

REFERENCES

- Bogaerts, A., Neyts, E., Gijbels, R., and Mullen, J. (2002). Gas discharge plasmas and their application. Spectrochimica Acta Part B, 57, 609-658.
- Chang, J., Lawless, P.A., Yamamoto, T. (1991). Corona discharge processes. IEEE Transactions on Plasma Science, 19, 1152-1166.
- Czernichowski, A. (1994). Gliding arc. Applications to engineering and environment control. Pure and Applied Chemistry, 66(6), 1301-1310.
- Fridman, A., Chirokov, A., and Gutsol, A. (2005) Non-thermal atmospheric pressure discharge. Journal of Physic D: Applied Physics, 38, R1-R24.
- Fridman, A., and Kennedy, L.A. (2004). Plasma Physics and Engineering. New York: Taylor & Francis Books.
- Fridman, A., Nester, S., Kennedy, L.A., Saveliev, A., and Mutaf-Yardimici, O. (1999). Gliding arc gas discharge. Progress in Energy and Combustion Science, 25, 211-231.
- Liu, C.J., Xu, C.-H., and Wang, T. (1999). Non-thermal plasma approaches in CO₂ utilization. Fuel Processing Technology, 58, 119-134.
- McTaggart, F.K. (1967). Plasma Chemistry in Electrical Discharges. Amsterdam: Elsevier Publishing Company.
- Mutaf-Yardimci, O., Savaliev, A.V., Fridman, A.A., and Kennedy, L.A. (1998). Employing plasma as catalyst in hydrogen production. International Journal of Hydrogen Energy, 23(2), 1109-1111.
- Nasser, E. (1971). Fundamentals of Gaseous Ionization and Plasma Electronics. USA: John Wiley & Sons.
- PTT Public Company Limited "Natural Gas Information." pttinternet.pttplc 14 Aug 2001. 12 Jan 2006
<http://pttinternet.pttplc.com/csc_gas/csc_ind/information/ngi_04.asp>
- Rojey, A., Jaffret, C., Cornot-Gandolphe, S., Durand, B., Jullian, S., and Valais, M. (1997). Natural Gas Production Processing Transport. Paris: Technip.
- Roth, J.R. (1995). Industrial Plasma Engineering Volume 1: Principles. UK: IOP Publishing.

- Vergara, W., Hay, N.E., and Hall, C.W. (1990). Natural Gas Its Role and Potential in Economic Development. Boulder: Westview Press.
- Victor, D.G., Jaffe, A.M., and Hayes, M.H. (2006). Natural Gas and Geopolitics From 1970 to 2040. Cambridge: Cambridge University Press.
- Wilkes, O.J. (1973). Gas Making & Natural Gas. London: BP Trading.
- Xu, X. (2001). Dielectric barrier discharge — properties and applications. Thin Solid Films, 390, 237-242.

APPENDICES

Appendix A Reforming of CO₂-Containing Natural Gas Using an AC Gliding Arc System: Effect of Gas Components in Natural Gas

Table A1 Effect of feed flow rate on CH₄ conversion and product yields of pure methane feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	CH ₄ conversion (%)	Product yield (%)	
		H ₂	C ₂
25	18.10	9.08	10.37
50	11.34	4.83	7.16
75	6.80	2.88	4.65
100	5.34	2.39	4.01
125	4.77	2.03	3.70
150	4.13	1.60	3.54

Table A2 Effect of feed flow rate on concentrations of outlet gas of pure methane feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Concentration of outlet gas (%)						
	CH ₄	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
25	73.95	16.39	1.83	1.40	1.46	0.05	0.10
50	84.32	9.19	1.15	1.02	1.07	0.03	0.07
75	90.55	5.59	0.78	0.80	0.69	0.02	0.05
100	92.01	4.65	0.62	0.73	0.61	0.02	0.04
125	92.02	3.91	0.55	0.69	0.55	0.01	0.03
150	93.34	3.11	0.45	0.63	0.64	0.01	0.03

