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APPENDIX A

VAPOR PRESSURE OF ETHANOL

The partial vapor pressure of the ethanol to the requirement was set by adjusting the temperature of saturator following Antoine equation [24];

$$\ln P = A - \frac{B}{(t+C)}$$

When P = vapor pressure of reactant, mm Hg

t = temperature, °C

A, B and C are constants shown in Table A-1

Table A-2 reports the calculation results for the range of temperature of 50-57°C. It was found that temperature around 51°C would provide ca. 30% ethanol by stream volume.

Table A-1 The values of constants.

Constant	Value of constant
A	8.32
B	1718.10
C	237.52

Table A-2 The value % mole of ethanol.

% ethanol	Temperature(°C)
29.15	50
30.57	51
32.06	52
36.88	55
40.43	57

APPENDIX B

CALCULATION OF CATALYST PREPARATION

The example of calculation shown below is for 2wt%Pd/ y wt% La₂O₃/SiO₂ catalyst. The silica support weight used for all preparation was 2.0 g.

Based on catalyst 100 g, in order to prepare 2wt%Pd/ y wt% La₂O₃/SiO₂, the catalyst is composed of

Palladium	2	g
Lanthana	y	g
Silica support	98-y	g

The palladium compound used is Palladium (II) Chloride (PdCl₂), which has a molecular weight of 177.0, and the molecular weight of palladium is 106.4.

The lanthana (La₂O₃) used is Lanthanum nitrate hydrate, which has a molecular weight of 443.0, and the molecular weight of Lanthanum (La) is 138.9.

The calculation of the amount of each ingredient for required composition of the 2wt%Pd/ywt%La₂O₃/SiO₂ catalyst is shown as follows:

For 2.0 g of silica support used:

1. Lanthana amount

In 100 g of 2wt%Pd/ywt%La₂O₃/SiO₂ catalyst has lanthana = y g

In 100 g of 2wt%Pd/ywt%La₂O₃/SiO₂ catalyst has silica = 100-y g

$$\text{Therefore, for 2.0 g of silica, lanthana required} = \frac{2y}{(100-y)} \text{ g}$$

$$\text{Lanthana (La}_2\text{O}_3\text{) 325.91 g has lanthanum (La)} = 277.82 \text{ g}$$

$$\text{Lanthanum nitrate hydrate (La(NO}_3\text{)}_3\cdot 6\text{H}_2\text{O) 433.01 g has lanthanum} = 38.91 \text{ g}$$

Lanthana $2y/(100-y)$ g required Lanthanum nitrate hydrate

$$= (433.10/138.91) \times (277.82/325.91) \times (2y/(100-y)) \text{ g}$$

$$= 5.3161 \times y/(100-y) \text{ g}$$

Therefore, required Lanthanum nitrate hydrate for 2.0 g of silica

$$= 0.1063 \times y/(100-y) \text{ g}$$

2. Palladium amount

$$\text{In 100 g of 2wt\%Pd/ywt\%La}_2\text{O}_3\text{/SiO}_2 \text{ catalyst has Palladium} = 2 \text{ g}$$

$$\begin{aligned} \text{In 100 grams of 2wt\%Pd/ywt\%La}_2\text{O}_3\text{/SiO}_2 \text{ catalyst} \\ \text{has ywt\%La}_2\text{O}_3\text{/SiO}_2 = 98 \text{ g} \end{aligned}$$

$$\text{If used ywt\%La}_2\text{O}_3\text{/SiO}_2 \text{ 2 g required palladium} = 0.0408 \text{ g}$$

$$\text{Palladium (II) Chloride (PdCl}_2\text{) 177 g has Palladium (Pd)} = 106.40 \text{ g}$$

$$\text{Palladium 0.0408 g requires palladium (II) Chloride} = 0.0678 \text{ g}$$

$$\text{If used ywt\%La}_2\text{O}_3\text{/SiO}_2 \text{ 2 g requires palladium (II) Chloride} = 0.0678 \text{ g}$$

APPENDIX C

CALCULATION OF CRYSTALLITE DIAMETER

The mean metal crystallite diameter of the catalyst (D), can be calculated from the following equation:

$$D = \frac{k\lambda}{\beta \cos \theta}$$

where

$$\beta = \sqrt{B^2 - b^2}$$

where

k = shape factor, related to crystallite shape (take as 0.9)

λ = X-ray wavelength, for Cu K_{α} = 1.5418 Å

θ = diffraction angle

β = Pure breadth of a powder diffraction

B = Breadth at half the maximum intensity of sample

b = Breadth at half the maximum intensity of metal standard

APPENDIX D

CALCULATION OF METAL ACTIVE SITES

The calculation of metal active sites of the catalyst by purity CO adsorption at room temperature has a procedure as follows:

Let the weight of catalyst used	= W	g
Height of CO peak after adsorption	= A	unit
Height of 40 μ l standard CO peak	= B	unit
Amounts of CO adsorbed on catalyst	= B-A	unit
Volume of CO adsorbed on catalyst	= [(B-A)/B] \times (40)	μ l
Volume of CO 1 mole at 30°C	= 24.86 $\times 10^6$	μ l
Mole of CO adsorbed on catalyst	= $\frac{[(B-A)/B] \times (40)}{24.86 \times 10^6}$	mole
Molecule of CO adsorbed on catalyst	= $\frac{[(B-A)/B] (6.02 \times 10^{23})}{24.86 \times 10^6}$	molecules
Metal active sites	= $\frac{9.68 \times 10^7 \times [(B-A)/B]}{W}$	site /g cat

APPENDIX E

CALIBRATION CURVE

The thermal conductivity detector, model 14B, was used to analyze the concentration of ethanol and products of the reaction by using Porapak N column while carbon dioxide for TPO technique was analyzed by GC 8AIT equipped with Porapak Q column.

