IF ( Z(i) .GT. Z(j3) ) THEN
        s = Z(i)
        Z(i) = Z(j3)
        Z(j3) = s
      END IF
60      CONTINUE
      GOTO 50
    END IF

```

Z1 = Z(1)

Z2 = Z(2)

Z3 = Z(3)

40 RETURN

END

CC

CC Calculate average density

CC

SUBROUTINE MWDENSG(X,T,P,MWA,DENSA)

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION X(20),TR(20),MI(20),ALPHA(20),ACI(20),AI(20),BI(20)

REAL MW,MWA,MI,GC

DENSA=0.0

MWA=0.

CC

CC Define constant value

CC

GC = 10.731

KIJ = 0.001

SUMAL = 0.0

SUMBL = 0.0

SUMATL = 0.0

```

DO 1 J=1,NC
TR(J) = T/TC(J)
ACI(J) = (0.42748/(TR(J)**2.5*PC(J)))**0.5
AI(J) = ACI(J)
BI(J) = 0.0867/TR(J)/PC(J)
SUMBL = SUMBL + X(J)*BI(J)
SUMAL = SUMAL + X(J)*AI(J)
1 CONTINUE

```

AL = SUMAL

BL = SUMBL

```

CALL NEWTON(AL,BL,P,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN
  IF ( Z2 .LE. 0 ) THEN
    ZL = Z3
  ELSE
    ZL = Z2
  END IF
ELSE
  ZL = Z1
END IF

```

VV = ZL*GC*T/P

```

DO 5 J=1,NC
5 MWA=X(J)*MW(J)+MWA
DENSA=1/(VV/MWA)

```

RETURN

END

CC

CC Buble point Calculation

CC

SUBROUTINE BUBPTGR(T,X,Y,P)

REAL GC,MI,KI,KIH,FSLOPE,F,y

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BV(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION X(20),Y(20),TR(20),MI(20),ALPHA(20),ACI(20),
+AI(20),BI(20),BIH(20),FIL(20),FIV(20),KI(20)

DIMENSION FILH(20),FIVH(20),APRIMEXH(20),APRIMEYH(20),KIH(20),
+ALPHAH(20),AIH(20),TRH(20)

CC

CC Define constant value

CC

GC = 1.986

KIJ = 0.001

DO 40 I = 1,NC

IF (Y(I) .EQ. 0.) THEN

ki(i) = 1.

Y(I) = KI(I)*X(I)

END IF

40 continue

LOOP = 0

10 LOOP=LOOP+1

SUMXA = 0.0



SUMYA = 0.0

SUMXAH = 0.0

SUMYAH = 0.0

SUMAL = 0.0

SUMAV = 0.0

SUMALH = 0.0

SUMAVH = 0.0

SUMBL = 0.0

SUMBV = 0.0

SUMBLH = 0.0

SUMBVH = 0.0

TH = T+1.0

IF(LOOP .GT. 8000).GOTO 30

SUMY=0.0

SUMYH = 0.0

DO 1 J=1,NC

TR(J) = T/TC(J)

TRH(J) = TH/TC(J)

ACI(J) = (0.4278/(TR(J)**2.5*PC(J)))**0.5

AI(J) = ACI(J)

AIH(J) = (0.4278/(TRH(J)**2.5*PC(J)))**0.5

BI(J) = 0.0867/TR(J)/PC(J)

BIH(J) = 0.0867/TRH(J)/PC(J)

SUMBL = SUMBL + X(J)*BI(J)

SUMBV = SUMBV + Y(J)*BI(J)

SUMBLH = SUMBLH + X(J)*BIH(J)

SUMBVH = SUMBVH + Y(J)*BIH(J)

SUMAL = SUMAL + X(J)*AI(J)

SUMAV = SUMAV + Y(J)*AI(J)

SUMALH = SUMALH + X(J)*AIH(J)

SUMAVH = SUMAVH + Y(J)*AIH(J)

1 CONTINUE

```
AL = SUMAL
ALH = SUMALH
AV = SUMAV
AVH = SUMAVH
BL = SUMBL
BLH = SUMBLH
BV = SUMBV
BVH = SUMBLH

CALL NEWTON(AL,BL,P,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN
    IF ( Z2 .LE. 0 ) THEN
        ZL = Z3
    ELSE
        ZL = Z2
    END IF
ELSE
    ZL = Z1
END IF

