REFERENCES

- Abou-Kassem, J.H. (1999). Screening of Oil Reservoirs for Selecting Candidates of Polymer Injection. <u>Energy Sources, Part A: Recovery, Utilization, and Environmental Effects</u>, 21(1-2), 5–15.
- AquaSilTM and SurfaSilTM Siliconizing Fluids data sheet (2003), Pierce Biotechnology, Inc., Rockford, Illinois.
- Balcom, B.J., MacGregor, R.P., Beyea, S.D., Green, D.P., Armstrong, R.L., and Bremner, T.W. (1996). Single-Point Ramped Imaging with T₁ Enhancement (SPRITE). Journal of Magnetic Resonance - Series A, 123(1), 131-134.
- Barrita, J.C. (2002), <u>Curing of High-Performance Concrete in Hot Dry Climates</u> <u>Studied Using Magnetic Resonance Imaging.</u> Ph.D. Thesis in Civil Engineering, University of New Brunswick.
- Beaumont, E.A., and Foster, N.H. (1987). <u>Reservoir I: Properties.</u> Oklahoma: The American association of petroleum geologists.
- Chen, Q., Halse, M., and Balcom, B.J. (2005). Centric scan SPRITE for spin density imaging of short relaxation time porous materials. <u>Magnetic Resonance</u> <u>Imaging</u>, 23(2), 263–266.
- Chen, Q., Rack, F.R., and Balcom, B.J. (2006). Quantitative magnetic resonance imaging methods for core analysis. <u>Geological Society Special Publication</u>, 267, 193–207.
- Dake, L.P. (2002). <u>Fundamentals of Reservoir Engineering</u>. Amsterdam: Elsevier Science B.V.
- Dawe, R.A. (2000). <u>Modern Petroleum Technology (Volume 1, Upstream)</u>. Chichester: John Wiley & Sons, Ltd.
- Gerding, M. (1986). <u>Fundamentals of Petroleum</u>. Texas: Petroleum Extension Service.
- Green, D.W., and Willhite, G.P. (1998). <u>Enhanced Oil Recovery</u>. Texas: Society of Petroleum Engineers.
- Halse, M. (2004), <u>Centric scan SPRITE MRI: Optimization of SNR, resolution and</u> relaxation time mapping with applications to quantitative sodium imaging. M. S. Thesis in Physics, University of New Brunswick.

- Halse, M., Goodyear, D.J., MacMillan, B., Szomolanyi, P., Matheson, D., and Balcom, B.J. (2003). Centric scan SPRITE magnetic resonance imaging. <u>Journal of Magnetic Resonance</u>, 165(2), 219–229.
- Halse, M., Rioux, J., Romanzetti, S., Kaffanke, J., MacMillan, B., Mastikhin, I., Shah, N.J., Aubanel, E., and Balcom, B.J. (2004). Centric scan SPRITE magnetic resonance imaging: optimization of SNR, resolution, and relaxation time mapping. Journal of Magnetic Resonance, 169(1), 102–117.
- Huang, D.D., and Honarpour, M.M. (1998). Capillary end effects in coreflood calculations. Journal of Petroleum Science and Engineering, 19, 103-117.
- Lake, L.W. (1989). Enhanced Oil Recovery. New Jersey: Prentice Hall.
- Li, L., Marica, F., Chen, Q., MacMillan, B., and Balcom, B.J. (2007). Quantitative discrimination of water and hydrocarbons in porous media by magnetization prepared centric-scan SPRITE. <u>Journal of Magnetic Resonance</u>, 186(2), 282–292.
- Liang, Z.P., and Lauterbur, P.C. (2000). <u>Principles of Magnetic Resonance Imag-</u> ing. New Jersey: Institute of Electrical and Electronics Engineers, Inc.
- Marica, F., Chen, Q., Hamilton, A., Hall, C., Al, T., and Balcom, B.J. (2006). Spatially resolved measurement of rock core porosity. <u>Journal of Magnetic</u> <u>Resonance</u>, 178(1), 136–141.
- Partain, C.L., James, A.E., Rollo, F.D., and Price, R.R. (1983). <u>Nuclear magnetic</u> resonance NMR imaging. Philadelphia: Saunders.
- Pitts, M.J., Campbell, T.A., Surkalo, H., and Wyatt, K. (1995). Polymer Flood of the Rapdan Pool. <u>SPE Reservoir Engineering</u>, 10(3), 183–186.
- Romero-Zerón, L.B. (2004), <u>The role of porous media wettability on foamed gel</u> propagation and fluid diverting perforamance. Ph.D. Thesis in Chemical and Petroleum Engineering, University of Calgary.
- Sydansk, R.D. (1990). A Newly Developed Chromium(III) Gel Technology. <u>SPE</u> <u>Reservoir Engineering</u>, 5(3), 346–352.
- Sydansk, R.D., and Southwell, G.P. (2000). More Than 12 Years' Experience With a Successful Conformance-Control Polymer-Gel Technology. <u>SPE Produc-</u> <u>tion & Facilities</u>, 15(4), 270–278.

