

REFERENCES

- Abasaeed, A.E., and Mansour, M.E. (1992). Thermal effects on acid hydrolysis of cellulose. *Bioresource Technology*, 40, 221-224.
- Altaf, Md., Naveena, B.J., Reddy, G. (2007). Use of inexpensive nitrogen sources and starch for L(+) lactic acid production in anaerobic submerged fermentation. *Bioresource Technology*, 98, 498-503.
- Balat, M. (2011). Production of bioethanol from lignocellulosic materials via the biochemical pathway: A review. *Energy Conversion and Management*, 52, 858-875.
- Chang, K.-L., Thitikorn-amorn, J., Hsieh, J.-F., Ou, B.-M., Chen, S.-H., Ratanakhanokchai, K., Huang, P.-J., and Chen, S.-T. (2010). Enhanced enzymatic conversion with freeze pretreatment of rice straw. *Biomass and Bioenergy*, 35, 90-95.
- Chen, M., Xia, L., and Xue, P. (2007). Enzymatic hydrolysis of corncob and ethanol production from cellulosic hydrolysate. *International Biodeterioration and Biodegradation*, 59, 85-89.
- Crofcheck, C.L., and Montross, M.D. (2004). Effect of stover fraction on glucose production using enzymatic hydrolysis. *Transactions of the American Society of Agricultural Engineers*, 47, 841-844.
- Demirbas, A. (2008). Products from lignocellulosic materials via degradation processes. *Energy Sources Part A*, 30, 27-37.
- Eourarekullart, W. (2011). *Conversion of Corncob to Sugars by Microbial Hydrllysis*. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University, Bangkok, Thailand.
- Hamelinck, C.N., Van Hooijdnk, G., and Faaij, A.P.C. (2005) Ethanol from lignocellulosic biomass: techno-economic performance in short-, middle-, and long-term. *Biomass and Bioenergy*, 28, 384-410.
- Harun, R.H., Jason, W.S.Y., Cherrington, T., and Danquah, M.K. (2010). Microalgal biomass as a cellulosic fermentation feedstock for bioethanol production. *Chemical Technology and Biotechnology*, 85, 199-203.

- Hayes, D.J. (2009). An examination of biorefining processes, catalysts and challenges. *Catalysis Today*, 145, 138-151.
- Kaliyan, N., and Morey, R.V. (2010). Densification characteristics of corn cobs. *Fuel Processing Technology*, 91, 559-565.
- Kumar, P., Barrett, D.M., Delwiche, M.J., and Stroeve, P. (2009). Methods for pretreatment of lignocellulosic biomass for efficient hydrolysis and biofuel production. *Industrial and Engineering Chemistry Research*, 48, 3713-3729.
- Liming, X., and Xueliang, S. (2004). High-yield cellulase production by *Trichoderma reesei* ZU-02 on corn cob residue. *Bioresource Technology*, 91, 259-262.
- Lin, L., Yan, R., Liu, Y., and Jiang, W. (2010). In-depth investigation of enzymatic hydrolysis of biomass wastes based on three major component: Cellulose, hemicelluloses and lignin. *Bioresource Technology*, 101, 8217-8223.
- Martins, L.F., Kolling, D., Camassola, M., Dillon, A.J.P. and Ramos, L.P. (2008). Comparison of *Penicillium echinulatum* and *Trichoderma reesei* cellulases in relation to their activity against various cellulosic substrates. *Bioresource Technology*, 99, 1417 – 1424.
- Mousdale, D.M. (2008). *Biofuels : biotechnology, chemistry, and sustainable development*. New York: Taylor and Francis Group.
- Movagharnejad, K. and Sohrabi, M. (2003). A model for the rate of enzymatic hydrolysis of some cellulosic waste materials in heterogeneous solid–liquid systems. *Biochemical Engineering Journal*, 14, 1 – 8.
- Mussatto, S.I., Fernandes, M., Milagres, A.M.F., and Roberto, I.C. (2008). Effect of hemicellulose and lignin on enzymatic hydrolysis of cellulose from brewer's spent grain. *Enzyme and Microbial Technology*, 43, 124-129.
- Mussatto, S.I., and Teixeira, J.A. (2010). Lignocellulose as raw material in fermentation processes. *Current research topics in Applied Microbiology and Microbial Biotechnology*, 897-907.
- Rivers, D.R. (1988). Factors affecting the enzymatic hydrolysis of bagasse and rice straw. *Biological Wastes*, 26, 85 – 95.