Table A3 Effect of feed flow rate on product selectivities of pure methane feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Product selectivity (%)						Product molar ratio		
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀	H ₂ /C ₂	C ₂ H ₆ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
25	50.17	50.17	22.34	22.34	17.11	17.85	3.50	1.04	0.77
50	42.59	42.59	21.40	21.40	22.40	19.32	2.83	1.05	0.89
75	42.31	42.31	23.51	23.51	24.10	20.85	2.47	0.87	1.03
100	44.79	44.79	23.73	23.73	27.95	23.41	2.39	0.84	1.18
125	42.49	42.49	23.97	23.97	29.78	23.97	2.19	0.80	1.24
150	38.75	38.75	22.54	22.54	31.29	31.94	1.81	1.02	1.39

Table A4 Effect of feed flow rate on CH₄ conversion and product yields of methane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	CH ₄ conversion (%)	Product yield (%)	
		H ₂	C ₂
50	8.31	3.23	7.07
75	6.40	2.41	5.85
100	6.57	2.31	5.61
125	5.51	1.67	4.53
150	5.50	1.65	4.53

Table A5 Effect of feed flow rate on concentrations of outlet gas of methane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Concentration of outlet gas (%)						
	CH ₄	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
50	61.23	0.53	0.73	1.11	0.05	0.04	0.53
75	62.39	0.39	0.63	0.93	0.03	0.03	0.39
100	62.88	0.43	0.63	0.84	0.03	0.03	0.43
125	64.97	0.32	0.55	0.69	0.02	0.02	0.32
150	65.22	0.31	0.56	0.69	0.02	0.02	0.31

Table A6 Effect of feed flow rate on product selectivities of methane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Product selectivity (%)						Product molar ratio		
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀	H ₂ /C ₂	C ₂ H ₆ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
50	38.88	18.94	26.30	39.94	2.74	3.24	1.83	1.52	1.39
75	37.67	18.35	29.71	44.32	2.50	3.04	1.63	1.49	1.62
100	35.20	19.32	28.26	37.80	1.82	2.65	1.65	1.34	1.46
125	30.24	16.85	29.22	36.22	1.50	2.23	1.47	1.24	1.73
150	30.05	16.48	29.37	36.49	1.39	2.22	1.46	1.24	1.78

Table A7 Effect of feed flow rate on reactant conversions and product yields of methane/ethane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Reactant conversion (%)		Product yield (%)	
	CH ₄	C ₂ H ₆	H ₂	C ₂
50	9.43	20.28	13.07	16.85
75	7.46	19.62	10.08	13.76
100	5.72	18.02	8.67	12.73
125	5.08	13.11	6.26	11.40
150	4.24	7.30	4.28	7.63

Table A8 Effect of feed flow rate on concentrations of outlet gas of methane/ethane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Concentration of outlet gas (%)						
	CH ₄	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
50	58.49	6.60	0.99	1.27	3.70	0.09	0.08
75	60.80	4.70	0.70	1.03	3.86	0.07	0.06
100	62.76	3.72	0.57	0.91	3.91	0.06	0.05
125	63.47	3.07	0.49	0.84	4.01	0.05	0.04
150	63.66	2.43	0.39	0.74	3.88	0.04	0.03

Table A9 Effect of feed flow rate on product selectivities of methane/ethane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Product selectivity (%)					Product molar ratio		
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₃ H ₈	C ₄ H ₁₀	H ₂ /C ₂ H ₄	H ₂ /C ₂ H ₂	C ₂ H ₄ /C ₂ H ₂
50	43.98	24.79	31.93	3.23	4.16	5.18	6.68	1.29
75	37.22	20.50	30.31	2.93	3.50	4.57	6.76	1.48
100	36.52	20.59	33.05	3.01	3.48	4.08	6.54	1.61
125	34.41	20.10	35.51	3.01	3.44	3.61	6.38	1.77
150	37.06	22.90	43.21	3.31	3.85	3.28	6.19	1.89

Table A10 Effect of feed flow rate on reactant conversions and product yields of methane/ethane/propane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Reactant conversion (%)			Product yield (%)	
	CH ₄	C ₂ H ₆	C ₃ H ₈	H ₂	C ₂
75	9.23	21.90	41.54	16.92	24.98
100	7.61	17.05	34.97	14.42	22.18
125	6.64	10.91	30.43	11.50	19.27
150	5.26	8.18	24.59	9.52	16.74
175	4.38	7.83	21.39	8.01	14.76