CALL NEWTON(ALH,BLH,P,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN
    IF ( Z2 .LE. 0 ) THEN
        ZLH = Z3
    ELSE
        ZLH = Z2
    END IF
ELSE
    ZLH = Z1
END IF

CALL NEWTON(AV,BV,P,Z1,Z2,Z3)
ZV = Z3
CALL NEWTON(AVH,BVH,P,Z1,Z2,Z3)
ZVH = Z3
```

DO 15 I=1,NC

```

FIL(I) = EXP((ZL-1)*BI(I)/BL-ALOG(ZL-BL*p)-AL**2/BL*
+(2*AI(I)/AL-BI(I)/BL)*ALOG(1+BL*p/ZL))

FILH(I) = EXP((ZLH-1)*BIH(I)/BLH-ALOG(ZLH-BLH*p)-ALH**2/BLH*
+(2*AIH(I)/ALH-BIH(I)/BLH)*ALOG(1+BLH*p/ZLH))

FIV(I) = EXP((ZV-1)*BI(I)/BV-ALOG(ZV-BV*p)-AV**2/BV*
+(2*AI(I)/AV-BI(I)/BV)*ALOG(1+BV*p/ZV))

FIVH(I) = EXP((ZVH-1)*BIH(I)/BVH-ALOG(ZVH-BVH*p)-AVH**2/BVH*
+(2*AIH(I)/AVH-BIH(I)/BVH)*ALOG(1+BVH*p/ZVH))

```

KI(I) = FIL(I)/FIV(I)

KIH(I) = FILH(I)/FIVH(I)

SUMY = SUMY +X(I)*KI(I)

SUMYH = SUMYH +X(I)*KIH(I)

15 CONTINUE

IF(LOOP .EQ. 1) THEN

DO 16 I = 1,NC

Y(I) = KI(I)*X(I)/SUMY

16 CONTINUE

GOTO 10

END IF

IF (ABS(SUMY-SUMYZ) .GE. 1E-3) THEN

DO 17 I = 1,NC

Y(I) = KI(I)*X(I)/SUMY

17 CONTINUE

SUMYZ = SUMY

GOTO 10

END IF

```
IF ( ABS(SUMY-1.) .LT. 1E-3) RETURN
F=SUMY-1.0
FH = SUMYH-1.0
FSLOPE=(FH-F)/1.
T=T-F/FSLOPE
GOTO 10

1000 WRITE(*,*) ' ***** Converged !'
read(*,*)
WRITE(*,*) '      TEMP      SUMY      LOOP '
WRITE(*,*) '      T, SUMY, LOOP '
READ(*,*)
WRITE(*,*) '      yi      ki'
write(*,*)
DO 1010 I = 1,NC
WRITE(*,*) Y(I),KI(I)
READ(*,*)
1010 CONTINUE
stop