The calibration curve of methane, carbon monoxide, carbon dioxide, ethylene, ethane, ethanol, acetaldehyde, hydrogen, and carbon dioxide (for TPO technique) are illustrated in the following figures.

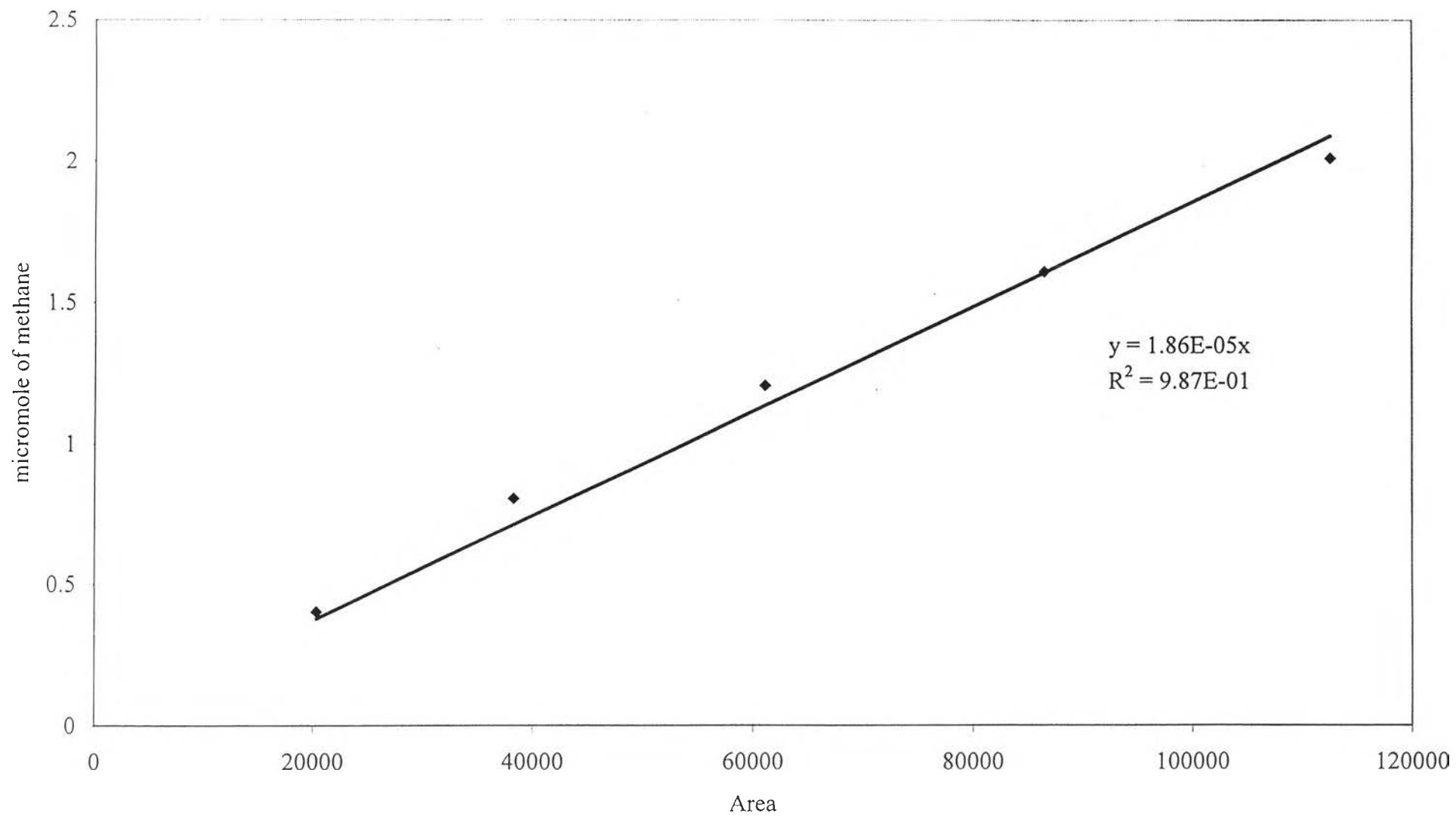


Figure E-1 The calibration curve of methane.