- Schulz, M.W., Slaytor, M., Hogan, M. and O'Brien, R.W. (1986). Components of cellulose from the higher termite, *Nasutitermes Walkeri*. Insect Biochemistry, 16, 929 – 932.
- Sun, Y., and Cheng, J. (2002). Hydrolysis of lignocellulosic materials for ethanol production: a review. Bioresource Technology, 83, 1-11.
- Taechapopoempol, K., Sreethawong, T., Rangsuvigit, P., Namprohm, W., Thamprajamchit, B., Rengpipat, S., and Chavadej, S. (2011). Isolation of Cellulose-Degrading Bacteria from Termites *Microcerotermes* sp. Applied Biochemistry and Biotechnology, 164, 204-219.
- Taherzadeh, M.J., and Karimi, K. (2007). Acid-based hydrolysis processes for ethanol from lignocellulosic materials: a review. BioResources, 2, 472-499.
- Van Dyk, J.S., and Pletschke, B.I. (2012). A review of lignocellulose bioconversion using enzymatic hydrolysis and synergistic cooperative between enzymes-Factors affecting enzymes, conversion and synergy. Biotechnology Advances. (In press)
- Wang, L., Hanna, M.A., Weller, C.L., and Jones, D.D. (2009). Technical and economical analyses of combined heat and power generation from distillers grains and corn stover in ethanol plants. Energy Conversion and Management, 50, 1704–1713.
- Worasamutprakarn, C. (2010). Conversion of Cellulose to Glucose by Microbes Isolated from Higher Termites. M.S. Thesis, The Petroleum and Petrochemical College, Chulalongkorn University, Bangkok, Thailand.
- Yat, S.C., Berger, A., and Shonnard, D.R. (2008). Kinetic characterization for dilute sulfuric acid hydrolysis of timber varieties and switchgrass. Bioresource Technology, 99, 3855-3863.
- Yeh, A.-I., Huang, Y.-C., and Chen, S.H. (2010). Effect of particle size on the rate of enzymatic hydrolysis of cellulose. Carbohydrate Polymers, 79, 192-199.
- Zhang, Y.-H.P., Himmel, M.E., and Mielenz, J.R. (2006). Outlook for cellulase improvement: Screening and selection strategies. Biotechnology Advances, 24, 452–481.

APPENDICES

Appendix A Standard Calibration Curve

Glucose Calibration Curve

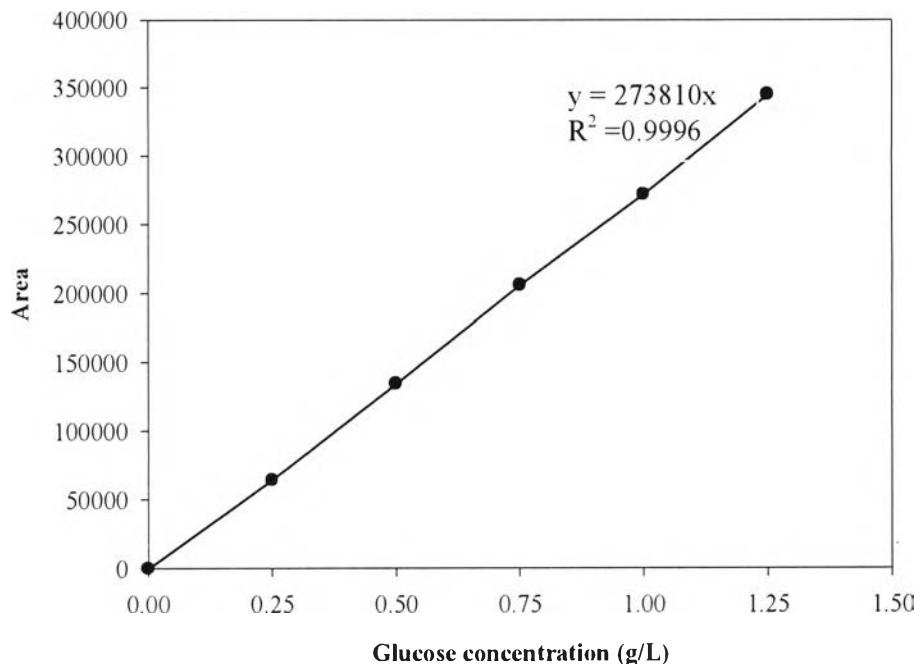


Figure A1 The relationship between glucose concentration (g/L) and area.

Table A1 Glucose calibration curve

Glucose concentration (g/L)	Area(glucose)
0.00	0
0.25	64231
0.50	134469
0.75	206002
1.00	272024
1.25	345123

Appendix B Media for Microorganisms

1. 65 modified DSMZ broth medium 2

Approximate Formula* Per Liter

Carboxymethyl Cellulose (CMC) 5.0 g

Yeast extract 4.0 g

Malt extract 10.0 g

Dissolve and adjust pH to 7.2

Autoclave at 121 °C and pressure at 15 pounds/square inch for 15 minutes

2. 65 modified DSMZ agar medium 2

Approximate Formula* Per Liter

Carboxymethyl cellulose (CMC) 5.0 g

Yeast extract 4.0 g

Malt extract 10.0 g

Agar 12.0 g

Dissolve and adjust pH to 7.2

Autoclave at 121°C and pressure at 15 pounds/square inch for 15 minutes

Appendix C Reagent Preparations

1. 0.85%(w/v) NaCl in 1000 mL

Sodium chloride (NaCl)	8.5	g
Distilled water	1000	mL

2. Hydrochloric acid 1 M in 100 mL

Hydrochloric acid (HCl)	8.29	mL
Distilled water	91.71	mL

3. Sodium hydroxide 0.5 M in 1000 mL

Sodium hydroxide (NaOH)	5.0	g
Distilled water	1000	mL

4. Sulfuric acid 0.72 M in 1000 mL

Sulfuric acid (H_2SO_4 conc.)	72	mL
Distilled water	28	mL

5. 0.05 M Acetate buffer solution in 1000 mL

0.2 M Acetic acid (CH_3COOH)	7.47	mL
0.2 M Sodium acetate (CH_3COONa)	42.53	mL

6. 0.2 M Acetate acid in 1000 mL

Acetate acid (CH_3COOH)	11.6	mL
Distilled water	988.4	mL

7. 0.2 M Sodium acetate in 1000 mL

Sodium acetate (CH_3COONa)	16.4	mL
Distilled water	983.6	mL

Appendix D Bacteria Concentration

Bacteria concentration was determined using total nitrogen test kit.

