

REFERENCES

- (1) N. Pasquini. Polypropylene Handbook Hanser Publishers, Munich, 2nd ed. (2005)
- (2) T. Garoff, U. Palmqvist, M. Sutela, P. Waldvogel, A. Kostianen. Procatalyst for ethylene polymer production method for its preparation and use. U.S. Pat., 5,770,540. 1998.
- (3) R. Jamjah, G. H. Zohuri, J. Ahmadjo, M. Nekomanesh, M. Pouryari. Morphological study of spherical $MgCl_2 \cdot nEtOH$ supported $TiCl_4$ Ziegler-Natta catalyst for polymerization of ethylene. J. Appl. Polym. Sci. 101 (2006): 3829-3834.
- (4) M. Chang, X. Liu, P.J. Nelson, G.R. Munzing, T.A. Gegan, Y. V. Kissin. Ziegler-Natta catalysts for propylene polymerization: Morphology and crystal structure of fourth-generation catalyst. J. Cat. 239 (2006): 347-353.
- (5) Z-Y. Ye, L. Wang, L-F. Feng, X-P. Gu, H-H. Chen, P-Y. Zhang. Novel spherical Ziegler-Natta catalyst for polymerization and copolymerization. I. Spherical $MgCl_2$ support. J. Polym. Sci., Part A: Polym. Chem. 40(2002): 3112-3119.
- (6) L. Wang, H-J. YU, Z-L. Ma, Z-Y. Ye, S. Jiang, L-F. Feng, X-P. Gu. Preparation of novel $MgCl_2$ -adduct supported spherical Ziegler-Natta for α -olefin polymerization. J. Appl. Polym. Sci. 99 (2006): 945-948.
- (7) B. L. Goodall. A. A Van der Nat, W. Sgardijn. Olefin polymerization catalyst compositions and a process for the polymerization of olefins employing such compositions. U.S. Pat., 4,414,132, 1983.
- (8) B. Diedrich, K. D. Keil. Process for the polymerization of olefins. U.S. Pat., 3,644,318, 1972
- (9) Hoechst Aktiengesellschaft. THS/G catalyst. W/O 91/1834, 1991.
- (10) K-K. Kang, K-S. Kim, D-H. Lee, Y-T. Jeong. Propylene polymerization by using $TiCl_4$ catalyst supported on solvent-activated $Mg(OEt)_2$. J. Appl. Polym. Sci. 81(2001): 460-467.
- (11) C. Vasile.; Handbook of Polyolefins: Synthesis and properties Marcel Dekker Inc, New York, editor in chief (1993).
- (12) C. Jenny, P. Maddox. Supported polyolefin catalysts. J. Solid State & Mater. Sci. 3 (1998): 94-103.

- (13) Z. Zhu, M. Chang, C. J. Aarons. High activity and good hydrogen response Ziegler-Natta polyethylene catalyst. U.S. Pat., 7153803B2, 2006.
- (14) R. A. Meyers. Handbook of Petrochemicals production process McGraw Hill, New York, editor in chief. (2005).
- (15) R. C. Job. Olefin polymerization catalyst component. U.S. Pat., 4,710,482, 1987.
- (16) S. M. Nestlerode, K. G. Burstain, R. C. Job. Olefin polymerization catalyst composition. U.S. Pat., 4,728,705, 1988.
- (17) S. A. Cohen, N. M. Karayannis, J. A. Streeky, B. S. Tovrog. Olefin polymerization and copolymerization process. U.S. Pat., 5,218,052, 1993.
- (18) H. Rauleder, B. Standke, H-J Kotsch, R. Schork. Storage-stable solution of a mixture of carbonated magnesium methoxide, carbonated magnesium ethoxide and their carbonated mixed alkoxide in a combination of methanol and ethanol and uses thereof. U.S. Pat., 5,468,706, 1995.
- (19) G. G. Arzoumanidis, S. S. Lee. Magnesium hydrocarbyl carbonate supports. U.S. Pat., 4,540,679, 1985.
- (20) R. C. Job. Olefin polymerization catalyst. U.S. Pat., 5,281,567, 1994.
- (21) H. Rauleder, B. Standke, H-J Kotsch, R. Schork. Storage-stable solution of carbonated magnesium ethylate in ethanol and their preparation and use. U.S. Pat., 5,456,801, 1995.
- (22) B. E. Wagner, D. P. Zilker, Jr, R. J. Jorgensen. Shape-Shifted magnesium alkoxide component for polymerizing olefins. U.S. Pat., 5,604,172, 1993.
- (23) S. S. Lee, M. K. Trost, S. A. Cohen. Morphology controlled olefin polymerization catalyst form an emulsion. U.S. Pat., 5,953,966, 1999.
- (24) N. M. Karayannis, S. A. Cohen, J. L. Ledermann. Olefin polymerization and copolymerization catalyst. U.S. Pat., 6,051,524, 2000.
- (25) D. B. Morse. Process for preparing olefin polymerization catalyst mixture. U.S. Pat., 6,429,270, 2002.
- (26) E. S. Shamshoum, C. G. Bauch, D.J. Rauscher. Polyolefin catalyst for polymerization of propylene and a method of making and using thereof. U.S. Pat., 5,849,665, 1998.
- (27) R. C. Job. Methods of making magnesium / transition metal alkoxide complexes and polymerization catalysts made therefrom. U.S. Pat., 6,511,935, 2003.