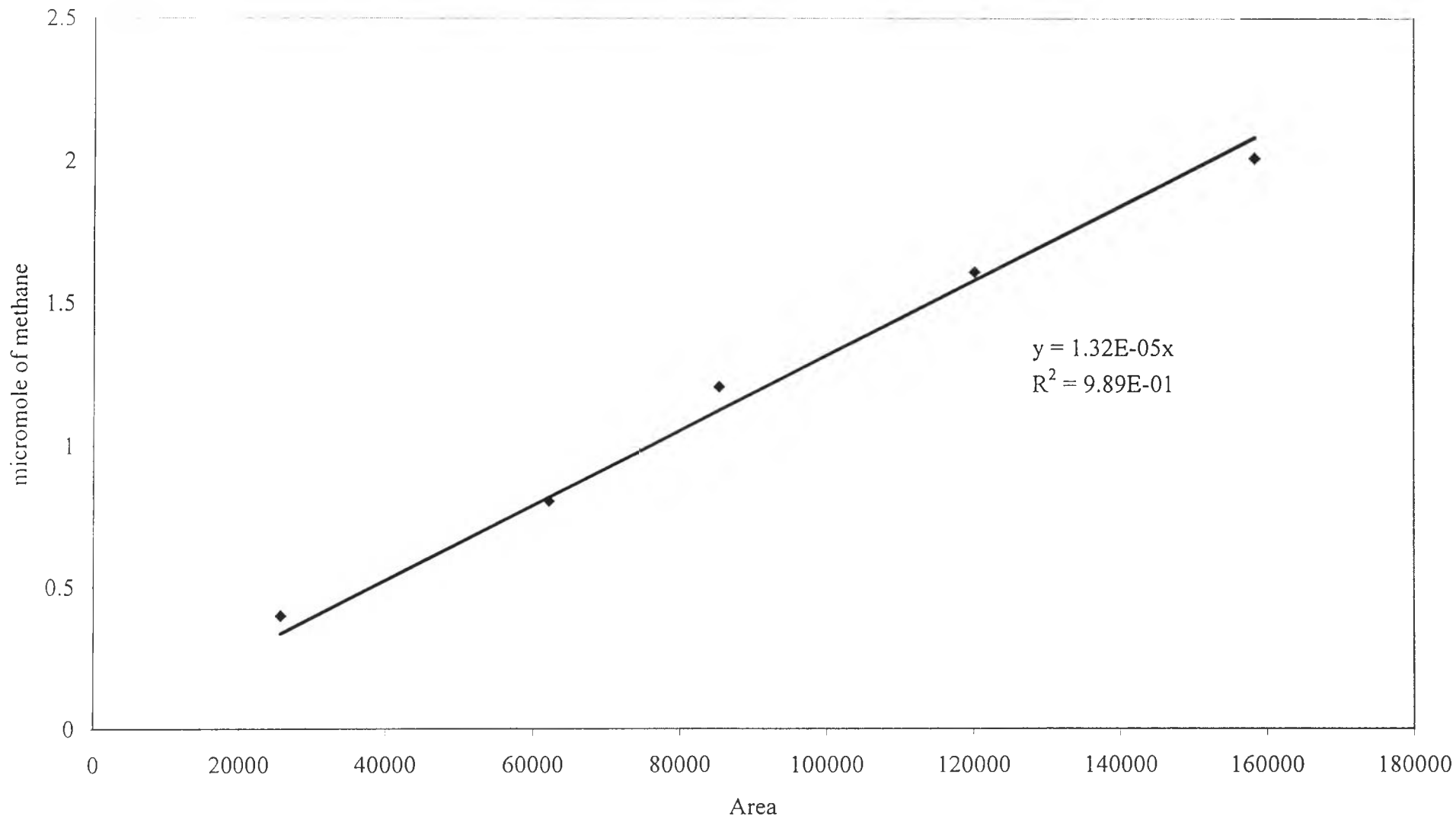


Figure E-2 The calibration curve of carbon monoxide.