- Sydansk, R.D. (2005). <u>SPE Petroleum Engineering Handbook, Reservoir Engineer-</u> ing Section Chapter 13: Polymers. Gels, Foams, and Resins. Texas. In press.
- Synchro-lectric Viscometer LVF Model, Instruction Manual, Brookfield engineering laboratories, Stoughton, Massachusetts.
- Szomolanyi, P., Goodyear, D., Balcom, B., and Matheson, D. (2001). SPIRAL-SPRITE: a rapid single point MRI technique for application to porous media. <u>Magnetic Resonance Imaging</u>, 19(3-4), 423–428.
- Torsæter, O., and Abtahi, M. (1996). Experimental Reservoir Engineering Laboratory Workbook. Trondheim: Department of Petroleum Engineering and Applied Geophysics, Norwegian University of Science and Technology.
- Wassmuth, F.R., Hodgins, L.A., Schramm, L.L., and Kutay, S.M. (2001). Screening and Coreflood Testing of Gel Foams To Control Excessive Gas Production in Oil Wells. <u>SPE Reservoir Evaluation & Engineering</u>, 4(3), 187–194.

APPENDICES

Appendix A Sand-pack Calculations for Sand pack Without Channel

A.1 Pore Volume and Porosity Calculations

Without channel



Volume of sample can be divided into three parts i.e. Sand-pack body, Inlet part and Outlet part.

Sand-pack body:

Inside Diameter 2.6 cm, Length 7 cm

Volume =
$$\frac{\pi}{4} \cdot I.D.^2 \cdot L$$
 where *I.D.* = Inside Diameter, *L* = Length
= $\frac{\pi}{4} \cdot 2.6^2 \cdot 7.0 = 37.1650 \text{ cm}^3$

Inlet part:



Inlet part can be separated into three parts

1. Valve: Inside Diameter 0.5 cm, Length 0.6 cm

Volume = $\frac{\pi}{4} \cdot I.D.^2 \cdot L$ where I.D. = Inside Diameter, L = Length = $\frac{\pi}{4} \cdot 0.5^2 \cdot 0.6 = 0.1178 \text{ cm}^3$

2. Connection: Inside Diameter 0.15 cm, Length 1 cm

Volume =
$$\frac{\pi}{4} \cdot I.D.^2 \cdot L$$
 where *I.D.* = Inside Diameter, *L* = Length
= $\frac{\pi}{4} \cdot 0.15^2 \cdot 1.0 = 0.0177 \text{ cm}^3$

3. Cone shape: Big cone, Inside Diameter 2.6 cm, Length 0.7647 cm

Small cone in connection,

Inside Diameter 0.9 cm, Length 0.2647 cm

Volume =
$$\left[\frac{\pi}{3} \cdot \left(\frac{I.D.}{2}\right)^2 \cdot L\right]_{big \ cone} - \left[\frac{\pi}{3} \cdot \left(\frac{I.D.}{2}\right)^2 \cdot L\right]_{small \ cone \ in \ connection}$$

where I.D. = Inside Diameter, L = Length

$$= \left[\frac{\pi}{3} \cdot \left(\frac{2.6}{2}\right)^2 \cdot 0.7647\right] - \left[\frac{\pi}{3} \cdot \left(\frac{0.9}{2}\right)^2 \cdot 0.2647\right] = 1.2972 \text{ cm}^3$$

Total Volume in Inlet part: 0.1178 + 0.0177 + 1.2972 = 1.4327 cm³

Outlet part:



Outlet part can be separated into three parts

1. Cap: Inside Diameter 0.4 cm, Length 2.1 cm

Volume =
$$\frac{\pi}{4} \cdot I.D.^2 \cdot L$$
 where *I.D.* = Inside Diameter, *L* = Length
= $\frac{\pi}{4} \cdot 0.4^2 \cdot 2.1 = 0.2639 \text{ cm}^3$