- (28) Y-P. Chen, Z-Q. Fan, J-H. Liao, S-Q Liao. Molecular weight distribution of polyethylene catalyzed by Ziegler-Natta catalyst supported on $MgCl_2$ doped with $AlCl_3$. J. Appl. Polym. Sci. 102 (2006): 1768- 1772.
- (29) J-C. Chien, J-C. Wu, C-I. Kuo. Magnesium chloride support high mileage catalyst for olefin polymerization. I. Chemical composition and oxidation state of titanium J. Polym. Sci., Polym. Chem. 20 (1982): 2019-2032.
- (30) C. R. Wolf, M. M. Forte, J. Z. Santos. Characterization of nature of chemical species of heterogeneous Ziegler-Natta catalysts for production of HDPE. J. Catalysis Today. 107-108 (2005): 451-457.
- (31) A. Adoni, J. C. Chadwick, H-J. W. Niemantsverdict, P. C. Thune. The role of electron donors on the lateral surfaces of $MgCl_2$ -supported Ziegler-Natta catalysts: observation by AFM and SEM. J. Cat. 257 (2008):81-86.
- (32) A. G. Potapov, G. D. Bukatov, V. A. Zakharov. DRIFT study of internal donors in supported Ziegler-Natta catalysts. J. Molecular Catalysis A: Chemical. 246 (2006) : 248-254.
- (33) M. A. S. Costa, R. A. Pereira. F. M. B. Coutinho. Effect of di-n-butyl ether on the synthesis of Ziegler-Natta catalyst for propylene polymerization. Eur. Polym. J. 35 (1999): 1327-1333.
- (34) J. Berthold, B. Diedrich, R. Franke, J. Hartlapp, W. Schafer, W. Strobel. Process for the preparation of polyolefin and a catalyst for this process. U.S. Pat., 4,447,587, 2003.

APPENDICES

APPENDIX A

Table A-1. Properties of catalysts at different Al₂Et₃Cl₃/Mg molar ratios

(Ti:Mg molar ratio = 3:1).

