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APPENDICES

Appendix A The methanol conversion and hydrogen yield of catalysts

The methanol conversion and hydrogen yield are calculated by Equation A1–A2.

$$X = \frac{CO + CO_2 + CH_4}{MeOH_{(in)}} \times 100(\%)$$
 (A1)

where:

$$X$$
 = methanol conversion (%)

 $MeOH_{(in)}$ = mole of methanol inlet

$$Y_{H_2} = X \times S_{H_2} \tag{A2}$$

where:

 Y_{H_2} = hydrogen yield (%)

 H_2 = mole of hydrogen in the product stream

CO = mole of carbon monoxide in the product stream

 CO_2 = mole of carbon dioxide in the product stream

 CH_4 = mole of carbon methane in the product stream

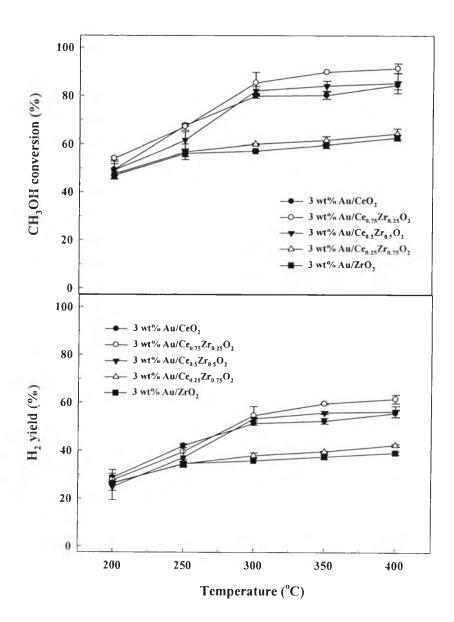


Figure A1 Effect of Ce/(Ce+Zr) atomic ratio on the methanol conversion and hydrogen yield over 3 wt% of Au/CeO₂–ZrO₂ catalysts calcined at 400 °C. (Reaction conditions: $O_2/H_2O/CH_3OH$ molar ratio = 0.6:2:1).

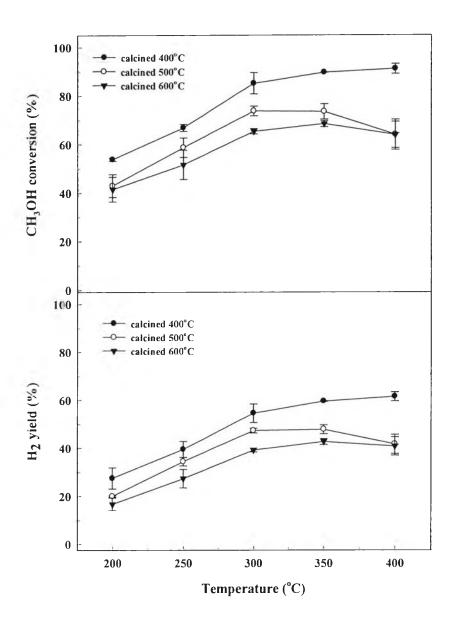


Figure A2 Effect of calcination temperature on the methanol conversion and hydrogen yield over 3 wt% of Au/Ce_{0.75}Zr_{0.25}O₂ catalysts. (Reaction conditions: $O_2/H_2O/CH_3OH$ molar ratio = 0.6:2:1).

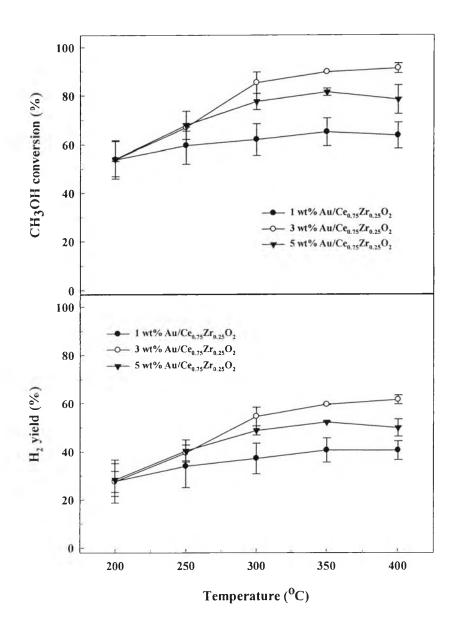


Figure A3 Effect of Au content on the methanol conversion and hydrogen yield over Au/Ce_{0.75}Zr_{0.25}O₂ catalysts. (Reaction conditions: $O_2/H_2O/CH_3OH$ molar ratio = 0.6:2:1).