30 WRITE(*,*) 'The calculation does not converge !'
STOP
END
```



CC RUN PR MODEL

CC

CC key = 8.3

CC

CC

CC Assign temperature in Degree Rangin

CC

9800 TFL = TFL + 460.

TFV = TFV + 460.

TB = TB + 460.

TD = TD + 460.+115.0

DO 18 N = 1,NT

T(N) = T(N) + 460.

18 CONTINUE

CC

CC CALCULATE PRESSURE PROFILE

CC

CALL drawlines()

DO 35 N=1,NT

35 P(N)=(PB-(N*(PB-PD))/NT)

DELTA = 0.0001

WRITE(*,37) DELTA

37 FORMAT(1X,' DELTA = ', F8.5)

TIME = 0.

TPRINT = 0.

CALL ENTHPR(TFL,P(NF),XF,YF,HLF,HVF)

CC

CC CALL INTITIAL HOLDUPS

CC

CALL MWDENSPR(XB,TB,PB,MWA,DENSA)

MB=MVB*DENSA/MWA

DO 20 N=1,NF

DO 21 J=1,NC

21 XX(J) = X(N,J)

CALL MWDENSPR(XX,T(N),P(N),MWA,DENSA)

LV(N) = LO(N)*MWA/DENSA

L(N) = LO(N)

HFLOW = (LV(N)/(999.*WLS))**.66667

MV(N) = (HFLOW+WHS/12.)*3.1416*DS*DS/(4.*144.)

M(N) = MV(N)*DENSA/MWA

20 CONTINUE

DO 25 N = NF+1,NT

DO 26 J = 1,NC

26 XX(J) = X(N,J)

CALL MWDENSPR(XX,T(N),P(N),MWA,DENSA)

LV(N) = LO(N)*MWA/DENSA

L(N) = LO(N)

HFLOW = (LV(N)/(999.*WLR))**.66667

MV(N) = (HFLOW+WHR/12.)*3.1416*DR*DR/(4.*144.)

M(N) = MV(N)*DENSA/MWA

25 CONTINUE

DO 30 N=1,NT

DO 31 J=1,NC

XM(N,J)=M(N)*X(N,J)

31 CONTINUE

30 CONTINUE

CALL MWDENSPR(XD,TD,PD,MWA,DENSA)

MD=MVD*DENSA/MWA

CC
 CC Initial Guess of V(5) for first efficiency calculation
 CC

V(NF) = 822.

CC
 CC Main Loop for each time step
 CC
 xxx=0

100 CONTINUE

write(*,*) xxx
 CALL BUBPTPR (TB,XB,YB,PB)
 CALL ENTHPR (TB,PB,XB,YB,HLB,HVB)
 DO 105 J=1,NC

105 XX(J)=X(1,J)
 CALL BUBPTPR (T(1),XX,YY,P(1))
 DO 106 J=1,NC

Y(1,J)=YB(J)+EFF*(YY(J)-YB(J))
 106 YY(J)=Y(1,J)
 CALL ENTHPR(T(1),P(1),XX,YY,HL(1),HV(1))

DO 110 N=2,NF
 DO 111 J=1,NC
 111 XX(J)=X(N,J)
 CALL BUBPTPR(T(N),XX,YY,P(N))
 DO 112 J = 1,NC

Y(N,J)=(YY(J)-Y(N-1,J))*EFF+Y(N-1,J)
 112 YY(J)=Y(N,J)
 CALL ENTHPR(T(N),P(N),XX,YY,HL(N),HV(N))

110 CONTINUE

DO 113 J=1,NC

113 XX(J)=X(NF+1,J)

CALL BUBPTPR(T(NF+1),XX,YY,P(NF+1))

DO 114 J=1,NC

YAV(J)=(YF(J)*FV+Y(NF,J)*V(NF))/(V(NF)+FV)

Y(NF+1,J)=(YY(J)-YAV(J))*EFF+YAV(J)

114 YY(J)=Y(NF+1,J)

CALL ENTHPR(T(NF+1),P(NF+1),XX,YY,HL(NF+1),HV(NF+1))

DO 115 N=NF+2,NT

DO 116 J=1,NC

116 XX(J)=X(N,J)

CALL BUBPTPR(T(N),XX,YY,P(N))

DO 117 J=1,NC

Y(N,J)=(YY(J)-Y(N-1,J))*EFF+Y(N-1,J)

117 YY(J)=Y(N,J)

CALL ENTHPR (T(N),P(N),XX,YY,HL(N),HV(N))

115 CONTINUE

CALL BUBPTPR (TD,XD,YD,PD)

CALL ENTHPR(TD,PD,XD,YD,HLD,HVD)

CC

CC CALCULATE VAPOR RATES

CC

VB=(QR*1000.-L(1)*(HLB-HL(1)))/(HVB-HLB)

B = L(1)-VB

CC IF (B .LT. 0.) THEN

CC WRITE(*,*) ' ***** B IS LESS THAN 0 *****'

CC STOP

CC END IF

V(1)=(HL(2)*L(2)+HVB*VB-HL(1)*L(1))/HV(1)

DO 120 N=2,NF-1

$V(N) = (HL(N+1)*L(N+1) + HV(N-1)*V(N-1) - HL(N)*L(N)) / HV(N)$

120 CONTINUE

$V(NF) = (HL(NF+1)*L(NF+1) + HV(NF-1)*V(NF-1) - HL(NF)*L(NF) + HLF*FL) / HV(NF)$

$V(NF+1) = (HL(NF+2)*L(NF+2) + HV(NF)*V(NF) + HVF*FV - HL(NF+1)*L(NF+1)) / HV(NF+1)$

DO 130 N=NF+2,NT-1

130 $V(N) = (HL(N+1)*L(N+1) + HV(N-1)*V(N-1) - HL(N)*L(N)) / HV(N)$

$V(NT) = (HLD*R + HV(NT-1)*V(NT-1) - HL(NT)*L(NT)) / HV(NT)$

$DL = V(NT) - DV - R$

CC IF (DL .LT. 0) THEN

CC WRITE(*,*) '***** DL IS LESS THAN 0 *****'

CC STOP

CC END IF

CC

CC EVALUATE DERIVATIVES

CC

$DM(1) = L(2) + VB - V(1) - L(1)$

DO 140 N=2,NF-1

140 $DM(N) = L(N+1) + V(N-1) - L(N) - V(N)$

$DM(NF) = L(NF+1) + FL + V(NF-1) - L(NF) - V(NF)$

$DM(NF+1) = L(NF+2) + FV + V(NF) - L(NF+1) - V(NF+1)$

DO 150 N=NF+2,NT-1

150 $DM(N) = L(N+1) + V(N-1) - L(N) - V(N)$

$DM(NT) = R + V(NT-1) - L(NT) - V(NT)$

DO 160 J=1,NC

$DXB(J) = (X(1,J)*L(1) - YB(J)*VB - XB(J)*B) / MB$

$DXM(1,J) = X(2,J)*L(2) + YB(J)*VB - X(1,J)*L(1) - Y(1,J)*V(1)$

DO 165 N=2,NF-1

165 $DXM(N,J) = X(N+1,J)*L(N+1) + Y(N-1,J)*V(N-1) - X(N,J)*L(N) - V(N)*Y(N,J)$

$DXM(NF,J) = X(NF+1,J)*L(NF+1) + Y(NF-1,J)*V(NF-1) - X(NF,J)*L(NF) - V(NF)*Y(NF,J) + FL*XF(J)$