1. The bacteria concentration from enzymatic hydrolysis

During enzymatic hydrolysis, bacteria growth was monitored by withdrawing samples from the hydrolysis reactor periodically. Solid that obtained from centrifuging of the sample, contained of corncob and bacteria. Method that can calculate weight of bacteria and corncob is shown in equation D1.

$$\text{wt. Solid} = \text{wt. Corncob} + \text{wt. Bacteria} \quad (\text{D1})$$

Then, a concentration of bacteria was determined by the total nitrogen test kit.

$$\text{wt. Bacteria} = \frac{\text{g Nitrogen contained in sample}}{(\text{g Nitrogen} / 1 \text{ g Bacteria})} \quad (\text{D2})$$

1.1 The amount of nitrogen in bacteria

The amount of nitrogen in each strain was determined in triplicates by using the total nitrogen test kit. Figure F1 shows procedure for determination

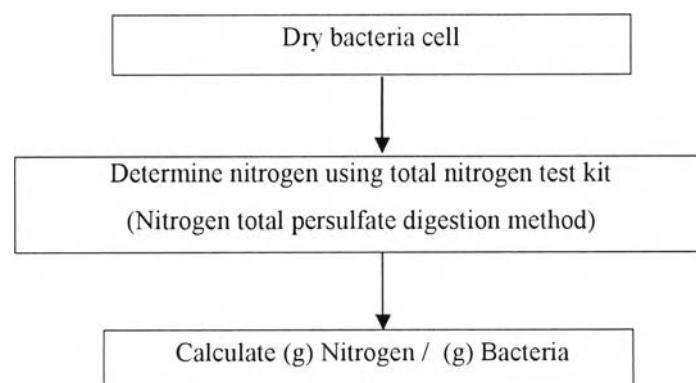


Figure D1 Diagram for determination the amount of nitrogen in bacteria.

Procedure

Nitrogen total persulfate digestion method is conducted in order to check amount of nitrogen which directly related to amount of bacteria during hydrolysis.