Item	Ex.1		Ex.2		Ex.3		Ex.4		Ex.5	
EASC: Mg molar ratio	0.0625		0.125		0.25		0.5		1	
% Preactivation (Ti ⁺³ :Ti total)	-		-		-		-		47.5	
Ratio (Mg:Ti:Cl)	1: 0.11 :2.30		1 : 0.09 :2.38		1: 0.07 :2.21		1 : 0.07:2.38		1: 0.39 :3.36	
%Ti (w/w)	2.0		2.9		2.6		2.4		4.8	
%Mg (w/w)	20.3		16.5		17.8		20.7		9.6	
%Cl (w/w)	65.8		65.2		65.5		68.8		38.3	
APS (μm)	9.3		10.7		8.8		7.0		13.6	
PSD	1.4		3.2		2.6		2.6		7.1	
Polymerization	H ₂ feeding		H ₂ feeding		H ₂ feeding		H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar
Yield (kgPE/mmol Ti)	6.4	4.7	15.3	10.1	16.7	8.8	40.0	23.4	10.1	5.0
Yield (kgPE /g cat)	6.7	4.9	9.3	6.1	9.1	4.8	20.1	14.7	10.2	5.0
Melt flow properties										
MFI _{2.16} (g/10 min)	0.88	8.90	0.80	10.5	0.85	12.0	1.05	10.7	1.25	10.7
MFI ₅ (g/10 min)	1.62	25.7	1.50	21.1	1.63	26.2	1.98	20.8	2.72	20.7
MFI _{21.6} (g/10 min)	17.2	270	15.2	202	15.4	294	11.2	206	27.5	216
MFR (MFI _{21.6} / MFI ₅)	10.6	10.5	10.1	9.6	9.4	11.2	8.8	9.9	10.1	10.4
APS (μm)	129	94	108	110	101	90	100	97	120	110
Bulk density (g/cm ³)	0.37	0.33	0.30	0.31	0.35	0.35	0.33	0.34	0.32	0.31

Table A-2. Properties and activities of catalysts at different Ti: Mg molar ratios
(Al₂Et₃Cl₃: Mg molar ratio = 0.5:1 and agitation speed = 400 rpm)

Item	Ex. 6	Ex.4	Ex. 7	Ex.8				
Ti:Mg molar ratio	2	3	4	5				
Ratio(Mg:Ti:Cl)	1 : 0.04 : 2.28	1 : 0.07 : 2.38	1 : 0.09: 2.36	1 : 0.10 :3.39				
%Ti (w/w)	0.5	2.4	2.8	2.8				
%Mg (w/w)	22.6	20.7	21.8	22.4				
%Cl (w/w)	70.2	68.8	66.6	69.5				
APS (μ m)	7.4	7.0	5.0	5.6				
PSD	1.8	2.6	2.5	5.8				
POLYMERIZATION								
	H ₂ feeding		H ₂ feeding		H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar
Yield (kg PE/mmol Ti)	2.6	None reacted	40.0	23.4	19.7	14.4	4.5	2.5
Yield (kg PE /g cat)	0.27		20.1	14.7	11.5	8.4	2.6	1.5
Melt flow properties								
MFI _{2.16} (g/10 min)	1.05	-	1.05	10.7	1.93	9.42	1.85	5.43
MFI ₅ (g/10 min)	0.26		1.86	11.75	3.51	28.4	3.82	10.7
MFI _{21.6} (g/10 min)	2.66		17.7	143	35.2	310	38.5	112
MFR(MFI _{21.6} / MFI ₅)	10.4		9.5	12.1	10.0	10.9	10.1	10.5
APS (μ m)	96		100	97	80	83	74	62
Bulk density (g/cm ³)	0.26		0.33	0.34	0.20	0.19	0.18	0.16

Table A-3. Properties and activities of catalysts at different numbers of titanation (Ti:Mg molar ratio = 3:1, Al₂Et₃Cl₃:Mg molar ratio = 0.5:1, and agitation speed = 400 rpm)

Item	Ex.4		Ex.9		Ex.10	
number of titanation	1		2		3	
Ratio (Mg:Ti:Cl)	1 : 0.07 : 2.38		1: 0.15: 2.57		1: 0.16 : 2.48	
%Ti (w/w)	2.4		3.3		3.4	
%Mg (w/w)	20.7		16.8		17.2	
%Cl (w/w)	68.8		65.3		63.5	
APS (μm)	7.0		10.0		10.4	
PSD	2.6		2.5		2.7	
POLYMERIZATION	H ₂ feeding		H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar
Yield (kgPE/mmol Ti)	40.0	23.5	28.4	15.0	13.5	8.5
Yield (kgPE /g cat)	20.1	11.7	19.5	10.3	9.6	6.0
Melt flow properties						
MFI _{2.16} (g/10 min)	1.10	19.2	1.08	14.5	1.13	15.8
MFI ₅ (g/10 min)	1.86	20.8	1.9	16.8	1.85	17
MFI _{21.6} (g/10 min)	17.7	206	18.6	163	17.9	168
MFR(MFI _{21.6} / MFI ₅)	9.5	9.9	9.8	9.7	9.7	9.9
APS (μm)	100	97	130	111	120	105
Bulk density (g/cm ³)	0.32	0.34	0.31	0.30	0.32	0.30

Table A-4. Properties and activities of catalysts at different treatment time.