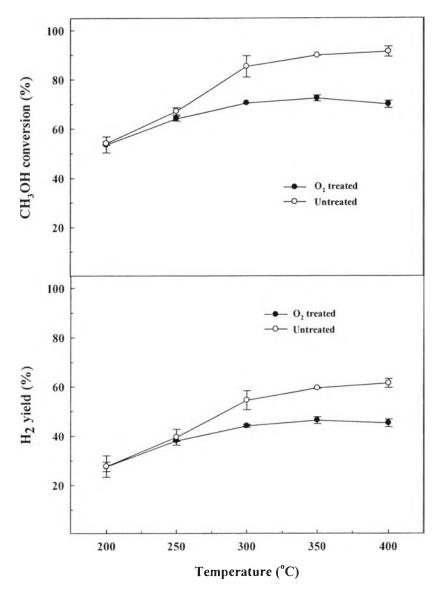


Figure A4 Effect of O_2 pretreatment on the methanol conversion and hydrogen yield over 3 wt%Au/Ce_{0.75}Zr_{0.25} O_2 catalysts. (Reaction conditions: $O_2/H_2O/CH_3OH$ molar ratio = 0.6:2:1).

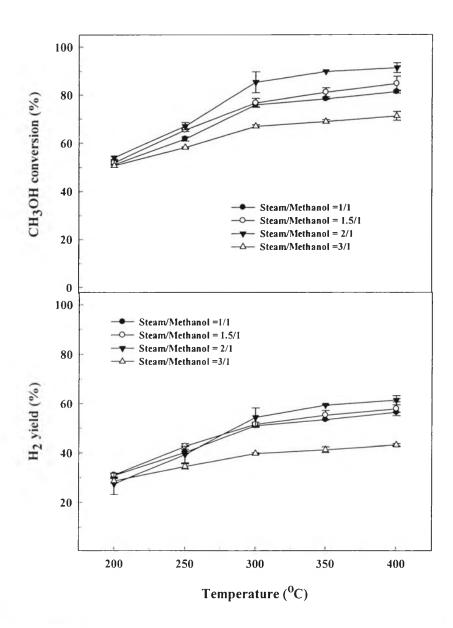


Figure A5 Effect of H_2O/CH_3OH molar ratio on the methanol conversion and hydrogen yield over 3 wt%Au/Ce_{0.75}Zr_{0.25}O₂ catalysts calcined at 400 °C.

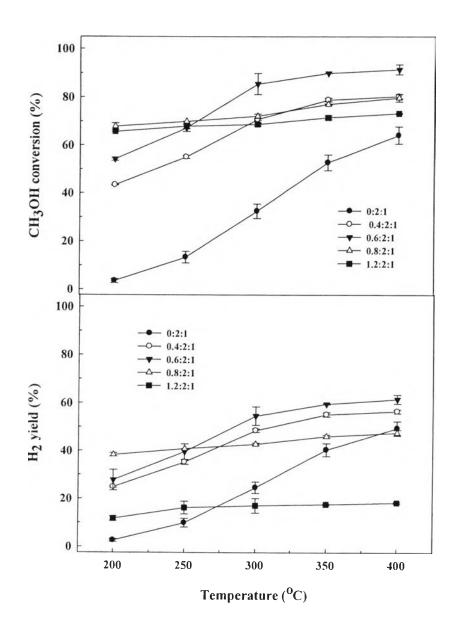


Figure A6 Effect of $O_2/H_2O/CH_3OH$ molar ratio on the methanol conversion and hydrogen yield over 3 wt%Au/Ce_{0.75}Zr_{0.25}O₂ catalysts calcined at 400 °C.

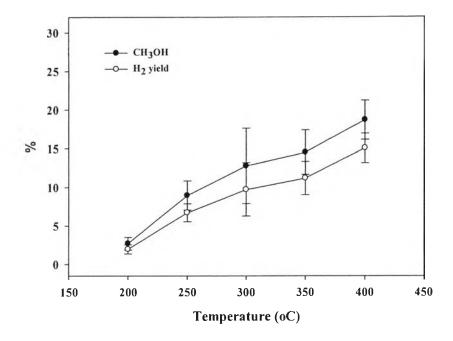


Figure A7 The methanol conversion and hydrogen yield over 3 wt%Au/Ce $_{0.75}$ Zr $_{0.25}$ O $_2$ catalyst in the methanol decomposition reaction.