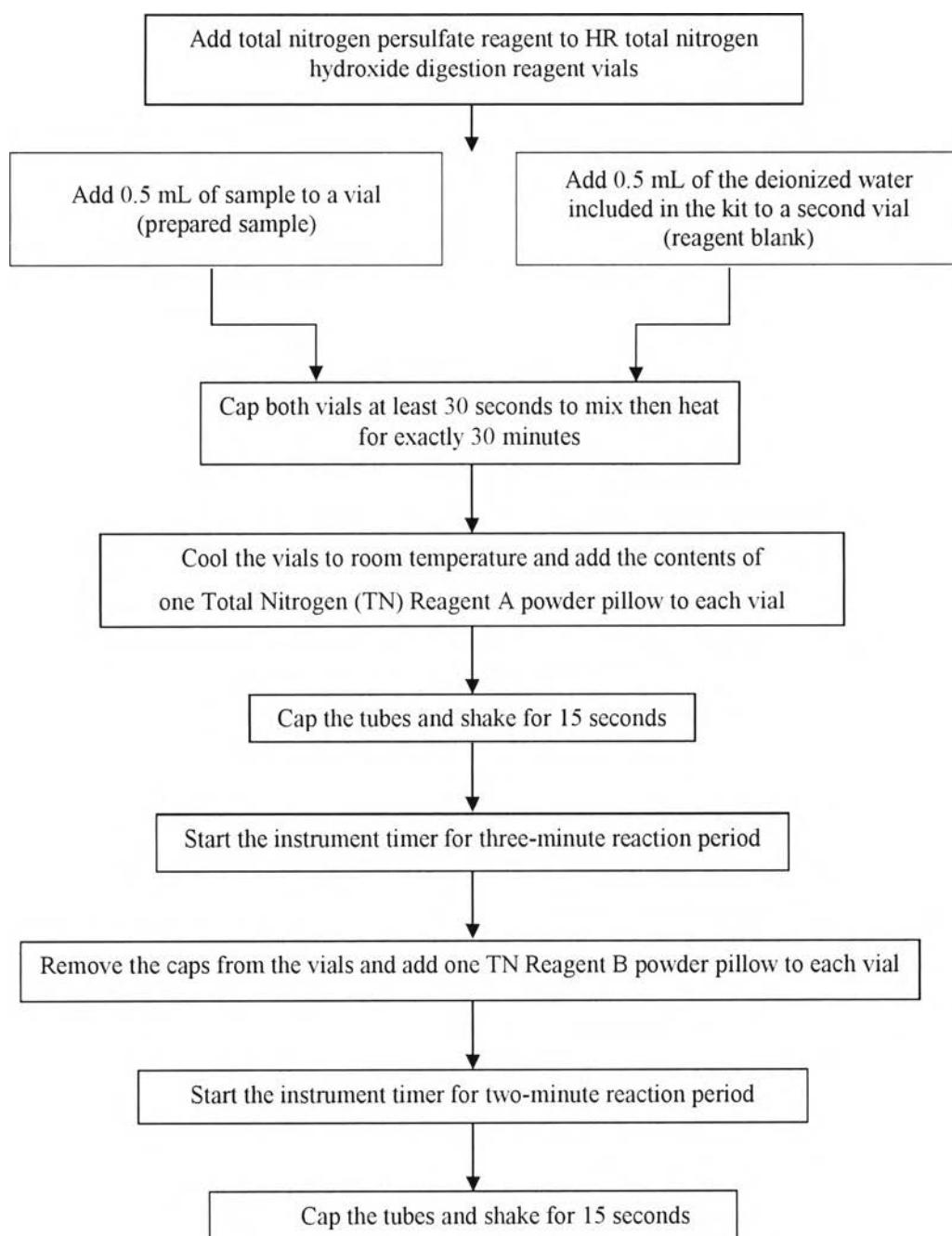


Figure D2 Procedure for analyzing amount of nitrogen.

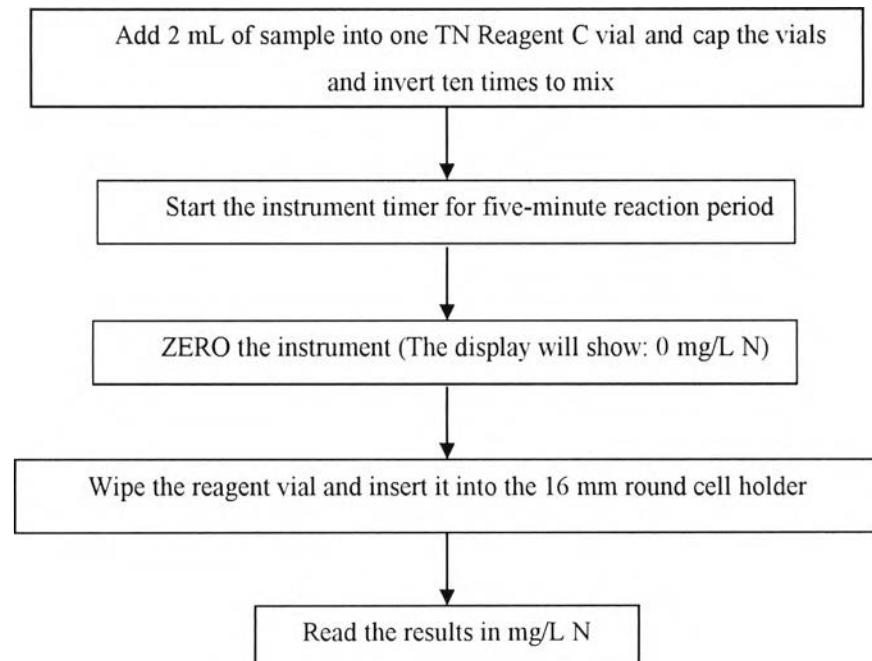


Figure D2 Procedure for analyzing amount of nitrogen (continued).

Appendix E Experiment Data of Hydrolysis

Table E1 Glucose produced from the hydrolysis of 40–60 mesh corncob using the bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	94161	0.344
1	82901	0.303
2	78151	0.285
3	75478	0.276
4	89106	0.325
5	97523	0.356
6	105926	0.387
8	107257	0.392
10	96622	0.353
12	79008	0.289
16	59124	0.216
20	51846	0.189
24	32039	0.117

Table E2 Glucose produced from the hydrolysis of 60–80 mesh corncob using the bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	92600	0.338
1	83520	0.305
2	88038	0.322
3	97925	0.358
4	104563	0.382
5	124302	0.454
6	131861	0.482
8	131979	0.482
10	118773	0.434
12	97189	0.355
16	74057	0.270
20	59411	0.217
24	31663	0.116

Table E3 Glucose produced from the hydrolysis of 80–100 mesh corncob using the bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	93380	0.341
1	22617	0.083
2	48551	0.177
3	97709	0.357
4	121240	0.443
5	141984	0.519
6	165975	0.606
8	130857	0.478
10	107941	0.394
12	77031	0.281
16	13063	0.048
20	12850	0.047
24	13849	0.051

Table E4 Glucose produced from the hydrolysis of 40–60 mesh corncob using the bacterial strain M 015 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	102361	0.374
1	91097	0.333
2	86275	0.315
3	85746	0.313
4	87061	0.318
5	84585	0.309
6	97794	0.357
8	104094	0.380
10	113949	0.416
12	103497	0.378
16	103141	0.377
20	91143	0.333
24	60709	0.222