Table A11 Effect of feed flow rate on concentrations of outlet gas of methane/ethane/propane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Concentration of outlet gas (%)						
	CH ₄	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
75	62.81	5.86	1.04	1.61	3.90	3.21	0.24
100	63.92	4.79	0.85	1.39	3.75	3.23	0.20
125	64.40	4.03	0.75	1.30	3.95	3.54	0.19
150	65.09	3.33	0.61	1.13	4.48	3.59	0.19
175	66.58	2.67	0.47	1.01	4.66	3.58	0.14

Table A12 Effect of feed flow rate on product selectivities of methane/ethane/propane/helium feed system at an applied voltage of 15.5 kV, a frequency of 200 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Product selectivity (%)				Product molar ratio		
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₄ H ₁₀	H ₂ /C ₂ H ₄	H ₂ /C ₂ H ₂	C ₂ H ₄ /C ₂ H ₂
50	23.29	13.50	20.88	6.34	3.64	5.63	1.55
75	24.18	14.14	23.06	6.78	3.45	5.63	1.63
100	23.96	14.77	25.40	7.44	3.11	5.35	1.72
125	25.04	15.15	27.74	9.24	2.96	5.43	1.83
150	23.85	13.98	29.96	8.30	2.63	5.64	2.14

Table A13 Effect of feed flow rate on reactant conversions and product yields of methane/ethane/propane/carbon dioxide feed system at an applied voltage of 15.5 kV, a frequency of 300 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Reactant conversion (%)				Product yield (%)	
	CH ₄	C ₂ H ₆	C ₃ H ₈	CO ₂	H ₂	C ₂
75	10.04	17.72	41.00	5.52	16.75	27.99
100	8.72	12.91	32.54	5.11	13.28	23.19
125	7.90	12.04	29.80	4.34	12.17	20.46
150	6.79	12.10	25.76	4.53	10.59	19.84
175	6.99	10.74	24.90	3.28	9.75	18.66
200	6.21	6.21	22.30	3.04	8.22	16.30

Table A14 Effect of feed flow rate on concentrations of outlet gas of methane/ethane/propane/carbon dioxide feed system at an applied voltage of 15.5 kV, a frequency of 300 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Concentration of outlet gas (%)								
	CH ₄	H ₂	CO	CO ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
75	61.34	6.02	0.47	17.54	1.16	1.65	4.14	3.00	0.22
100	62.48	5.11	0.39	17.71	1.02	1.42	4.59	3.56	0.18
125	64.66	4.51	0.34	17.76	0.88	1.27	4.62	3.60	0.15
150	65.36	3.92	0.30	17.90	0.81	1.17	4.66	3.65	0.14
175	65.11	3.76	0.29	18.25	0.83	1.15	4.69	3.73	0.14
200	65.44	3.40	0.25	18.33	0.71	1.14	4.80	4.14	0.14

Table A15 Effect of feed flow rate on product selectivities of methane/ethane/propane/carbon dioxide feed system at an applied voltage of 15.5 kV, a frequency of 300 Hz and an electrode gap distance of 6 mm

Feed flow rate (cm ³ /min)	Product selectivity (%)					Product molar ratio			
	H ₂	C ₂ H ₂	C ₂ H ₄	CO	C ₄ H ₁₀	H ₂ /CO	H ₂ /C ₂ H ₂	H ₂ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
75	24.36	15.57	22.11	2.97	5.83	12.75	5.19	3.66	3.66
100	24.52	16.35	22.76	2.90	5.90	13.12	5.01	3.60	3.60
125	24.47	16.11	23.37	2.90	5.59	13.26	5.14	3.54	3.54
150	23.72	16.49	23.85	2.84	5.59	12.90	4.83	3.34	3.34
175	22.88	17.03	23.62	2.80	5.73	12.96	4.54	3.27	3.27
200	23.66	16.54	26.63	2.74	6.47	13.64	4.82	2.99	2.99

Appendix B Reforming of CO₂-Containing Natural Gas Using an AC Gliding Arc System: Effects of Operational Parameters and Oxygen Addition in Feed

Table B1 Effect of applied voltage on reactant conversions and product yields of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, a frequency of 300 Hz and an electrode gap distance of 6 mm

