# DEVELOPMENT OF A PROBE FOR MEASURING HYDROGEN CONCENTRATION IN THE PRESENCE OF MOIST CHLORINE

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#### **ABSTRACT**

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The presence of hydrogen gas as an impurity in chlorine gas and caustic soda generated by electrolysis of an aqueous sodium chloride solution in a Chlor-alkali plant leads to lowering plant efficiency and it can be hazardous if the hydrogen concentration exceeds 6 %. The development of an instrument for monitoring hydrogen concentration in moist chlorine gas at various locations of the Chlor-alkali plant has been performed at the Centre for Nuclear Energy Research (CNER). A series of hydrogen and chlorine permeability coefficient experiments was carried out using a test cell to identify effective coating materials for blocking chlorine, but at the same time, allowing the passage of hydrogen. It was found that Fluorodyn Caulk and Derakane Resin are the promising candidates as coating materials for blocking such chlorine.

## บทคัดย่อ

นางสาวพรรณี กิจเจริญวงศ์: การพัฒนาเครื่องมือสำหรับวัคความเข้มข้นของก๊าซ ไฮโครเจนในก๊าซคลอรีนชื้น (Development of a Probe for Measuring Hydrogen Concentration in the Presence of Moist Chlorine.) อ. ที่ปรึกษา : ศ. คร. แฟรงค์ สจ็วต และ ผศ.คร. ธีรศักดิ์ ฤกษ์สมบูรณ์ 105 หน้า ISBN 974-334-145-5

ก๊าซไฮโดรเจนเป็นสิ่งเจือปนในก๊าซคลอรีนและโซเดียมไฮดรอกไซด์ที่เกิดจากปฏิกิริยา อิเล็กโตรไลซิสของสารละลายเกลือหรือโซเดียมคลอไรด์ในโรงงานคลออัลคาไลน์ซึ่งทำให้ประสิทธิภาพการผลิตลดต่ำลง นอกจากนี้ยังเป็นอันตรายเมื่อความเข้มข้นของก๊าซไฮโดรเจนเกิน 6% ซึ่งเป็นส่วนที่ก๊าซไฮโดรเจนระเบิดได้ ดังนั้นจึงได้มีการพัฒนาเครื่องมือเพื่อทำการวัดความเข้มข้นของก๊าซไฮโดรเจนในก๊าซคลอรีนชื้นที่ตำแหน่งต่างๆของโรงงานคลออัลคาไลน์ โดยได้ทำการทดลองและวัดค่าสัมประสิทธิ์ในการแพร่ผ่านวัสดุต่างๆของก๊าซไฮโดรเจนและก๊าซคลอรีนโดยการใช้เทสต์เซลเพื่อที่จะหาวัสดุที่มีประสิทธิภาพในการป้องกันไม่ให้ก๊าซคลอรีนแพร่ผ่านไปได้ แต่ในขณะเดียวกันสามารถให้ก๊าซไฮโดรเจนแพร่ผ่านไปได้ จากการทดลอง พบว่าฟลูโอโรดินคอล์ค (Fluorodyn Caulk) และ เดราเคน เรซิน (Derakane Resin) เป็นวัสดุที่มีประสิทธิภาพในการป้องกันไม่ให้ก๊าซคลอรีนแพร่ผ่านไปได้

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### LIST OF SYMBOLS

a Anolyte

A Area of the electrode (cm<sup>2</sup>)

a Fe<sup>2+</sup> Acitivity of Fe<sup>2+</sup> ion

a<sub>Fe</sub>3+ Acitivity of Fe<sup>3+</sup> ion

a<sub>H3O+</sub> Acitivity of H<sub>3</sub>O<sup>+</sup> ion

b Affinity constant [ cm<sup>3</sup> (STP) /cm<sup>3</sup> ]

B/T Breakthrough time

c Catholyte

 $C_i$  Concentration of  $H_2$  in the collection gas at time  $t_i$ ,

(ppm)

C<sub>i</sub>, C<sub>o</sub> Concentration of the reacting substance remote

from the electrode and immediately adjoining its

surface, respectively.