2. Connection: Inside Diameter 0.6 cm, Length 0.1 cm

Volume =
$$\frac{\pi}{4} \cdot I.D.^2 \cdot L$$
 where *I.D.* = Inside Diameter, *L* = Length
= $\frac{\pi}{4} \cdot 0.6^2 \cdot 0.1 = 0.0283 \text{ cm}^3$

3. Outlet end: Inside Diameter 0.2 cm, Length 4.0 cm

Volume =
$$\frac{\pi}{4} \cdot I.D.^2 \cdot L$$
 where *I.D.* = Inside Diameter, *L* = Length
= $\frac{\pi}{4} \cdot 0.2^2 \cdot 4.0 = 0.1257 \text{ cm}^3$

Total Volume in Outlet part: 0.2639 + 0.0283 + 0.1257 = 0.4178 cm³

Porosity Determination by Liquid Saturating Method

- 1. Weight of sample container, $W_{container} = 31.02$ g.
- 2. Weight of dry sand sample, $W_{dry} = 68.48$ g.
- 3. Weigh the saturated sample, $W_{sat} = 113.97$ g.
- 4. Calculate the saturated distilled water weight,

 $W_{water} = W_{sat} - W_{dry} - W_{container}$ = 113.97 - 68.48 - 31.02 = 14.47 g.

5. Calculate the total volume of water displaced in whole sample,

 $V_{water} = W_{water} / \rho_{water}$ where $\rho_{water} = 1.0 \text{ g/ cm}^3$ = 14.47/1.0 = 14.47 cm³.

6. Calculate the pore volume by subtracted the volume of water in inlet part and outlet part,

$$V_p = V_{water} - V_{lnlet} - V_{Outlet}$$

= 14.47 - 1.4327 - 0.4178 = 12.62 cm³.

7. Calculate the porosity,

 $\phi = V_p/V_b$ where V_b = Volume in sand-pack body = 37.1650 cm³ = 12.62/37.1650 = 0.3395 = 33.95%

A.2 Permeability Calculations



Sand-pack body:

Inside Diameter 2.6 cm, Length 7 cm

Cross-sectional area, $A = \frac{\pi}{4} \cdot I.D.^2$ where *I.D.* = Inside Diameter = $\frac{\pi}{4} \cdot 2.6^2 = 5.3093 \text{ cm}^2$

Absolute Permeability Measurement of Water

1. Record the water level difference in manometer under and operational flow rate measured by volume of water produced from the system in a period of time.

| Experiment # | 1 | 2 | 3 | 4 | 5 |
|--|-----|-----|-----|------|------|
| Volume of water produced, V_w (cm ³) | 8 | 8 | 8 | 8 | 8 |
| Period of time, ΔT (sec) | 344 | 441 | 588 | 1022 | 2727 |
| Water level difference in manometer, h (cm) | 3.4 | 2.9 | 2.3 | 1.5 | 0.8 |

2. Calculate the operational flow rate in cm³/sec and pressure drop in atm.

For Example: Experiment # 1

2.1 Operational flow rate in cm^3/sec .

Flow rate =
$$\frac{Volume \ of \ water \ produced, V_w(cm^3)}{Period \ of \ time, \Delta T(sec)}$$

$$=\frac{8}{344}=0.0233$$
 cm³/sec

2.2 Pressure drop in atm.

Level of water in manometer, h = 3.4 cm = 0.034 m

Pressure drop = $\rho g h$, when ρ (density of water) = 1000 kg/m³

g (gravity force) =
$$9.81 \text{ m/s}^2$$

$$= 1000 \cdot 9.81 \cdot 0.034$$

$$= 333.54 \text{ Pa} \cdot \frac{1 \text{ atm}}{101325 \text{ Pa}} = 0.0033 \text{ atm}$$

| Experiment # | 1 | 2 | 3 | 4 | 5 |
|---|--------|--------|--------|--------|--------|
| Flow rate, Q_w (cm ³ /sec) | 0.0233 | 0.0181 | 0.0136 | 0.0078 | 0.0029 |
| Pressure drop, ΔP (atm) | 0.0033 | 0.0028 | 0.0022 | 0.0015 | 0.0008 |

3. From Darcy's Law, the equation can be rewritten as followed,

.

$$\frac{Q_w}{A} = \frac{K}{\mu} \frac{\Delta P}{L}$$

where Q_w is the flow rate, in cm³/sec, A is the cross-sectional area = 5.3093 cm², K is the permeability, in Darcys, μ is the water viscosity = 1 cP, ΔP is the pressure drop, in atm, L is the length = 7 cm.