Applied voltage (kV)	Reactant conversion (%)				Product yield (%)	
	CH ₄	C ₂ H ₆	C ₃ H ₈	CO ₂	H ₂	C ₂
12.5	5.55	1.92	10.17	23.76	10.73	18.69
13.5	5.94	4.19	12.73	25.81	11.83	21.23
15.5	7.90	4.34	12.04	29.80	12.68	22.16
17.5	7.99	5.79	19.05	32.20	16.32	26.23
19.5	8.00	4.67	24.83	39.82	24.01	33.46
21.5	16.30	9.53	34.00	45.98	27.75	35.32

Table B2 Effect of applied voltage on concentrations of outlet gas of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, a frequency of 300 Hz and an electrode gap distance of 6 mm

Applied voltage (kV)	Concentration of outlet gas (%)								
	CH ₄	H ₂	CO	CO ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
12.5	66.06	3.77	0.37	18.28	0.76	1.12	4.22	3.76	0.14
13.5	66.01	4.07	0.37	18.27	0.86	1.16	4.15	3.70	0.14
15.5	64.97	4.39	0.33	17.68	0.85	1.25	4.11	3.28	0.15
17.5	64.72	5.60	0.38	17.99	1.16	1.31	3.85	3.35	0.15
19.5	63.29	7.36	0.42	17.75	1.43	1.53	3.50	2.94	0.18
21.5	58.72	10.63	0.49	17.31	2.02	1.57	3.13	2.70	0.15

Table B3 Effect of applied voltage on product selectivities and product molar ratios of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, a frequency of 300 Hz and an electrode gap distance of 6 mm

Applied voltage (kV)	Product selectivity (%)					Product molar ratio			
	H ₂	C ₂ H ₂	C ₂ H ₄	CO	C ₄ H ₁₀	H ₂ /CO	H ₂ /C ₂ H ₂	H ₂ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
12.5	27.18	18.29	26.85	4.28	6.83	10.12	4.94	3.37	1.47
13.5	26.58	18.56	25.04	3.73	6.23	10.87	4.74	3.52	1.35
15.5	23.98	15.56	22.87	2.82	5.45	13.26	5.14	3.54	1.45
17.5	27.55	18.93	21.39	2.84	4.78	14.83	4.85	4.29	1.13
19.5	33.06	20.93	22.35	2.87	5.13	17.66	5.15	4.82	1.07
21.5	28.82	18.79	14.60	2.09	2.83	21.72	5.25	6.76	0.78

Table B4 Effect of applied voltage on specific energy consumption and current of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, a frequency of 300 Hz and an electrode gap distance of 6 mm

Applied voltage (kV)	Energy consumption (x10 ¹⁸ Ws per H ₂ molecule produced)	Energy consumption (x10 ¹⁸ Ws per reactant molecule converted)	Current (mA)
12.5	5.30	3.40	1.2308
13.5	5.42	3.22	1.3077
15.5	6.34	3.36	1.5385
17.5	5.13	3.11	2.0000
19.5	3.57	2.78	2.0000
21.5	2.34	1.45	1.8462

Table B5 Effect of input frequency on reactant conversions and product yields of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV and an electrode gap distance of 6 mm

Input frequency (Hz)	Reactant conversion (%)				Product yield (%)	
	CH ₄	C ₂ H ₆	C ₃ H ₈	CO ₂	H ₂	C ₂
250	9.16	24.96	37.35	4.51	25.21	33.67
300	7.99	19.05	32.20	5.79	16.32	26.23
400	6.87	13.17	26.01	4.14	11.92	20.91
500	5.92	10.33	23.01	2.90	9.30	18.09
600	4.51	7.24	18.25	3.06	8.05	15.76
700	2.85	2.79	13.08	1.19	5.48	11.34

Table B6 Effect of input frequency on concentrations of outlet gas of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV and an electrode gap distance of 6 mm

Input frequency (Hz)	Concentration of outlet gas (%)								
	CH ₄	H ₂	CO	CO ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₃ H ₈	C ₄ H ₁₀
250	61.95	8.13	0.44	17.63	1.61	1.47	3.45	2.97	0.16
300	64.72	5.60	0.38	17.99	1.16	1.31	3.85	3.35	0.15
400	65.18	4.31	0.38	18.24	0.92	1.15	4.10	3.68	0.14
500	66.09	3.40	0.38	18.46	0.77	1.07	4.25	3.83	0.13
600	66.97	2.95	0.40	18.55	0.65	0.92	4.41	4.09	0.11
700	67.60	2.03	0.36	18.76	0.42	0.77	4.57	4.30	0.10