Table E5 Glucose produced from the hydrolysis of 60–80 mesh corncob using the bacterial strain M 015 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	101255	0.370
1	89599	0.327
2	91335	0.334
3	103128	0.377
4	104250	0.381
5	102996	0.376
6	107161	0.391
8	114012	0.416
10	118160	0.432
12	107503	0.393
16	105515	0.385
20	77327	0.282
24	57120	0.209

Table E6 Glucose produced from the hydrolysis of 80–100 mesh corncob using the bacterial strain M 015 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	111323	0.407
1	90886	0.332
2	107221	0.392
3	110414	0.403
4	109486	0.400
5	112719	0.412
6	120857	0.441
8	125769	0.459
10	106723	0.390
12	107547	0.393
16	100179	0.366
20	81812	0.299
24	61566	0.225

Table E7 Glucose produced from the hydrolysis of 80–100 mesh corncob using malt extract loading 12 g/L and bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	94051	0.343
1	47470	0.173
2	34637	0.127
3	80681	0.295
4	85262	0.311
5	111717	0.408
6	219508	0.802
8	133258	0.487
10	140588	0.513
12	130418	0.476
14	100965	0.369
16	87803	0.321
20	88868	0.325
24	87304	0.319

Table E8 Glucose produced from the hydrolysis of 80–100 mesh corncob using malt extract loading 10 g/L and bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	71193	0.260
1	33753	0.123
2	23873	0.087
3	54836	0.200
4	59781	0.218
5	79599	0.291
6	176008	0.643
8	111416	0.407
10	117070	0.428
12	107854	0.394
14	81798	0.299
16	67297	0.246
20	65679	0.240
24	64277	0.235

Table E9 Glucose produced from the hydrolysis of 80–100 mesh corncob using malt extract loading 8 g/L and bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	54160	0.198
1	28821	0.105
2	23873	0.087
3	46895	0.171
4	61249	0.224
5	78438	0.286
6	131429	0.480
8	109524	0.400
10	99861	0.365
12	84810	0.310
14	67250	0.246
16	60266	0.220
20	55438	0.202
24	55786	0.204

Table E10 Glucose produced from the hydrolysis of 80–100 mesh corncob using malt extract loading 6 g/L and bacterial strain A 002 at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	35656	0.130
1	29571	0.108
2	19397	0.071
3	61336	0.224
4	72198	0.264
5	85453	0.312
6	113823	0.416
8	93005	0.340
10	57032	0.208
12	48366	0.177
14	42361	0.155
16	36189	0.132
20	35560	0.130
24	34429	0.126

Table E11 Glucose produced from the enzymatic hydrolysis of 80–100 mesh corncob using 100 U cellulase enzyme loading at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	0	0.000
2	9663	0.035
4	17532	0.064
6	23427	0.086
8	27696	0.101
10	31836	0.116
12	36053	0.132
24	49603	0.181
48	63779	0.233
72	69871	0.255

Table E12 Glucose produced from the enzymatic hydrolysis of 80–100 mesh corncob using 200 U cellulase enzyme loading at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	0	0.000
2	17674	0.065
4	33150	0.121
6	45734	0.167
8	57207	0.209
10	66476	0.243
12	72190	0.264
24	98287	0.359
48	119173	0.435
72	129841	0.474

Table E13 Glucose produced from the enzymatic hydrolysis of 80–100 mesh corncob using 300 U cellulase enzyme loading at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	0	0.000
2	21119	0.077
4	46466	0.170
6	64069	0.234
8	81787	0.299
10	92047	0.336
12	102441	0.374
24	136878	0.500
48	163300	0.596
72	181197	0.662

Table E14 Glucose produced from the enzymatic hydrolysis of 80–100 mesh corncob using 400 U cellulase enzyme loading at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	0	0.000
2	25201	0.092
4	57103	0.209
6	78230	0.286
8	97170	0.355
10	112736	0.412
12	119159	0.435
24	154018	0.563
48	182054	0.665
72	199410	0.728

Table E15 Glucose produced from the enzymatic hydrolysis of 80–100 mesh corncob using 500 U cellulase enzyme loading at 37 °C.

Time (h)	Glucose	
	Area	Concentration (g/L)
0	0	0.000
2	25527	0.093
4	61123	0.223
6	83309	0.304
8	102514	0.374
10	118133	0.431
12	129134	0.472
24	166222	0.607
48	200445	0.732
72	220759	0.806

Table E16 Bacteria evolution from the hydrolysis of 80–100 mesh corncob with the bacterial strain A 002 at 37 °C.

Time (h)	Nitrogen bacteria (g/L)	Bacterial (g/L)
0	0.062	0.55
3	0.085	0.75
6	0.088	0.78
8	0.087	0.77
10	0.094	0.83
12	0.096	0.85
16	0.111	0.98
20	0.123	1.09
24	0.172	1.53

Table E17 Bacteria evolution from the hydrolysis of 80–100 mesh corncob with the bacterial strain M 015 at 37 °C.