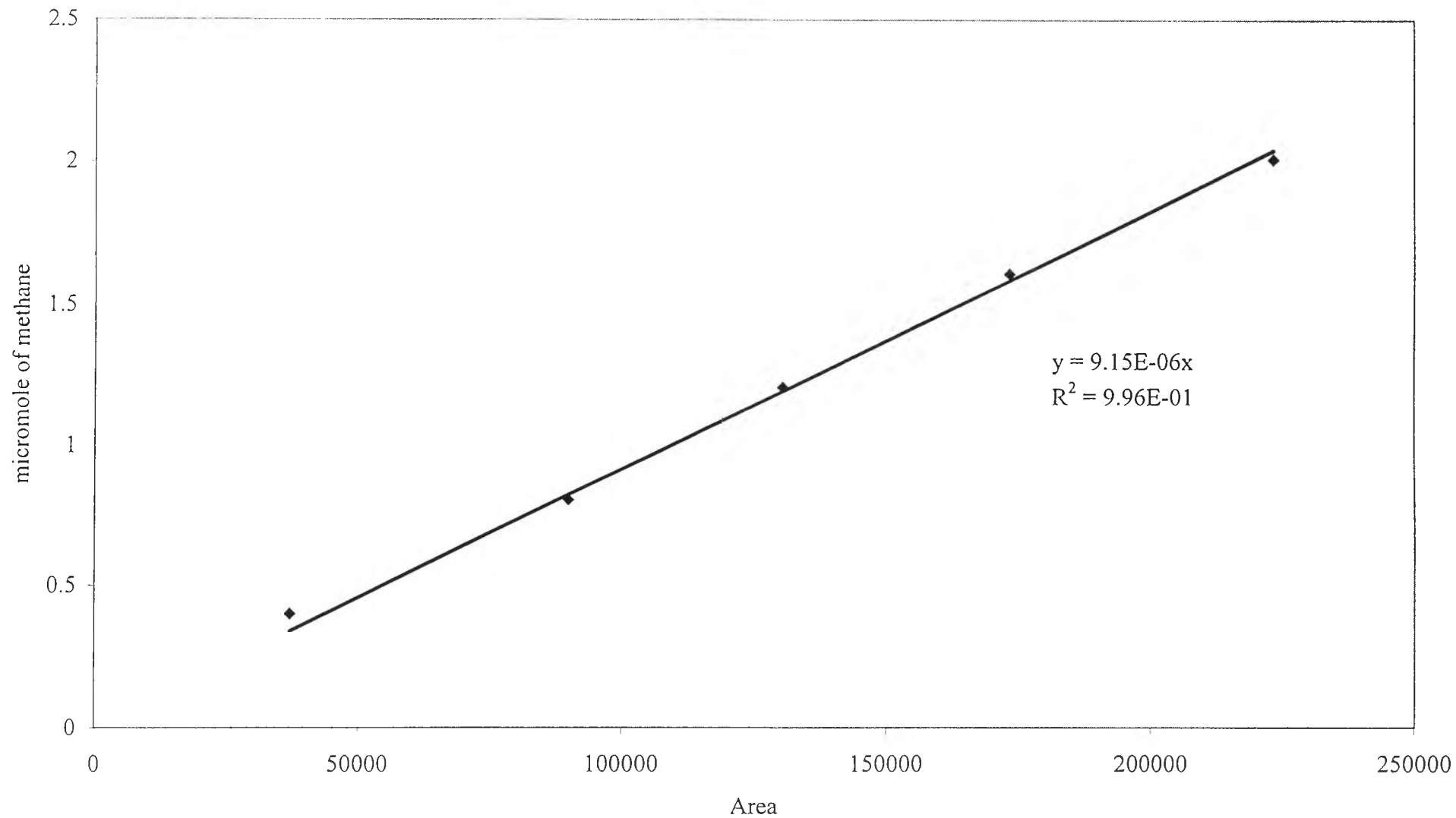


Figure E-3 The calibration curve of carbon dioxide.