CoH Catholyte caustic concentration (g/L)

c<sub>S</sub>' Langmuir capacity constant[ cm<sup>3</sup> (STP) /cm<sup>3</sup> ]

 $C_z(y)$  Concentration in grams per liter of z in medium y

d Depleted brine

 $D_0, P_0, \, S_0 \qquad \qquad \text{The constants , cm$^2/s , [cm$^3(STP) .cm]/}$ 

 $(cm^2.s.cmHg)$ , and  $[cm^3(STP)]/cm^3.cmHg)$ 

,respectively.

D<sub>app</sub> Apparent diffusivity

D<sub>i</sub> Diffusion coefficient of species i

E Cell potential E which is the difference of two half

cell electrode potentials at interface I and II.

$E_0$	A constant which is determined	by calibration of the
-------	--------------------------------	-----------------------

sensor with pure hydrogen gas at 1 atm.

E<sub>b</sub> Intramolecular activation energy

E<sub>D</sub> Activation energy for diffusion, cal/(gmol)

E<sub>1</sub> Half cell electrode potential at interface i

E<sub>i</sub> Intermolecular activation energy

E<sub>I</sub><sup>0</sup> Standard electrode potential

E<sub>II</sub> Half cell electrode potential at interface II

 $E_{II}^{0}$  Standard electrode potential for  $Fe^{3+}/Fe^{2+}$  redox

reaction

E<sub>P</sub> Activation energy for permeation, cal/(gmol)

F Faraday constant ( = 96,487 C/mol )

f Feed brine

I the current( A )

I<sub>L</sub> Limiting current(A)

J The flux of species (mol.sec<sup>-1</sup>.cm<sup>-2</sup>)

k a constant

 $k_g$  a constant at a given temperature.  $(k_g = kK_g^{-1/2})$ 

 $K_g(T)$  The equilibrium constant between hydrogen

molecule in bulk gas and H-atom in Palladium

L Specimen thickness

p Feed brine flow rate (L/s)

P Membrane permeability coefficient

p<sub>H2</sub> Partial pressure of hydrogen in the contacting gas.

 $P_{H2}$ ,  $P_{H2O}$  Ratio of hydrogen partial pressure or water vapor

pressure to the standard atmospheric

pressure, respectively.

$P_i(t_i)$	Permeation rate at any time t <sub>i</sub> , (cm <sup>3</sup> H <sub>2</sub> cm <sup>-2</sup> min	
	1)	
q	Depleted brine flow rate (L/s)	
Q	Total amount of permeate passing through the	
	polymer from t=0 to t=t [cm <sup>3</sup> (STP) /cm <sup>2</sup> ]	
R	Gas constant	
$R(T,x_H=0)$	Resistance of the pure palladium wire	
$R(T,x_H)$	Resistance of a palladium wire containing hydrogen	
	at temperature T	
S <sup>-</sup>	Henry's Law sorption coefficient	
S	Segment length	
T	Absolute temperature (K)	
$x_{H}$	Mole fraction of hydrogen atom in palladium	
Z	The number of electrons per mol	
$\eta_{\text{NaOH}}$	Caustic efficiency for membrane cells	
$\eta_{\text{Cl2}}$	Chlorine efficiency for membrane cells	
δ	Thickness of the diffusion layer	
θ	Diffusion time lag	
ε	Porosity	
$\rho(x_H)$	Ratio of the resistance $R(T,x_H)$ of a palladium wire	
	containing hydrogen at temperature T, to the	
	resistance of the pure palladium wire $R(T,x_H = 0)$	
$^{\scriptscriptstyle 1}\sigma_{\scriptscriptstyle c}$	Average diameter of the high polymer molecule	
$lpha_{ij}$	Selectivity which is the ratio of the permeability	
	coefficient of component i and component j	
$\sigma_{p}$	Penetrant molecule diameter	