Table B7 Effect of input frequency on product selectivities and product molar ratios, of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV and an electrode gap distance of 6 mm

Input frequency (Hz)	Product selectivity (%)					Product molar ratio			
	H ₂	C ₂ H ₂	C ₂ H ₄	CO	C ₄ H ₁₀	H ₂ /CO	H ₂ /C ₂ H ₂	H ₂ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
250	35.28	23.17	21.15	2.97	4.52	18.63	5.06	5.54	0.91
300	27.55	18.93	21.39	2.84	4.78	14.83	4.85	4.29	1.13
400	25.88	18.54	23.13	3.51	5.44	11.47	4.68	3.75	1.25
500	23.68	17.86	25.04	4.20	6.21	8.87	4.44	3.17	1.40
600	26.84	19.71	27.96	5.61	6.85	7.34	4.55	3.21	1.42
700	29.29	19.95	37.02	8.07	9.81	5.71	4.87	2.63	1.86

Table B8 Effect of input frequency on specific energy consumption and current of the simulated CO₂-containing natural gas reforming at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV and an electrode gap distance of 6 mm

Input frequency (Hz)	Energy consumption (x10 ¹⁸ Ws per H ₂ molecule produced)	Energy consumption (x10 ¹⁸ Ws per reactant molecule converted)	Current (mA)
	250	3.24	
300	5.13	3.11	2.0000
400	6.22	3.57	1.3077
500	5.90	3.16	1.2308
600	5.82	3.44	1.0769
700	8.95	6.10	0.9231

Table B9 Effect of HCs/O₂ feed molar ratio on reactant conversions and product yields of the simulated CO₂-containing natural gas reforming using feeds with pure oxygen added, and feed in the absence of oxygen at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV, frequency of 300 Hz and an electrode gap distance of 6 mm

HCs/O ₂ feed molar ratio	Reactant conversion (%)					Product yield (%)		
	CH ₄	C ₂ H ₆	C ₃ H ₈	CO ₂	O ₂	H ₂	C ₂	CO
1/0	7.99	19.05	32.20	5.79	-	16.32	23.89	3.11
2/1	23.20	35.85	45.66	-2.67	36.89	48.21	35.06	57.45
3/1	21.57	29.73	45.24	5.12	37.50	37.50	35.11	29.48
4/1	17.32	24.52	40.63	2.34	31.25	32.04	29.99	24.59
5/1	14.78	29.17	40.91	4.81	31.45	31.94	30.57	21.25
7/1	13.20	27.42	39.62	5.95	33.91	26.72	28.40	15.13
10/1	8.02	21.22	34.43	2.55	28.63	22.87	27.13	9.75
15/1	7.43	20.07	34.70	3.49	28.54	19.30	25.25	8.02
20/1	6.20	14.91	29.78	1.93	23.19	14.86	20.96	3.36

Table B10 Effect of HCs/O₂ feed molar ratio on reactant conversions and product yields of the simulated CO₂-containing natural gas reforming using feeds with air added, and feed in the absence of oxygen at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV, frequency of 300 Hz and an electrode gap distance of 6 mm

HCs/O ₂ feed molar ratio	Reactant conversion (%)					Product yield (%)		
	CH ₄	C ₂ H ₆	C ₃ H ₈	CO ₂	O ₂	H ₂	C ₂	CO
1/0	7.99	19.05	32.20	5.79	-	16.32	23.89	3.11
2/1	31.78	42.48	50.79	4.31	43.35	58.07	49.75	61.58
5/1	18.39	31.03	42.37	5.82	31.28	37.18	37.86	21.37
10/1	13.44	29.25	42.45	3.37	30.71	34.70	37.63	14.31
15/1	10.85	26.77	40.06	4.68	29.21	27.25	32.50	9.25
20/1	10.81	26.74	40.04	3.69	29.00	26.74	32.55	8.74

Table B11 Effect of HCs/O₂ feed molar ratio on product selectivities and product molar ratio of the simulated CO₂-containing natural gas reforming using feeds with pure oxygen added, and feed in the absence of oxygen at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV, frequency of 300 Hz and an electrode gap distance of 6 mm