```

DXM(NF+1,J)=X(NF+2,J)*L(NF+2)+Y(NF,J)*V(NF)-X(NF+1,J)*L(NF+1)
+-V(NF+1)*Y(NF+1,J)+FV*YF(J)

DO 170 N=NF+2,NT-1

170 DXM(N,J)=X(N+1,J)*L(N+1)+Y(N-1,J)*V(N-1)-X(N,J)*L(N)-V(N)*Y(N,J)
DXM(NT,J)=XD(J)*R+Y(NT-1,J)*V(NT-1)-X(NT,J)*L(NT)-Y(NT,J)*V(NT)
DXD(J)=(V(NT)*Y(NT,J)-DV*YD(J)-(R+DL)*XD(J))/MD

160 CONTINUE

IF (TIME .GT. 4e-2) GOTO 9000
IF (TIME .LT. TPRINT) GOTO 210

CALL drawlines()
WRITE(5,201)

201 FORMAT (5X,'TIME      T      X1      X2      X3      X4
           +      X5      L')
WRITE(5,202) TIME,TB,(XB(J),J=1,NC),B

202 FORMAT (1X,F5.4,3X,F7.2,8F14.6,F10.1)

DO 203 N=1,NT

203 WRITE(5,204) N,T(N),(X(N,J),J=1,NC),L(N)
204 FORMAT (3X,I3,3X,F7.2,8F14.6,F10.1)
WRITE(5,205) TD,(XD(J),J=1,NC),R

205 FORMAT (9X,F7.2,8F14.6,F10.1)
WRITE(5,206) (YD(J),J=1,NC),DL

206 FORMAT(16X,8F14.6,F10.1)

TPRINT = TPRINT + .001

cc  CALL settextposition( 24, 5, curpos )
cc  CALL outtext( 'Press ENTER to continue ...' )
cc  READ(*,*)

CC
CC      INTEGRATION ALA EULER
CC

210 TIME = TIME + DELTA
cc  WRITE(*,*) TIME
cc  READ(*,*)
```

```

DO 215 N=1,NT
215 M(N)=M(N)+DM(N)*DELTA
DO 220 J = 1,NC
XB(J)=XB(J)+DXB(J)*DELTA
IF (XB(J) .LT. 0.) XB(J) = 0.0
IF (XB(J) .GT. 1.) XB(J) = 1.
DO 225 N=1,NT
XM(N,J)=XM(N,J)+DXM(N,J)*DELTA
X(N,J)=XM(N,J)/M(N)
IF (X(N,J) .GT. 1.) X(N,J) = 1.
IF (X(N,J) .LT. 0.) X(N,J) = 0.0
225 CONTINUE
XD(J)=XD(J)+DXD(J)*DELTA
IF (XD(J) .LT. 0.) XD(J)=0.
IF (XD(J) .GT. 1.) XD(J)=1.
220 CONTINUE

```