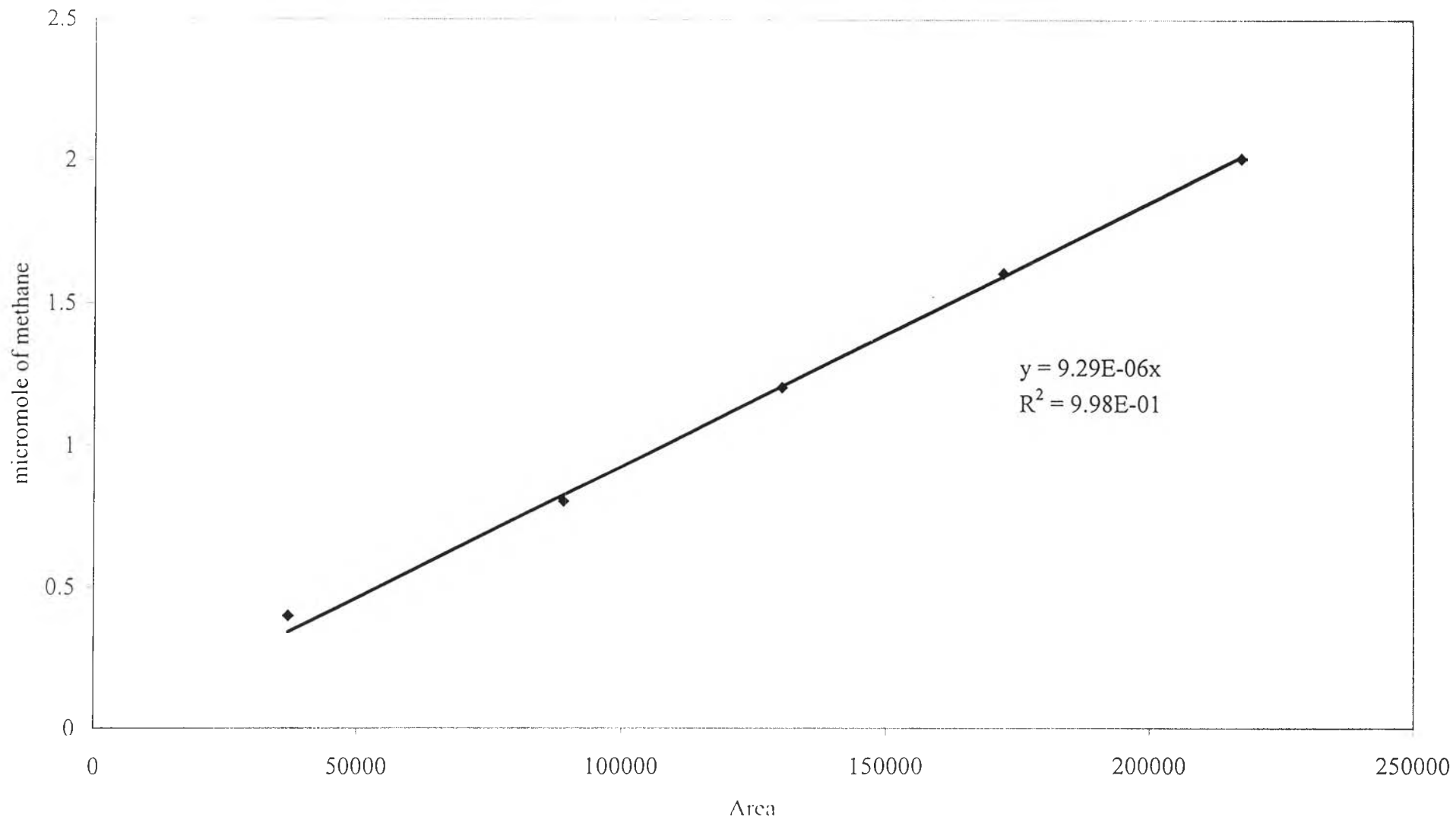


Figure E-4 The calibration curve of ethylene.

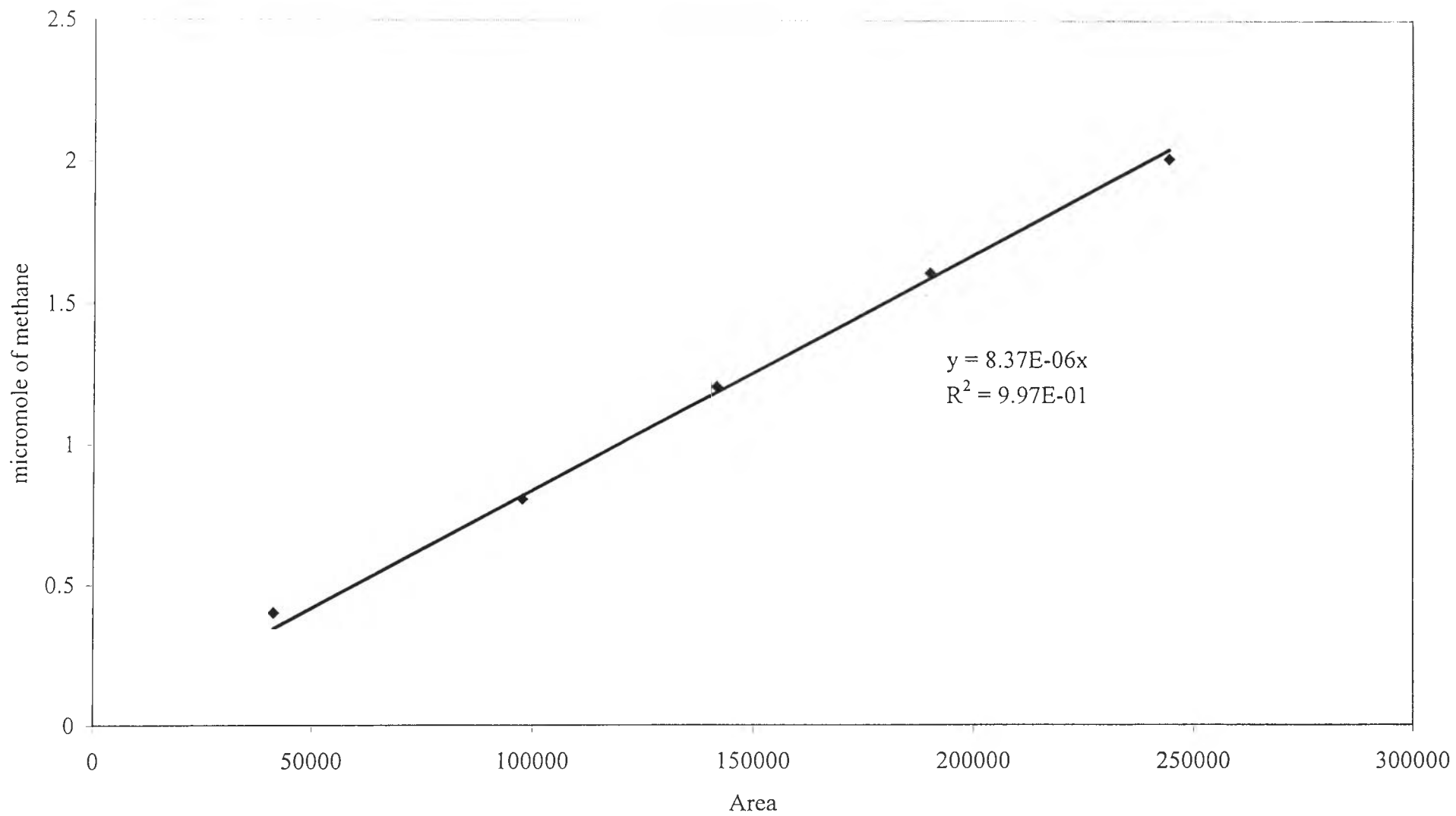


Figure E-5 The calibration curve of ethane.