Appendix B Calibration Curve of Gas Products

The relationship between the peak area from GC analysis and the gas concentration was conducted for the possible gas products such as hydrogen, carbon dioxide, carbon monoxide, oxygen and methane.

Hydrogen (H₂)

Peak Area	Amount (%mole, %vol.)
0	0
35241.5	21.35
60376	27.26
76992.5	33.57

Carbon monoxide (CO)

Amount (%mole, %vol.)
0
4.50
5.76
7.51

Carbon dioxide (CO₂)

Peak Area	Amount (%mole, %vol.)
0	0
168757	1.33
243160.7	2.24
423115.5	3.41

Methane (CH₄)

Peak Area	Amount (%mole, %vol.)
0	0
676791	12.03
1294423	18.88
2028339.5	24.46
2714826.5	29.71

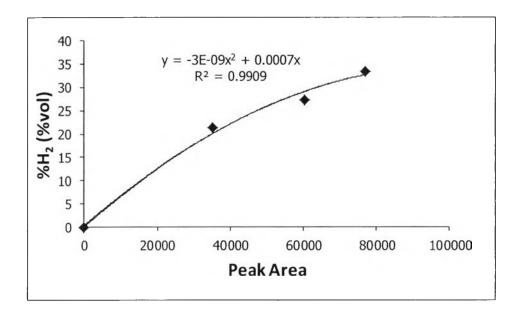


Figure B1 Calibration curve of hydrogen gas.

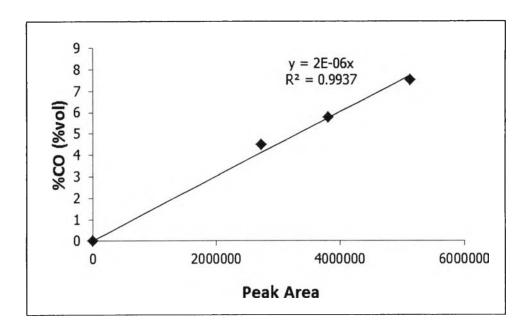


Figure B2 Calibration curve of carbon monoxide gas.

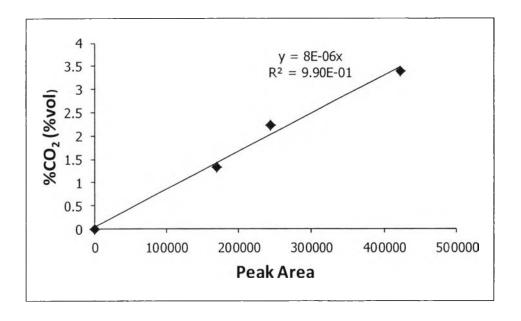


Figure B3 Calibration curve of carbon dioxide gas.

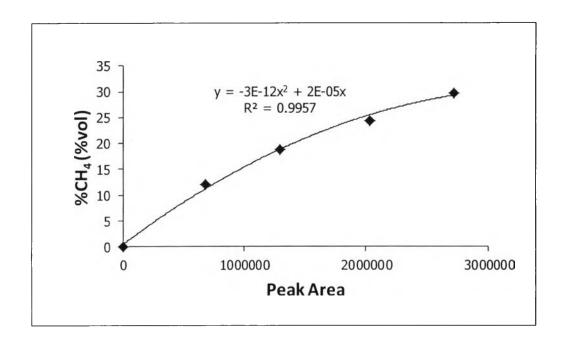


Figure B4 Calibration curve of methane gas.

Where x is peak area from GC analysis y is concentration (%)

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- 1. Nakaranuwattana, W., Luengnaruemitchai, A., and Gulari, E. (2013, April 10-11) Effect of Au Loading on The Catalytic Performance of Supported Au Catalysts. Poster present at Symposium on catalysis for fine chemicals, Palermo, Italy.
- 2. Nakaranuwattana, W., Luengnaruemitchai, A., and Gulari, E. (2013, April 23) Hydrogen Production from Oxidative Steam Reforming of Methanol over Au/CeO₂–ZrO₂ Catalysts. Poster present at <u>The 4th Research Symposium on Petrochemical and Materials Technology and The 19th PPC Symposium on Petroleum, Petrochemicals, and Polymers, Bangkok, Thailand.</u>