Time (h)	Nitrogen bacteria (g/L)	Bacterial (g/L)
0	0.089	0.79
3	0.090	0.80
6	0.092	0.82
8	0.100	0.89
10	0.102	0.91
12	0.109	0.97
16	0.110	0.98
20	0.112	0.99
24	0.145	1.29

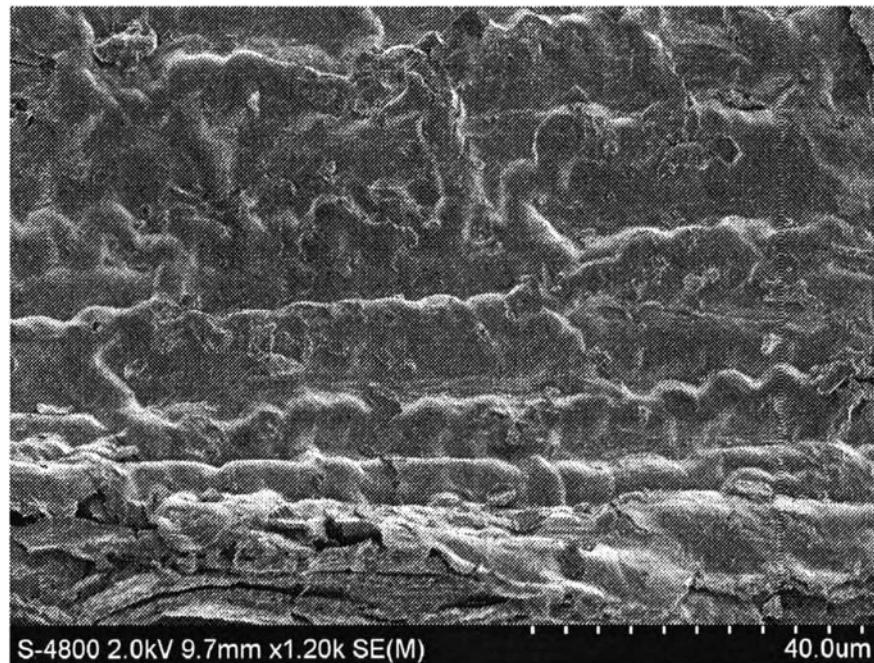
Appendix F SEM images of before and after hydrolysis of corncob

Figure F1 Scanning electron micrographs of the corncob surface before hydrolysis.

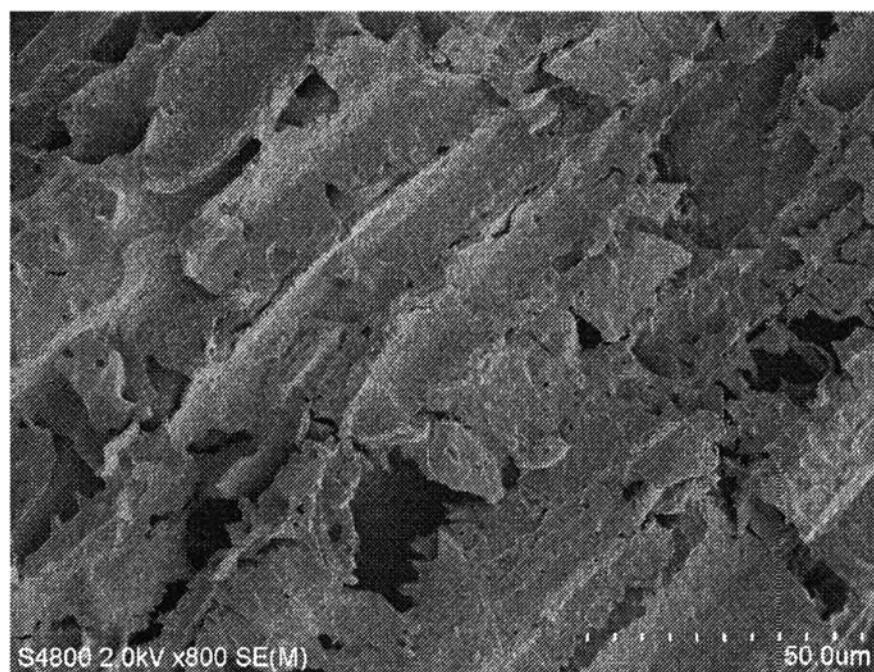


Figure F2 Scanning electron micrographs of the 60–80 mesh corncob surface after hydrolysis using strain A 002 at 37 °C.