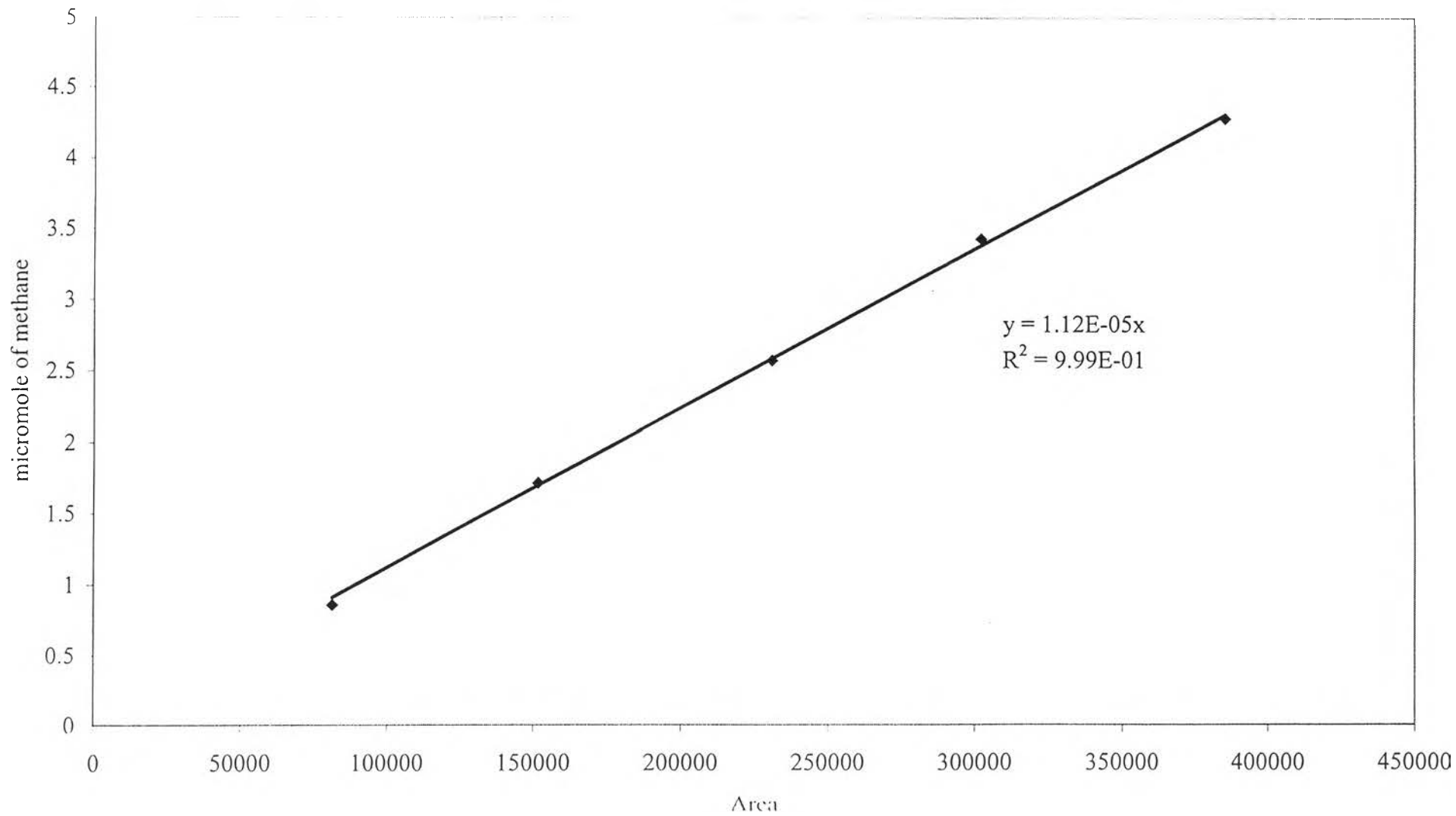


Figure E-6 The calibration curve of ethanol.