```

CC
CC  CALCULATE NEW LIQUID RATES
CC

```

```

DO 270 N=1,NF
DO 271 J=1,NC
XX(J)=X(N,J)
271 CONTINUE
CALL HYDRAU(P(N),M(N),T(N),XX,L(N),WHS,WLS,DS)
270 CONTINUE
DO 273 N=NF+1,NT
DO 275 J=1,NC
275 XX(J)=X(N,J)
CALL HYDRAU(P(N),M(N),T(N),XX,L(N),WHR,WLR,DR)
273 CONTINUE
xxx=xxx+1.0
GOTO 100

```

400 STOP

END

CC

CC Calculate Liquid tray holdup by Francis Wier equation

CC

SUBROUTINE HYDRAU(P,M,T,X,L,WH,WL,DCOL)

REAL M,L,MW,MWA

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+ BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION X(20)

CALL MWDENSPR(X,T,P,MWA,DENSA)

CONST=183.2*M*MWA/(DENSA*DCOL*DCOL)-WH/12.

IF (CONST .LE. 0.) GOTO 10

L=DENSA*WL*999.*((183.2*M*MWA/(DENSA*DCOL*DCOL)-WH/12.)**1.5)/MWA

RETURN

10 L=0.

RETURN

END

CC

CC Enthalpy calculation

CC

SUBROUTINE ENTHPR(T,P,X,Y,HL,HV)

REAL GC,MI

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),

```
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)
```

```
DIMENSION X(20),Y(20),TR(20),MI(20),ALPHA(20),ACI(20),AI(20),
+BI(20),HLS(20)
```

CC

CC Define constant value

CC

GC = 1.986

KIJ = 0.001

HL = 0.0

HV = 0.0

HLS1 = 0.0

HVS = 0.0

SUMAL = 0.0

SUMAV = 0.0

SUMBL = 0.0

SUMBV = 0.0

SUMATL = 0.0

SUMATV = 0.0

SUMPL = 0.0

SUMPV = 0.0

DO 1 J=1,NC

TR(J) = T/TC(J)

MI(J) = 0.37464+1.54226*W(J)-0.26992*W(J)**2

ALPHA(J) = (1.0+MI(J)*(1-TR(J)**(0.5)))**2

ACI(J) = 0.45724*(GC*TC(J))**2/PC(J)

AI(J) = ALPHA(J)*ACI(J)

BI(J) = 0.07780*GC*TC(J)/PC(J)

SUMBL = SUMBL + X(J)*BI(J)

SUMBV = SUMBV + Y(J)*BI(J)

1 CONTINUE

```

DO 2 I = 1,NC
DO 3 J = 1,NC
SUMAL = SUMAL+X(I)*X(J)*(AI(I)*AI(J))**0.5*(1-KIJ)
SUMAV = SUMAV+Y(I)*Y(J)*(AI(I)*AI(J))**0.5*(1-KIJ)
SUMATL = SUMATL+X(I)*X(J)*MI(J)*(AI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)
SUMATV = SUMATV+Y(I)*Y(J)*MI(J)*(AI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)
SUMPL = SUMPL+X(I)*X(J)*MI(J)*(ACI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)
SUMPV = SUMPV+Y(I)*Y(J)*MI(J)*(ACI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)

```

3 CONTINUE

2 CONTINUE

```

AL = SUMAL*P/(GC*T)**2
AV = SUMAV*P/(GC*T)**2
BL = SUMBL*P/(GC*T)
BV = SUMBV*P/(GC*T)
CALL NEWTON(AL,BL,Z1,Z2,Z3)
IF ( Z1 .LE. 0 ) THEN

```

IF (Z2 .LE. 0) THEN

ZL = Z3

ELSE

ZL = Z2

END IF

ELSE

ZL = Z1

END IF

CALL NEWTON(AV,BV,Z1,Z2,Z3)

ZV = Z3

DO 4 I = 1,NC