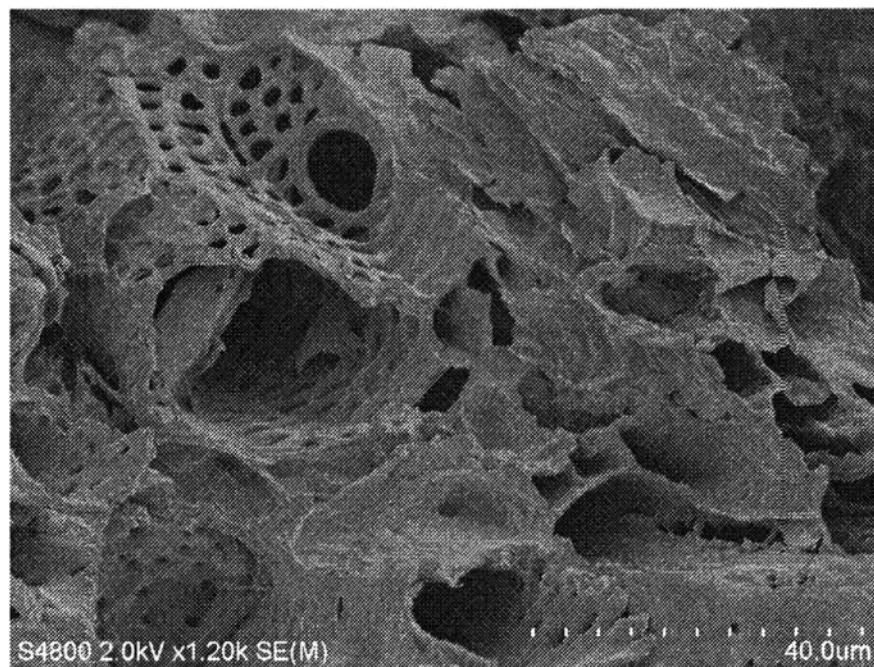


Figure F3 Scanning electron micrographs of the 80–100 mesh corncob surface after hydrolysis using strain A 002 at 37 °C.

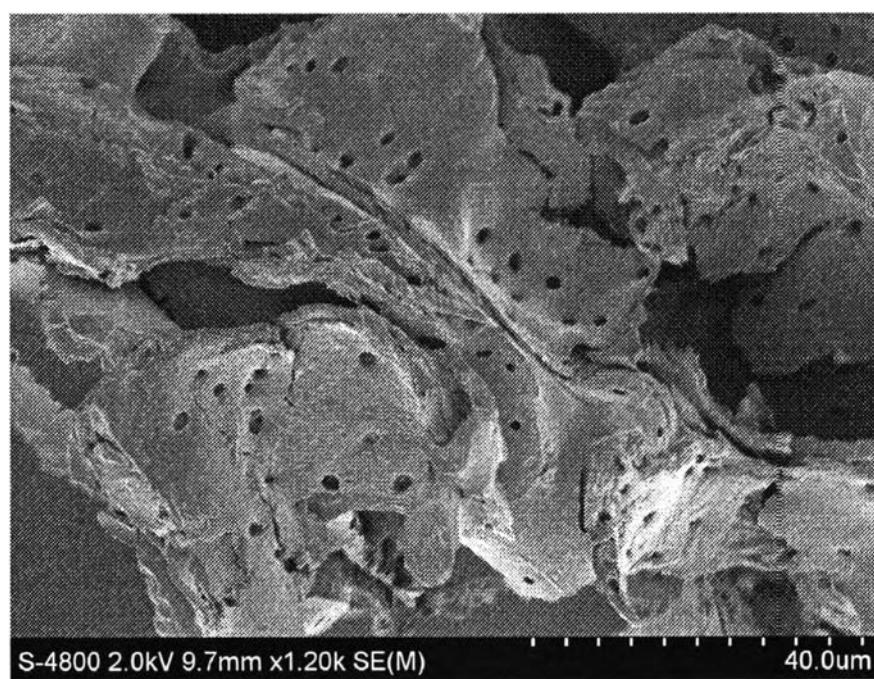


Figure F4 Scanning electron micrographs of the 80–100 mesh corncob surface after hydrolysis using strain M 015 at 37 °C.

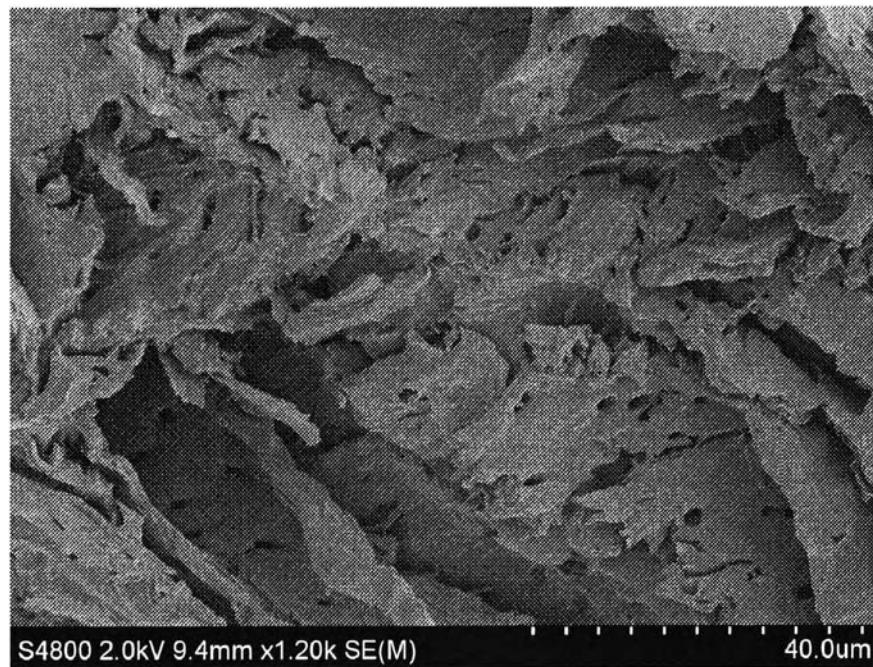


Figure F5 Scanning electron micrographs of the 80–100 mesh corncob surface after enzymatic hydrolysis using 100 U cellulase enzyme loading at 37 °C.