Therefore, a plot of $\Delta P/L$ and Q_w/A give a slope of K/μ .

| Experiment # | 1 | 2 | 3 | 4 | 5 |
|-----------------------|--------|--------|--------|--------|--------|
| $\Delta P/L$ (atm/cm) | 0.0005 | 0.0004 | 0.0003 | 0.0002 | 0.0001 |
| Q_w/A (cm/sec) | 0.0044 | 0.0034 | 0.0026 | 0.0015 | 0.0006 |



4. Calculate K from slope,

when Slope = $10.457 \text{ cm}^2/\text{atm sec}$ and $\mu = 1 \text{ cP}$ Slope = K/μ , $\therefore K = \text{Slope} \ \mu = 10.457 \text{ cm}^2/\text{atm} \text{ sec} \ 1 \text{ cP}$ = 10.457 Darcys = 10,457 mD ~ 10,460 mD

A.3 Fluid Saturations in Sample

_ .

. .

Based on the Frontal Advanced Rate (FAR) of 2 ft/day, the flow rate used in the experiment was calculated into cm³/min by

Flow rate =
$$A^{*}FAR \phi$$
 when A is the cross-sectional area = 5.3093 cm²
 FAR is Frontal Advanced Rate = 2 ft/day
 ϕ is porosity = 0.3395
Flow rate = 5.3093 cm² 2 ft/day $\cdot \frac{30.48 \text{ cm}}{1 \text{ ft}} \cdot \frac{1 \text{ day}}{24 \text{ hr}} \cdot \frac{1 \text{ hr}}{60 \text{ min}} = 0.3395$
= 0.0763 cm³/min

In order to saturate the sample 1 PV, the approximately total time was

Fotal time for 1 PV =
$$\frac{Pore \ volume \ , V_p}{Flow \ rate}$$

= $\frac{12.62 \ cm^3}{0.0763 \ cm^3 \ / \min} \cdot \frac{1 \ hr}{60 \ min}$
= 2.76 hr

The sample was saturated first with water and then oil under this flow rate. To correct end effect, high flow rate of oil was used in the last step. The total water removed after saturated with oil was measured in order to calculate the initial oil saturation and the irreversible water saturation in the sample. Initial oil saturation in the sand-pack body was calculated from the total water removed subtracted by water in the inlet part (1.4327 cm³) and the outlet part (0.4178 cm³).

Total water removed = 13.30 cm^3

Initial oil saturation in the sand-pack body = 13.30 - 1.4327 - 0.4178

Irreversible water saturation in the sand-pack body was calculated from the pore volume, V_p (12.62 cm³) subtracted by initial oil saturation in the sand-pack body (11.45 cm³).

Irreversible water saturation in the sand-pack body = $12.62 - 11.45 = 1.17 \text{ cm}^3$

From the above calculations, the percentages of initial oil saturation and irreversible water saturation in the sand-pack body were calculated by

Initial oil saturation =
$$\frac{11.45}{12.62}$$
 100 = 90.73%

Irreversible water saturation = $\frac{1.17}{12.62}$ 100 = 9.27%

After flooding process, waterflooding was proceeded in this sample, the amount of oil recovery was recorded to calculate residual oil saturation and oil recovery. Oil recovery from sand-pack body was calculated from the total oil recovery subtracted by oil in the inlet part (1.4327 cm³) and the outlet part (0.4178 cm³).

Total oil recovery after waterflooding = 10.50 cm^3 Oil recovery from sand-pack body = $10.50 - 1.4327 - 0.4178 = 8.65 \text{ cm}^3$ Residual oil saturation in the sand-pack body = $11.45 - 8.65 = 2.8 \text{ cm}^3$ Percentage of oil recovery = $\frac{8.65}{11.45}$ 100 = 75.55% Percentage of residual oil saturation = $\frac{2.8}{11.45}$ 100 = 24.45%

Appendix B Sand-pack Calculations for Channel sample #1

B.1 Pore Volume and Porosity Calculations

Channel sample # 1



Channel volume:

Inside Diameter 0.23 cm, Length 9.5 cm

Volume =
$$\frac{\pi}{4} \cdot I.D.^2 \cdot L$$
 where $I.D.$ = Inside Diameter, L = Length
= $\frac{\pi}{4} \cdot 0.23^2 \cdot 9.5 = 0.395 \text{ cm}^3$

Sand-pack body:

Volume = $\frac{\pi}{4} \cdot I.D^2_{\text{syringe}} \cdot L_{\text{syringe}} - \frac{\pi}{4} \cdot O.D^2_{\text{channel}} \cdot L_{\text{channel}}$

where I.D. = Inside Diameter, O.D. = Outside Diameter, L = Length

$$= \frac{\pi}{4} \cdot 2.6^2 \cdot 7.5 - \frac{\pi}{4} \cdot 0.41^2 \cdot 9.5 = 38.565 \text{ cm}^3$$

Total Volume in Inlet part: 1.4327 cm³ (from Appendix A.1)

Total Volume in Outlet part: 0.4178 cm³ (from Appendix A.1)

Porosity Determination by Liquid Saturating Method

- 1. Weight of sample container (including channel), $W_{container} = 38.22$ g.
- 2. Weight of dry sand sample, $W_{dry} = 71.28$ g.
- 3. Weigh the saturated sample, $W_{sat} = 124.47$ g.

4. Calculate the saturated distilled water weight,

 $W_{water} = W_{sat} - W_{dry} - W_{container}$ = 124.47-71.28-38.22 = 14.97 g.

5. Calculate the total volume of water displaced in whole sample,

$$V_{water} = W_{water} / \rho_{water}$$
 where $\rho_{water} = 1.0 \text{ g/ cm}^3$
= 14.97/1.0 = 14.97 cm³.

6. Calculate the pore volume by subtracted the volume of water in inlet part and outlet part,

$$V_p = V_{water} - V_{Inlet} - V_{Outlet}$$

= 14.97 - 1.4327 - 0.4178 = 13.12 cm³.

7. Calculate the porosity,

$$\phi = V_p/V_b$$
 where V_b = Volume in sand-pack body = 38.565 cm³

B.2 Permeability Calculations

Sand-pack body:

Inside Diameter 2.6 cm, Length 7 cm

Cross-sectional area,
$$A = \frac{\pi}{4} \cdot I.D._{syringe}^2 - \frac{\pi}{4} \cdot O.D._{channel}^2$$

where I.D. = Inside Diameter, O.D. = Outside Diameter

$$= \frac{\pi}{4} \cdot 2.6^2 - \frac{\pi}{4} \cdot 0.41^2 = 5.177 \text{ cm}^2$$

Absolute Matrix Permeability Measurement of Water

1. Record the water level difference in manometer under and operational flow rate measured by volume of water produced from the system in a period of time.

| Experiment # | | 2 | 3 | 4 | 5 |
|--|-----|-----|-----|-----|------|
| Volume of water produced, V_w (cm ³) | 8 | 8 | 8 | 8 | 8 |
| Period of time, ΔT (sec) | 332 | 400 | 535 | 807 | 1641 |
| Water level difference in manometer, h (cm) | 2.8 | 2.5 | 1.8 | 1.5 | 0.7 |

2. Calculate the operational flow rate in cm^3/sec and pressure drop in atm.

For Example: Experiment #1

2.1 Operational flow rate in cm^3/sec .

Flow rate =
$$\frac{Volume \ of \ water \ produced, V_w(cm^3)}{Period \ of \ time, \Delta T \ (sec)}$$

$$=\frac{8}{332}=0.0241$$
 cm³/sec

2.2 Pressure drop in atm.

Level of water in manometer, h = 2.8 cm = 0.028 m

Pressure drop = $\rho g h$, when ρ (density of water) = 1000 kg/m³

g (gravity force) =
$$9.81 \text{ m/s}^2$$

 $= 1000 \cdot 9.81 \cdot 0.028$

$$= 274.68 \text{ Pa} \cdot \frac{1 \text{ atm}}{101325 \text{ Pa}} = 0.0027 \text{ atm}$$

| Experiment # | 1 | 2 | 3 | 4 | 5 |
|---|--------|--------|--------|--------|--------|
| Flow rate, Q_w (cm ³ /sec) | 0.0241 | 0.0200 | 0.0150 | 0.0099 | 0.0049 |
| Pressure drop, ΔP (atm) | 0.0027 | 0.0024 | 0.0017 | 0.0015 | 0.0007 |

3. From Darcy's Law, the equation can be rewritten as followed,

$$\frac{Q_w}{A} = \frac{K_{matrix}}{\mu} \frac{\Delta P}{L}$$

where Q_w is the flow rate, in cm³/sec, A is the cross-sectional area of sand pack body subtracting the channel = 5.177 cm², K_{matrix} is the matrix permeability, in Darcys, μ is the water viscosity = 1 cP, ΔP is the pressure drop, in atm, L is the length = 7.5 cm.