HCs/O ₂ feed molar ratio	Product selectivity (%)					Product molar ratio			
	H ₂	C ₂ H ₂	C ₂ H ₄	CO	C ₄ H ₁₀	H ₂ /CO	H ₂ /C ₂ H ₂	H ₂ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
1/0	27.55	18.93	21.39	2.84	4.78	14.83	4.29	4.85	1.13
2/1	46.04	20.71	12.77	56.30	1.88	1.46	12.63	7.79	0.62
3/1	38.85	20.83	15.53	29.00	2.67	2.06	10.86	7.14	0.66
4/1	38.85	20.83	15.53	29.00	2.67	2.29	8.72	6.50	0.75
5/1	37.64	19.73	16.29	23.70	2.99	2.60	7.92	6.54	0.83
7/1	33.30	18.16	17.23	17.55	3.37	3.04	6.58	6.25	0.95
10/1	35.93	19.43	23.18	14.73	4.91	3.88	5.12	6.11	1.19
15/1	31.02	16.37	24.22	12.21	5.43	3.95	4.20	6.21	1.48
20/1	29.20	14.84	26.35	9.93	6.36	4.66	3.64	6.45	1.78

Table B12 Effect of HCs/O₂ feed molar ratio on product selectivities and product molar ratio of the simulated CO₂-containing natural gas reforming using feeds with air added, and feed in the absence of oxygen at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV, frequency of 300 Hz and an electrode gap distance of 6 mm

HCs/O ₂ feed molar ratio	Product selectivity (%)					Product molar ratio			
	H ₂	C ₂ H ₂	C ₂ H ₄	CO	C ₄ H ₁₀	H ₂ /CO	H ₂ /C ₂ H ₂	H ₂ /C ₂ H ₄	C ₂ H ₄ /C ₂ H ₂
1/0	46.44	27.98	11.81	1.34	47.60	1.70	14.02	5.92	0.42
2/1	40.51	25.35	15.89	2.28	21.90	3.06	8.85	5.55	0.63
5/1	40.76	25.00	19.20	3.27	16.17	4.12	7.19	5.52	0.77
10/1	35.07	21.16	20.68	3.95	11.24	4.95	5.67	5.54	0.98
15/1	34.46	21.21	20.74	3.96	10.76	5.13	5.55	5.43	0.98
20/1	46.44	27.98	11.81	1.34	47.60	1.70	14.02	5.92	0.42

Table B13 Effect of HCs/O₂ feed molar ratio on energy consumption of the simulated CO₂-containing natural gas reforming using feeds with pure oxygen added, and feed in the absence of oxygen at a feed flow rate of 125 cm³/min, an applied voltage of 17.5 kV, frequency of 300 Hz and an electrode gap distance of 6 mm

HCs/O ₂ feed molar ratio	Energy consumption (x10 ¹⁸ Ws per H ₂ molecule produced)	Energy consumption (x10 ¹⁸ Ws per reactant molecule converted)
1/0	5.13	3.11
2/1	1.89	2.08
3/1	2.49	2.28
4/1	2.27	2.01
5/1	2.23	1.89
7/1	2.94	2.17
10/1	3.84	3.30
15/1	4.44	3.26
20/1	6.04	4.28

Appendix C Non-Oxidative Methane Reforming in an AC Gliding Arc Microreactor: Effects of Operational Parameters and the Presence of Catalyst

Table C1 Effect of input power on methane conversion and product yields of the non-oxidative methane reforming at a feed flow rate of 200 cm³/min, an electrode gap distance of 4 mm and a reactor width of 1.25 mm

Input power (W)	CH ₄ conversion (%)	Product yield (%)	
		H ₂	C ₂
4	24.42	17.94	19.25
6	29.61	21.87	24.82
8	30.69	22.88	26.40
10	30.44	22.90	26.18
12	31.98	23.74	28.92

Table C2 Effect of input power on product selectivities of the non-oxidative methane reforming at a feed flow rate of 200 cm³/min, an electrode gap distance of 4 mm and a reactor width of 1.25 mm