(Ti:Mg molar ratio = 3:1, Al₂Et₃Cl₃:Mg molar ratio = 0.5:1, agitation speed = 400 rpm, and treatment temperature = 110°C)

Item	Ex.11	Ex.4	Ex.12	Ex.13				
Treatment (h)	0	2	5	10				
Ratio (Mg:Ti:Cl)	1:0.05:2.27	1:0.07:2.38	1:0.12:2.61	1:0.12:2.54				
%Ti (w/w)	1.8	2.4	2.6	2.6				
%Mg (w/w)	19.0	20.7	19.8	25.2				
%Cl (w/w)	66.0	68.8	60.5	63.7				
APS (μm)	17.6	7.0	16.1	21.7				
PSD	2.4	2.6	2.0	2.5				
POLYMERIZATION	H ₂ feeding		H ₂ feeding		H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar
Yield (kgPE/mmol Ti)	7.7	6.8	40.0	23.4	18.0	10.0	16.5	8.6
Yield (kgPE /g cat)	2.9	2.5	20.1	14.7	9.8	5.4	8.6	4.4
Melt flow properties								
MFI _{2.16} (g/10 min)	1.6	8.1	1.1	9.5	0.4	2.3	0.3	2
MFI ₅ (g/10 min)	1.13	20.1	1.86	20.8	0.85	6.08	0.67	5.8
MFI _{21.6} (g/10 min)	11.54	212.6	17.7	142.7	2.28	31.5	6.8	57.8
MFR (MFI _{21.6} MFI ₅)	10.2	10.6	9.5	12.1	11.3	10.4	10.1	9.9
APS (μm)	120	81	100	97	93	79	112	68
Bulk density (g/cm ³)	0.33	0.30	0.33	0.34	0.23	0.23	0.19	0.28
AB	4.8		3.1		1.3		1.3	

AB = [average CA x log[(MFI₂/MFI₂)]/|ΔCA|: where, MFI₂* = melt flow index at H₂ pressure = 3 bar, MFI₂ = melt flow index at H₂ pressure = 1 bar, CA = catalyst activity

Table A-5. Properties and activities of catalysts with ethyl benzoate (EB) addition (Ti:Mg molar ratio = 3:1, Al₂Et₃Cl₃:Mg molar ratio = 0.5:1, agitation speed = 400 rpm, treatment temperature = 110°C and treatment time = 2 h).

Item	Ex. 4		Ex.14		Ex. 15		Ex. 16	
EB : Mg molar ratio	0		0.06		0.12		0.25	
Ratio (Mg:Ti:Cl)	1: 0.07: 3.32		1: 0.06: 3.58		1: 0.05: 3.50		1: 0.05 :4.96	
%Ti (w/w)	2.4		2.2		2.1		1.3	
%Mg (w/w)	20.7		19		18.6		13	
%Cl (w/w)	68.8		68		65.1		64.5	
APS (μm)	11.9		13.5		13.1		12.1	
PSD	1.7		1.6		1.8		1.7	
POLYMERIZATION	H ₂ feeding		H ₂ feeding		H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar
Yield (kgPE/mmol Ti)	40.0	29.4	22.5	18.5	17.7	15.0	17.5	6.5
Yield (kgPE /g cat)	20.1	14.7	11.5	9.2	9.5	8.3	4.8	1.8
Melt flow properties								
MFI _{2.16} (g/10 min)	1.05	9.5	1.56	10.5	1.86	12.3	2.00	20.1
MFI ₅ (g/10 min)	1.86	20.8	3.15	22.8	3.99	25.4	4.62	43.8
MFI _{21.6} (g/10 min)	none	none	none	none	none	none	none	none
MFR (MFI _{21.6} / MFI ₅)	none	none	none	none	none	none	none	none
APS (μm)	133	108	130	100	129	105	135	97
Bulk density (g/cm ³)	0.33	0.34	0.34	0.32	0.35	0.33	0.33	0.34
AB	3.1		3.7		6.1		1.1	