Therefore, a plot of $\Delta P/L$ and Q_w/A give a slope of K_{matrix}/μ .

| Experiment # | 1 | 2 | 3 | 4 | 5 |
|-----------------------|--------|--------|--------|--------|--------|
| $\Delta P/L$ (atm/cm) | 0.0004 | 0.0003 | 0.0002 | 0.0002 | 0.0001 |
| Q_w/A (cm/sec) | 0.0047 | 0.0039 | 0.0029 | 0.0019 | 0.0009 |



- 4. Calculate K_{matrix} from slope, Slope = K_{matrix}/μ , when Slope = 13.627 cm²/atm sec and μ = 1cP $\therefore K_{matrix}$ = Slope μ = 13.627 cm²/atm sec 1 cP = 13.627 Darcys = 13,627 mD.
- 5. Calculate K_{channel} from the following equation,

 $K_{channel} = 20 \cdot 10^6 I.D_{channel}^2$ where *I.D.* = Inside Diameter of the channel in inch

$$K_{channel} = 20 \cdot 10^6 \cdot \left(0.23 \ cm \cdot \frac{0.3937 \ in}{1 \ cm} \right)^2 = 163,990 \ Darcys$$

6. Calculate $K_{average}$ from the following equation,

$$K_{av}A = K_{matrix}(A - A_{O.D. channel}) + K_{channel}A_{I.D. channel}$$
$$K_{av} \cdot \left(\frac{\pi}{4} \cdot 2.6^{2}\right) = 13.627 \cdot \left(\frac{\pi}{4} \cdot 2.6^{2} - \frac{\pi}{4} \cdot 0.41^{2}\right) + 163,990 \cdot \left(\frac{\pi}{4} \cdot 0.23^{2}\right)$$
$$\therefore K_{av} = 1296.63 \text{ Darcys}$$



CURRICULUM VITAE

Name: Ms. Sureerat Ongsurakul

Date of Birth: November 14, 1983

Nationality: Thai

University Education:

2000 – 2004 Bachelor Degree of Science, 2nd class honour, in Chemical Technology, Faculty of Science, Chulalongkorn University, Bangkok, Thailand

Working Experience:

| 2006 - 2007 | Position: | Research Technician |
|-------------|------------------|-----------------------------|
| | University name: | University of New Brunswick |
| 2004 | Position: | Intern |
| | Company name: | Unocal Thailand, Ltd |
| | | (Chevron Corporation) |

Publications:

- Romero-Zerón L., Ongsurakul, S., Li, L., and Balcom, B.J. (November, 2007) Magnetic Resonance Imaging of Phase Trapping and In-situ Permeability Modification in Unconsolidated Porous Media. <u>Journal of Petroleum Science and Engineering</u>, submitted.
- Romero-Zerón L., Ongsurakul, S., Li, L., and Balcom, B.J. (August, 2007) Visualization of the Effect of Porous Media Wettability on Polymer Flooding Performance through Unconsolidated Porous Media using Magnetic Resonance Imaging. Journal of Petroleum Science and Engineering, submitted PETROL2167.
- Romero-Zerón L., Ongsurakul, S., Li, L., and Balcom, B.J. (July, 2007) Visualization of Mobility-Control by Polymer Waterflooding through Unconsolidated Porous Media using Magnetic Resonance Imaging. <u>Journal of</u> <u>Petroleum Science and Engineering</u>, submitted PETROL2118.
- Romero-Zerón L., Li, L., Ongsurakul, S., and Balcom, B.J. (February, 2007) Visualization of Immiscible Displacement through porous media using MRI. Journal of Petroleum Science and Engineering, submitted PETROL1946.

Presentations:

- Ongsurakul, S., Romero-Zerón, L., Li, L., and Balcom, B.J. (2007, October 28-31) Imaging of Polymer Flooding using MRI. Oral presentation at <u>57th Canadian</u> <u>Chemical Engineering Conference</u>, Edmonton, Alberta, Canada.
- Li, L., Ongsurakul, S., Romero-Zerón, L., MacMillan, B., and Balcom, B.J. (2007, September 3-7) Visualization of Polymer Flooding in Heterogeneous Material with SPRITE Imaging Methodology. Poster presentation at 9th <u>International Conference on Magnetic Resonance Microscopy</u>, Aachen, Germany.

10