Input power (W)	Product selectivity (%)					
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₄ H ₆	carbon
4	73.48	68.42	7.29	3.14	9.11	12.04
6	73.86	77.36	4.70	1.78	8.31	7.85
8	74.56	80.83	3.95	1.24	6.22	7.76
10	75.25	81.26	3.71	1.04	4.82	9.17
12	74.26	85.74	3.78	0.94	4.58	4.97

Table C3 Effect of electrode gap distance on methane conversion and product yields of the non-oxidative methane reforming at a feed flow rate of 200 cm³/min, an input power of 6 W and a reactor width of 1.25 mm

Electrode gap distance (mm)	CH ₄ conversion (%)	Product yield (%)	
		H ₂	C ₂
2	18.77	14.07	15.57
3	26.54	19.73	22.26
4	29.61	21.87	24.82
5	31.57	23.25	26.44

Table C4 Effect of electrode gap distance on product selectivities of the non-oxidative methane reforming at a feed flow rate of 200 cm³/min, an input power of 6 W and a reactor width of 1.25 mm

Electrode gap distance (mm)	Product selectivity (%)					
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₄ H ₆	carbon
2	74.95	76.51	4.55	1.90	5.92	11.12
3	74.32	77.79	4.47	1.62	7.40	8.71
4	73.86	77.36	4.70	1.78	8.31	7.85
5	73.67	76.86	5.06	1.84	8.55	7.69

Table C5 Effect of reactor width on methane conversion and product yields of the non-oxidative methane reforming at a feed flow rate of 200 cm³/min, an input power of 6 W and a electrode gap distance of 4 mm

Reactor width (mm)	CH ₄ conversion (%)	Product yield (%)	
		H ₂	C ₂
0.65	25.84	19.06	21.36
1.25	29.61	21.87	24.82
2.25	33.13	24.55	27.58
3.25	39.94	29.62	32.47
4.25	42.69	31.68	34.16

Table C6 Effect of reactor width on product selectivities of the non-oxidative methane reforming at a feed flow rate of 200 cm³/min, an input power of 6 W and an electrode gap distance of 4 mm

Reactor width (mm)	Product selectivity (%)					
	H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₄ H ₆	carbon
0.65	73.77	74.62	5.63	2.40	7.90	9.45
1.25	73.86	77.36	4.70	1.78	8.31	7.85
2.25	74.09	76.94	4.73	1.58	8.34	8.41
3.25	74.16	74.20	5.25	1.87	8.72	9.98
4.25	74.20	72.66	5.41	1.94	9.25	10.74

Table C7 Effect of the presence of catalyst on methane conversion of the combined catalytic-plasma non-oxidative methane reforming at an electrode gap distance of 4 mm and an input power of 6 W

Catalyst distance (mm)	System	Feed flow rate (cm ³ /min)	Residence time (s)	CH ₄ conversion (%)	Product yield (%)	
					H ₂	C ₂
0.2	plasma alone	75	0.0836	40.54	30.81	34.59
		100	0.0627	34.07	26.01	28.13
		200	0.0314	25.78	19.05	21.83
	plasma+unloaded cat.	75	0.0836	49.96	38.33	40.98
		100	0.0627	45.39	34.47	37.64
		200	0.0314	31.97	23.51	26.49
	plasma+Ni-loaded cat.	75	0.0836	53.41	40.90	43.92
		100	0.0627	48.75	37.17	39.81
		200	0.0314	32.92	24.16	27.31
0.5	plasma alone	75	0.1100	44.52	34.31	36.24
		100	0.0825	41.02	31.35	33.57
		200	0.0413	29.50	21.78	24.74
	plasma+unloaded cat.	75	0.1100	50.29	38.33	42.57
		100	0.0825	44.38	33.84	36.49
		200	0.0413	30.66	22.72	25.43
	plasma+Ni-loaded cat.	75	0.1100	53.54	41.17	44.01
		100	0.0825	46.88	36.13	37.03
		200	0.0413	31.89	23.56	26.49

Table C8 Effect of the presence of catalyst on product selectivities of the combined catalytic-plasma non-oxidative methane reforming at an electrode gap distance of 4 mm and an input power of 6 W