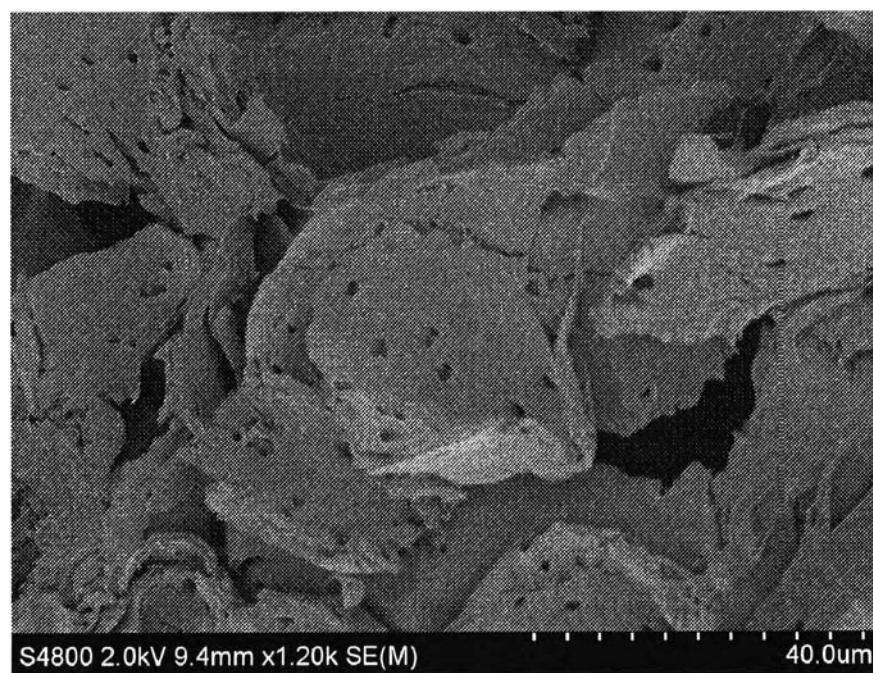


Figure F6 Scanning electron micrographs of the 80–100 mesh corncob surface after enzymatic hydrolysis using 300 U cellulase enzyme loading at 37 °C.

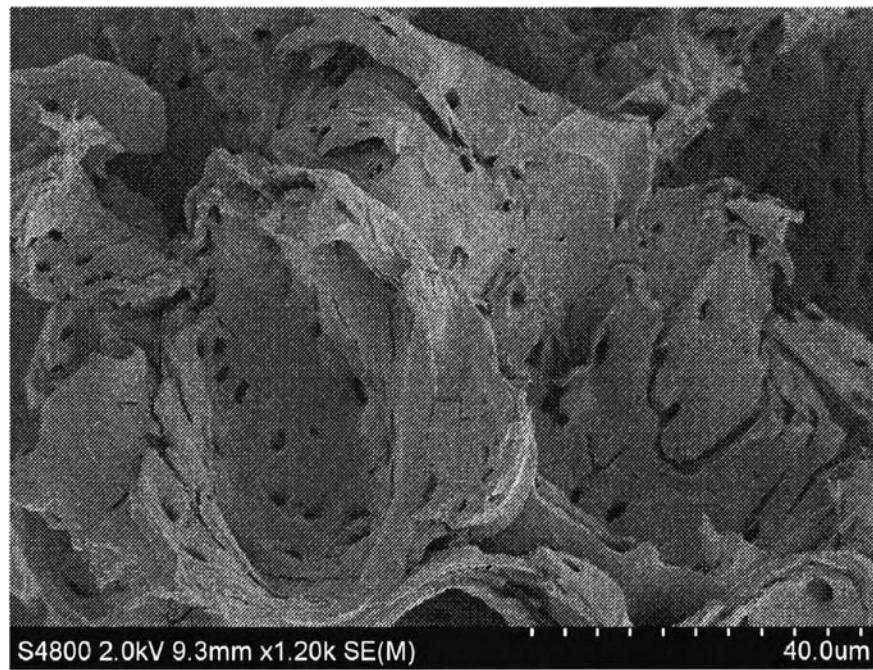


Figure F7 Scanning electron micrographs of the 80–100 mesh corncob surface after enzymatic hydrolysis using 500 U cellulase enzyme loading at 37 °C.

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1. Hokittikul, N., Rangsuvigit, P., and Chavadej, S., (2013, May 12-16) Glucose Production from Corncob by Microbial Hydrolysis. Poster presentation of 2th International Conference on Materials for Energy EnMat II, Karlsruhe, Germany.
2. Hokittikul, N., Rangsuvigit, P., and Chavadej, S., (2013, April 23) Glucose Production from Corncob by Microbial Hydrolysis Using Bacteria Isolated from Thai Higher Termites. Proceedings of The 4th Research Symposium on Petrochemical and Materials Technology and The 19th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.