```

HLS(I) = A1(I)*(T-460.)+A2(I)/2*(T-460.)**2+A3(I)/3*(T-460.)**3+
+A4(I)/4*(T-460.)**4+A5(I)/5*(T-460.)**5
HLS1 = HLS1+X(I)*HLS(I)
HVS = HVS +Y(I)*HLS(I)

```

4 CONTINUE

$$\begin{aligned} \text{HL} &= (\text{ZL}-1-\text{AL}/(2.8284*\text{BL})*(1-\text{SUMPL}/\text{SUMAL})*\text{ALOG}((\text{ZL}+2.4142*\text{BL})/ \\ &+(\text{ZL}-0.4142*\text{BL}))) * \text{GC} * \text{T} + \text{HLS1} \\ \text{HV} &= (\text{ZV}-1-\text{AV}/(2.8284*\text{BV})*(1-\text{SUMPV}/\text{SUMAV})*\text{ALOG}((\text{ZV}+2.4142*\text{BV})/ \\ &+(\text{ZV}-0.4142*\text{BV}))) * \text{GC} * \text{T} + \text{HVS} \end{aligned}$$

RETURN

END

CC

CC Calculate the root of Z by newton's technique

CC

SUBROUTINE NEWTON(A,B,Z1,Z2,Z3)

DIMENSION Z(3)

Z01 = -10

L = 1

10 IF (L .GT. 8000) THEN

 WRITE(*,*) ' ***** NOT CONVERGE !! *****'

 STOP

END IF

FZ1 = Z01**3-Z01**2+(A-B-B**2)*Z01-A*B

DFZ1 = 3*Z01**2-2*Z01+(A-B-B**2)

Z1 = Z01-FZ1/DFZ1

IF (ABS(Z01-Z1) .LT. 1E-3) THEN

 GOTO 20

END IF

Z01 = Z1

L = L+1

GOTO 10

20 ZO2 = 0

```
L1 = 1
25 IF ( L1 .GT. 8000 ) THEN
    WRITE(*,*) ' ***** NOT CONVERGE !! *****'
    STOP
END IF
FZ2 = ZO2**3-ZO2**2+(A-B-B**2)*ZO2-A*B
DFZ2 = 3*ZO2**2-2*ZO2+(A-B-B**2)
Z2 = ZO2-FZ2/DFZ2
IF (ABS(ZO2-Z2) .LT. 1E-3) THEN
GOTO 30
END IF
ZO2 = Z2
L1 = L1+1
GOTO 25

30 ZO3 = 10
L2 = 1
35 IF ( L2 .GT. 8000 ) THEN
    WRITE(*,*) ' ***** NOT CONVERGE !! *****'
    STOP
END IF
FZ3 = ZO3**3-ZO3**2+(A-B-B**2)*ZO3-A*B
DFZ3 = 3*ZO3**2-2*ZO3+(A-B-B**2)
Z3 = ZO3-FZ3/DFZ3
IF (ABS(ZO3-Z3) .LT. 1E-3) THEN
GOTO 40
END IF
ZO3 = Z3
L2 = L2+1
GOTO 35

Z(1) = Z1
Z(2) = Z2
Z(3) = Z3
```

```

jump = 3
50 jump = jump/2
IF ( jump .NE. 0 ) THEN
    j2 = 3-jump
    DO 60 j = 1,j2
        DO 60 i = j,1,-jump
            j3 = i+jump
            IF ( Z(i) .GT. Z(j3) ) THEN
                s = Z(i)
                Z(i) = Z(j3)
                Z(j3) = s
            END IF
60      CONTINUE
        GOTO 50
    END IF

```

```

Z1 = Z(1)
Z2 = Z(2)
Z3 = Z(3)

```

```

40 RETURN
END

```

```

CC
CC      Calculate average density
CC

```

SUBROUTINE MWDENSPR(X,T,P,MWA,DENSA)

```

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

```

DIMENSION X(20),TR(20),MI(20),ALPHA(20),ACI(20),AI(20),BI(20)

REAL MW,MWA,MI,GC

DENSA=0.0

MWA=0.

CC

CC Define constant value

CC

GC = 10.731

KIJ = 0.001

SUMAL = 0.0

SUMBL = 0.0

SUMATL = 0.0

DO 1 J=1,NC

TR(J) = T/TC(J)

MI(J) = 0.37464+1.54226*W(J)-0.26992*W(J)**2

ALPHA(J) = (1.0+MI(J)*(1-TR(J)**(0.5)))**2

ACI(J) = 0.45724*(GC*TC(J))**2/PC(J)

AI(J) = ALPHA(J)*ACI(J)

BI(J) = 0.07780*GC*TC(J)/PC(J)

SUMBL = SUMBL + X(J)*BI(J)

1 CONTINUE

DO 2 I = 1,NC

DO 3 J = 1,NC

SUMAL = SUMAL+X(I)*X(J)*(AI(I)*AI(J))**0.5*(1-KIJ)

SUMATL = SUMATL+X(I)*X(J)*MI(J)*(AI(I)*ACI(J)*TR(J))**0.5*(1-KIJ)

3 CONTINUE

2 CONTINUE

AL = SUMAL*P/(GC*T)**2

BL = SUMBL*P/(GC*T)

CALL NEWTON(AL,BL,Z1,Z2,Z3)

IF (Z1 .LE. 0) THEN

 IF (Z2 .LE. 0) THEN

 ZL = Z3

 ELSE

 ZL = Z2

 END IF

ELSE

 ZL = Z1

END IF

VV = ZL*GC*T/P

DO 5 J=1,NC

5 MWA=X(J)*MW(J)+MWA

DENSA=1/(VV/MWA)

RETURN

END

CC

CC Buble point Calculation

CC

SUBROUTINE BUBPTPR(T,X,Y,P)

REAL GC,MI,KI, APRIMEX,APRIMEY,APRIMEXH,APRIMEYH,KIH,
+FSLOPE,F,y

COMMON NC,MW(20),DENS(20),C1(20),C2(20),C3(20),BPT(20),AVP(20),
+BVP(20),tc(20),pc(20),zc(20),w(20),a1(20),a2(20),a3(20),a4(20),
+a5(20)

DIMENSION X(20),Y(20),TR(20),MI(20),ALPHA(20),ACI(20),
+AI(20),BI(20),FIL(20),FIV(20),KI(20),APRIMEX(20),APRIMEY(20)