Catalyst distance (mm)	System	Residence time (s)	Product selectivity (%)					
			H ₂	C ₂ H ₂	C ₂ H ₄	C ₂ H ₆	C ₄ H ₆	carbon
0.2	plasma alone	0.0836	76.01	80.53	3.81	0.98	3.24	11.43
		0.0627	76.35	77.64	3.78	1.14	3.98	13.45
		0.0314	73.87	78.24	4.67	1.77	7.73	7.58
	plasma+unloaded cat.	0.0836	76.73	76.92	3.99	1.12	3.23	14.74
		0.0627	75.93	77.62	4.06	1.24	4.53	12.55
		0.0314	73.55	75.57	5.20	2.10	9.03	8.10
	plasma+Ni-loaded cat.	0.0836	76.58	77.21	3.99	1.04	3.58	14.18
		0.0627	76.24	76.16	4.18	1.32	4.37	13.96
		0.0314	73.38	75.52	5.32	2.12	9.28	7.75
0.5	plasma alone	0.1100	77.07	76.96	3.59	0.87	3.31	15.27
		0.0825	76.43	76.95	3.79	1.09	4.31	13.86
		0.0413	73.84	77.42	4.72	1.75	8.35	7.76
	plasma+unloaded cat.	0.1100	76.22	79.64	4.02	1.00	2.95	12.39
		0.0825	76.25	77.27	3.83	1.11	4.51	13.29
		0.0413	74.11	76.55	4.66	1.74	8.32	8.73
	plasma+Ni-loaded cat.	0.1100	76.89	77.34	3.91	0.96	2.94	14.86
		0.0825	77.06	73.99	3.83	1.16	4.43	16.59
		0.0413	73.88	76.67	4.65	1.75	8.82	8.10

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1. Rueangjitt, N., Akarawitoo, C., Sreethawong, T. and Chavadej, S. (2007) Reforming of CO₂-containing natural gas using an AC gliding arc system: Effects of gas components. Plasma Chemistry and Plasma Processing, 27(5), 559-576.
2. Rueangjitt, N., Sreethawong, T. and Chavadej, S. (2008) Reforming of CO₂-containing natural gas using an AC gliding arc system: Effects of operational parameters and oxygen addition in feed. Plasma Chemistry and Plasma Processing, 28(1), 49-67.
3. Rueangjitt, N., Sreethawong, T., Chavadej, S. and Sekiguchi, H. Non-oxidative methane reforming in an AC gliding arc microreactor: Effects of operational parameters and the presence of catalyst. International Journal of Plasma Environmental Science & Technology. (in preparation).
4. Rueangjitt, N., Jittiang, W., Sreethawong, T. and Chavadej, S. Combined reforming and partial oxidation of CO₂-containing natural gas using low-



temperature gliding arc discharge: Effect of stage number of plasma reactors. Plasma Chemistry and Plasma Processing. (in preparation).

Proceedings and Presentations:

1. Rueangjitt, N., Akarawitoo, C. and Chavadej, S. (2006) Hydrogen production from natural gas reforming in gliding arc discharge. Paper presented at AICHE Annual Meeting 2006, November 12-17, San Francisco, USA.
2. Rueangjitt, N., Akarawitoo, C., Sreethawong, T. and Chavadej, S. (2007) Reforming of CO₂-containing natural gas using an AC gliding arc system: Effects of feed components. Proceedings of the 18th International Plasma Symposium on Plasma Chemistry (ISPC 2007), August 26-31, Kyoto, Japan.
3. Sreethawong, T., Rueangjitt, N., and Chavadej, S. (2007) Reforming of CO₂-containing natural gas using an AC gliding arc system: Effects of applied voltage and frequency. Proceedings of the 18th International Plasma Symposium on Plasma Chemistry (ISPC 2007), August 26-31, Kyoto, Japan.
4. Chavadej, S., Sreethawong, T., and Rueangjitt, N. (2007) Reforming of CO₂-containing natural gas with partial oxidation using an AC gliding arc system. Proceedings of the 18th International Plasma Symposium on Plasma Chemistry (ISPC 2007), August 26-31, Kyoto, Japan.
5. Akarawitoo, C., Chavadej, S., and Rueangjitt, N. (2006) Hydrogen production from biogas reforming using a multi-stage gliding arc system. Proceedings of the 13th Regional Symposium on Chemical Engineering (RSCE 2006), December 3-5, Singapore.