AB = [average CA x log[(MFI₂/MFI₂)]/|ΔCA|: where, MFI₂* = melt flow index at H₂ pressure = 3 bar, MFI₂ = melt flow index at H₂ pressure = 1 bar, CA = catalyst activity

Table A-6. Properties and activities of catalysts with ethyl benzoate (EB) addition by varying the aging time ($\text{Al}_2\text{Et}_3\text{Cl}_3$:Mg molar ratio = 0.5:1, Ti:Mg molar ratio = 3:1, EB:Mg molar ratio = 0.12:1, treatment temperature = 110°C but aging time was varied for 2, 5, and 10 h)

Item	Ex. 15		Ex. 17		Ex. 18	
Aging time (h)	2		5		10	
Ratio (Mg:Ti:Cl)	1:0.05:3.50		1:0.07:3.60		1:0.12:3.65	
%Ti (w/w)	2.1		2.8		3.2	
%Mg (w/w)	18.6		18.0		17.6	
%Cl (w/w)	65.1		64.5		63.8	
APS (μm)	13.1		12.5		14.0	
PSD	1.8		2.0		2.3	
POLYMERIZATION	H ₂ feeding		H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar	1 bar	3 bar
Yield (kgPE/mmol Ti)	17.7	15.0	25.5	22.6	29.5	25.5
Yield (kgPE /g cat)	9.5	8.3	15.0	13.2	17.3	15.0
Melt flow properties						
MFI _{2.16} (g/10 min)	1.86	12.3	1.30	10.5	0.98	10.3
MFI ₅ (g/10 min)	3.99	25.4	3.00	24.5	3.12	27.4
MFI _{21.6} (g/10 min)	none	none	none	none	none	ncne
MFR (MFI _{21.6} / MFI ₅)	none	none	none	none	none	none
APS (μm)	129	105	133	98	135	105
Bulk density (g/cm ³)	0.35	0.33	0.33	0.32	0.35	0.33
AB	6.1		7.1		7.2	

AB = [average CA x log[(MFI₂/MFI₂)]/| Δ CA|: where, MFI₂* = melt flow index at H₂ pressure = 3 bar, MFI₂ = melt flow index at H₂ pressure =1 bar. CA = catalyst activity

Table A-7. Properties and activities of catalyst with dicyclopentylmethoxysilane (DCPDMS) addition (Ti:Mg molar ratio = 3:1, Al₂Et₃Cl₃: Mg molar ratio = 0.5:1, and agitation speed = 400 rpm, EB:Mg molar ratio = 0.12:1, treatment temperature 110°C, treatment time = 10 h)

Item	Ex. 18		Ex.19	
DCPDMS:Mg molar ratio	0		0.25	
Ratio (Mg:Ti:Cl)	1:0.12:3.65		1:0.07:3.45	
%Ti (w/w)	3.2		2.4	
%Mg (w/w)	17.6		19.5	
%Cl (w/w)	63.8		64.8	
APS (μm)	14.0		33.5	
PSD	2.3		2.0	
POLYMERIZATION	H ₂ feeding		H ₂ feeding	
	1 bar	3 bar	1 bar	3 bar
Yield (kgPE/mmol Ti)	29.5	25.5	20.5	16.4
Yield (kgPE /g cat)	17.3	15.0	12.0	9.4
Melt flow properties				
MFI _{2.16} (g/10 min)	0.98	10.3	2.05	51.2
MFI ₅ (g/10 min)	3.12	27.4	5.10	115
MFI _{21.6} (g/10 min)	none	none	none	none
MFR (MFI _{21.6} / MFI ₅)	none	none	none	none
APS (μm)	135	105	260	200
Bulk density (g/cm ³)	0.35	0.33	0.36	0.35
AB	7.2		5.8	

AB = [average CA x log[(MFI₂/MFI₂)]/|ΔCA|: where, MFI₂* = melt flow index at H₂ pressure = 3 bar, MFI₂ = melt flow index at H₂ pressure = 1 bar. CA = catalyst activity