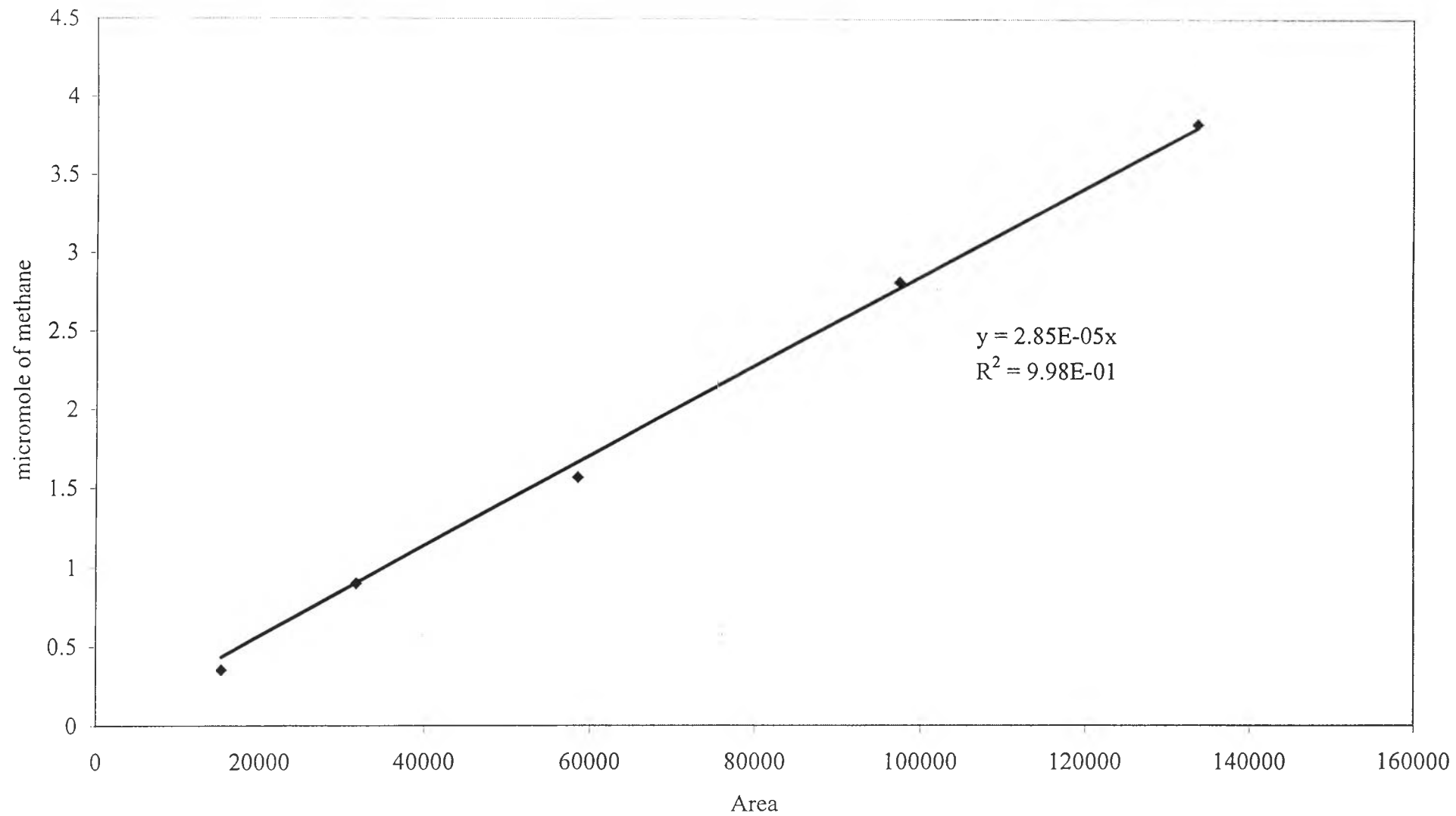


Figure E-7 The calibration curve of acetaldehyde.