```
DIMENSION FILH(20),FIVH(20),APRIMEXH(20),APRIMEYH(20),KIH(20),
+ALPHAH(20),AIH(20),TRH(20)
```

CC

CC Define constant value

CC

GC = 1.986

KIJ = 0.001

DO 40 I = 1,NC

IF (Y(I) .EQ. 0.) THEN

 ki(i) = 1.

 Y(I) = KI(I)*X(I)

END IF

40 continue

LOOP = 0

10 LOOP=LOOP+1

SUMXA = 0.0

SUMYA = 0.0

SUMXAH = 0.0

SUMYAH = 0.0

SUMAL = 0.0

SUMAV = 0.0

SUMALH = 0.0

SUMAVH = 0.0

SUMBL = 0.0

SUMBV = 0.0

TH = T+1.0

```

IF(LOOP .GT. 8000) GOTO 30
SUMY=0.0
SUMYH = 0.0

DO 1 J=1,NC
TR(J) = T/TC(J)
TRH(J) = TH/TC(J)
MI(J) = 0.37464+1.54226*W(J)-0.26992*W(J)**2
ALPHA(J) = (1.0+MI(J)*(1-TR(J)**(0.5)))**2
ALPHAH(J) = (1.0+MI(J)*(1-TRH(J)**(0.5)))**2
ACI(J) = 0.45724*(GC*TC(J))**2/PC(J)
AI(J) = ALPHA(J)*ACI(J)
AIH(J) = ALPHAH(J)*ACI(J)
BI(J) = 0.07780*GC*TC(J)/PC(J)
SUMXA = SUMXA+X(J)*AI(J)**0.5*(1-KIJ)
SUMXAH = SUMXAH+X(J)*AIH(J)**0.5*(1-KIJ)
SUMYA = SUMYA+Y(J)*AI(J)**0.5*(1-KIJ)
SUMYAH = SUMYAH+Y(J)*AIH(J)**0.5*(1-KIJ)
SUMBL = SUMBL + X(J)*BI(J)
SUMBV = SUMBV + Y(J)*BI(J)

1 CONTINUE

DO 2 I = 1,NC
DO 3 J = 1,NC
SUMAL = SUMAL+X(I)*X(J)*(AI(I)*AI(J))**0.5*(1-KIJ)
SUMALH = SUMALH + X(I)*X(J)*(AIH(I)*AIH(J))**0.5*(1-KIJ)
SUMAV = SUMAV+Y(I)*Y(J)*(AI(I)*AI(J))**0.5*(1-KIJ)
SUMAVH = SUMAVH + Y(I)*Y(J)*(AIH(I)*AIH(J))**0.5*(1-KIJ)