APPENDIX B

Distribution Plots

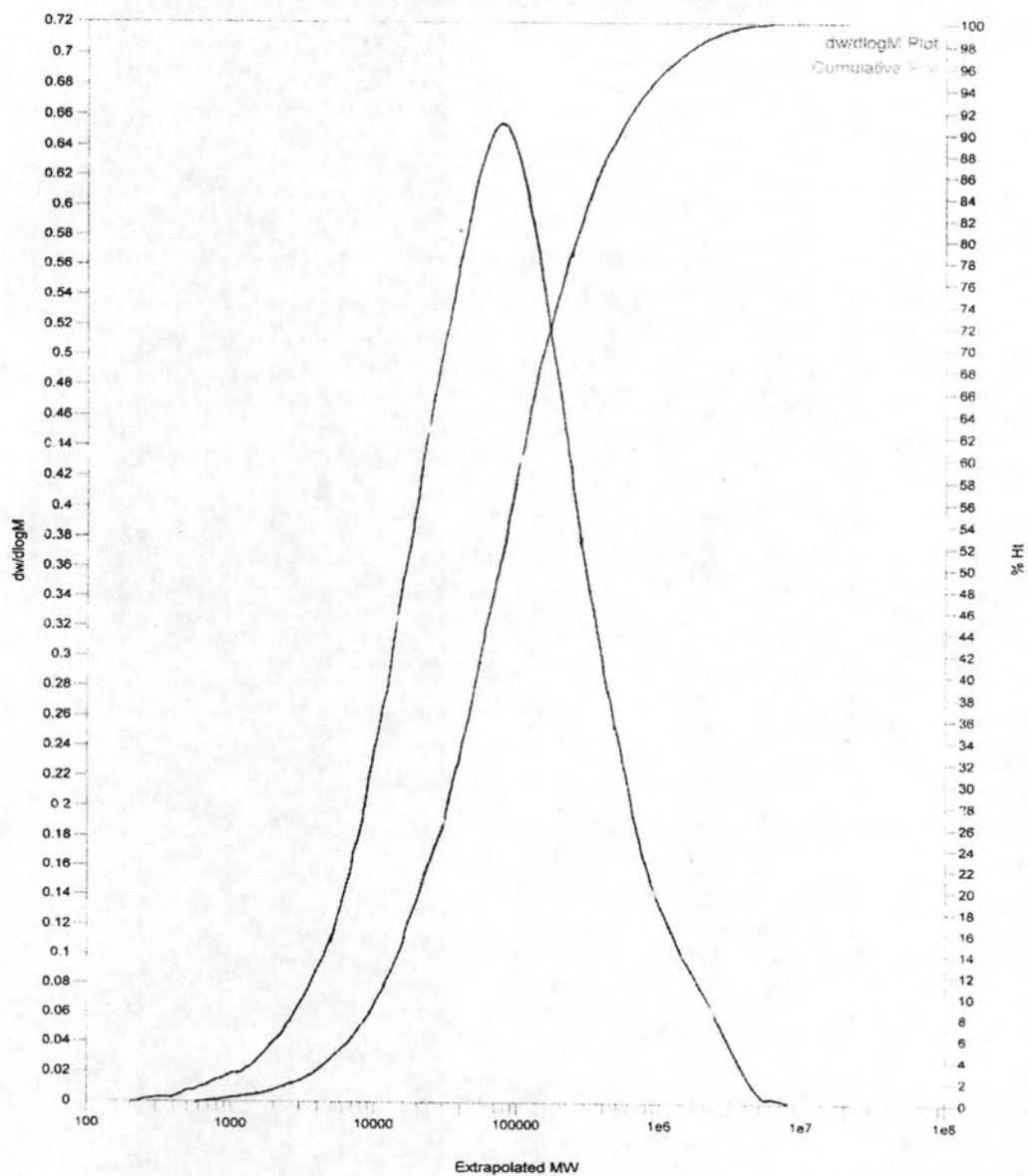


Figure B-1 GPC curve of PE obtained from the prepared catalyst.

VITA

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