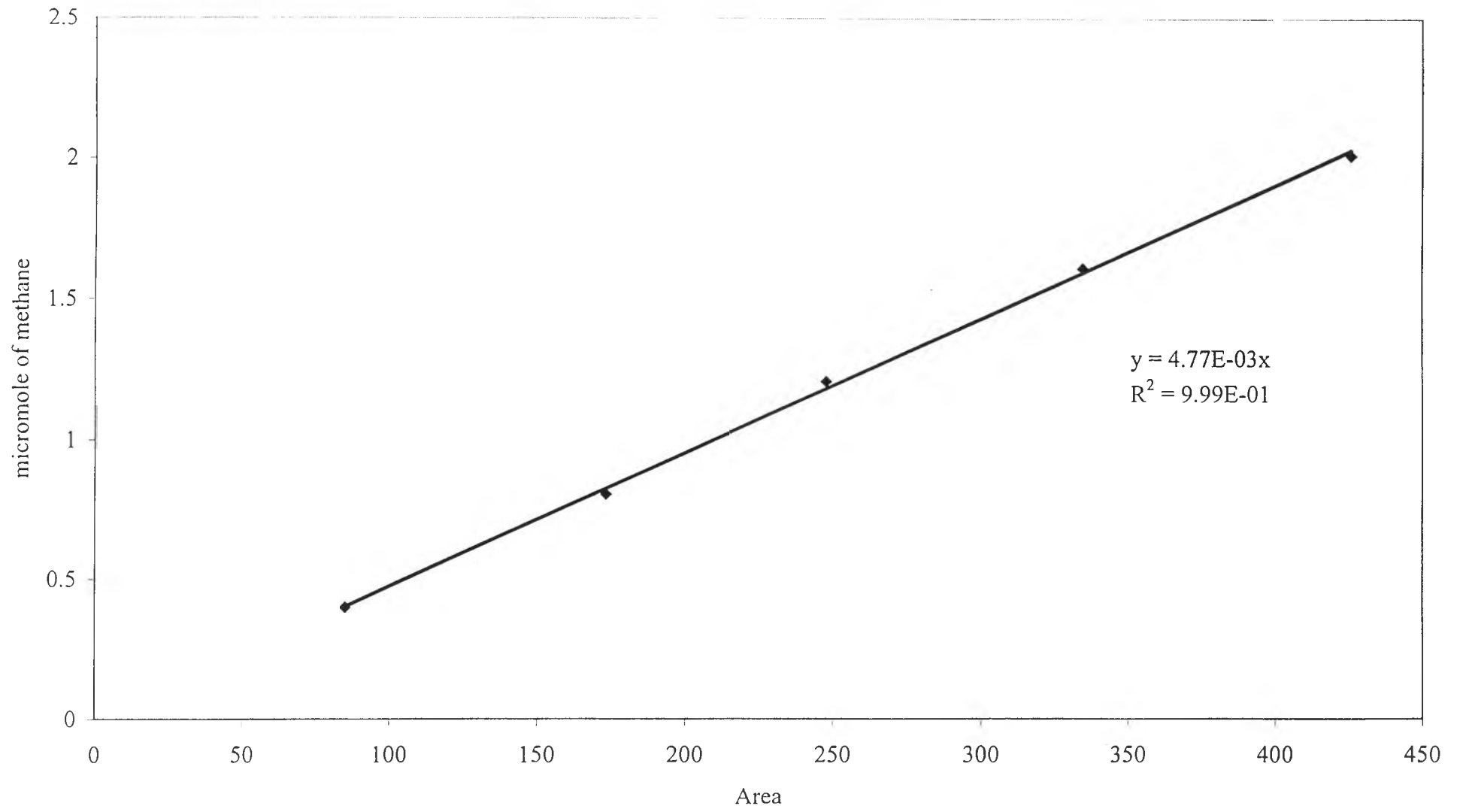


Figure E-8 The calibration curve of hydrogen.

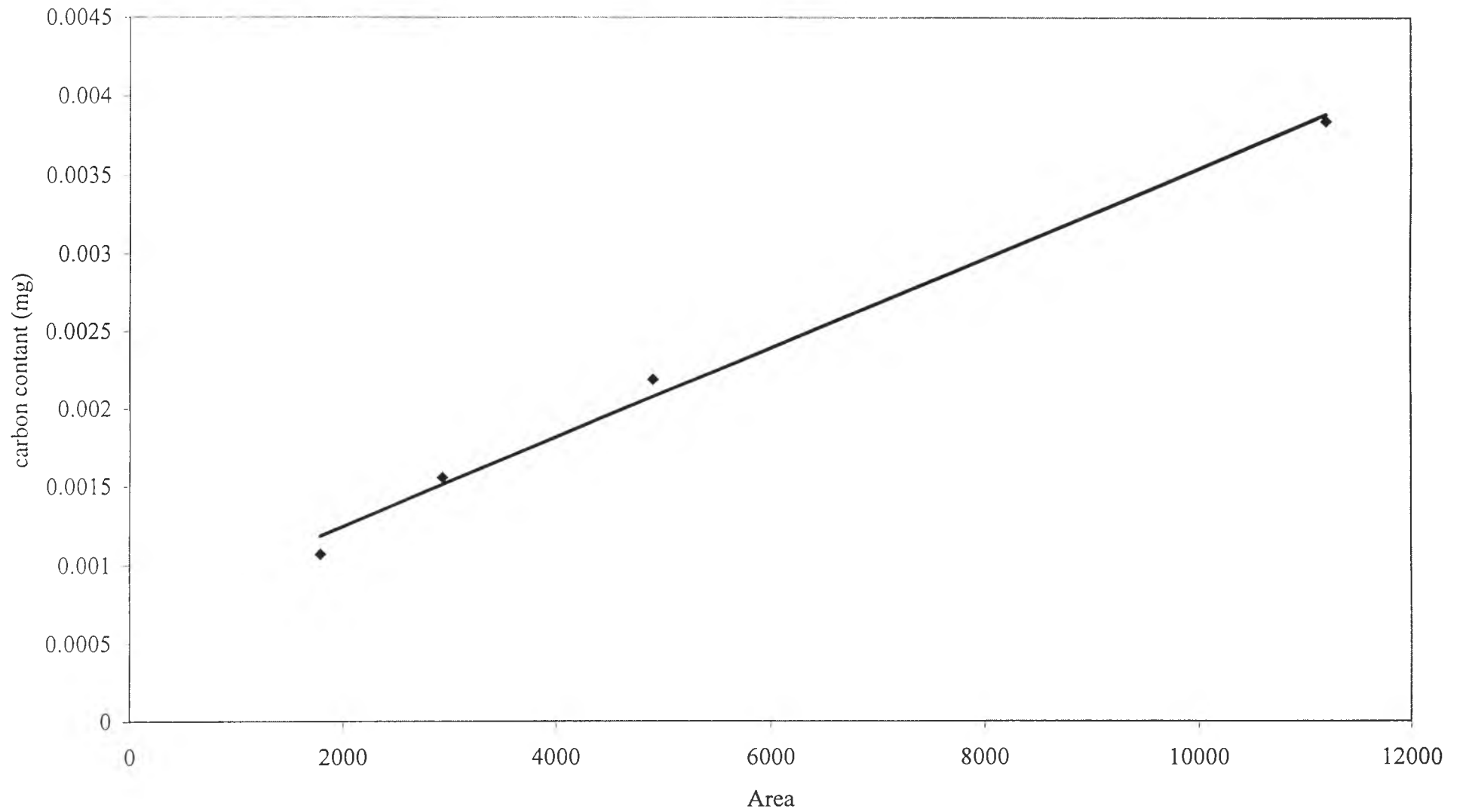


Figure E-9 The calibration curve of carbon dioxide on GC 8 AIT.

VITA

Mr. Arthit Neramittagapong was born on August 11, 1974 in Bangkok, Thailand. He finished his secondary school from Udonpitayanukul school in 1993. After that, he studied in the major of Chemical Engineering in Faculty of Engineering at Khon Kaen University in 1997. He continued his further study for Master's degree in Chemical Engineering at Chulalongkorn University. He proudly participated in the Petrochemical Engineering Research Laboratory and achieved his Master's degree in June 2000.