3 CONTINUE
2 CONTINUE

AL = SUMAL*P/(GC*T)**2
ALH = SUMALH*P/(GC*TH)**2
AV = SUMAV*P/(GC*T)**2
AVH = SUMAVH*P/(GC*TH)**2

```

```

BL = SUMBL*P/(GC*T)
BLH = SUMBL*P/(GC*TH)
BV = SUMBV*P/(GC*T)
BVH = SUMBL*P/(GC*TH)

```

```
CALL NEWTON(AL,BL,Z1,Z2,Z3)
```

```
IF ( Z1 .LE. 0 ) THEN
```

```
    IF ( Z2 .LE. 0 ) THEN
```

```
        ZL = Z3
```

```
    ELSE
```

```
        ZL = Z2
```

```
    END IF
```

```
ELSE
```

```
    ZL = Z1
```

```
END IF
```

```
CALL NEWTON(ALH,BLH,Z1,Z2,Z3)
```

```
IF ( Z1 .LE. 0 ) THEN
```

```
    IF ( Z2 .LE. 0 ) THEN
```

```
        ZLH = Z3
```

```
    ELSE
```

```
        ZLH = Z2
```

```
    END IF
```

```
ELSE
```

```
    ZLH = Z1
```

```
END IF
```

```
CALL NEWTON(AV,BV,Z1,Z2,Z3)
```

```
ZV = Z3
```

```
CALL NEWTON(AVH,BVH,Z1,Z2,Z3)
```

```
ZVH = Z3
```

```
DO 15 I=1,NC
```

```
APRIMEX(I) = 1.0/SUMAL*(2*AI(I)**0.5*SUMXA)
```

```
APRIMEXH(I) = 1.0/SUMALH*(2*AIH(I)**0.5*SUMXAH)
```

```
APRIMEY(I) = 1.0/SUMAV*(2*AI(I)**0.5*SUMYA)
```

```
APRIMEYH(I) = 1.0/SUMAVH*(2*AIH(I)**0.5*SUMYAH)
```



252

```

FIL(I) = EXP(BI(I)/SUMBL*(ZL-1)-ALOG(ZL-BL)-AL/(2.82843*BL)*
+(APRIMEX(I)-BI(I)/SUMBL)*ALOG((ZL+2.4142*BL)/(ZL-0.4142*BL)))

FILH(I) = EXP(BI(I)/SUMBL*(ZLH-1)-ALOG(ZLH-BLH)-ALH/(2.82843*BLH)*
+(APRIMEXH(I)-BI(I)/SUMBL)*ALOG((ZLH+2.4142*BLH)/(ZLH-0.4142*BLH)))

FIV(I) = EXP(BI(I)/SUMBV*(ZV-1)-ALOG(ZV-BV)-AV/(2.82843*BV)*
+(APRIMEY(I)-BI(I)/SUMBV)*ALOG((ZV+2.4142*BV)/(ZV-0.4142*BV)))

FIVH(I) = EXP(BI(I)/SUMBV*(ZVH-1)-ALOG(ZVH-BVH)-AVH/(2.82843*BVH)*
+(APRIMEYH(I)-BI(I)/SUMBV)*ALOG((ZVH+2.4142*BVH)/(ZVH-0.4142*BVH)))

KI(I) = FIL(I)/FIV(I)

KIH(I) = FILH(I)/FIVH(I)

SUMY = SUMY +X(I)*KI(I)

SUMYH = SUMYH +X(I)*KIH(I)

```

15 CONTINUE

IF(LOOP .EQ. 1) THEN

DO 16 I = 1,NC

Y(I) = KI(I)*X(I)/SUMY

16 CONTINUE

GOTO 10

END IF

IF (ABS(SUMY-SUMYZ) .GE. 1E-3) THEN

DO 17 I = 1,NC

Y(I) = KI(I)*X(I)/SUMY

17 CONTINUE

SUMYZ = SUMY

GOTO 10

END IF

IF (ABS(SUMY-1) .LT. 1E-3) RETURN

F=SUMY-1.0

FH = SUMYH-1.0

FSLOPE=(FH-F)/1.

```
T=T-F/FSLOPE
GOTO 10

1000 WRITE(*,*) ' ****Converged !!
read(*,*)
WRITE(*,*) '      TEMP      SUMY      LOOP '
WRITE(*,*) 
WRITE(*,*) T, SUMY, LOOP
READ(*,*) 
WRITE(*,*) 
WRITE(*,*) '      yi      ki'
write(*,*) 
DO 1010 I = 1,NC
WRITE(*,*) Y(I),KI(I)
READ(*,*) 
1010 CONTINUE
stop

30 WRITE(*,*) 'The calculation does not converge !!
STOP
END
```



VITA

Miss Kallaya Klaithong graduated high school from Benchama Ratrungsarit school in 1986 and received Bachelor Degree in Chemical Engineering from the Department of Chemical Technology, Faculty of Science, Chulalongkorn University in 1990. After then she subsequently studied for a requirement of the Master's Degree in Chemical Engineering at the Department of Chemical Engineering, Faculty of Engineering, Chulalongkorn University from 1992 till 1994.

She also has an experience in working as process engineer at The Bangchak Petroleum Public Company Limited in 1990 uptill the present.